# 1R-463

### REPORTS

## DATE: 6 - 19 - 13



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### MOBILE DUAL PHASE EXTRACTION REPORT OCD D.S. HUGH GATHERING 4 INCH PIPELINE RELEASE LEA COUNTY, NEW MEXICO SRS # 2000-10807 NMOCD# 1R-0463

**PREPARED FOR:** 

PLAINS MARKETING, L.P. 333 CLAY STREET SUITE 1600 HOUSTON, TEXAS 77002

### **PREPARED BY:**

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STATE OF TEXTO STATE OF TEXTO SHANE B. CURBLE GEOLOGY 1801 CENSED SCOME A JUSTICE

JUNE 19, 2013

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### I. MDPE SUMMARY REPORT AND WASTE DISPOSITION

### A. MDPE Results

The following report summarizes data collected during the 12-hour High Vacuum Multi-Phase Extraction (MDPE) event conducted on March 12 -13, 2013 at the D.S. Hugh Gathering 4 Inch Pipeline release site, located in Lea County, New Mexico. The objective of the MDPE treatment was to remove both vapor and liquid phase separated hydrocarbons (PSH) from onsite groundwater wells. Talon/LPE utilized an MDPE unit which consisted of an SVE extraction pump capable of generating vacuum up to 25" hg. Off gas vapors extracted from the extraction wells were destroyed using a propane-fired 1000-SCFM thermal oxidizer capable of processing 172.96 lbs/hr of gasoline.

A total of 12 hours (0.5 days) of PSH recovery was performed on MW-1 for 12 hours.

Prior to and immediately following the event, the groundwater wells were gauged for groundwater elevation and PSH. Depth to groundwater ranges were measured in feet below the top of casing. Refer to Attachment 1 for a summary of data collected during the MDPE event.

The volume of PSH removed during the MDPE event is shown to reflect the portions of PSH in the liquid phase and as off-gas vapor. Air removal rates were calculated from velocity measurements recorded at the influent manifold prior to entry into the MDPE unit. PSH recovery and air flow data has been detailed and is contained in Table 1. Two influent air samples were collected over the course of the event. These samples were submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. Both influent samples were tested for Total-Gas Analysis (Hydrocarbon Composition) by GPA 2261-C6+. Laboratory analytical results can be found in Attachment 2.

Based on a combination of field vapor screening and collected laboratory samples, a combined estimated total of **19.94 equivalent gallons of PSH (Total)** were removed during the event. The combined volume of PSH was comprised of approximately **3 gallons of PSH (liquid phase)** and approximately **16.94 gallons as off-gas vapor**.

The cumulative air flow measurements for the MDPE event were calculated using a combination of field data measurements and Preso® B+ manufacturer provided formulas. Air flow rates extracted from the recovery well averaged 29.97 SCFM during the event.

A portion of the extracted air flow rates measured is attributable to compressed air, which was "injected" into the extraction wells. This "injected" air is introduced into the extraction wells for the purpose of enhancing liquid recovery rates.

### B. Air Quality

Two influent air samples were collected during the event. These samples were submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The maximum concentration in air influent was recorded as 90,950 ppmv for Hydrocarbon Composition. Laboratory analytical results can be found in Attachment 2.

### C. Waste Management and Disposition

A cumulative total of 1,321 gallons of fluid were generated during this event. The fluids were temporarily transferred to an on-site storage tank prior to being transferred to an authorized disposal facility. A copy of the waste ticket can be found in Attachment 4.

### **II. SYSTEM OPERATION DATA AND MASS RECOVERY CALCULATIONS**

### Formulae:

Concentration (C_mg/l) =	C_ppmv x Mol. wt. in mg(estimated) x 1000 x 0.000001
	0.0821 x Temp (K)
Recovery Rate (lbs/hr) =	<u>(C_mg/l) x 2.2 x (Flowrate) x 60 x 28.32</u> 1,000,000

Recovery (lbs) = (lbs/hr) x (hrs)

Correction Factor (CF) =	FID Reading(ppmv)
	FID Reading at Time of Laboratory Analysis

<u>8.34 lbs</u>	x 0.66 average specific gravity of light crude =	5.5 lbs light crude
gallon water	(estimated)	gallon

Table 1 System Operation Data and Mass Recovery Calculations

Time	Period (hours)	Influent Temp. (°ກ	Vacuum (in, hg)	Vacuum (in. h20)	Differential pressur <del>e</del> (In. h20)	Flow (SCFM)	FID Readings (ppmv)	Lab Result (ppmv)	Assigned Lab Result (ppmv)	Correction Factor (CF)	Adjusted Lab Result (ppmv)	Adjusted Lab Result (mg/L)	Recovery (Ibs/hr)	Recovery in Period (lb <del>s</del> )	Total Recovery (lbs)
17:00	0.5	70	21	285.79	1.3	21.79	387.3	-	90950.00	0.68	62070	79.04	6.44	3.22	3.22
17:30	0.5	68	19	258,57	1.6	26.79	567.5	90950.00	90950.00	1.00	90950	116.25	11.64	5,82	9.04
18:30	1	67	19	258.57	1.7	27.64	487.6	-	90950.00	0.86	78145	100.08	10.34	10.34	19.38
19:30	1	65	19	258.57	1.2	23.27	2617		90950.00	4.61	419412	539.17	46.90	46.90	66.28
20:30	1	58	18.5	251.77	1.4	25.87	775.1	-	90950.00	1.37	124221	161.85	15.65	15.85	81.94
21:30	1	54	18	244.96	1.5	27.47	347.1	-	90950.00	0.61	55628	73.04	7.50	7.50	89.44
22:30	1	52	19	258.57	1.9	29.65	1059	-	90950.00	1.87	169720	223.73	24.80	24.80	114.23
23:30	1	50	19.5	285.38	2.8	35.23	338.2	-	1400.00	0.31	433	0.53	0.07	0.07	114.30
0:30	1	48	19	258.57	2.5	34.14	1531	-	1400.00	1.40	1961	2.39	0.30	0.30	114.61
1:30	1	48	18.5	251.77	2.2	32.75	2772	•	1400.00	2.54	3551	4.32	0.53	0.53	115.13
2:30	1	48	18	244.96	2.4	35.01	1612	-	1400.00	1.47	2065	2,52	0.33	0.33	115.47
3:30	1	48	18	244.96	2.5	35.74	1093	1400.00	1400.00	1.00	1400	1.71	0.23	0.23	115.69
4:30	1	46	18	244.96	2.3	34.28	975.2	-	1400.00	0.89	1249	1.53	0.20	0.20	115.89
Averages:		55.23	18.81	255.95	1.95	29.97	1120.15						Total	115.89	
										PSH Mass Re	covered in Va	or Phase =		16.94	gallons

### FID maximum Concentration = 50,000 PPM Ex: Conversion from ppmv to mg/L (influent 1)

LA. CONVEIS	ou nom hbu	a to mg/r (mu	uentij			
Measured Conc.	Molecular Wt.	Pressure	Gas Constant	Temp.	Temp.	Conc.
(C_ppmv)	(Grams)	(atm)	(atm.liter/K.m ole)	(F)	(К)	( C_mg/l)
62070	30.7481	1	0.0821	70	294.1111111	79.04014266

inputs are the green values.

Calculated values are yellow

Constants are purple salling.

Outpus are the blue values.

### Liquid-phase Hydrocarbon Recovery

(assumes gasoline product)

 $\prod * r^2 * h = volume$ 

### Gallons removed determined at time of pick up

PSH Volume in Gallons= PSH Mass in Pounds=

3 20.52

115.89 PSH Mass Recovered in Vapor Phase = lbs 18.94 aalle PSH Mass Recovered in Liquid Phase = 20.52 3.00 TOTAL = 136.41 Ibs 19.94 gailons

**Total Hydrocarbon Recovery** 

SG = 0.82

% Vol	(Wt. %) Hydrocarbon	to pomy - In	fluent 1		Molecula	r Weight Calculations			
	(W. %) Hydrocarboli	to ppint - in			component	Molecular Weight (g/mol)	mol%		
Compound	Molecular Weight (g/mol)	Wt. %	=	ppmv	Nitrogen (N2)	28.016	58.9080		
Methane (CH4)	16.04	7.371		73710.00	Methane (CH4)	18.0425	14.1230		
Ethane (C2H6)	30.07	0.379		3790.00	Carbon Dioxide (CO2)	44.011	25.9940		
Propane (C3H8)	44.10	0.208		2080.00	Ethane (C2H6)	30.069	0.3870		
iso-Butane (C4H10)	58.12	0.11		1100.00	Propane (C3H8)	44.0956	0.1450		
N-Butane (C4H10)	58.12	0.151		1510.00	Iso-Butane (C4H10)	58.1222	0.0580		
Iso-Pentane (C4H12)	72.15	0.099		990,00	N-Butane (C4H10)	58.1222	0.0800		
N-Pentane (C5H12)	72.15	0.092		920.00	Iso-Pentane (C4H12)	72.1488	0.0420		
Hexane+ (C6H14)	97.40	0.685		6850.00	N-Pentane (C5H12)	72.1488	0.0390		
			Total	90950.00	Hexane+	97.3966	0.2260		
	as 60% hexanes, 30 % hept	anes and 10 9	6 octanes, as	such its	1	Total	100		
"Hexane+ is treated			(0.6*93.1887)+(0.3*100.2019)+(0.1*114.2285) = 97.3966						
						Calculated MW	30.7481		
						Calculated MW	30.7481		
(0.6*9	3.1887)+(0.3*100.2019)+(0.1	*114.2285) = 8	97.3966		Molecula	Calculated MW	30.7481		
(0.6*9		*114.2285) = 8	97.3966		Molecula		30.7481 mol%		
(0.6*9 % Vol. Compound	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon 1 Molecular Weight (g/mol)	*114.2285) = 8	97.3966	ppmv		r Weight Calculations			
(0.6*9 % Vol. Compound Methane (CH4)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon t Molecular Weight (g/mol) 16.04	•114.2285) = 8 to ppmv - In	97.3966 Influent 2		component	r Weight Calculations Molecular Weight (g/mol)	moi%		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (C2H6)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon f Molecular Weight (g/mol) 16.04 30.07	*114.2285) = 8 to ppmv - In Wt. %	97.3966 Influent 2	ppmv	component Nitrogen (N2)	r Weight Calculations Molecular Weight (g/mol) 28.016	mo!% 99.1380		
(0.6*9 % Vol. Compound Methane (CH4)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon t Molecular Weight (g/mol) 16.04	*114.2285) = 8 to ppmv - In Wt. %	97.3966 Influent 2	ppmv0.00	component Nitrogen (N2) Methane (CH4)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425	mol% 99.1380 0.0000		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (C2H6)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon f Molecular Weight (g/mol) 16.04 30.07	*114.2285) = 8 to ppmv - In Wt. % 0 0.007	97.3966 Influent 2	0.00 70.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011	mol% 99.1380 0.0000 0.8120		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (C2H6) Propane (C3H8)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon 1 Molecular Weight (g/mol) 16.04 30.07 44.10	*114.2285) = { to ppmv - In Wt. % 0 0.007 0.003	97.3966 Influent 2	0.00 70.00 30.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H8)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011 30.069	mol% 99.1380 0.0000 0.8120 0.0070		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon 1 Molecular Weight (g/mol) 16.04 30.07 44.10 58.12 58.12 58.12 72.15	*114.2285) = \$ to ppmv - In Wt. % 0.007 0.003 0.004	97.3966 Influent 2	<u>ppmv</u> 0.00 70.00 30.00 40.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H8) Propane (C3H8)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011 30.069 44.0356	mol% 99.1380 0.0000 0.8120 0.0070 0.0020		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon f Molecular Weight (g/mol) 16.04 30.07 44.10 58.12 58.12 58.12 72.15 72.15	*114.2285) = 5 to ppmv - In Wt. % 0 0.007 0.003 0.004 0.004	97.3966 Influent 2	ppmv 0.00 70.00 30.00 40.00 40.00	Component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H8) Propane (C3H8) Iso-Butane (C4H10)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011 30.069 44.0956 56.1222	mol% 99.1380 0.0000 0.8120 0.0070 0.0020 0.0020		
(0.6*9 % Vol. Compound Methane (CH4) Ethane (CH4) Propane (C3H8) Iso-Butane (C4H10) Iso-Butane (C4H10) Iso-Pattane (C4H10)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon 1 Molecular Weight (g/mol) 16.04 30.07 44.10 58.12 58.12 58.12 72.15	*114.2285) = \$ to ppmv - In Wt. % 0 0.007 0.003 0.004 0.004 0	97.3966 Influent 2	0.00 70.00 30.00 40.00 40.00 0.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H8) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10)	r Weight Calculations Molecular Weight (g/mol) 28.016 18.0425 44.011 30.069 44.0956 56.1222 56.1222	mol% 99.1380 0.0000 0.8120 0.0070 0.0020 0.0020 0.0020		
(0.6*9 % Vol. Compound Meihane (CH4) Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12) Hexane+ (C6H14)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon f Molecular Weight (g/mol) 16.04 30.07 44.10 58.12 58.12 72.15 72.15 97.40	*114.2285) = 6 <b>ppmv</b> - Im <b>Wt.</b> % 0 0.007 0.003 0.004 0 0 0 0.122	97.3966 ifluent 2 = Total	0.00 70.00 30.00 40.00 0.00 0.00 1220.00 1400.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H8) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011 30.069 44.0556 56.1222 56.1222 72.1488	mol% 99.1380 0.0000 0.8120 0.0070 0.0020 0.0020 0.0020 0.0020		
(0.6*9 % Vol. Compound Meihane (CH4) Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12) Hexane+ (C6H14)	3.1887)+(0.3*100.2019)+(0.1 (Wt. %) Hydrocarbon f Molecular Weight (g/mol) 16.04 30.07 44.10 58.12 58.12 58.12 72.15 72.15	*114.2285) = 6 <b>ppmv</b> - Im <b>Wt.</b> % 0 0.007 0.003 0.004 0 0 0 0.122	97.3966 ifluent 2 = Total	0.00 70.00 30.00 40.00 0.00 0.00 1220.00 1400.00	component Nitrogen (N2) Methane (CH4) Carbon Dioxide (CO2) Ethane (C2H6) Propane (C3H6) Iso-Butane (C4H10) Iso-Pentane (C4H12) N-Pentane (C5H12)	r Weight Calculations Molecular Weight (g/mol) 28.016 16.0425 44.011 30.069 44.0956 56.1222 56.1222 56.1222 72.1488 72.1488	mol% 99.1380 0.0000 0.8120 0.0070 0.0020 0.0020 0.0020 0.0020 0.0000		

### sum (individual component MW x their reported mol%) 100 Calculated MW=

ppmv=

% Vol x 10,000

D.S. Hugh Gathering 4 Inch Line - 700376.129.02 - SRS# 2000-10807 - Event 2 - 12 Hour

ATTACHMENT 1 MDPE Field Logs

					MDPE FIE	LD NOTES	3		
Site Name	e:	D.S. Hugh	Gathering	4 Inch Line	)			Event #:	2
Location:		Lea Count						Arrive at site:	3/12/2013 15:45
Date:		3/12-13/20	013						
Job#:		700376.12	9.02		SRS#:	2000-108	07	Start Vac:	3/12/2013 16:30
Phase:		MDPE2			Unit:	1107		Stop Vac:	3/13/2013 6:30
Onsite Pe	rsonnel:	L. Bridges	& B. Huntir	ngton				Leave Site:	3/13/2013 9:30
					GAUGIN	IG DATA			
WELL#		BEFORE			AFTER			COMMEN	ITS
	PSH_	GW	PSH-T	PSH	GW	PSH-T			
MW-1	47.25	48.52	1.27	-	48.85	-	Stinger @ 48.6	5'	
MW-2	-	47.13	-		Not Gauge	d			
MW-3	-	47.46	-		Not Gauge	d			
MW-4	-	48.26	-		Not Gauge	d			
MW-5	-	48.65	-		Not Gauge	d			
MW-6	-	49.39	-		Not Gauge	d			
MW-7	-	48.88	-		Not Gauge	<u>d</u>			
WASTE:	H2O:	1318		PSH:	3		TOTAL (GAL):	1321	

Sample Name	Analysis	Date:	Time:	Comments:
INFLUENT	ASTM D 1945	3/12/2013	17:30	FID = 367.5
INFLUENT	ASTM D 1945	3/13/2013	3:30	FID = 1093
INFLUENT	-	-	-	-
EFFLUENT	-	-	-	-

Notes:

Tank #1 51.5" total PSH @51 3/8" 1321 gallons total with 1318 gallons water and 3 gallons PSH

Start Date:	3/12/2013						MDP	E FIELD DATA				
			Well Flow			Well Data						
TIME	SAMPLE	Inflent temp.	Diff.	Vac	Composite	Propane	EXHAUST			COMMENTS:		
	TAKEN	(°f)	Pressure	(In. hg)	FID	Tank	TEMP F	MW-1	$\searrow$	$\geq$	$\geq$	$\geq$
			(INH20)		(ppm)	(%-size)		VAC (INH2O)	VAC (INH2O)	VAC (INH2O)	VAC (INH2O)	VAC (INH2O)
	*		2" Preso			90%		() (O () () () () () () () () () () () () ()		,, io (iii i20)		() (0 () () () ()
17:00		70	1.3	21	387,5	89	1411	2	$\geq$	$\geq$	$\searrow$	$\geq$
17:30	*	68	1.6	19	567.5	88	1412	2.5	$\geq$	$\geq$	$>\!$	$>\!$
18:30		67	1.7	19	487.6	87	1406	2.7	$\geq$	$\sim$	$\geq$	$\geq$
19:30		65	1.2	19	2617	86	1414	3.1	$\searrow$	$\geq$	$\geq$	$\geq$
20:30		58	1.4	18.5	775.1	85	1406	2.9	$\searrow$	$\searrow$	$\searrow$	$\geq$
21:30		54	1.5	18	347.1	82	1405	3.9	$\searrow$	$\searrow$	$\searrow$	$\searrow$
22:30		52	1.9	19	1059	80	1406	4	$\searrow$	$\setminus$	$\searrow$	$\mathbb{X}$
23:30		50	2.8	19.5	338.2	77	1408	5	$\land$	$\wedge$	$\searrow$	$\geq$
0:30		48	2.5	19	1531	74	1410	4.6	$\searrow$	$\wedge$	$\geq$	$\geq$
1:30		48	2.2	18.5	2772	71	1409	3.8	$\searrow$	$>\!$	$\geq$	$\geq$
2:30		46	2.4	18	1612	68	1409	3.9	$\searrow$	$\geq$	$\searrow$	$\geq$
3:30	**	46	2.5	18	1093	65	1407	4	$\geq$	$\geq$	$\geq$	$\geq$
4:30		46	2.3	18	975.2	62	1406	3.8	$\searrow$	$\geq$	$\searrow$	$\searrow$

D.S. Hugh Gathering 4 Inch Line - 700376.129.02 - SRS# 2000-10807 - Event 2 - 12 Hour

### ATTACHMENT 2 Laboratory Analytical Results



### **Certificate of Analysis**

HOUSTON LABORATORIES 3820 INTERCHANGE DRIVE HOUSTON, TEXAS 77054 PHONE (713) 660-0901

Number: 1030-2013030374-001A

Simon I. Walshe, CAPM Talon/LPE 921 N. Bivins St. Amarillo Texas 79107

Sample ID: Station Name : Influent #1 Station Number : Station Location : Armarillo, TX Sample Point: Sampled By:LBSample Of:GasSpotSample Date:03/12/2013 17:30Sample Conditions:N.G. Pres. , N.G. Temp.PO / Ref. No:N.G. Pres. , N.G. Temp.

March 15, 2013

### ANALYTICAL DATA

Components	Mol %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	DK	3/15/2013 3:27:01 AM
Nitrogen	58.906	53.686				
Carbon Dioxide	25.994	37.219				
Methane	14.123	7.371				
Ethane	0.387	0.379	0.103			
Propane	0.145	0.208	0.040			
Iso Butane	0.058	0.110	0.019			
n-Butane	0.080	0.151	0.025			
lso Pentane	0.042	0.099	0.015			
n-Pentane	0.039	0.092	0.014			
Hexanes Plus	0.226	0.685	0.098			
	100.000	100.000	0.314			
	C2 +	C3 +	iC5 +			
GPM TOTAL :	0.314	0.211	0.127			
Relative Density	Real Gas			1.0622		
Calculated Molecular	Weight			30.74		
Compressibility Factor	r -			0.9986		
GPA 2172-09 Calculati	on :					
<b>Calculated Gross BT</b>	U per ft <sup>3</sup> @14.650	psia & 60°F				
Real Gas: Dry BT		•	172			
-	Sat. Gas_Base BTL	J:	169			
	Mol% - 1.75 Wt%					

as Staly

Hydrocarbon Laboratory Manager

Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated



### **Certificate of Analysis**

HOUSTON LABORATORIES \$920 INTERCHANGE DRIVE HOUSTON, TEXAS 77054 PHONE (713) 660-0901

Number: 1030-2013030374-002A

Simon I. Walshe, CAPM Talon/LPE 921 N. Bivins St. Amarillo Texas 79107

Sample ID: Station Name : Influent #2 Station Number : Station Location : Armarillo, TX Sample Point: Sampled By:LBSample Of:GasSpotSample Date:03/13/2013 03:30Sample Conditions:N.G. Pres. , N.G. Temp.PO / Ref. No:N.G. Pres. , N.G. Temp.

March 15, 2013

### ANALYTICAL DATA

Components	Mol %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	DK	3/15/2013 3:44:01 AM
Nitrogen	99.138	98.591				
Carbon Dioxide	0.812	1.269				
Ethane	0.007	0.007	0.002			
Propane	0.002	0.003	0.001			
Iso Butane	0.002	0.004	0.001			
n-Butane	0.002	0.004	0.001			
Hexanes Plus	0.037	0.122	0.016		,	
	100.000	100.000	0.021			
	C2 +	C3 +	iC5 +			
GPM TOTAL :	0.021	0.019	0.016			
Relative Density	Real Gas			0.9725		
Calculated Molecular	Weight			28.17		
<b>Compressibility Facto</b>	r			0.9997		
GPA 2172-09 Calculat	lon :					
Calculated Gross B	TU per ft <sup>3</sup> @14.650	psia & 60°F				
Real Gas: Dry BT	ານ:		2			
Water	Sat. Gas_Base BTl	J:	2			
Comments : H2C	) Mol% - 1.75_Wt%	- 1.126				

CR: Staling Hydrocarbon Laboratory Manager

**Quality Assurance:** 

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated

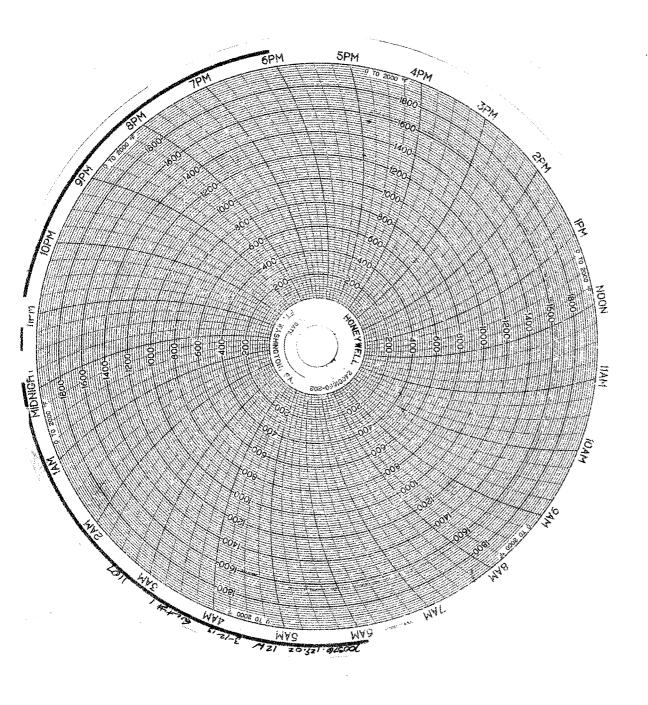
SPL, Inc. Analysis Request Chain of Custody Record

1 BIS			SPL Work Order No.:					Acct. Mate Code.							Dept. Code			SPL						
A A A								1	NEEDS CLIENT CO					DE					1					
Report To: (Company Name):	Name):															tation Location:					Requ	ested TAT		
Address: 921 N. Bivins St.				Influent Seil Veper XDE				376	5.129,02 E				Eunice NE:											
				Inducat Soil Vepor 20376, Special Instructions: DS High Cott					~~~~															
City/State/Zip: Amarillo TX 79107				-	1										10 bus	iness da	vs							
Contact:	ntact: Simon I, Walshe, CAPM swalshe@talonipe.com					Indicate Billing Type (Place "X", where Net 30 d				cct.	Check #												, -	
Phone:	806-350-8872 Fax: 806-467-0622								lit Card <			<					aymer	nt arra	ngeme	ents.				
Invoice To:	e To: Talon/I PE 1 td						1				Requ	uestec	Anal	nalysis						rges May App ote for details				
(Company Name):					┨───────────────────────					(PI	ace an	"X"	next t	<u>o'Sam</u>	nple ID below)							, 		
Address: 921 N. Bivins St.					<sup>T</sup> Terms: Cylinders will be rented for \$10/cyl. All cylinders checked out are to be returned within 21 days,																			
City/State/Zip:				TX		107		y contain san																
Contact:	Talon - Acco	unts Payable	a second s				Cylinders not returned after 30 days will be considered lost and will be									ĺ								
Phone: Client PO# or Ref. No.:	806-467-060	)7	Fax: N/A	1806-	372-66	03		urrent replacement cost.		6-0									Ì					
Contract/Proposal #:							1			-22	-73													
(i.e. SPLQ####	)	551								GPA-2261-C6+														
	Comple	Canala	Sample	ate	site		Cylinder Trac		Info	Ĭ													·	
Sample ID (used to log/track sample)	Sample Date	Sample Time	Type (Gas/Liq. /Solid)	Duplicate	Composite	Spot	Cylinder #	Date Out	Date In													C	omments	
Intlust#1	2-12-13	1730	GAS		1	1				X									1					
Influe, 7#2	3-13-13	0330	li							X														
				Τ															Γ	1	T	1		
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Sampled By-Print Name:						Received By-Company:																		
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Centred by Frink Hame.					1	ime: Received By-Print Name: Signature:														3-14-13	>			
Signature: 5/3/12 Relinquished By-Print Name: Date:					Time:								······ `	Date:	Time:									
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Relinquished By-Print Name: Date:				Time:								Date:	Time:											
Signature:					Signature:									*****	-									
Coldination .					-																			
Choose SPL Facility>>> Corporate HQ - Houston, TX					Shi	to Ad	idress:	ress: 8820 Interchange Dr.,					Houston,TX 77054									713.660.0901		

With Wate wAs account in the our clients, this form is available in 23 / Entropy format Disca contact one of our offices above for the term to be estimated to your

D.S. Hugh Gathering 4 Inch Line – 700376.129.02 - SRS# 2000-10807 – Event 2 – 12 Hour

ATTACHMENT 3 Oxidizer Charts



D.S. Hugh Gathering 4 Inch Line - 700376.129.02 - SRS# 2000-10807 - Event 2 - 12 Hour

ATTACHMENT 4 Waste Ticket

