Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Poo	1 Undesign	gnated	<del></del>	_Formation	n Pict	ured Cli	ffs	County_	Rio Ar	riba	
Ini	tial X		_Annual		Spec	ial		Date of	Test_	-1-58	
Com	pany <b>Kegn</b> o	clia Pet	roleum Co	ompany	Lease	Jiesrill	a *C*	Wel	1 No	6 UT-PC	
	t <u>M</u>										orp.
	ing 7 5/8*										
	ing 2 3/8" [										
	Pay: From										a
	ducing Thru										
Date	e of Complet	tion:	8-15-58	Packe	rNo	Sin <b>Be</b>	gle-Brade Reservo	enhead-G. oir Temp.	G. or (	.O. Dual	
						ED DATA		- <b>-</b>			
Test	ed Through	Pere	E) (Choke					Туре Тар	8	_	
		Fl	ow Data			Tubing	Data	Casing D			
No.	(Prover) (Line)	(Chok	e) Pres	Bs. Diff.	Temp.	Press.	Temp.			Durat	
27	Size	Siz	e psi	g h <sub>w</sub>	° <sub>F</sub> .		°F.	psig	<sup>⊃</sup> F•	of F	
SI 1.	2*	0,75	0" 18	3 -	64	910 183	64	9 <b>5</b> 7	-	3 hrs.	
1. 2. 3.											
4. 5.											
					FLOW CAL	CULATION	S				
No.	Coeffici			Pressure	Flow '	l'emp.	Gravity	Compre	ss.	Rate of Flo	wc
<del>,  </del>		r) 7	hwpf					Facto:		@ 15.025 ps	sia
1. 2. 3.	12.3650		-	195	0.996	2	0.9393	1.021		2303	
3. 4. 5.											
5.											
					ESSURE CA	LCU ATI	ONS				
as L ravi	iquid Hydro ty of Liqui	carbon F d Hydrod	carbons	-	cf/bbl. deg.		Speci Speci	fic Gravit fic Gravit	y Sepa	rator Gas_ ing Fluid <b>O</b>	680
c			(1-e <sup>-5</sup>	) -			Pc	69	P <sub>c</sub> 9	39.0	est)
	P <sub>w</sub>		Τ	<del></del>			<del></del>		<del>                                     </del>		
No.	Pt (psia)	$P_{t}^{2}$	F <sub>c</sub> Q	$(F_cQ)^2$	(F <sub>0</sub>	Q) <sup>2</sup> e-s)	P <sub>w</sub> 2	$P_c^2 - P_w^2$	Ca	) 74	
[. 2.	526			-		•	276.7	662.3	P	v 1 C	
3.									ļ — —		
5.											
bsol COMP	Lute Potent:		3103 Tolem C		_MCFPD;	n	0.85				
DDRI	ESS Box	2406. He	bbs. Nev	Mext eo		*					
VIIINE COMPA	r and TITLE ESSED	- M	<u> </u>	u mes	gan_	er. Ges	Engineer	Left.	<i>#</i> \		
OPIF	714 T		<del></del>	<del></del>	REMA	RKS		/ Kill			

Size   Size   psig   hw   OF.   psig   OF.   psig   OF.   psig   OF.   Psig   OF.   Psig   OF.	O. (Line Size				(FLEXE)				Type Tap	·s	
Choke   Cho	). (Line Size			ata			Tubing	Data	Casing D	at.a	T
Cline   Size   psig   hw   OF   psig   OF   psig   OF   Hr.	). (Line Size	er) (Ch	oke)	Press	Diff.	Temp.					Durati
Size   Size   psig   hw   oF,   psig   oF,	Size					remp.	11033.	1 cmb.	11655.	lemb.	1
PRESSURE CALCULATIONS   Pressure   Flow Temp.   Fravity   Compress.   Fact of Flow Temp.   Factor				1	1, 1	0-	١.	0_			of F1
Pressure   Flow Calculations   Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac		ະ   ວ	ıze	psig	l h <sub>w</sub> l	${}^{\circ}F$ .	psig	) F.	psig	F.	Hr.
Pressure   Flow Calculations   Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac	r <b>1</b>				<del>                                     </del>		03.0	<del>                                     </del>		<del> </del>	<del> </del>
Pressure   Flow Calculations   Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac		<del></del>	## A	1 3 4 4	<del>├</del> ─┈─┤		910	<del> </del>	95/		
Pressure   Flow Calculations   Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac		U.	<u>720"                                    </u>	183		64	183	64	514	-	3 hrs.
PLOW CALCULATIONS   Compress.   Rate of Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac	<u> </u>										
PLOW CALCULATIONS   Compress.   Rate of Flow Temp.   Gravity   Compress.   Rate of Flow Temp.   Gravity   Factor   Fac		ı									<del> </del>
FLOW CALCULATIONS  Coefficient  Pressure Flow Temp. Gravity Compress. Rate of Flow Temp.  (24-Hour) Vhwpf psia Ft Fg Fpv @ 15.025 ps  12.3650 - 195 0.9962 0.9393 1.021 2303  PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing FluidDevity of Liquid Hydrocarbons deg. Specific Gravity Flowing FluidDevity of Liquid Hydrocarbons deg.  Pc 939.0   Pw Pc Fc (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> Pw Pc Pc 939.0   Pw Pc 536 - 276.7 662.3				1				<del> </del>		<del> </del>	<del> </del>
FLOW CALCULATIONS  Coefficient  Pressure Flow Temp. Gravity Compress. Rate of Flow Temp.  (24-Hour) Vhwpf psia Ft Fg Fpv @ 15.025 ps  12.3650 - 195 0.9962 0.9393 1.021 2303  PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing FluidDevity of Liquid Hydrocarbons deg. Specific Gravity Flowing FluidDevity of Liquid Hydrocarbons deg.  Pc 939.0   Pw Pc Fc (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> Pw Pc Pc 939.0   Pw Pc 536 - 276.7 662.3	<del></del>			<del> </del>	<del> </del>					ļ	
Coefficient  (24-Hour)    (24-H				<del></del>	<u> </u>			<u> </u>		<u> </u>	
Coefficient  (24-Hour)    (24-H					τ	TOW CAT		C			
C24-Hour   The print   Factor   Facto	Coefi	ficient	<del> </del>	T D						<del></del>	
C24-Hour   V hwpf		. ICICIL		PI	essure			•	Compre	ss.	Rate of Flo
PRESSURE CALCULATIONS   PRESSURE CALCULATIONS   PRESSURE CALCULATIONS			<i> </i> —	<del></del>		Fac	tor	Factor	Facto	r	Q-MCFPD
PRESSURE CALCU'ATIONS  Liquid Hydrocarbon Ratio - cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 939.0 To Specific Gravity Separator Gas Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity Flowing FluidO.  Pc 949 Pc 92.0 To Specific Gravity FluidO.  Pc 949 Pc 92.0 T	(24-	-Hour)	√ hw	p <sub>f</sub>	psia	F.	+	F_	F	ł	
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Gravity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid Gravity Fluid Gravity Flowing Fluid Gravity Fluid Gravit	1 90 0/00		<del>+ ' - '</del>		<u> </u>				<del></del>		- 1/00~/ PS
PRESSURE CALCULATIONS  Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas Specific Gravity Flowing Fluid Gravity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid Grav Fluid Gravity Flowing Fluid Gravity Flo	12-3650	<u></u>	<del></del>		195	0.996	2	0.9393	1.021		2303
Liquid Hydrocarbon Ratio	<b></b>						T				
Liquid Hydrocarbon Ratio										+	<del></del>
Liquid Hydrocarbon Ratio			1				+-		<del></del>		<del></del>
Liquid Hydrocarbon Ratio			<del> </del>	<del></del>							
Liquid Hydrocarbon Ratio											
Pt (psia)  Pt FcQ (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> P <sub>w</sub> <sup>2</sup> P <sub>c</sub> -P <sub>w</sub> <sup>2</sup> Cal.  P <sub>w</sub>		<del></del>									
Pt (psia)  526  526  526  526  526  526  526  52	! Pw		2   _		<i>1</i> 2		.2		2 2		
Solute Potential: 3103 MCFPD; n 0.85  MPANY Magnolia Petroleus Company  DRESS Box 2/06, Hebbs, New Mexico  ENT and TITLE William a Zwayen Jr. Gas Engineer  (NESSED REMARKS	,	$P_{1}$	t F	c <sup>Q</sup>	(F <sub>c</sub> Q)~	(F <sub>0</sub>	<sub>2</sub> Q)~	P <sub>w</sub> 2	$P_{c}^{\sim}-P_{w}^{\sim}$	Ca	7   D
Solute Potential: 3103 MCFPD; n 0.85  MPANY Magnolia Petroleus Company  DRESS Box 2/06, Hebbs, New Mexico  ENT and TITLE William a Zwayen Jr. Gas Engineer  (NESSED REMARKS		.a)		Ĭ	_	(1)	_e-s )	W	C 17		
Solute Potential: 3103 MCFPD; n 0.85  PANY Magnolia Petrolema Company  ORESS Box 2406, Hobbs, New Mexico  ENT and TITLE William a Zaragan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi						,			F	Po
Solute Potential: 3103 MCFPD; n 0.85  PANY Magnolia Petrolema Company  ORESS Box 2406, Hobbs, New Mexico  ENT and TITLE William a Zaragan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi					<del></del>		00/ 5	//		
Solute Potential: 3103 MCFPD; n 0.85  PANY Magnolia Petrolema Company  ORESS Box 2406, Hobbs, New Mexico  ENT and TITLE William a Zaragan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi	-		-		<u>-</u>		276.7	662.3		
Solute Potential: 3103 MCFPD; n 0.85  PANY Magnolia Petrolema Company  ORESS Box 2406, Hobbs, New Mexico  ENT and TITLE William a Zaragan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi			-				276.7	662.3		
PANY Magnolia Petroleum Company  DRESS Box 2406, Hobbs, New Mexico  ENT and TITLE Zulliam a Zargan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi	•		-				276.7	662.3		
PANY Magnolia Petroleum Company  DRESS Box 2406, Hobbs, New Mexico  ENT and TITLE Zulliam a Zargan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi	•			•			276.7	662.3		
PANY Magnolia Petroleum Company  DRESS Box 2406, Hobbs, New Mexico  ENT and TITLE Zulliam a Zargan Jr. Gas Engineer  (NESSED  (PANY REMARKS	Pt (psi	•						276.7	662.3		
ORESS Box 2006, Robbs, New Mexico ENT and TITLE William a Zargan Jr. Gas Engineer (NESSED (PANY)  REMARKS	P+ (psi		27		•				662.3		
PANY REMARKS	pt (psi	ential:		L03					662.3		
PANY REMARKS	Pt (psi	ential:	Petrol	L03					662.3		
IPANY REMARKS	526  solute Por MPANY MORESS B	ential:	Petrol	LO3	pany	MCFPD;	n	υ <b>.</b> 85	662.3		
IPANYREMARKS	Solute Por MPANY M DRESS B	ential:	Petrol	LO3	pany	MCFPD;	n	υ <b>.</b> 85	662.3		
REMARKS	Solute Por MPANY M DRESS B	ential:	Petrol	LO3	pany	MCFPD;	n	υ <b>.</b> 85	662.3		
	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	υ <b>.</b> 85	662.3		
SEP 26 1958 OIL COM COM.	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	υ <b>.</b> 85	662.3		
OIL COM COM.	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		
OIL COM COM.	526 solute Pot MPANY MDRESS B	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		
Som.	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		
Same of the second seco	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		
	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		
	Solute Por MPANY M DRESS B ENT and TI	ential:	Petrol	LO3	pany	MCFPD;	n	0.85 Engineer	AIII.		

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q = Actual rate of flow at end of flow period at W. H. working pressure ( $P_{\rm W}$ ). MCF/da. @ 15.025 psia and 60° F.
- P<sub>c</sub>= 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw- Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- $P_{f}$  Meter pressure, psia.
- hw Differential meter pressure, inches water.
- Fg Gravity correction factor.
- Ft Flowing temperature correction factor.
- Fpv Supercompressability factor.
- n I Slope of back pressure curve.
- Note: If  $P_{\rm W}$  cannot be taken because of manner of completion or condition of well, then  $P_{\rm W}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\rm t}$ .

OIL CONSERVATION C	OMMI:	SSION
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