

GRI GlyCalc Information

Meter Number: 2273
Meter Name: SJ Blanco C Inlet 3-25-21
Location: SJ Blanco Plant
Sample Date: 3/25/2021
File name: SJ Blanco C Inlet 3-25-21_1.D

Flow Pressure: 128
Flow Temp: 65
H2O, Lb/MMCF: --
H2S, ppmmol: --
Type: Spot
Pulled by: Michael Fauteaux

Component	Mol%	Wt%	LV%
Carbon Dioxide	1.7251	3.7806	1.5863
Hydrogen Sulfide	0.0000	0.0000	0.0000
Nitrogen	0.1983	0.2766	0.1175
Oxygen	0.0000	0.0000	0.0000
Methane	84.4292	67.4490	77.1272
Ethane	7.5660	11.3292	10.9032
Propane	3.2654	7.1705	4.8477
Isobutane	0.6276	1.8165	1.1066
n-Butane	0.8756	2.5342	1.4874
Isopentane	0.3268	1.1740	0.6439
n-Pentane	0.2414	0.8671	0.4714
Cyclopentane	0.0169	0.0589	0.0269
n-Hexane	0.0810 % VOCs	0.3477	0.1795
Cyclohexane	0.0441 6.0815	0.1847	0.0808
Other Hexanes	0.1902	0.8116	0.4081
Heptanes	0.0967	0.4809	0.2359
Methylcyclohexane	0.0526	0.2573	0.1140
2,2,4 Trimethylpentane	0.0000	0.0000	0.0000
Benzene	0.0163	0.0635	0.0246
Toluene	0.0207	0.0948	0.0373
Ethylbenzene	0.0007	0.0038	0.0015
Xylenes	0.0063	0.0331	0.0130
C8+ Heavies	0.2192	1.2661	0.5870
Total	100.0000	100.0000	100.0000

tjlong	Dry Basis Mole %	MW	lb/lb-mol	lb/Mscf
CO ₂	1.73	44.01	0.76	2.00
H ₂ S	0.00	34.08		
N ₂	0.20	28.01	0.06	0.15
O ₂	0.00	16.00		
Methane	84.43	16.04	13.54	35.69
Ethane	7.57	30.07	2.28	6.00
Propane	3.27	44.10	1.44	3.79
i-butane	0.63	58.12	0.36	0.96
n-butane	0.88	58.12	0.51	1.34
i-pentane	0.33	72.15	0.24	0.62
n-pentane	0.24	72.15	0.17	0.46
Other C6+	0.74	86.117	0.64	1.69
Total:	100.0	Avg. MW = 20.00		
		VOC lb/MCF:		8.87

Density at STP calculated using the ideal gas law.
 $\text{lb voc/MCF} = ((\text{mol\%} * \text{MW})/100) * 1000/379.482$

Constants Used: GPA Standard 2145-16 (FPS)

GasCal - [Differential / Volume]

File

Differential / Volume

Differential for known Volume:	Static Pipeline Volume:	Pig Travel Time:
Meter Tube Size: 12	Pipe Diameter: 30	Pipe Diameter: 30
Orifice Plate Size: 3.5	Length: 2786	Length: 17
Pressure: 865	(F)eet or (M)iles: F	(F)eet or (M)iles: M
Volume (mcf): 12300	Pressure: 32	Volume (mcf): 200000
Temperature: 72	Temperature: 75	Upstream Pressure: 750
Gravity: 0.582	Pressure Base: 14.73	Downstream Pressure: 700
Mole % CO2: 0	Gravity: .644	Temperature: 60
Mole % N2: 0	Barometer: 14.6	Pressure Base: 14.73
Pressure Base: 14.73		Gravity: 0.6
Temperature Base: 60		Barometer: 14.73

Differential 1 Run: 25.5	Vol. (cu. ft.): 51,761.2	Hrs: 2 Min: 48 Sec: 49
Differential 2 Runs: 6.4	Lbs of Gas: 2,077.4	Miles per Hour: 6.04
	Tons of Gas: 1.039	

Main MenuGas Cal.Plate ChangeWeymouthAnalysisRetro/SetpointBlowdown Cal.

GasCal - [Differential / Volume]

File

Differential / Volume

Differential for known Volume:

Meter Tube Size: 12
Orifice Plate Size: 3.5
Pressure: 865
Volume (mcf): 12300
Temperature: 72
Gravity: 0.582
Mole % CO2: 0
Mole % N2: 0
Pressure Base: 14.73
Temperature Base: 60

Differential 1 Run: 25.5
Differential 2 Runs: 6.4

Static Pipeline Volume:

Pipe Diameter: 30
Length: 2786
(F)eeet or (M)iles: F
Pressure: 45
Temperature: 75
Pressure Base: 14.73
Gravity: .644
Barometer: 14.6

Vol. (cu. ft.): 42,168.0
Lbs of Gas: 2,077.4
Tons of Gas: 1.039

Pig Travel Time:

Pipe Diameter: 30
Length: 17
(F)eeet or (M)iles: M
Volume (mcf): 200000
Upstream Pressure: 750
Downstream Pressure: 700
Temperature: 60
Pressure Base: 14.73
Gravity: 0.6
Barometer: 14.73

Hrs: 2 Min: 48 Sec: 49
Miles per Hour: 6.04

Input Pressure (psig)

Main Menu

Gas Cal.

Plate Change

Weymouth

Analysis

Retro/Setpoint

Blowdown Cal.

GasCal - [Differential / Volume]

File

Differential / Volume

Differential for known Volume:	Static Pipeline Volume:	Pig Travel Time:
Meter Tube Size: 12	Pipe Diameter: 30	Pipe Diameter: 30
Orifice Plate Size: 3.5	Length: 2786	Length: 17
Pressure: 865	(F)eet or (M)iles: F	(F)eet or (M)iles: M
Volume (mcf): 12300	Pressure: 70	Volume (mcf): 200000
Temperature: 72	Temperature: 75	Upstream Pressure: 750
Gravity: 0.582	Pressure Base: 14.73	Downstream Pressure: 700
Mole % CO2: 0	Gravity: .644	Temperature: 60
Mole % N2: 0	Barometer: 14.6	Pressure Base: 14.73
Pressure Base: 14.73		Gravity: 0.6
Temperature Base: 60		Barometer: 14.73
Differential 1 Run: 25.5	Vol. (cu. ft.): 53,992.3	Hrs: 2 Min: 48 Sec: 49
Differential 2 Runs: 6.4	Lbs of Gas: 2,660.0	Miles per Hour: 6.04
	Tons of Gas: 1.330	

Input Pressure (psig)

Main Menu Gas Cal. Plate Change Weymouth Analysis Retro/Setpoint Blowdown Cal.

District I

1625 N. French Dr., Hobbs, NM 88240
Phone:(575) 393-6161 Fax:(575) 393-0720

District II

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Phone:(575) 748-1283 Fax:(575) 748-9720

District III

1000 Rio Brazos Rd., Aztec, NM 87410
Phone:(505) 334-6178 Fax:(505) 334-6170

District IV

1220 S. St Francis Dr., Santa Fe, NM 87505
Phone:(505) 476-3470 Fax:(505) 476-3462

State of New Mexico
Energy, Minerals and Natural Resources
Oil Conservation Division
1220 S. St Francis Dr.
Santa Fe, NM 87505

QUESTIONS

Action 33367

QUESTIONS

Operator: Enterprise Field Services, LLC PO Box 4324 Houston, TX 77210	OGRID: 241602
	Action Number: 33367
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS**Determination of Reporting Requirements**

Answer all questions that apply. The Reason(s) statements are calculated based on your answers and may provide additional guidance.

Was or is this venting or flaring caused by an emergency or malfunction	No
Did or will this venting or flaring last eight hours or more cumulatively within any 24-hour period from a single event	No
Is this considered a submission for a notification of a major venting or flaring	Yes, minor venting or flaring of natural gas.
The operator shall file a form C-141 instead of a form C-129 for a release that includes liquid during venting or flaring that is or may be a major or minor release under 19.13.29.7 NMAC.	
Was there or will there be at least 50 MCF of natural gas vented or flared during this event	Yes
Did this venting or flaring result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No

Unregistered Facility Site

Please provide the facility details, if the venting or flaring occurred or is occurring at a facility that does not have an Facility ID (##) yet.

Facility or Site Name	Blanco-Chaco 30 Inch Pipeline
Facility Type	Pipeline - Gas Gathering - (PGG)

Equipment Involved

Primary Equipment Involved	Not answered.
Additional details for Equipment Involved. Please specify	Not answered.

Representative Compositional Analysis of Vented or Flared Natural Gas

Please provide the mole percent for the percentage questions in this group.

Methane (CH4) percentage	84
Nitrogen (N2) percentage, if greater than one percent	0
Hydrogen Sulfide (H2S) PPM, rounded up	0
Carbon Dioxide (CO2) percentage, if greater than one percent	2
Oxygen (O2) percentage, if greater than one percent	0
If you are venting and/or flaring because of Pipeline Specification, please provide the required specifications for each gas.	
Methane (CH4) percentage quality requirement	Not answered.
Nitrogen (N2) percentage quality requirement	Not answered.
Hydrogen Sulfide (H2S) PPM quality requirement	Not answered.
Carbon Dioxide (CO2) percentage quality requirement	Not answered.
Oxygen (O2) percentage quality requirement	Not answered.

Date(s) and Time(s)

Date venting or flaring was discovered or commenced	06/22/2021
Time venting or flaring was discovered or commenced	09:00 PM
Is the venting or flaring event complete	Yes
Date venting or flaring was terminated	06/23/2021
Time venting or flaring was terminated	03:00 AM
Total duration of venting or flaring in hours, if venting or flaring has terminated	4
Longest duration of cumulative hours within any 24-hour period during this event	4

Measured or Estimated Volume of Vented or Flared Natural Gas

Natural Gas Vented (Mcf) Details	Cause: Normal Operations Pipeline (Any) Natural Gas Vented Spilled: 148 Mcf Recovered: 0 Mcf Lost: 148 Mcf
Natural Gas Flared (Mcf) Details	Cause: Normal Operations Pipeline (Any) Natural Gas Flared Spilled: 148 Mcf Recovered: 0 Mcf Lost: 148 Mcf
Other Released Details	Not answered.
Additional details for Measured or Estimated Volume(s). Please specify	Flaring was used to return the 30 Inch pipeline to service. Three separate events of flaring were required to return the pipeline to service. Total flaring for the three events was 147.85 MCF.
Is this a gas only submission (i.e. only Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.

Venting or Flaring Resulting from Downstream Activity

Was or is this venting or flaring a result of downstream activity	No
Date notified of downstream activity requiring this venting or flaring	05/20/2021
Time notified of downstream activity requiring this venting or flaring	08:00 AM

Steps and Actions to Prevent Waste	
For this event, the operator could not have reasonably anticipated the current event and it was beyond the operator's control.	False
Please explain reason for why this event was beyond your operator's control	None
Steps taken to limit the duration and magnitude of venting or flaring	None
Corrective actions taken to eliminate the cause and reoccurrence of venting or flaring	None

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CONDITIONS

Action 33367

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Operator: Enterprise Field Services, LLC PO Box 4324 Houston, TX 77210	OGRID: 241602
	Action Number: 33367
	Action Type: [C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
system	If the information provided in this report requires an amendment, submit a [C-129] Request to Amend Venting and/or Flaring Incident, utilizing your incident number from this event.	6/23/2021