State of New Mexico Energy, Minerals and Natural Resources Department

> Oil Conservation Division 1220 South St. Francis Dr. Santa Fe. NM 87505

Intment to Appropriate District Office NM OIL CONSERVATION

Submit Original

ARTESIA DISTRICT

AU

GAS CAPTURE PLAN

RECEIVED

🛛 Original

Date: 3/26/2018

Operator & OGRID No.: Mack Energy Corporation - 013837

Amended - Reason for Amendment:

This Gas Capture Plan outlines actions to be taken by the Operator to reduce well/production facility flaring/venting for new completion (new drill, recomplete to new zone, re-frac) activity.

Note: Form C479 must be submitted one approved providers wheng buskess of see, it's Rue (Subsection Ant 1948) AMAGE

Well(s)/Production Facility - Name of facility

The well(s) that will be located at the production facility are shown in the table below

Well Name	API	Well Location (ULSTR)	Footages	Expected MCF/D	Flared or Vented	Comments
Nome Federal #1H		Sec. 3 T16S R28E	1700 FSL & 1675 FWL	50		
30-0	15-45	151				

Gathering System and Pipeline Notification

Well(s) will be connected to a production facility after flowback operations are complete, if gas transporter system is in place. The gas produced from production facility is dedicated to DCP Midstream and will be connected to DCP Midstream low/high pressure gathering system located in <u>Chaves</u> County. New Mexico. It will require<u>0 (exising)</u> of pipeline to connect the facility to low/high pressure gathering system. Mack Energy Corporation provides (periodically) to DCP Midstream a drilling, completion and estimated first production date for wells that are scheduled to be drilled in the foreseeable future. In addition, Mack Energy Corporation and DCP Midstream have periodic conference calls to discuss changes to drilling and completion schedules. Gas from these wells will be processed at DCP Midstream linem Ranch Processing Plant located in Sec.<u>6</u>. Twn.<u>195</u>, Rng.<u>37E</u> <u>Lea</u> County, New Mexico. The actual flow of the gas will be based on compression operating parameters and gathering system pressures.

Flowback Strategy

After the fracture treatment/completion operations, well(s) will be produced to temporary production tanks and gas will be flared or vented. During flowback, the fluids and sand content will be monitored. When the produced fluids contain minimal sand, the wells will be turned to production facilities. Gas sales should start as soon as the wells start flowing through the production facilities, unless there are operational issues on DCP Midstream system at that time. Based on current information, it is Mack Energy Corporation belief the system can take this gas upon completion of the well(s).

Safety requirements during cleanout operations from the Use Of underbalanced air cleanout systems may necessitate that sand and non-pipeline quality gas be vented and/or flared rather than sold on a temporary basis.

Alternatives to Reduce Flaring

Below are alternatives considered from a conceptual standpoint to reduce the amount of gas flared.

- Power Generation On lease
- Only a portion of gas is consumed operating the generator, remainder of gas will be flared Compressed Natural Gas - On lease

Gas flared would be minimal, but might be uneconomical to operate when gas volume declines NGL Removal - On lease

Plants are expensive, residue gas is still flared, and uneconomical to operate when gas volume declines

Top of se	egment 2 (ft)	1785	S.F.	Actual		Desire
Select 3rd segment from bottom			collapse	8.717538	>=	1.125
-			burst-b	3.246357	>=	1.25
1785 ft to	0 ft		burst-t	3.316667		
7 26 HCP-110	D LT&C		jnt strngth	9.121422	>=	1.8
Top of se	egment 3 (ft)	0	S.F.	Actual		Desire
Select 4th segment from bo	ottom		collapse	#DIV/0!	>=	1.125
			burst-b	0	>=	1.25
Oft to	0 ft		burst-t	0		
0 0	0 0		jnt strngth	7.41049	>=	1.8
Top of se	egment 4 (ft)		S.F.	Actual		Desire
Select 5th segment from bottom			collapse	#DIV/0!	>=	1.125
-			burst-b	0	>=	1.25
Oft to	ft		burst-t	0		
0 0	0 0		jnt strngth	0	>=	1.8
Top of se	egment 5 (ft)	1	\$.F.	Actual		Desire
Select 6th segment from bo		collapse	#DIV/0!	>=	1.125	
-			burst-b	0	>=	1.25
Úft to	ft		burst-t	0		
0 0	0 0		jnt strngth	0	>=	1.8
Top of se	egment 6 (ft)		jnt strngth		>=	1.8

use in colapse calculations across different pressured formations

Three gra	dient press	ure functio	n					
Depth of	evaluation:	1,200	ft			516	psi @	1.200 ft
Т	op of salt:	2,400	ft	fx #1	516			
Ba	se of salt:	3,700	ft	fx #2	900			
TD of int	ermediate:	4,600	ft	fx #3	540			
Pressure g	radient to be	e used abo	ve e	ach top to	be used as a	a function	of depth.	ex. psi/ft
fx #1	fx #2	fx #3	1					
0.43	0.75	0.45						
			-					

1) Calculate neutral point for buckling with temperature affects computed also

and the second second 2) Surface burst calculations & kick tolerance in surface pressure for burst

Adjust for best combination of safety factors

3) Do a comparison test to determine which value is lower joint strength or body yield to use in tensile strength calculations

4) Raise joint strength safety factor up to next level on page #2

5) Sour service what pipe can be used with proper degrading of strength factors and as function of temp

Secon	dary
S.F. Collapse bottom of segment:	
S.F. Collapse top of segment: 6.55	434
S.F. Burst bottom of segment:	
S.F. Burst top of segment	
S.F. Joint strength bottom of segment: 795.	518
S.F. Joint strength top of segment:	
S.F. Body yield strength bottom of segment: 764.	706
S.F. Body yield strength top of segment: 7.21	499

Collapse calculations for 1st segment - casing evacuated

.

Buoyancy factor collapse:	0.85771	
calculations for bottom of segment @	2585 ft	
hydrostatic pressure collapse - backside:	1250.11 psi	
Axial load @ bottom of section	0 lbs	previous segments
Axial load factor:	0	load/(pipe body yield strength)
Collapse strength reduction factor:	1	Messrs, Westcott, Dunlop, Kemler, 1940
Adjusted collapse rating of segment:	8580 psi	
Actual safety factor	6.86342	adjusted casing rating / actual pressure