

NEW MEXICO OIL CONSERVATION COMMISSION  
 MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122  
 Revised 9-1-65

Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special		Test Date 9-16-77									
Company Harvey E. Yates Co., Inc.		Connection									
Pool Reeves Queen		Unit									
Completion Date 9-16-77	Total Depth 4699	Plug Back TD 4657	Elevation 3916 KB								
Farm or Lease Name Hanlad State			Well No. 1								
Csg. Size 4 1/2	Wt. 9.5	d 4.090	Set At 4699								
Perforations: From 4212 To 4220		Well No.									
Tbg. Size 2 3/8	Wt. 4.7	d 1.995	Set At 4162								
Perforations: From To		Unit	Sec.    Twp.    Rge.								
2    185    35E											
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single		Packer Set At 4162	County Lea								
Producing Thru Tubing	Reservoir Temp. *F 103@ 4116	Mean Annual Temp. *F	Baro. Press. - P <sub>a</sub>								
State New Mexico											
L 4216	H 4216	Gg .652	% CO <sub>2</sub> % N <sub>2</sub> % H <sub>2</sub> S								
Prover Pos. Ck.		Meter Run	Taps								
FLOW DATA											
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h <sub>w</sub>	Temp. *F	TUBING DATA		CASING DATA		Duration of Flow
SI				1303			Press. p.s.i.g.	Temp. *F	Press. p.s.i.g.	Temp. *F	
1.	2 X 6/64"			1285		76	1285	76	pkr		1 hr.
2.	2 X 7/64"			1273		78	1273	78	"		1 hr.
3.	2 X 9/64"			1245		77	1245	77	"		1 hr.
4.	2 X 11/64"			1209		77	1209	77	"		1 hr.
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P <sub>m</sub>	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, F <sub>pv</sub>	Rate of Flow Q, Mcfd				
1.	0.1880		1298.2	0.9850	1.238	1.124	334.52				
2.	0.2610		1286.2	0.9831	1.238	1.124	459.23				
3.	0.3346		1258.2	0.9840	1.238	1.122	575.42				
4.	0.5090		1222.2	0.9840	1.238	1.117	846.50				
5.											
NO.	P <sub>f</sub>	Temp. *R	T <sub>f</sub>	Z	Gas Liquid Hydrocarbon Ratio _____ Dry Gas _____ Mcf/lbl.						
1.	1.94	536	1.43	.791	A.P.I. Gravity of Liquid Hydrocarbons _____ None _____ Deg.						
2.	1.92	538	1.43	.792	Specific Gravity Separator Gas _____ 0.652 _____		X X X X X X X X X				
3.	1.88	537	1.43	.795	Specific Gravity Flowing Fluid _____ X X X X X						
4.	1.82	537	1.43	.801	Critical Pressure _____ 670 _____ P.S.I.A.		P.S.I.A.				
5.					Critical Temperature _____ 375 _____ R		R				
P <sub>f</sub> 1512.2		P <sub>f</sub> 2287									
NO.	P <sub>i</sub> <sup>2</sup>	P <sub>s</sub>	P <sub>s</sub> <sup>2</sup>	P <sub>f</sub> <sup>2</sup> - P <sub>s</sub> <sup>2</sup>	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 8.13879$		(2) $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.85286$				
1	1499.2	2248	39		AOF = Q $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2414.943$						
2	1484.2	2203	84								
3	1455.2	2118	169								
4	1416.2	2006	281								
5											
Absolute Open Flow _____ 2414.943 _____ Mcfd @ 15.025		Angle of Slope @ _____ 63° 30'		Slope, n _____ 0.5000							
Remarks: BHP measured with Amerada RPG-3 gauge serial No. 32030, 0-4000 PSIG											
Approved By Commission:			Conducted By: Tefteller, Inc.			Calculated By: B. Combest			Checked By:		

