NEW MEXICO OIL CONSERVATION COMMSSION

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

Type Test: [X] Initial [ ] Annual [ ] Special				Test Date: 7-31-80	
Company: El Paso Natural Gas Company			Connection: Northwest Pipeline		
Pool: Basin			Formation: Dakota		Unit: San Juan 27-4 Unit
Completion Date: 6-12-80	Total Depth: 8426		Plug Back TD: 8418	Elevation: 7114 GR	Farm or Lease Name: San Juan 27-4 Unit
Csg. Size: 7.00 / Wt.: 23 / d: 6.366 / Set At: 6753			Perforations: From *8176 To 8384		Well No.: #133 (DK)
Tbg. Size: 2.375 / Wt.: 4.7 / d: 1.995 / Set At: 8390			Perforations: From To		Unit: K / Sec.: 27 / Twp.: 27 / Rge.: 4
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: G.G. Dual			Packer Set At: 6578		County: Rio Arriba
Producing Thru: Tbg.	Reservoir Temp. °F: @	Mean Annual Temp. °F	Baro. Press. – P_a		State: New Mexico
L	H	Gg: 0.67	% CO_2	% N_2	% H_2S / Prover / Meter Run: 4" / Taps: Flg.

	FLOW DATA				TUBING DATA		CASING DATA		
NO.	Prover Line Size X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI					925				49 Days
1.	4" X 2.75"	6	2.0	71	25				3 Hrs.
2.									
3.									
4.									
5.									

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	41.10	8.486	18	0.9896	1.222	1.004	423
2.							
3.							
4.							
5.							

NO.	P_r	Temp. °R	T_r	Z
1.	.027	531	1.390	.965
2.				
3.				
4.				
5.				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXX
Specific Gravity Flowing Fluid _____ XXXXX
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

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OIL CON. COM.
DIST. 3

P_c 937 P_c^2 877,969

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1	324	75	5625	872344
2				
3				
4				
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.0064$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.0048$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 425$

Absolute Open Flow 425 Mcfd @ 15.025 | Angle of Slope θ _____ | Slope, n .75

Remarks: * 4.500 Liner - 6604' - 8426
Liquids - 18.8 Bbls Oil, 15.0 Bbls Water
Gas Vented 50 MCF

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
	Roger Hardey	Bill Clark	