



AKM MEASUREMENT SERVICES,LLC. Natural Gas Analysis Report
GPA 2172-09/API 14.5 Report with GPA 2145-16 Physical Properties

	Sample Information
Sample Name	LOST TANK 18 FACILITY PRODUCTION 1 (FMP) V-1010
Technician	ANTHONY DOMINGUEZ
Analyzer Make & Model	INFICON MICRO GC
Last Calibration/Validation Date	04-06-2023
Meter Number	16411P
Air temperature	63
Flow Rate (MCF/Day)	
Heat Tracing	HEATED HOSE & GASIFIER
Sample description/mtr name	LOST TANK 18 FACILITY PRODUCTION 1 (FMP) V-1010
Sampling Method	FILL & EMPTY
Operator	OCCIDENTAL PETROLEUM
State	NEW MEXICO
Region Name	PERMIAN_RESOURCES
Asset	NEW MEXICO
System	EAST
FLOC	OP-DELNE-BT010
Sample Sub Type	CTB
Sample Name Type	METER
Vendor	AKM MEASUREMENT
Cylinder #	4167
Sampled by	JONATHAN ALDRICH
Sample date	4-8-2023
Analyzed date	4-10-2023
Method Name	C9
Injection Date	2023-04-10 09:18:59
Report Date	2023-04-10 09:25:26
EZReporter Configuration File	1-16-2023 OXY GPA C9+ H2S #2.cfgx
Source Data File	a4b4c3ad-880e-4e70-ae7f-6123500a4a18
NGA Phys. Property Data Source	GPA Standard 2145-16 (FPS)
Data Source	INFICON Fusion Connector

Component Results

Component Name	Peak Area	Raw Amount	Response Factor	Norm Mole%	Gross HV (Dry) (BTU / Ideal cu.ft.)	Relative Gas Density (Dry)	GPM (Dry) (Gal. / 1000 cu.ft.)	
Nitrogen	28519.4	1.6111	0.00005649	1.6150	0.0	0.01562	0.178	
Methane	968118.0	70.6847	0.00007301	70.8588	717.3	0.39249	12.064	
CO2	5851.5	0.2751	0.00004701	0.2757	0.0	0.00419	0.047	
Ethane	304222.8	13.8686	0.00004559	13.9027	246.6	0.14434	3.734	
H2S	0.0	0.0000	0.00000000	0.0000	0.0	0.00000	0.000	
Propane	235337.4	7.6632	0.00003256	7.6820	193.7	0.11696	2.125	
iso-butane	91235.3	1.0106	0.00001108	1.0131	33.0	0.02033	0.333	
n-Butane	241056.1	2.6359	0.00001093	2.6424	86.4	0.05303	0.837	
iso-pentane	59104.7	0.5690	0.00000963	0.5704	22.9	0.01421	0.209	
n-Pentane	69774.6	0.6563	0.00000941	0.6579	26.4	0.01639	0.239	
hexanes	49905.0	0.3756	0.00000753	0.3765	17.9	0.01120	0.155	
heptanes	45290.0	0.2787	0.00000615	0.2794	15.4	0.00967	0.129	
octanes	19578.0	0.1086	0.00000555	0.1089	6.8	0.00430	0.056	
nonanes+	2768.0	0.0172	0.00000621	0.0172	1.2	0.00076	0.010	
Total:		99.7546		100.0000	1367.8	0.80347	20.118	

Results Summary

Result	Dry	Sat.
Total Un-Normalized Mole%	99.7546	
Pressure Base (psia)	14.730	
Temperature Base (Deg. F)	60.00	
Flowing Temperature (Deg. F)	93.0	
Flowing Pressure (psia)	99.0	
Gross Heating Value (BTU / Ideal cu.ft.)	1367.8	1344.0
Gross Heating Value (BTU / gal.)	1373.9	1350.6

Result	Dry	Sat.	
Relative Density (G), Real	0.8067	0.8039	

Monitored Parameter Report

Parameter	Value	Lower Limit	Upper Limit	Status	
Total un-normalized amount	99.7546	97.0000	103.0000	Pass	

UPSET FLARING EVENT SPECIFIC JUSTIFICATIONS FORM**Facility:** Lost Tank 18 CPF**Flare Date:** 6/20/2023**Duration of event:** 9 Minutes**MCF Flared:** 456**Start Time:** 11:50 PM**End Time:** 11:59 PM**Cause:** Emergency Flare > Third Party > USA Compression > Lost Tank 13 BOO > Equipment Issues**Method of Flared Gas Measurement:** Gas Flare Meter

1. Reason why this event was beyond Operator's control:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction or complete shut-in of a gas pipeline by a third-party pipeline operator, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to foresee, avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. In this case, Lost Tank Boo 13 compressor station, third party owned and operated by USA Compression, lost two (2) compressor units (#5 on cat engine failure and #7 on high third stage discharge pressure), which then instigated a sudden and unexpected restriction of gas flow which in turn, prompted Oxy's Lost Tank 18 CPF to pressure up automatically and trigger a flaring event to occur. This event could not have been foreseen, avoided or prevented from happening as this event occurred with no advance notice or warning to Oxy and its field personnel from USA Compression personnel. Lost Tank 13 Boo compressor station is the first stopping point, where OXY sends its sales gas from its facility, before it is pushed further down the pipeline for further processing at Mark West, a downstream gathering system facility, which is downstream of Oxy's control.

2. Steps Taken to limit duration and magnitude of venting or flaring:

It is OXY's policy to route its stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, that is beyond Oxy's control to avoid, prevent or foresee, to minimize emissions as much as possible as part of the overall steps taken to limit duration and magnitude of flaring. The flare at this facility has a 98% combustion efficiency to lessen emissions as much as possible. In this case, third party owned and operated compressor station, Lost Tank 13 Boo compressor station, third party owned and operated by USA Compression, lost two (2) compressor units (#5 on cat engine failure and #7 on high third stage discharge pressure), which then instigated a sudden and unexpected restriction of gas flow which in turn, prompted Oxy's Lost Tank 18 CPF to pressure up automatically and trigger a flaring event to occur. As soon as the Oxy production tech, who was on-site, saw flaring occur, he began to make phone calls to USA Compression personnel to see why gas pipeline was experiencing high line pressure. The Oxy production tech then contacted Oxy's personnel to begin making injection rate changes, so that field pressure would stay below the flare trigger setpoints of the CTB to cease flaring. This event is out of OXY's control, yet OXY made every effort to control and minimize emissions as much as possible.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

Oxy cannot take any corrective actions to eliminate the cause and potential reoccurrence of a third-party owned and operated compressor station's sudden and unexpected gas flow intake restriction or shut-in, as this control issue is downstream of Oxy's custody transfer point and out of Oxy's control to foresee, avoid, prevent from happening or reoccur. Third-party downstream compression station owner operators may have equipment issues, which will reoccur from time to time, which in turn, directly impacts Oxy's ability to send its sales gas to them, and potentially triggering a flaring event. OXY makes every effort to control and minimize emissions as much as possible. The only actions that Oxy can take and handle that is within its control, is to continually communicate with USA Compression and Mark West personnel, who operate the Lost Tank 13 Boo Compressor Station and MPLX Gas Plants, when possible, during these types of circumstances.

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District IV
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Phone:(505) 476-3470 Fax:(505) 476-3462

State of New Mexico
Energy, Minerals and Natural Resources
Oil Conservation Division
1220 S. St Francis Dr.
Santa Fe, NM 87505

DEFINITIONS

Action 236251

DEFINITIONS

Operator: OXY USA INC P.O. Box 4294 Houston, TX 772104294	OGRID: 16696
	Action Number: 236251
	Action Type: [C-129] Venting and/or Flaring (C-129)

DEFINITIONS

For the sake of brevity and completeness, please allow for the following in all groups of questions and for the rest of this application: • this application's operator, hereinafter "this operator"; • venting and/or flaring, hereinafter "vent or flare"; • any notification or report(s) of the C-129 form family, hereinafter "any C-129 forms"; • the statements in (and/or attached to) this, hereinafter "the statements in this"; • and the past tense will be used in lieu of mixed past/present tense questions and statements.
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QUESTIONS

Action 236251

QUESTIONS

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	Action Number: 236251
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Prerequisites Any messages presented in this section, will prevent submission of this application. Please resolve these issues before continuing with the rest of the questions.	
Incident Well	Unavailable.
Incident Facility	[fAPP2226965761] Lost Tank 18 CPF

Determination of Reporting Requirements Answer all questions that apply. The Reason(s) statements are calculated based on your answers and may provide additional guidance.	
Was this vent or flare caused by an emergency or malfunction	Yes
Did this vent or flare last eight hours or more cumulatively within any 24-hour period from a single event	No
Is this considered a submission for a vent or flare event	Yes, minor venting and/or flaring of natural gas.
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during venting and/or flaring that is or may be a major or minor release under 19.15.29.7 NMAC.	
Was there at least 50 MCF of natural gas vented and/or flared during this event	Yes
Did this vent or flare result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No
Was the vent or flare within an incorporated municipal boundary or withing 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	No

Equipment Involved	
Primary Equipment Involved	Other (Specify)
Additional details for Equipment Involved. Please specify	Emergency Flare > Third Party > USA Compression > Lost Tank 13 BOO > Equipment Issues

Representative Compositional Analysis of Vented or Flared Natural Gas Please provide the mole percent for the percentage questions in this group.	
Methane (CH4) percentage	71
Nitrogen (N2) percentage, if greater than one percent	2
Hydrogen Sulfide (H2S) PPM, rounded up	0
Carbon Dioxide (C02) percentage, if greater than one percent	0
Oxygen (O2) percentage, if greater than one percent	0
If you are venting and/or flaring because of Pipeline Specification, please provide the required specifications for each gas.	
Methane (CH4) percentage quality requirement	Not answered.
Nitrogen (N2) percentage quality requirement	Not answered.
Hydrogen Sufide (H2S) PPM quality requirement	Not answered.
Carbon Dioxide (C02) percentage quality requirement	Not answered.
Oxygen (O2) percentage quality requirement	Not answered.

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QUESTIONS, Page 2

Action 236251

QUESTIONS (continued)

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	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Date(s) and Time(s)	
Date vent or flare was discovered or commenced	06/20/2023
Time vent or flare was discovered or commenced	11:50 PM
Time vent or flare was terminated	11:59 PM
Cumulative hours during this event	0

Measured or Estimated Volume of Vented or Flared Natural Gas	
Natural Gas Vented (Mcf) Details	Not answered.
Natural Gas Flared (Mcf) Details	Cause: Other Gas Compressor Station Natural Gas Flared Released: 456 Mcf Recovered: 0 Mcf Lost: 456 Mcf.
Other Released Details	Not answered.
Additional details for Measured or Estimated Volume(s). Please specify	Gas Flare Meter
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.

Venting or Flaring Resulting from Downstream Activity	
Was this vent or flare a result of downstream activity	No
Was notification of downstream activity received by this operator	Not answered.
Downstream OGRID that should have notified this operator	Not answered.
Date notified of downstream activity requiring this vent or flare	Not answered.
Time notified of downstream activity requiring this vent or flare	Not answered.

Steps and Actions to Prevent Waste	
For this event, this operator could not have reasonably anticipated the current event and it was beyond this operator's control.	True
Please explain reason for why this event was beyond this operator's control	The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction or complete shut-in of a gas pipeline by a third-party pipeline operator, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to foresee, avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. In this case, Lost Tank Boo 13 compressor station, third party owned and operated by USA Compression, lost two (2) compressor units (#5 on cat engine failure and #7 on high third stage discharge pressure), which then instigated a sudden and unexpected restriction of gas flow which in turn, prompted Oxy's Lost Tank 18 CPF to pressure up automatically and trigger a flaring event to occur. This event could not have been foreseen, avoided or prevented from happening as this event occurred with no advance notice or warning to Oxy and its field personnel from USA Compression personnel. Lost Tank 13 Boo compressor station is the first stopping point, where OXY sends its sales gas from its facility, before it is pushed further down the pipeline for further processing at Mark West, a downstream gathering system facility, which is downstream of Oxy's control.
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Steps taken to limit the duration and magnitude of vent or flare	minimize emissions as much as possible as part of the overall steps taken to limit duration and magnitude of flaring. The flare at this facility has a 98% combustion efficiency to lessen emissions as much as possible. In this case, third party owned and operated compressor station, Lost Tank 13 Boo compressor station, third party owned and operated by USA Compression, lost two (2) compressor units (#5 on cat engine failure and #7 on high third stage discharge pressure), which then instigated a sudden and unexpected restriction of gas flow which in turn, prompted Oxy's Lost Tank 18 CPF to pressure up automatically and trigger a flaring event to occur. As soon as the Oxy production tech, who was on-site, saw flaring occur, he began to make phone calls to USA Compression personnel to see why gas pipeline was experiencing high line pressure. The Oxy production tech then contacted Oxy's personnel to begin making injection rate changes, so that field pressure would stay below the flare trigger setpoints of the CTB to cease flaring. This event is out of OXY's control, yet OXY made every effort to control and minimize emissions as much as possible.
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ACKNOWLEDGMENTS

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[C-129] Venting and/or Flaring (C-129)	

ACKNOWLEDGMENTS

☒	I acknowledge that I am authorized to submit a <i>Venting and/or Flaring</i> (C-129) report on behalf of this operator and understand that this report can be a complete C-129 submission per 19.15.27.8 and 19.15.28.8 NMAC.
☒	I acknowledge that upon submitting this application, I will be creating a new incident file (assigned to this operator) to track any C-129 forms, pursuant to 19.15.27.7 and 19.15.28.8 NMAC and understand that this submission meets the notification requirements of Paragraph (1) of Subsection G and F respectively.
☒	I hereby certify the statements in this report are true and correct to the best of my knowledge and acknowledge that any false statement may be subject to civil and criminal penalties under the Oil and Gas Act.
☒	I acknowledge that the acceptance of any C-129 forms by the OCD does not relieve this operator of liability should their operations have failed to adequately investigate, report, and remediate contamination that poses a threat to groundwater, surface water, human health, or the environment.
☒	I acknowledge that OCD acceptance of any C-129 forms does not relieve this operator of responsibility for compliance with any other applicable federal, state, or local laws and/or regulations.

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CONDITIONS

Action 236251

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CONDITIONS

Created By	Condition	Condition Date
marialuna2	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	7/5/2023