

NEW MEXICO OIL CONSERVATION COMMISSION  
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122  
Revised 9-1-65

Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special					Test Date <b>12-19-69</b>					
Company <b>PAN AMERICAN PETROLEUM CORP.</b>				Connection <b>None</b>						
Pool <b>Ballard</b>				Formation <b>Pictured Cliffs</b>				Unit		
Completion Date <b>12-12-69</b>		Total Depth <b>2952</b>		Plug Back TD <b>2914</b>		Elevation / <b>HSS</b> <b>GL 7198/ 7212</b>		Farm or Lease Name <b>Jicarilla Tribal 390</b>		
Csg. Size <b>4.500</b>	Wt. <b>9.5</b>	d <b>4.090</b>	Set At <b>2948</b>	Perforations: From <b>2829</b> To <b>2852</b>			Well No. <b>2</b>			
Tbg. Size <b>1.660</b>	Wt. <b>2.4</b>	d <b>1.380</b>	Set At <b>2842</b>	Perforations: From <b>Open End</b> To			Unit <b>I</b>	Sec. <b>24</b>	Twp. <b>23</b>	Rge. <b>4</b>
Type Well - Single - Bradenhead - G.G. or G.O. Multiple <b>Single</b>					Packer Set At <b>None</b>			County <b>Sandoval</b>		
Producing Thru <b>Tubing</b>		Reservoir Temp. °F <b>90 @ TD</b>		Mean Annual Temp. °F <b>Est. 60°</b>		Baro. Press. - P <sub>a</sub> <b>12 PSIA Est.</b>		State <b>New Mexico</b>		
L <b>2841</b>	H <b>2841</b>	G <sub>g</sub> <b>.650</b>	% CO <sub>2</sub>	% N <sub>2</sub>	% H <sub>2</sub> S	Prover	Meter Run	Taps		
FLOW DATA					TUBING DATA		CASING DATA		Duration of Flow	
NO.	Line Size	X Size Choke	Press. p.s.i.g.	Diff. h <sub>w</sub>	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI	<b>7 Days</b>					<b>701</b>		<b>700</b>		
1.	<b>2 Inch</b>	<b>.750</b>	<b>74</b>			<b>74</b>	<b>60° Est.</b>	<b>356</b>		<b>3 Hrs.</b>
2.										
3.										
4.										
5.										
RATE OF FLOW CALCULATIONS										
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P <sub>m</sub>	Flow Temp. Factor Ft.	Gravity Factor F <sub>g</sub>	Super Compress. Factor, F <sub>pv</sub>	Rate of Flow Q, Mcfd			
1	<b>12.3650</b>		<b>86</b>	<b>1.000</b>	<b>.9600</b>	<b>1.010</b>	<b>1032</b>			
2.										
3.										
4.										
5.										
NO.	P <sub>r</sub>	Temp. °R	T <sub>r</sub>	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.					
1.					A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.					
2.					Specific Gravity Separator Gas _____			X X X X X X X X X X		
3.					Specific Gravity Flowing Fluid _____			X X X X X		
4.					Critical Pressure _____ P.S.I.A.			P.S.I.A.		
5.					Critical Temperature _____ R			R		
P <sub>c</sub> <b>713</b>		P <sub>c</sub> <sup>2</sup> <b>508,369</b>								
NO.	P <sub>t</sub> <sup>2</sup>	P <sub>w</sub>	R <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> - R <sub>w</sub> <sup>2</sup>	(1) $\frac{P_c^2}{P_c^2 - R_w^2} = 1.3631$		(2) $\left[ \frac{P_c^2}{P_c^2 - R_w^2} \right]^n = 1.3011$			
1		<b>368</b>	<b>135,424</b>	<b>372,945</b>						
2										
3										
4										
5										
AOF = Q $\left[ \frac{P_c^2}{P_c^2 - R_w^2} \right]^n = 1343$										
Absolute Open Flow <b>1343</b> Mcfd @ 15.025					Angle of Slope $\theta$ _____			Slope, n <b>.85</b>		
Remarks: _____										
Approved By Commission:			Conducted By: <b>B. D. Dukes</b>			Calculated By:			Checked By: <b>J. J. Layton</b>	

