

NEW MEXICO OIL CONSERVATION COMMISSION  
 MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122  
 Revised 9-1-65

|   |             |                                    |                                       |
|---|-------------|------------------------------------|---------------------------------------|
| Type Test<br><input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special |             | Test Date<br>7-10-69               |                                       |
| Company<br>Burleson and Huff  |             | Connection<br>None                 |                                       |
| Pool<br>Jalmat  |             | Formation<br>Yates                 |                                       |
| Completion Date<br>7-10-69  |             | Total Depth<br>2463                | Elevation<br>3018                     |
| Csg. Size<br>7  | Wt.<br>2263 | Perforations:<br>From Open To Hole | Well No.<br>1                         |
| Tbg. Size<br>2 1/2  | Wt.<br>2250 | Perforations:<br>From Open To End  | Unit<br>28                            |
| Type Well - Single - Bradenhead - G.G. or G.O. Multiple<br>Single   |             | Plug Back TD                       | County<br>Lea                         |
| Producing Thru<br>Tbg.  |             | Reservoir Temp. °F<br>60           | Baro. Press. - P <sub>a</sub><br>13.2 |
| L   | H           | Gg<br>.641                         | % CO <sub>2</sub><br>1.27             |
|   |             | % N <sub>2</sub><br>1.59           | % H <sub>2</sub> S<br>.50%            |
|   |             | Prover<br>2"                       | Meter Run<br>Taps                     |

| FLOW DATA |                  |   |              |                 |                      | TUBING DATA |                 | CASING DATA |                 | Duration of Flow |   |
|-----------|------------------|---|--------------|-----------------|----------------------|-------------|-----------------|-------------|-----------------|------------------|---|
| NO.       | Prover Line Size | X | Orifice Size | Press. p.s.i.g. | Diff. h <sub>w</sub> | Temp. °F    | Press. p.s.i.g. | Temp. °F    | Press. p.s.i.g. | Temp. °F         |   |
| SI        |                  |   |              |                 |                      |             | 796             | 74          | 797             |                  |   |
| 1.        | 2"               | x | 7/32         | 786             |                      | 74          | 786             |             | 788             |                  | 1 |
| 2.        | 2"               | x | 5/16         | 768             |                      | 74          | 768             |             | 778             |                  | 1 |
| 3.        | 2"               | x | 1/2          | 679             |                      | 65          | 679             |             | 731             |                  | 1 |
| 4.        | 2"               | x | 3/4          | 481             |                      | 64          | 481             |             | 658             |                  | 1 |
| 5.        | 2"               | x | 1.000        | 323             |                      | 50          | 323             |             | 605             |                  | 1 |

| RATE OF FLOW CALCULATIONS |                       |                  |                         |                       |                   |                            |                      |
|---------------------------|-----------------------|------------------|-------------------------|-----------------------|-------------------|----------------------------|----------------------|
| NO.                       | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure P <sub>m</sub> | Flow Temp. Factor Ft. | Gravity Factor Fg | Super Compress. Factor Fpv | Rate of Flow Q, Mcfd |
| 1                         | .8393                 |                  | 799.2                   | .9868                 | 1.249             | 1.075                      | 889                  |
| 2                         | 1.672                 |                  | 781.2                   | .9869                 | 1.249             | 1.073                      | 1,728                |
| 3                         | 4.279                 |                  | 692.2                   | .9952                 | 1.249             | 1.070                      | 3,940                |
| 4                         | 9.453                 |                  | 404.2                   | .9962                 | 1.249             | 1.049                      | 6,023                |
| 5                         | 17.09                 |                  | 336.2                   | 1.001                 | 1.249             | 1.033                      | 7,421                |

| NO. | P <sub>i</sub> | Temp. °R | T <sub>r</sub> | Z    | Gas Liquid Hydrocarbon Ratio | A.P.I. Gravity of Liquid Hydrocarbons | Specific Gravity Separator Gas | Specific Gravity Flowing Fluid | Critical Pressure | Critical Temperature |
|-----|----------------|----------|----------------|------|------------------------------|---------------------------------------|--------------------------------|--------------------------------|-------------------|----------------------|
|     |                |          |                |      | Dry                          |                                       |                                |                                |                   |                      |
| 1.  | 1.19           | 534      | 1.41           | .856 |                              |                                       |                                |                                |                   |                      |
| 2.  | 1.17           | 534      | 1.41           | .858 |                              |                                       |                                |                                |                   |                      |
| 3.  | 1.03           | 525      | 1.41           | .873 |                              |                                       |                                |                                |                   |                      |
| 4.  | .74            | 524      | 1.41           | .908 |                              |                                       |                                |                                |                   |                      |
| 5.  | .50            | 519      | 1.40           | .937 |                              |                                       |                                |                                |                   |                      |

| NO. | P <sub>i</sub> <sup>2</sup> | P <sub>w</sub> | P <sub>w</sub> <sup>2</sup> | P <sub>c</sub> <sup>2</sup> - P <sub>w</sub> <sup>2</sup> | (1) $\frac{P_c^2}{P_c^2 - P_w^2} =$ | (2) $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n =$ |
|-----|-----------------------------|----------------|-----------------------------|---|-------------------------------------|--|
|     |                             |                |                             |   | 2.394                               | 1.776  |
| 1   |                             | 801.2          | 641.9                       | 14.5  |                                     |  |
| 2   |                             | 791.2          | 626.0                       | 30.4  |                                     |  |
| 3   |                             | 744.2          | 553.8                       | 102.6   |                                     |  |
| 4   |                             | 671.2          | 450.5                       | 205.9   |                                     |  |
| 5   |                             | 618.2          | 382.2                       | 274.2   |                                     |  |

AOF = Q  $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 13,180$

Absolute Open Flow 13,180 Mcfd @ 15.025 Angle of Slope  $\theta$  57 Slope, n .658

Remarks:

Approved By Commission: *[Signature]*  
 Conducted By: Don Read, J. C. Roberts  
 Calculated By: Don Read, J. C. Roberts  
 Checked By: