EFTELLER, INC.
reservoir engineering data
MIDLAND, TEXAS

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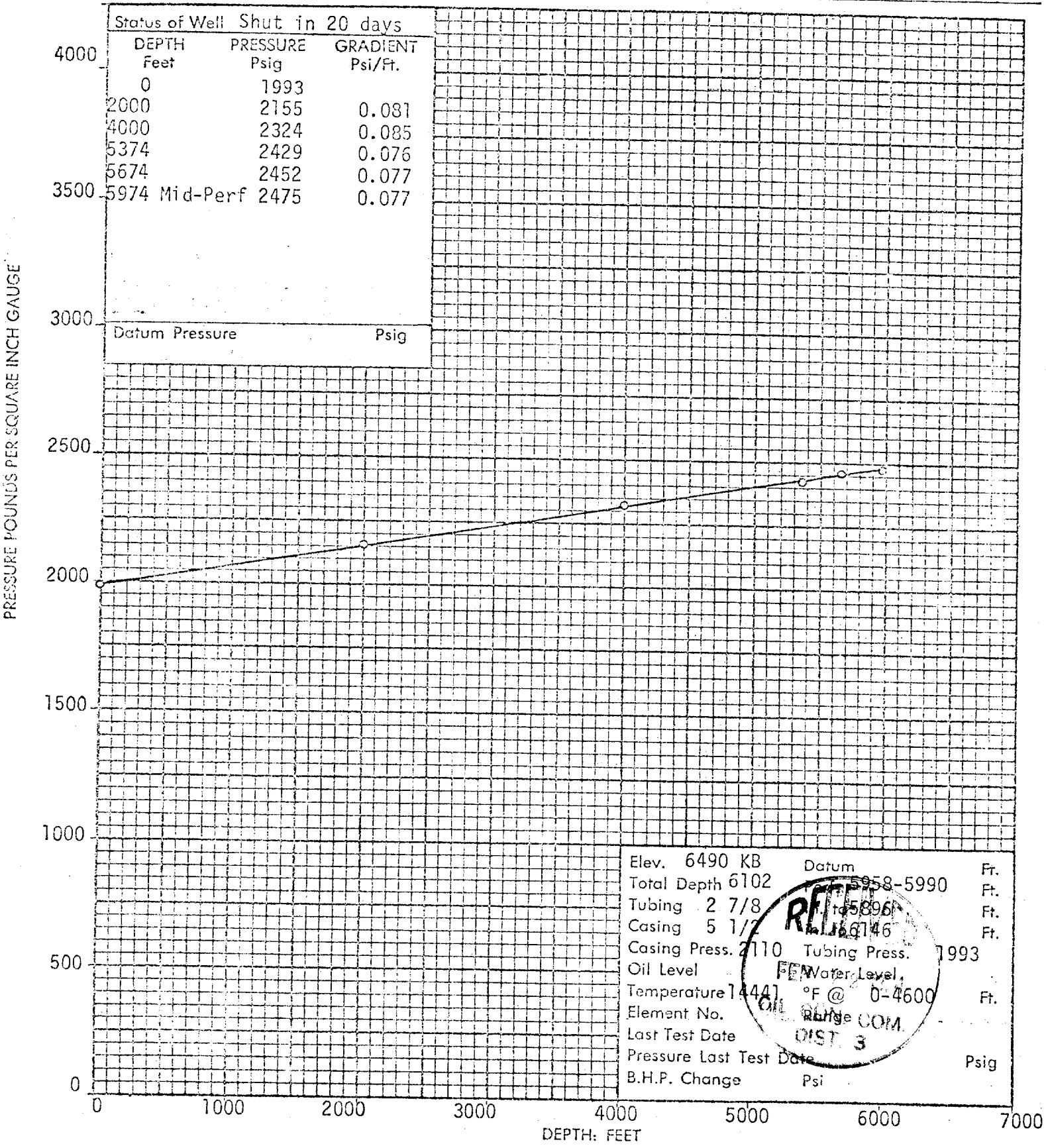
File 2-5475-P

Company TENNECO OIL COMPANY Lease CANYON Well No. 8
Field BASIN DAKOTA County SAN JUAN State NEW MEXICO
Formation DAKOTA Test Date JANUARY 30, 1974

Status of Well Shut in 20 days

DEPTH Feet	PRESSURE Psig	GRADIENT Psi/Ft.
0	1993	
2000	2155	0.081
4000	2324	0.085
5374	2429	0.076
5674	2452	0.077
5974 Mid-Perf	2475	0.077

Datum Pressure Psig



Elev. 6490 KB Datum Ft.
Total Depth 6102 Ft. 5958-5990 Ft.
Tubing 2 7/8 Ft. to 5896 Ft.
Casing 5 1/2 Ft. to 6146 Ft.
Casing Press. 2110 Tubing Press. 1993
Oil Level Ft. Water Level,
Temperature 144] °F @ 0-4600 Ft.
Element No. Range
Last Test Date
Pressure Last Test Date Psig
B.H.P. Change Psi

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NEW MEXICO OIL CONSERVATION COMMSSION

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

Type Test: [X] Initial [ ] Annual [ ] Special			Test Date: 1-11-74	
Company: Tenneco Oil Company		Connection		
Pool: Basin Dakota		Formation: Dakota		Unit
Completion Date	Total Depth	Plug Back TD: 6102	Elevation: 6490 KB	Farm or Lease Name: Canyon
Csg. Size: 5 1/2 / Wt. / d / Set At: 6146		Perforations: From 5958 To 5990		Well No.: 8
Tbg. Size: 2 7/8 / Wt. / d / Set At: 5896		Perforations: From To		Unit: L Sec.: 11 Twp.: 25 Rge.: 11
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single		Packer Set At		County: San Juan
Producing Thru: Tubing	Reservoir Temp. °F	Mean Annual Temp. °F	Baro. Press. – P_a: 12.0	State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
						X		

	FLOW DATA				TUBING DATA		CASING DATA		
NO.	Prover Line Size X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI					2019		2115		72
1.	2 x 3/4				691	60	1167		3 hrs
2.									
3.									
4.									
5.									

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	12.3650		703	1.000	.9608	1.063	8878
2.							
3.							
4.							
5.							

NO.	P_r	Temp. °R	T_r	Z
1				
2.				
3.				
4.				
5.				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

P_c 2127 P_c^2 4524129

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1		1179	1411263	3112866
2				
3				
4				
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.4534$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.3236$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 11751$

Absolute Open Flow 11751 Mcfd @ 15.025 Angle of Slope θ _____ Slope, n .75

Remarks: _____

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Approved By Commission:	Conducted By:	Calculated By:	Checked By:
	Tefteller, Inc.	N. Tefteller	