

NEW MEXICO OIL CONSERVATION COMMISSION  
 MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS

4151 file  
 Form C-122  
 Revised 9-1-65

NOV 1 1982

|   |                             |                                  |                                     |   |   |  |
|---|-----------------------------|----------------------------------|-------------------------------------|---|---|--|
| Type Test<br><input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special |                             | Test Date<br>10/3/82             |                                     | O. C. D.  |   |  |
| Company<br>Yates Petroleum Corporation  |                             |                                  | Connection<br>Transwestern Pipeline |   |   |  |
| Pool<br>Pecos Slope - Abo Gas   |                             |                                  | Formation<br>Abo                    |   |   |  |
| Completion Date<br>5/30/82  |                             | Total Depth<br>4175'             | Plug Back TD<br>4119'               | Elevation<br>3768' GL                                     |   |  |
| Csg. Size<br>4 1/2"   | Wt.<br>9.5#                 | d<br>4.090                       | Set At<br>4165'                     | Perforations:<br>From 3768 To 3962                        |   |  |
| Tub. Size<br>2 3/8"   | Wt.<br>4.7#                 | d<br>1.995                       | Set At<br>3730                      | Perforations:<br>From To                                  |   |  |
| Type Well - Single - Bradenhead - G.G. or G.O. Multiple<br>Single   |                             |                                  | Packer Set At<br>None               |   |   |  |
| Producing Thru<br>Tubing  |                             | Reservoir Temp. °F<br>104°@ 3730 | Mean Annual Temp. °F<br>62°         | Baro. Press. - P <sub>a</sub><br>13.2 psi                 |   |  |
| L<br>3730   | H<br>3730                   | G <sub>g</sub><br>.632           | % CO <sub>2</sub><br>0.04           | % N <sub>2</sub><br>3.75                                  | % H <sub>2</sub> S<br>0                                       |  |
| Prover<br>---   |                             | Meter Run<br>2"                  |                                     | Taps<br>Flanged   |   |  |
| FLOW DATA   |                             |                                  | TUBING DATA                         |   | CASING DATA   |  |
| NO.   | Prover Line Size            | X                                | Orifice Size                        | Press. p.s.i.g.   | Diff. h <sub>w</sub>  |  |
| NO.   | Press. p.s.i.g.             | Temp. °F                         | Press. p.s.i.g.                     | Temp. °F  | Duration of Flow  |  |
| SI  | 1015                        |                                  |                                     |   | 24 hr.  |  |
| 1.  | 210                         | 72°                              | 922                                 | 62°   | 24 hr.  |  |
| 2.  | 220                         | 72°                              | 910                                 | 62°   | 24 hr.  |  |
| 3.  | 290                         | 72°                              | 890                                 | 62°   | 24 hr.  |  |
| 4.  | 280                         | 72°                              | 875                                 | 62°   | 24 hr.  |  |
| 5.  |                             |                                  |                                     |   |   |  |
| RATE OF FLOW CALCULATIONS   |                             |                                  |                                     |   |   |  |
| NO.   | Coefficient (24 Hour)       | $\sqrt{h_w P_m}$                 | Pressure P <sub>m</sub>             | Flow Temp. Factor Ft.                                     | Gravity Factor F <sub>g</sub>                                 | Super Compress. Factor, F <sub>pv</sub>                    |
| 1.  | 8.120                       | 71.7                             | 223.2                               | .9887   | 1.258   | 1.019  |
| 2.  | 8.120                       | 79.2                             | 233.2                               | .9887   | 1.258   | 1.019  |
| 3.  | 8.120                       | 87.8                             | 303.2                               | .9887   | 1.258   | 1.025  |
| 4.  | 8.120                       | 101.3                            | 293.2                               | .9887   | 1.258   | 1.024  |
| 5.  |                             |                                  |                                     |   |   |  |
| NO.   | R <sub>f</sub>              | Temp. °R                         | T <sub>r</sub>                      | z   | Gas Liquid Hydrocarbon Ratio                                  | Rate of Flow O, Mcfd                                       |
| 1.  | .34                         | 532                              | 1.49                                | .964  | Dry   | 738  |
| 2.  | .35                         | 532                              | 1.49                                | .963  | A.P.I. Gravity of Liquid Hydrocarbons                         | 815  |
| 3.  | .46                         | 532                              | 1.49                                | .952  | Specific Gravity Separator Gas .632                           | 909  |
| 4.  | .44                         | 532                              | 1.49                                | .954  | Specific Gravity Flowing Fluid X X X X X                      | 1048   |
| 5.  |                             |                                  |                                     |   | Critical Pressure 663 P.S.I.A.                                |  |
|   |                             |                                  |                                     |   | Critical Temperature 357 R                                    | 357 P.S.I.A.   |
| P <sub>c</sub> <sup>2</sup>   | 1028.2                      | P <sub>c</sub> <sup>2</sup>      | 1057.2                              |   |   |  |
| NO.   | P <sub>1</sub> <sup>2</sup> | P <sub>w</sub> <sup>2</sup>      | P <sub>w</sub> <sup>2</sup>         | P <sub>c</sub> <sup>2</sup> - P <sub>w</sub> <sup>2</sup> | (1) $\frac{P_c^2}{P_c^2 - P_w^2} = 4.156$                     | (2) $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 3.730$ |
| 1.  | 874.6                       |                                  | 881.5                               | 175.4   |   |  |
| 2.  | 852.3                       |                                  | 860.7                               | 196.5   |   |  |
| 3.  | 815.8                       |                                  | 826.3                               | 230.9   | AOF = Q $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 3908$ |  |
| 4.  | 788.9                       |                                  | 802.8                               | 254.4   |   |  |
| 5.  |                             |                                  |                                     |   |   |  |
| Absolute Open Flow 3908 Mcfd @ 15.025   |                             |                                  | Angle of Slope θ                    |   | Slope, n .924   |  |
| Remarks:  |                             |                                  |                                     |   |   |  |
| Approved By Commission:   |                             | Conducted By:<br>David Weaver    |                                     | Calculated By:<br>Andie Alderson                          |   | Checked By:  |

COMPANY Yates Petroleum Corp. LEASE Kingsway 50" WELL NO. 2 DATE 10/20/82

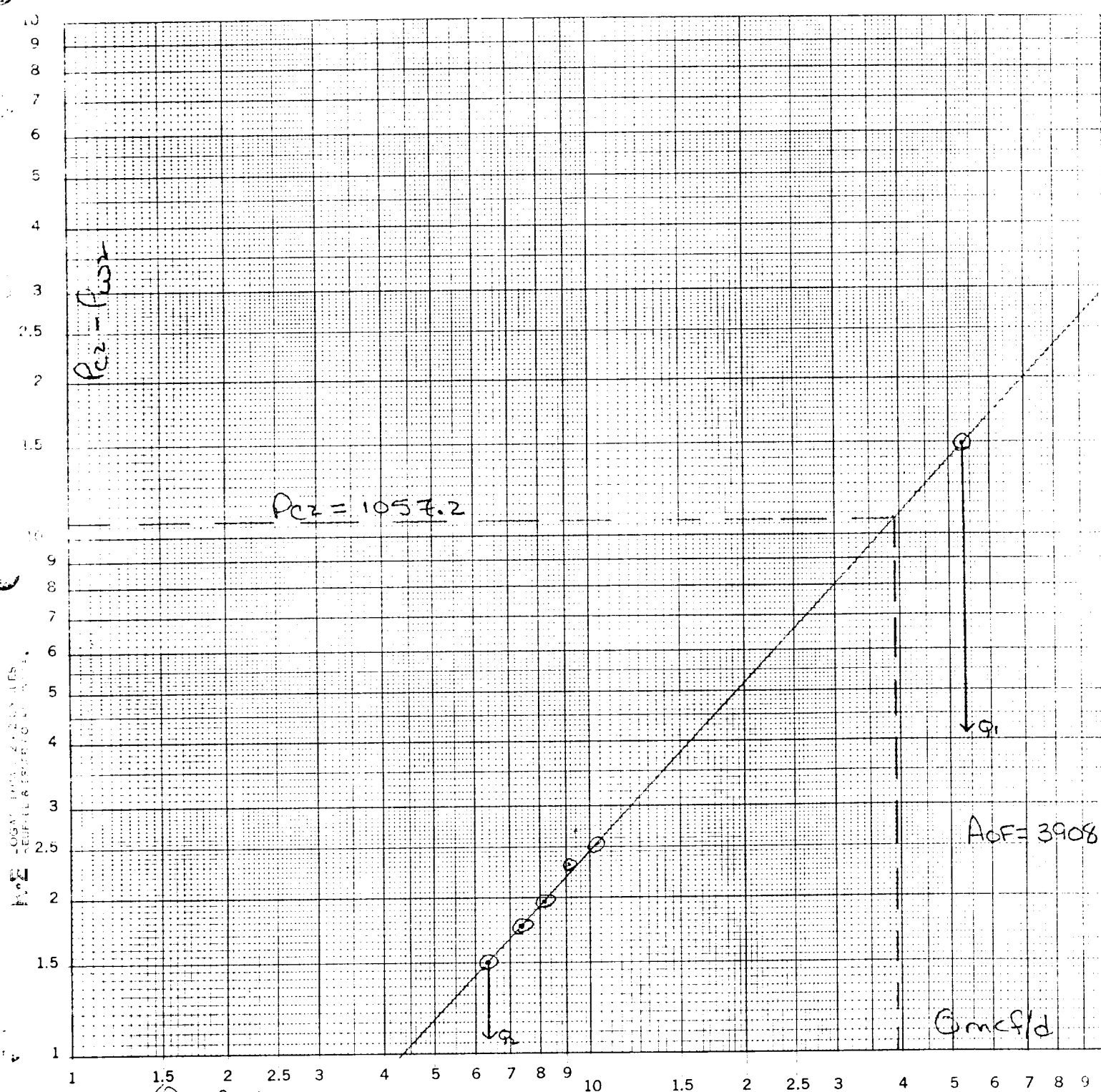
LOCATION: Unit 0 Section 24 Township 6S Range 7SE

L 3730 H 3730 LH 1 G 632 %CO<sub>2</sub> 0.04 %N<sub>2</sub> 3.75 %H<sub>2</sub>S 0

D 1995 F<sub>1</sub> .01823 GH 2357 P<sub>cr</sub> 663 T<sub>cr</sub> 357

| LINE  | 1ST    | 2ND     | 3RD    | 4TH    |
|---|--------|---------|--------|--------|
| 1 Q <sub>m</sub>  | .738   | .815    | .909   | 1.048  |
| 2 T <sub>g</sub> (W.H. 9R)  | 522    | 522     | 522    | 522    |
| 3 T <sub>s</sub> (B.H. 9R)  | 564    | 564     | 564    | 564    |
| 4 T = (LW <sup>2</sup> /15)   | 543    | 543     | 543    | 543    |
| 5 Z (Est.)  | .867   | .869    | .871   | .872   |
| 6 T <sub>2</sub>  | 470.78 | 471.867 | 472.95 | 473.5  |
| 7 GH/TZ   | 5.007  | 4.995   | 4.984  | 4.978  |
| 8 e <sup>s</sup> (Table XIV)  | 1.207  | 1.206   | 1.206  | 1.205  |
| 9 1-e <sup>s</sup> (Table XIV)  | .171   | .171    | .171   | .170   |
| 10 P <sub>1</sub>   | 925.2  | 923.2   | 903.2  | 888.2  |
| 11 P <sub>1</sub> 2/1000  | 874.6  | 852.3   | 815.8  | 788.9  |
| 12 F <sub>1</sub> (Table XV)  | .01823 | .01823  | .01823 | .01823 |
| 13 F <sub>c</sub> = F <sub>1</sub> TZ   | 8.582  | 8.602   | 8.622  | 8.632  |
| 14 F <sub>c</sub> Q <sub>m</sub>  | 6.334  | 7.011   | 7.837  | 9.046  |
| 15 L/H (F <sub>c</sub> Q <sub>m</sub> ) <sup>2</sup>                                      | 40.117 | 47.150  | 61.424 | 81.833 |
| 16 F <sub>w</sub> = L/H (F <sub>c</sub> Q <sub>m</sub> ) <sup>2</sup> (1-e <sup>s</sup> ) | 6.860  | 8.405   | 10.503 | 13.912 |
| 17 P <sub>w</sub> <sup>2</sup> = P <sub>1</sub> <sup>2</sup> + F <sub>w</sub>             | 881.5  | 860.7   | 826.3  | 802.8  |
| 18 F <sub>s</sub> <sup>2</sup> = e <sup>s</sup> P <sub>w</sub> <sup>2</sup>               | 1063.9 | 1038.0  | 996.5  | 967.4  |
| 19 F <sub>s</sub>   | 1031.5 | 1018.8  | 998.2  | 983.6  |
| 20 P = (P <sub>1</sub> + P <sub>s</sub> )   | 983.3  | 971.0   | 950.7  | 935.9  |
| 21 P <sub>1</sub> = (P/P <sub>1</sub> )   | 1.48   | 1.46    | 1.43   | 1.41   |
| 22 T <sub>1</sub> = (T/T <sub>1</sub> )   | 1.52   | 1.5     | 1.5    | 1.5    |
| 23 Z (Table XII)  | 1.67   | 1.67    | 1.67   | 1.67   |

Yates Petroleum Co.  
 Kilgore '30" #2  
 Unit B 24-65-25E  
 Chaves County



$$(P_z - P_{wz})_1 = 1500$$

$$(P_z - P_{wz})_2 = 150$$

$$Q_1 = 5350$$

$$Q_2 = 658$$

$$\log Q_1 = 3.72835$$

$$\log Q_2 = 2.80482$$

$$n = .92353 = .924$$