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Analytical Report

12/26/2024

Customer:	Occidental Permian Ltd.	Order:	4690-7807
Location:	South Hobbs RCF	Received:	12/17/2024
Description:	Monthly Collection	Primary Contact:	Richard Sanders

REPORT DISTRIBUTION:

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We appreciate you choosing Pantechs Laboratories. If you have any questions concerning this report, please feel free to contact us at any time.

Sample List							
Fluid	Operator	Location	Site	Sample Point	Date	Time	
CO2	Occidental Permian Ltd.	New Mexico Measurement	SHU7200	SHRCF Plant CO2 Discharge	12/17/2024	11:41 AM	
Gas	Occidental Permian Ltd.	New Mexico Measurement	FE1022	SHU Battery 31C Meter Run	12/17/2024	10:42 AM	
Gas	Occidental Permian Ltd.	New Mexico Measurement	FE7100	North Hobbs to South Hobbs	12/17/2024	11:11 AM	
Gas	Occidental Permian Ltd.	New Mexico Measurement	SHU1013	SHRCF Plant Inlet	12/17/2024	11:35 AM	
Gas	Occidental Permian Ltd.	South Hobbs RCF	DEX PRO	Inlet	12/17/2024	11:22 AM	
Gas	Occidental Permian Ltd.	South Hobbs RCF	DEX PRO	Outlet	12/17/2024	11:23 AM	
Liquid	Occidental Permian Ltd.	South Hobbs RCF	DEX PRO	Gasoline	12/17/2024	11:17 AM	

No Sample List				
Operator	Location	Site	Sample Point	Comment

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	1655 psig	
Location	New Mexico Measurement	Sample Temp	103 F	
Site	SHU7200	Atm Temp	60 F	
Site Type	Meter	Collection Date	12/17/2024	
Sample Point	SHRCF Plant CO2 Discharge	Collection Time	11:41 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID	SHU7200	Pressure Base	15.025 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	CO2	Container(s)	YZ12123	

GPA 2177-20 CO2 Fractional Analysis

COMPOUND	FORMULA	MOL%	VOL%	WT%
NITROGEN	N2	3.781	2.399	2.515
CARBON DIOXIDE	CO2	85.806	84.629	89.654
HYDROGEN SULFIDE	H2S	1.526	1.190	1.235
METHANE	C1	4.713	4.622	1.795
ETHANE	C2	0.872	1.350	0.623
PROPANE	C3	1.670	2.663	1.748
I-BUTANE	iC4	0.401	0.759	0.553
N-BUTANE	nC4	0.830	1.514	1.145
I-PENTANE	iC5	0.196	0.415	0.336
N-PENTANE	nC5	0.122	0.256	0.209
HEXANES PLUS	C6+	0.083	0.203	0.187
TOTALS:		100.000	100.000	100.000

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

Liquid Phase Properties

SCF/Gal (Ideal)	CF/Gal (Ideal) SCF/Gal (Real) Mol Weight		Relative Density (60/60)	Vapor Pressure 100F, psia
56.730	56.402	42.121	0.772	10.0

Vapor Phase Properties

ITEM	BTU/CF	Specific Gr.	Z Factor
DRY	176.70	1.462	0.994
WATER SATURATED	174.62	1.449	0.994

Onsite Testing by Stain Tube

METHOD	ТҮРЕ	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	1.5258	968.87	15,405.0	726.6

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	323 psig	
Location	New Mexico Measurement	Sample Temp	71 F	
Site	FE1022	Atm Temp	60 F	
Site Type	Meter	Collection Date	12/17/2024	
Sample Point	SHU Battery 31C Meter Run	Collection Time	10:42 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID	FE1022	Pressure Base	15.025 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Gas	Container(s)	PL1019	

GPA 2261-20 Gas Fractional Analysis

COMPOUND	FORMULA	MOL%	WT%	GPM
NITROGEN	N2	2.794	1.882	0.314
CARBON DIOXIDE	CO2	84.879	89.821	14.842
HYDROGEN SULFIDE	H2S	0.661	0.542	0.091
METHANE	C1	7.486	2.888	1.302
ETHANE	C2	1.171	0.847	0.321
PROPANE	C3	1.586	1.682	0.448
I-BUTANE	iC4	0.259	0.362	0.087
N-BUTANE	nC4	0.550	0.769	0.178
I-PENTANE	iC5	0.193	0.335	0.072
N-PENTANE	nC5	0.156	0.271	0.058
HEXANES PLUS	C6+	0.265	0.601	0.116
TOTALS:		100.000	100.000	17.829

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

LIQUID YIELD	C2+	C3+	C4+	C5+	26# Liquid	10# Liquid
GAL/MSCF (GPM)	1.280	0.959	0.511	0.246	0.375	0.218

GPA 2172/ASTM D3588 CALCULATED PROPERTIES

WATER CONTENT	BTU/CF, Gross	BTU/CF, Net	Specific Gr.	Z Factor	Mol Weight	Wobbe IDX
DRY	199.95	182.78	1.444	0.994	41.588	166.41
SATURATED	197.49	179.65	1.430	0.994	40.879	

Onsite Testing by Stain Tube

METHOD	TYPE	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	0.6608	419.62	6,672.0	314.7

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	325 psig	
Location	New Mexico Measurement	Sample Temp	65 F	
Site	FE7100	Atm Temp	60 F	
Site Type	Meter	Collection Date	12/17/2024	
Sample Point	North Hobbs to South Hobbs	Collection Time	11:11 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID	FE7100	Pressure Base	15.025 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Gas	Container(s)	PL1601	

GPA 2261-20 Gas Fractional Analysis

COMPOUND	FORMULA	MOL%	WT%	GPM
NITROGEN	N2	2.809	1.893	0.316
CARBON DIOXIDE	CO2	84.823	89.813	14.832
HYDROGEN SULFIDE	H2S	0.669	0.549	0.092
METHANE	C1	7.523	2.904	1.308
ETHANE	C2	1.177	0.852	0.323
PROPANE	C3	1.590	1.687	0.449
I-BUTANE	iC4	0.261	0.365	0.088
N-BUTANE	nC4	0.552	0.772	0.179
I-PENTANE	iC5	0.193	0.335	0.072
N-PENTANE	nC5	0.155	0.269	0.058
HEXANES PLUS	C6+	0.248	0.562	0.108
TOTALS:	100.000	100.000	17.825	

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

LIQUID YIELD	C2+	C3+	C4+	C5+	26# Liquid	10# Liquid
GAL/MSCF (GPM)	1.277	0.954	0.505	0.238	0.361	0.205

GPA 2172/ASTM D3588 CALCULATED PROPERTIES

WATER CONTENT	BTU/CF, Gross	BTU/CF, Net	Specific Gr.	Z Factor	Mol Weight	Wobbe IDX
DRY	199.76	182.58	1.443	0.994	41.564	166.30
SATURATED	197.30	179.45	1.430	0.994	40.856	

Onsite Testing by Stain Tube

METHOD	TYPE	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	0.6691	424.91	6,756.1	318.6

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	293 psig	
Location	New Mexico Measurement	Sample Temp	62 F	
Site	SHU1013	Atm Temp	60 F	
Site Type	Meter	Collection Date	12/17/2024	
Sample Point	SHRCF Plant Inlet	Collection Time	11:35 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID	SHU1013	Pressure Base	15.025 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Gas	Container(s)	PL0965	

GPA 2261-20 Gas Fractional Analysis

COMPOUND	FORMULA	MOL%	WT%	GPM
NITROGEN	N2	2.566	1.690	0.289
CARBON DIOXIDE	CO2	87.007	90.030	15.218
HYDROGEN SULFIDE	H2S	0.563	0.451	0.078
METHANE	C1	4.942	1.864	0.860
ETHANE	C2	0.891	0.630	0.245
PROPANE	C3	1.752	1.816	0.495
I-BUTANE	iC4	0.452	0.618	0.152
N-BUTANE	nC4	1.008	1.377	0.326
I-PENTANE	iC5	0.320	0.543	0.120
N-PENTANE	nC5	0.227	0.385	0.084
HEXANES PLUS	C6+	0.272	0.596	0.119
TOTALS:		100.000	100.000	17.986

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

LIQUID YIELD	C2+	C3+	C4+	C5+	26# Liquid	10# Liquid
GAL/MSCF (GPM)	1.541	1.296	0.801	0.323	0.477	0.234

GPA 2172/ASTM D3588 CALCULATED PROPERTIES

WATER CONTENT	BTU/CF, Gross	BTU/CF, Net	Specific Gr.	Z Factor	Mol Weight	Wobbe IDX
DRY	202.33	185.55	1.477	0.994	42.533	166.49
SATURATED	199.83	182.38	1.463	0.994	41.808	

Onsite Testing by Stain Tube

METHOD	TYPE	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	0.5630	357.48	5,683.9	268.1

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	280 psig	
Location	South Hobbs RCF	Sample Temp	58 F	
Site	DEX PRO	Atm Temp	60 F	
Site Type	Station	Collection Date	12/17/2024	
Sample Point	Inlet	Collection Time	11:22 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID		Pressure Base	14.650 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Gas	Container(s)	PL1807	

GPA 2261-20 Gas Fractional Analysis

COMPOUND	FORMULA	MOL%	WT%	GPM
NITROGEN	N2	2.506	1.651	0.275
CARBON DIOXIDE	CO2	86.946	89.988	14.826
HYDROGEN SULFIDE	H2S	0.662	0.531	0.089
METHANE	C1	4.997	1.885	0.847
ETHANE	C2	0.912	0.645	0.244
PROPANE	C3	1.741	1.805	0.480
I-BUTANE	iC4	0.438	0.599	0.143
N-BUTANE	nC4	0.960	1.312	0.303
I-PENTANE	iC5	0.303	0.514	0.111
N-PENTANE	nC5	0.220	0.373	0.080
HEXANES PLUS	C6+	0.315	0.697	0.134
TOTALS:	100.000	100.000	17.532	

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

LIQUID YIELD	C2+	C3+	C4+	C5+	26# Liquid	10# Liquid
GAL/MSCF (GPM)	1.495	1.251	0.771	0.325	0.487	0.259

GPA 2172/ASTM D3588 CALCULATED PROPERTIES

WATER CONTENT	BTU/CF, Gross	BTU/CF, Net	Specific Gr.	Z Factor	Mol Weight	Wobbe IDX
DRY	197.90	181.54	1.476	0.994	42.523	162.87
SATURATED	195.41	178.37	1.462	0.994	41.780	

Onsite Testing by Stain Tube

METHOD	TYPE	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	0.6615	420.06	6,679.0	315.0

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	270 psig	
Location	South Hobbs RCF	Sample Temp	58 F	
Site	DEX PRO	Atm Temp	60 F	
Site Type	Station	Collection Date	12/17/2024	
Sample Point	Outlet	Collection Time	11:23 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID		Pressure Base	14.650 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Gas	Container(s)	PL2202	

GPA 2261-20 Gas Fractional Analysis

COMPOUND	FORMULA	MOL%	WT%	GPM
NITROGEN	N2	2.019	1.334	0.221
CARBON DIOXIDE	CO2	88.155	91.514	15.030
HYDROGEN SULFIDE	H2S	0.649	0.522	0.087
METHANE	C1	4.995	1.890	0.847
ETHANE	C2	0.911	0.646	0.244
PROPANE	C3	1.676	1.743	0.462
I-BUTANE	iC4	0.409	0.561	0.134
N-BUTANE	nC4	0.796	1.091	0.251
I-PENTANE	iC5	0.190	0.323	0.070
N-PENTANE	nC5	0.122	0.208	0.044
HEXANES PLUS	C6+	0.078	0.168	0.033
TOTALS:	100.000	100.000	17.423	

Value of "0.000" in fractional interpreted as below detectable limit. Onsite H2S value is used in fractional table if performed.

LIQUID YIELD	C2+	C3+	C4+	C5+	26# Liquid	10# Liquid
GAL/MSCF (GPM)	1.238	0.994	0.532	0.147	0.208	0.071

GPA 2172/ASTM D3588 CALCULATED PROPERTIES

WATER CONTENT	BTU/CF, Gross	BTU/CF, Net	Specific Gr.	Z Factor	Mol Weight	Wobbe IDX
DRY	168.98	154.67	1.472	0.994	42.395	139.29
SATURATED	166.98	151.96	1.458	0.994	41.654	

Onsite Testing by Stain Tube

METHOD	TYPE	MOL%	GRAINS/100	PPMV	LB/MMSCF
GPA2377	hydrogen sulfide	0.6494	412.39	6,557.0	309.2

SAMPLE ID		COLLECTION DATA		
Operator	Occidental Permian Ltd.	Pressure	260 psig	
Location	South Hobbs RCF	Sample Temp	N/A	
Site	DEX PRO	Atm Temp	60 F	
Site Type	Station	Collection Date	12/17/2024	
Sample Point	Gasoline	Collection Time	11:17 AM	
Spot/Comp	Spot	Collection By	Cody Carson	
Meter ID		Pressure Base	14.650 psi	
Regulatory ID		Temperature Base	60 F	
Fluid	Liquid	Container(s)	PL2229, PL2213	

GPA 2177-20 Liquid Fractional Analysis

COMPOUND	FORMULA	MOL%	VOL%	WT%
NITROGEN	N2	0.029	0.010	0.013
CARBON DIOXIDE	CO2	24.502	13.780	17.471
HYDROGEN SULFIDE	H2S	0.233	0.104	0.129
METHANE	C1	0.299	0.167	0.078
ETHANE	C2	1.115	0.984	0.543
PROPANE	C3	9.737	8.853	6.957
I-BUTANE	iC4	6.441	6.953	6.065
N-BUTANE	nC4	19.038	19.804	17.928
I-PENTANE	iC5	12.328	14.891	14.411
N-PENTANE	nC5	10.318	12.331	12.061
HEXANES PLUS	C6+	15.960	22.123	24.344
TOTALS:	100.000	100.000	100.000	

Value of "0.000" in fractional interpreted as below detectable limit.

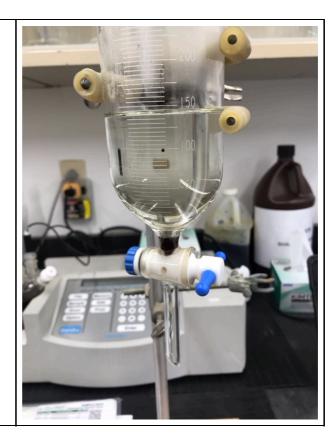
Calculated Properties

SCF/Gal (Ideal)	SCF/Gal (Real)	Mol Weight	Relative Density (60/60)	Vapor Pressure 100F, psia	Reid VP Equivalent, psi
33.179	32.073	61.722	0.641	38.7	36.5

Fluid Determination by Gravity Separation

FLUID	VOLUME	UNITS	PERCENT OF TOTAL
Water	0.50	ml	0.36%
Liquid	139.50	ml	99.64%
TOTAL:	140.00	ml	100.00%





Analysis Methods And Description

ITEM	METHOD	FLUID	DESCRIPTION
COGSEP		Liquid	Fluid Volume Determination in a single sample by Gravity Separation
NGC6+	GPA 2261-20	Gas	Analysis for Natural Gas and Similar Gaseous Mixtures by Gas Chromatography through C6+
NGLC6+	GPA 2177-20	CO2	Analysis of Natural Gas Liquid Mixtures Containing Nitrogen and Carbon Dioxide by Gas Chromatography Through C6+
NGLC6+	GPA 2177-20	Liquid	Analysis of Natural Gas Liquid Mixtures Containing Nitrogen and Carbon Dioxide by Gas Chromatography Through C6+
OSST	GPA 2377	CO2	Test for Hydrogen Sulfide and Carbon Dioxide in Natural Gas Using Length of Stain Tubes
OSST	GPA 2377	Gas	Test for Hydrogen Sulfide and Carbon Dioxide in Natural Gas Using Length of Stain Tubes

Sampling Methods And Description

Fluid	Method	Description
Gas	GPA 2166	Obtaining Natural Gas Samples for Analysis by Gas Chromatography
Liquid	GPA 2174	Obtaining Liquid Hydrocarbons Samples For Analysis by Gas Chromatography

Calculation Methods And Description

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Method	Description	
GPA 2145	Table of Physical Properties for Hydrocarbons and Other Compounds of Interest to the Natural Gas and Natural Gas Liquids Industries	
GPA 2172	Calculation of Gross Heating Value, Relative Density, Compressibility and Theoretical Hydrocarbon Liquid Content for Natural Gas Mixtures for Custody Transfer	
ASTM 3588	Standard Practice for Calculating Heat Value, Compressibility Factor, and Relative Density of Gaseous Fuels	

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UPSET FLARING EVENT SPECIFIC JUSTIFICATIONS FORM

Facility ID: fjXK1530631838 Operator: Occidental Permian LTD.

Facility: South Hobbs RCF Flare Date: 08/17/2025

Duration of Event: 19 Minutes MCF Flared: 486

Start Time: 05:36 PM End Time: 05:55 PM

Cause: Emergency Flare > Compressor Shut Down > Train C > Severe Weather

Method of Flared Gas Measurement: Gas Flare Meter

1. Reason why this event was beyond Operator's control:

This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. Oxy engages in respectable and effective facility operation practices while maintaining a continuous preventative maintenance program for its equipment. In this instance, the south field had a power outage due to severe thunderstorm. This incident was unforeseen, unavoidable, and occurred without prior notice or warning. Oxy's facilities require consistent power to function; intermittent power outages can cause equipment such as pumps, valves, and compressors to cease functioning, potentially leading to overpressure in critical equipment, which poses risks of rupture or explosions. Although flaring is not OXY's preferred method for handling excess gas, it is necessary to ensure the safety of our operations, equipment, and field personnel. OXY made every effort to control and minimize emissions as much as possible during this event and ensured all its operational equipment was slowly brought back to normal operations and running efficiently once power was fully restored to the facility. The occurrence of this event was beyond OXY's control. OXY took all possible measures to manage and reduce emissions to the greatest extent.

2. Steps Taken to limit duration and magnitude of venting or flaring:

It is OXY's policy to route its stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, that is beyond Oxy's control to avoid, prevent or foresee, to minimize emissions as much as possible as part of the overall steps taken to limit duration and magnitude of flaring. The flare at this facility has 98% combustion efficiency to lessen emissions as much as possible. In this instance, the south field had a power outage due to severe thunderstorms which caused the plant to lose all incoming gas, keeping the compressors from operating. Operations flared each time the unit went down until the field team was able to bring back gas into the plant. This incident was unforeseen, unavoidable, and occurred without prior notice or warning. Oxy's facilities require consistent power to function; intermittent power outages can cause equipment such as pumps, valves, and compressors to cease functioning, potentially leading to overpressure in critical equipment, which poses risks of rupture or explosions. Although flaring is not OXY's preferred method for handling excess gas, it is necessary to ensure the safety of our operations, equipment, and field personnel. OXY controlled and minimized emissions during this event, by manually choking back wells and ensuring operational equipment was gradually returned to normal operations and running efficiently once power was restored to the facility. Once power was fully restored and gas was sent back to the plant, operations were able to bring the compression equipment online and running at full capacity. This event occurred beyond OXY's control, and all possible measures were taken to manage and reduce emissions.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. It is OXY's policy to route all stranded sales gas to a flare during an unforeseen and unavoidable emergency or malfunction, in order to minimize emissions as much as possible.

Sante Fe Main Office Phone: (505) 476-3441

General Information Phone: (505) 629-6116

Online Phone Directory https://www.emnrd.nm.gov/ocd/contact-us

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

DEFINITIONS

Action 500707

DEFINITIONS

Operator:	OGRID:
OCCIDENTAL PERMIAN LTD	157984
P.O. Box 4294	Action Number:
Houston, TX 772104294	500707
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

DEFINITIONS

For the sake of brevity and completeness, please allow for the following in all groups of questions and for the rest of this application:

- this application's operator, hereinafter "this operator";
- venting and/or flaring, hereinafter "vent or flare";
- any notification or report(s) of the C-129 form family, hereinafter "any C-129 forms";
- the statements in (and/or attached to) this, hereinafter "the statements in this";
- and the past tense will be used in lieu of mixed past/present tense questions and statements.

Sante Fe Main Office Phone: (505) 476-3441 General Information

Phone: (505) 629-6116
Online Phone Directory
https://www.emnrd.nm.gov/ocd/contact-us

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

QUESTIONS

Action 500707

Q	UESTIONS	
Operator: OCCIDENTAL PERMIAN LTD P.O. Box 4294 Houston, TX 772104294		OGRID: 157984 Action Number: 500707 Action Type: [C-129] Venting and/or Flaring (C-129)
QUESTIONS		[O 120] Volking disdroi Flaming (O 120)
Prerequisites	those issues before continuing wi	the the rest of the supertions
Any messages presented in this section, will prevent submission of this application. Please resolve	these issues before continuing wit	in the rest of the questions.
Incident Well	Unavailable.	
Incident Facility	[fJXK1530631838] SOUTH	HOBBS UNIT RCF
Determination of Reporting Requirements		
Answer all questions that apply. The Reason(s) statements are calculated based on your answers are	nd may provide addional quidance	
Was this vent or flare caused by an emergency or malfunction	Yes	•
Did this vent or flare last eight hours or more cumulatively within any 24-hour period from a single event	No	
Is this considered a submission for a vent or flare event	Yes, minor venting and/or	flaring of natural gas.
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during v	renting and/or flaring that is or may	be a major or minor release under 19.15.29.7 NMAC.
Was there at least 50 MCF of natural gas vented and/or flared during this event	Yes	
Did this vent or flare result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No	
Was the vent or flare within an incorporated municipal boundary or withing 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	No	
Equipment Involved		
Primary Equipment Involved	Other (Specify)	
Additional details for Equipment Involved. Please specify	Emergency Flare > Compre	essor Shut Down > Train C > Severe Weather
Representative Compositional Analysis of Vented or Flared Natural Gas		
Please provide the mole percent for the percentage questions in this group.	•	
Methane (CH4) percentage	5	
Nitrogen (N2) percentage, if greater than one percent	3	
Hydrogen Sulfide (H2S) PPM, rounded up	6,620	
Carbon Dioxide (C02) percentage, if greater than one percent	87	
Oxygen (02) percentage, if greater than one percent	0	
If you are venting and/or flaring because of Pipeline Specification, please provide the required spec	ifications for each gas.	
Methane (CH4) percentage quality requirement	Not answered.	
Nitrogen (N2) percentage quality requirement	Not answered.	
Hydrogen Sufide (H2S) PPM quality requirement	Not answered.	
Carbon Dioxide (C02) percentage quality requirement	Not answered.	

Not answered.

Oxygen (02) percentage quality requirement

Sante Fe Main Office Phone: (505) 476-3441 General Information

Phone: (505) 629-6116

Online Phone Directory
https://www.emnrd.nm.gov/ocd/contact-us

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

QUESTIONS, Page 2

Action 500707

QUESTI	ONS (continued)
Operator: OCCIDENTAL PERMIAN LTD	OGRID: 157984
P.O. Box 4294	Action Number:
Houston, TX 772104294	500707 Action Type:
	[C-129] Venting and/or Flaring (C-129)
QUESTIONS	
Date(s) and Time(s)	
Date vent or flare was discovered or commenced	08/17/2025
Time vent or flare was discovered or commenced	05:36 PM
Time vent or flare was terminated	05:55 PM
Cumulative hours during this event	0
Measured or Estimated Volume of Vented or Flared Natural Gas	
Natural Gas Vented (Mcf) Details	Not answered.
Natural Gas Flared (Mcf) Details	Cause: Other Other (Specify) Natural Gas Flared Released: 63 Mcf Recovered: 0 Mcf Lost: 63 Mcf.
Other Released Details	Cause: Other Other (Specify) Carbon Dioxide Released: 423 Mcf Recovered: 0 Mcf Lost: 423 Mcf.
Additional details for Measured or Estimated Volume(s). Please specify	Not answered.
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.
Venting or Flaring Resulting from Downstream Activity	
Was this vent or flare a result of downstream activity	No
Was notification of downstream activity received by this operator	Not answered.
Downstream OGRID that should have notified this operator	Not answered.
Date notified of downstream activity requiring this vent or flare	Not answered.
Time notified of downstream activity requiring this vent or flare	Not answered.
Steps and Actions to Prevent Waste	
For this event, this operator could not have reasonably anticipated the current event and it was beyond this operator's control.	True
	This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. Oxy engages in

respectable and effective facility operation practices while maintaining a continuous preventative maintenance program for its equipment. In this instance, the south field had a power outage due to severe thunderstorm. This incident was unforeseen, unavoidable, and occurred without prior notice or warning. Oxy's facilities require consistent power to function;

manage and reduce emissions to the greatest extent.

intermittent power outages can cause equipment such as pumps, valves, and compressors to cease functioning, potentially leading to overpressure in critical equipment, which poses risks of rupture or explosions. Although flaring is not OXY's preferred method for handling excess gas, it is necessary to ensure the safety of our operations, equipment, and field personnel. OXY made every effort to control and minimize emissions as much as possible during this event and ensured all its operational equipment was slowly brought back to normal operations and running efficiently once power was fully restored to the facility. The occurrence of this event was beyond OXY's control. OXY took all possible measures to

It is OXY's policy to route its stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, that is beyond Oxy's control to avoid, prevent or foresee, to minimize emissions as much as possible as part of the overall steps taken to limit duration

Please explain reason for why this event was beyond this operator's control

Steps taken to limit the duration and magnitude of vent or flare	and magnitude of flaring. The flare at this facility has 98% combustion efficiency to lessen emissions as much as possible. In this instance, the south field had a power outage due to severe thunderstorms which caused the plant to lose all incoming gas, keeping the compressors from operating. Operations flared each time the unit went down until the field team was able to bring back gas into the plant. This incident was unforeseen, unavoidable, and occurred without prior notice or warning. Oxy's facilities require consistent power to function; intermittent power outages can cause equipment such as pumps, valves, and compressors to cease functioning, potentially leading to overpressure in critical equipment, which poses risks of rupture or explosions. Although flaring is not OXY's preferred method for handling excess gas, it is necessary to ensure the safety of our operations, equipment, and field personnel. OXY controlled and minimized emissions during this event, by manually choking back wells and ensuring operational equipment was gradually returned to normal operations and running efficiently once power was restored to the facility. Once power was fully restored and gas was sent back to the plant, operations were able to bring the compression equipment online and running at full capacity. This event occurred beyond OXY's control, and all possible measures were taken to manage and reduce emissions.
Corrective actions taken to eliminate the cause and reoccurrence of vent or flare	The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. It is OXY's policy to route all stranded sales gas to a flare during an unforeseen and unavoidable emergency or malfunction, in order to minimize emissions as much as possible

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ACKNOWLEDGMENTS

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ACKNOWLEDGMENTS

V	I acknowledge that I am authorized to submit a <i>Venting and/or Flaring</i> (C-129) report on behalf of this operator and understand that this report can be a complete C-129 submission per 19.15.27.8 and 19.15.28.8 NMAC.
V	I acknowledge that upon submitting this application, I will be creating a new incident file (assigned to this operator) to track any C-129 forms, pursuant to 19.15.27.7 and 19.15.28.8 NMAC and understand that this submission meets the notification requirements of Paragraph (1) of Subsection G and F respectively.
V	I hereby certify the statements in this report are true and correct to the best of my knowledge and acknowledge that any false statement may be subject to civil and criminal penalties under the Oil and Gas Act.
V	I acknowledge that the acceptance of any C-129 forms by the OCD does not relieve this operator of liability should their operations have failed to adequately investigate, report, and remediate contamination that poses a threat to groundwater, surface water, human health, or the environment.
V	I acknowledge that OCD acceptance of any C-129 forms does not relieve this operator of responsibility for compliance with any other applicable federal, state, or local laws and/or regulations.

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CONDITIONS

Action 500707

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Houston, TX 772104294	500707
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	[C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
srojas	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	8/29/2025