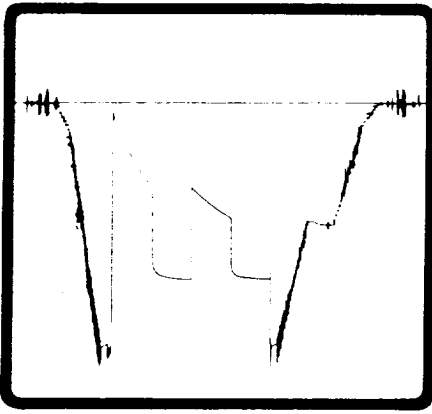


FORMATION TESTING SERVICE REPORT



~~PRODUCTION WELL FILE~~

~~EXPLORATION WELL FILE~~



Duncan, Oklahoma 73536

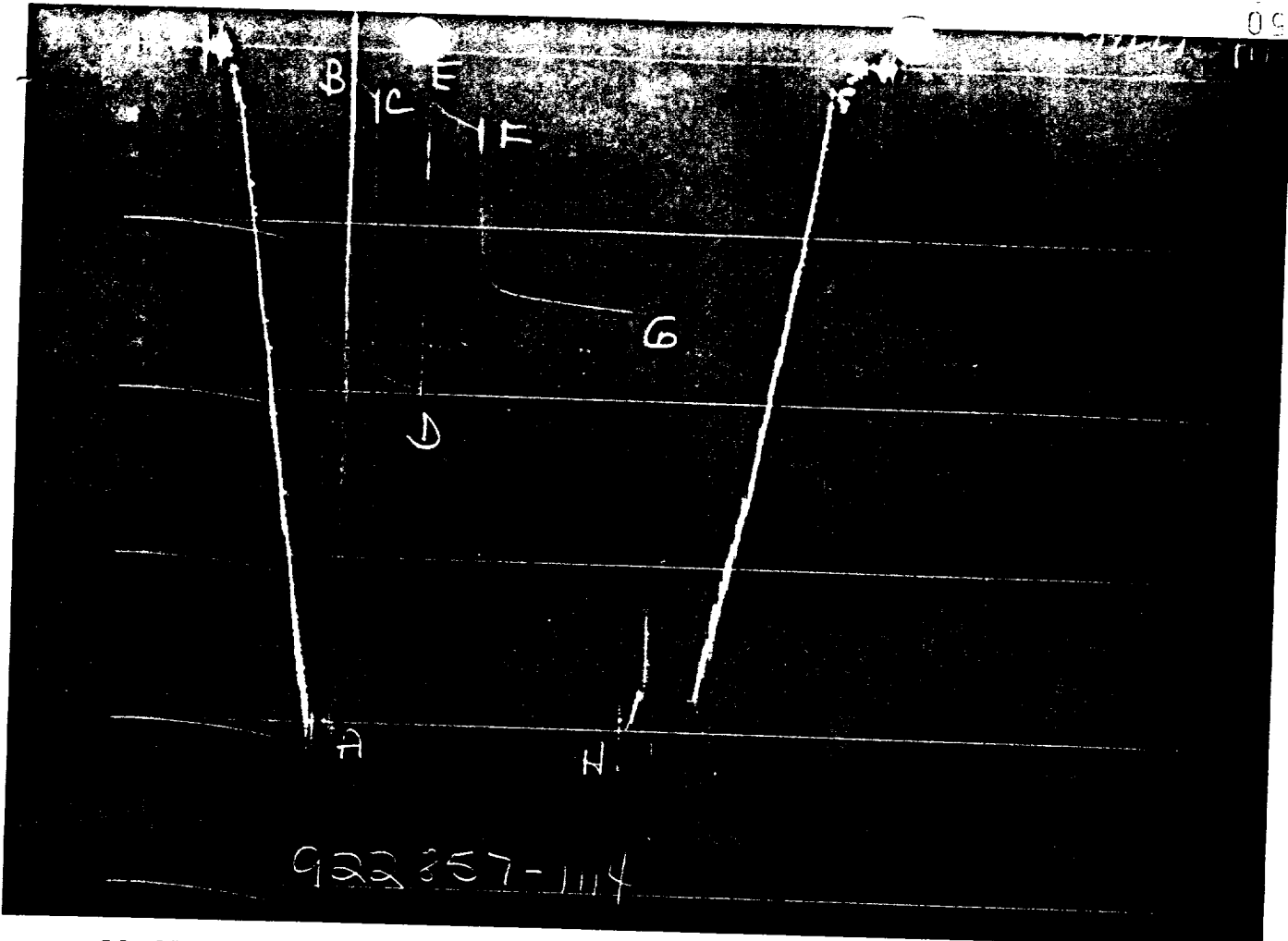


A Halliburton Company

LEASE NAME: GRAHAM & FEDERAL
WELL NO.: 1
TEST NO.: 2
TESTED INTERVAL: 8430.1 - 8540.1
LEASE OWNER/COMPANY NAME: HELMERICH & PRYNE, INCORPORATED

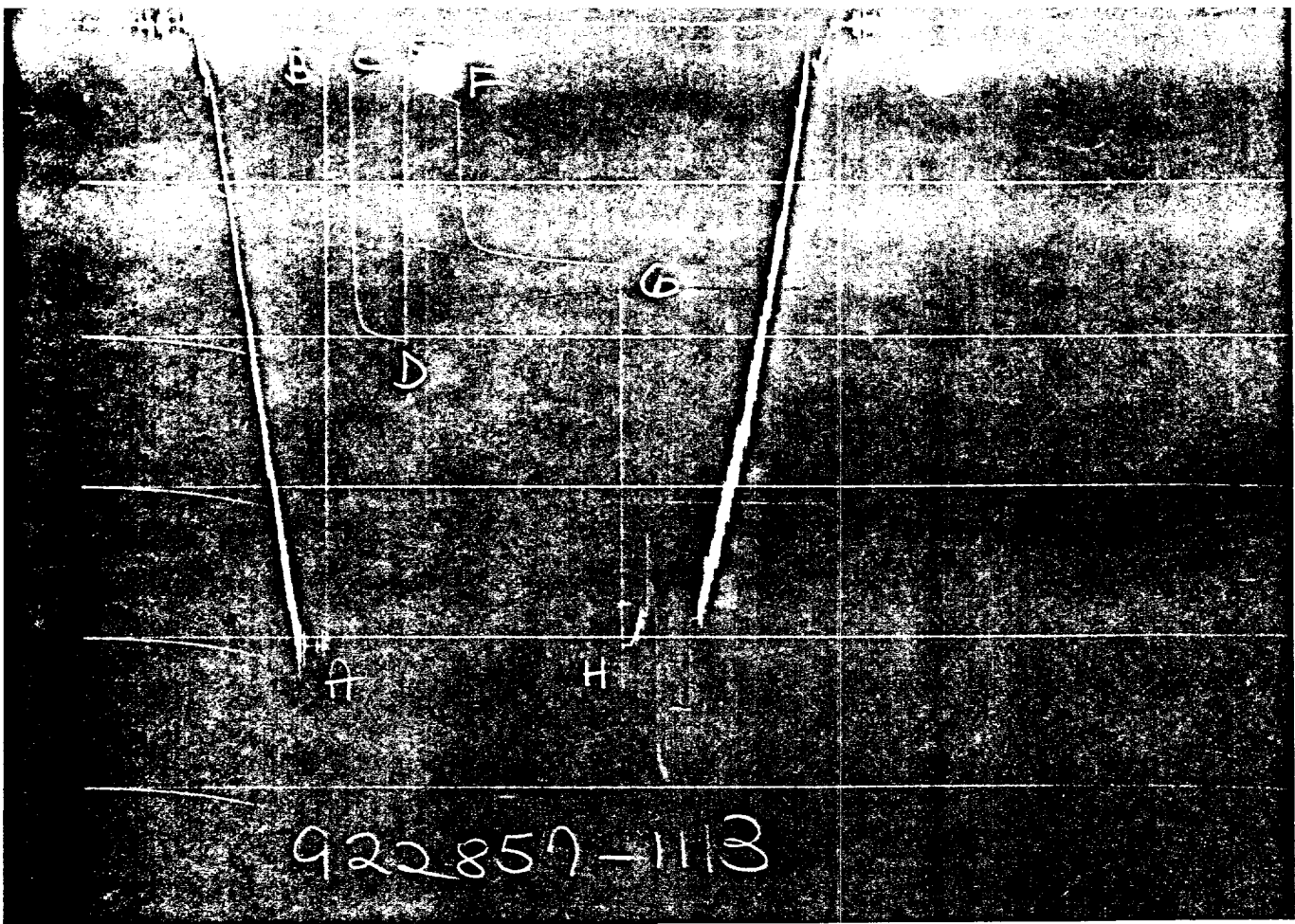
NOMENCLATURE

B	= Formation Volume Factor (Res Vol / Std Vol)	—
c_t	= System Total Compressibility	(Vol / Vol) / psi
DR	= Damage Ratio	—
h	= Estimated Net Pay Thickness	Ft
k	= Permeability	md
m	$\left\{ \begin{array}{l} \text{(Liquid) Slope Extrapolated Pressure Plot} \\ \text{(Gas) Slope Extrapolated } m(P) \text{ Plot} \end{array} \right.$	psi/cycle
		MM psi ² /cp/cycle
$m(P^*)$	= Real Gas Potential at P^*	MM psi ² /cp
$m(P_f)$	= Real Gas Potential at P_f	MM psi ² /cp
AOF_1	= Maximum Indicated Absolute Open Flow at Test Conditions	MCFD
AOF_2	= Minimum Indicated Absolute Open Flow at Test Conditions	MCFD
P^*	= Extrapolated Static Pressure	Psig
P_f	= Final Flow Pressure	Psig
Q	= Liquid Production Rate During Test	BPD
Q_1	= Theoretical Liquid Production w/ Damage Removed	BPD
Q_g	= Measured Gas Production Rate	MCFD
r_i	= Approximate Radius of Investigation	Ft
r_w	= Radius of Well Bore	Ft
S	= Skin Factor	
t	= Total Flow Time Previous to Closed-in	Minutes
Δt	= Closed-in Time at Data Point	Minutes
T	= Temperature Rankine	R
ϕ	= Porosity	—
μ	= Viscosity of Gas or Liquid	cp
Log	= Common Log	



GAUGE NO: 1114 DEPTH: 8409.0 BLANKED OFF: NO HOUR OF CLOCK: 24

ID	DESCRIPTION	PRESSURE		TIME		TYPE
		REPORTED	CALCULATED	REPORTED	CALCULATED	
A	INITIAL HYDROSTATIC	3989	3991.0			
B	INITIAL FIRST FLOW	160	163.9			
C	FINAL FIRST FLOW	272	273.2	30.0	27.6	F
C	INITIAL FIRST CLOSED-IN	272	273.2			
D	FINAL FIRST CLOSED-IN	1973	1969.1	60.0	60.6	C
E	INITIAL SECOND FLOW	288	304.7			
F	FINAL SECOND FLOW	431	438.1	60.0	60.1	F
F	INITIAL SECOND CLOSED-IN	431	438.1			
G	FINAL SECOND CLOSED-IN	1479	1472.8	180.0	181.8	C
H	FINAL HYDROSTATIC	4037	3990.4			



GAUGE NO: 1113 DEPTH: 8537.0 BLANKED OFF: YES HOUR OF CLOCK: 24

ID	DESCRIPTION	PRESSURE		TIME		TYPE
		REPORTED	CALCULATED	REPORTED	CALCULATED	
A	INITIAL HYDROSTATIC	4225	4057.0			
B	INITIAL FIRST FLOW	217	227.0			
C	FINAL FIRST FLOW	325	326.0	30.0	27.6	F
C	INITIAL FIRST CLOSED-IN	325	326.0			
D	FINAL FIRST CLOSED-IN	2057	2029.0	60.0	60.6	C
E	INITIAL SECOND FLOW	507	357.0			
F	FINAL SECOND FLOW	479	486.0	60.0	60.1	F
F	INITIAL SECOND CLOSED-IN	460	460.0			
G	FINAL SECOND CLOSED-IN	1900	1800.0	150.0	151.8	C
H	FINAL HYDROSTATIC	2000	1900.0			

EQUIPMENT & HOLE DATA

FORMATION TESTED: BONESPRING

NET PAY (ft): _____

GROSS TESTED FOOTAGE: 110.0

ALL DEPTHS MEASURED FROM: KB

CASING PERFS. (ft): _____

HOLE OR CASING SIZE (in): 7.875

ELEVATION (ft): 3803

TOTAL DEPTH (ft): 8540.0

PACKER DEPTH(S) (ft): 8424, 8430

FINAL SURFACE CHOKE (in): 0.387

BOTTOM HOLE CHOKE (in): 0.750

MUD WEIGHT (lb/gal): 9.20

MUD VISCOSITY (sec): 28

ESTIMATED HOLE TEMP. (°F): _____

ACTUAL HOLE TEMP. (°F): 123 @ 8536.0 ft

TICKET NUMBER: 92285700

DATE: 12-3-84 TEST NO: 2

TYPE DST: OPEN HOLE

HALLIBURTON CAMP: ARTESIA

TESTER: STAN MC KEE

WITNESS: KYLE POSSEY
J.B. JOHNSON

DRILLING CONTRACTOR: MC VAY #4

FLUID PROPERTIES FOR RECOVERED MUD & WATER

SOURCE	RESISTIVITY	CHLORIDES
<u>MUD PIT</u>	<u>0.090 @ 65 °F</u>	<u>89000 ppm</u>
<u>BOTTOM RECOVERY</u>	<u>0.090 @ 65 °F</u>	<u>85000 ppm</u>
<u>MIDDLE RECOVERY</u>	<u>0.090 @ 65 °F</u>	<u>89000 ppm</u>
_____	_____ @ _____ °F	_____ ppm
_____	_____ @ _____ °F	_____ ppm
_____	_____ @ _____ °F	_____ ppm

SAMPLER DATA

Pstg AT SURFACE: _____

cu.ft. OF GAS: _____

cc OF OIL: _____

cc OF WATER: _____

cc OF MUD: _____

TOTAL LIQUID cc: _____

HYDROCARBON PROPERTIES

OIL GRAVITY (°API): 37.5 @ 60 °F

GAS/OIL RATIO (cu.ft. per bbl): _____

GAS GRAVITY: _____

CUSHION DATA

TYPE	AMOUNT	WEIGHT
_____	_____	_____
_____	_____	_____

RECOVERED:

5.3 BBLS. OF OIL
3 BBLS. OF OIL & GAS CUT DRILLING FLUID

MEASURED FROM
TESTER VALVE

REMARKS:

FLUID PROPERTIES COULD NOT BE DETERMINED FOR THE TOP RECOVERY - CONSISTED OF OIL.

TICKET NO: 92285706

CLOCK NO: 13736 HOUR: 24



GAUGE NO: 1114

DEPTH: 8409.0

REF	MINUTES	PRESSURE	AP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
FIRST FLOW					
B	1	0.0	163.9		
	2	2.0	167.7	3.8	
	3	4.0	173.4	7.7	
	4	6.0	179.9	4.5	
	5	8.0	184.5	4.5	
	6	10.0	191.8	7.4	
	7	12.0	201.3	9.4	
	8	14.0	210.5	9.3	
	9	16.0	223.7	13.1	
	10	18.0	234.2	10.5	
	11	20.0	241.9	7.7	
	12	22.0	250.2	8.3	
	13	24.0	259.0	8.8	
	14	26.0	268.1	9.1	
C	15	27.6	273.2	5.1	
FIRST CLOSED-IN					
C	1	0.0	273.2		
	2	1.0	865.7	592.5	1.0 1.444
	3	2.0	1288.7	1015.5	1.8 1.177
	4	3.0	1476.9	1203.7	2.7 1.005
	5	4.0	1607.5	1334.2	3.5 0.895
	6	5.0	1679.6	1406.4	4.2 0.814
	7	6.0	1737.0	1463.8	4.9 0.748
	8	7.0	1779.2	1506.0	5.6 0.694
	9	8.0	1807.1	1533.9	6.2 0.650
	10	9.0	1829.9	1556.7	6.8 0.608
	11	10.0	1844.8	1571.6	7.3 0.574
	12	12.0	1866.5	1593.3	8.3 0.519
	13	14.0	1882.4	1609.2	9.3 0.473
	14	16.0	1894.4	1621.2	10.1 0.435
	15	18.0	1902.7	1629.5	10.9 0.403
	16	20.0	1910.2	1637.0	11.6 0.377
	17	22.0	1916.1	1642.9	12.2 0.352
	18	24.0	1921.5	1648.3	12.8 0.332
	19	26.0	1925.8	1652.6	13.4 0.313
	20	28.0	1930.2	1657.0	13.9 0.297
	21	30.0	1933.4	1660.2	14.4 0.283
	22	35.0	1941.4	1668.2	15.4 0.252
	23	40.0	1948.1	1674.9	16.3 0.228
	24	45.0	1954.5	1681.3	17.1 0.208
	25	50.0	1959.9	1686.7	17.8 0.191
	26	55.0	1964.5	1691.3	18.4 0.176
D	27	60.6	1969.1	1695.9	18.9 0.163
SECOND FLOW					
E	1	0.0	304.7		
	2	4.0	290.1	-14.6	

REF	MINUTES	PRESSURE	AP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
SECOND FLOW - CONTINUED					
	3	8.0	282.0	-8.1	
	4	12.0	305.5	23.5	
	5	16.0	322.4	16.9	
	6	20.0	342.4	20.0	
	7	24.0	355.0	12.6	
	8	28.0	361.8	6.7	
	9	32.0	373.3	11.5	
	10	36.0	381.9	8.6	
	11	40.0	393.4	11.5	
	12	44.0	401.6	8.2	
	13	48.0	412.0	10.4	
	14	52.0	422.2	10.2	
	15	56.0	428.6	5.4	
F	16	60.1	438.1	9.5	
SECOND CLOSED-IN					
F	1	0.0	438.1		
	2	1.0	893.0	454.9	1.0 1.949
	3	2.0	976.4	538.3	1.9 1.659
	4	3.0	1050.9	612.8	2.9 1.477
	5	4.0	1105.9	667.8	3.8 1.364
	6	5.0	1147.2	709.1	4.7 1.266
	7	6.0	1178.0	739.9	5.6 1.196
	8	7.0	1205.5	767.4	6.5 1.132
	9	8.0	1226.9	788.9	7.3 1.080
	10	9.0	1245.5	807.4	8.1 1.032
	11	10.0	1260.1	822.1	9.0 0.990
	12	12.0	1287.8	849.7	10.5 0.920
	13	14.0	1307.6	869.6	12.1 0.862
	14	16.0	1321.1	883.1	13.6 0.811
	15	18.0	1333.2	895.1	14.9 0.769
	16	20.0	1341.6	903.6	16.3 0.732
	17	22.0	1349.7	911.7	17.6 0.697
	18	24.0	1357.0	919.0	18.9 0.667
	19	26.0	1362.0	923.9	20.0 0.641
	20	28.0	1365.5	927.4	21.2 0.617
	21	30.0	1369.6	931.5	22.4 0.593
	22	35.0	1373.0	940.9	25.0 0.545
	23	40.0	1385.3	947.3	27.5 0.504
	24	45.0	1391.8	953.8	29.7 0.470
	25	50.0	1397.9	959.8	31.9 0.440
	26	55.0	1402.0	963.9	33.8 0.414
	27	60.0	1406.1	968.1	35.6 0.391
	28	70.0	1414.1	976.0	38.9 0.353
	29	80.0	1422.0	984.0	41.8 0.321
	30	90.0	1427.6	989.5	44.4 0.295
	31	100.0	1433.6	995.6	46.7 0.273
	32	110.0	1440.1	1002.1	48.8 0.255
	33	120.0	1445.7	1007.6	50.7 0.238
	34	135.0	1452.9	1014.8	53.2 0.217
	35	150.0	1459.7	1021.6	55.3 0.200
	36	165.0	1465.9	1027.8	57.3 0.185

REMARKS:

TICKET NO: 92285700

CLOCK NO: 13736 HOUR: 24



GAUC NO: 1114

DEPTH: 8409.0

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
SECOND CLOSED-IN - CONTINUED					
G 37	181.8	1472.8	1034.8	59.1	0.171

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
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REMARKS:

TICKET NO: 92265700
 CLOCK NO: 4365 HOUR: 24



GAUGE NO: 1113
 DEPTH: 8537.0

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
FIRST FLOW					
B 1	0.0	227.5			
2	2.0	224.7	-2.6		
3	4.0	226.7	2.0		
4	6.0	231.5	4.9		
5	8.0	235.5	4.0		
6	10.0	242.2	6.7		
7	12.0	250.3	8.1		
8	14.0	260.5	10.1		
9	16.0	273.5	13.0		
10	18.0	285.4	11.9		
11	20.0	294.2	8.9		
12	22.0	301.5	7.2		
13	24.0	309.4	7.9		
14	26.0	318.1	8.7		
C 15	27.6	326.0	7.9		
FIRST CLOSED-IN					
C 1	0.0	326.0			
2	1.0	771.1	445.1	1.0	1.447
3	2.0	1075.6	749.6	1.8	1.173
4	3.0	1378.7	1052.7	2.7	1.007
5	4.0	1538.5	1212.5	3.5	0.897
6	5.0	1658.1	1332.1	4.2	0.815
7	6.0	1730.6	1404.6	4.9	0.749
8	7.0	1785.1	1459.1	5.6	0.692
9	8.0	1823.2	1497.2	6.2	0.649
10	9.0	1857.9	1531.9	6.8	0.607
11	10.0	1878.6	1552.6	7.4	0.574
12	12.0	1909.2	1583.2	8.4	0.517
13	14.0	1928.8	1602.8	9.3	0.472
14	16.0	1943.4	1617.4	10.1	0.434
15	18.0	1953.4	1627.4	10.9	0.403
16	20.0	1961.2	1635.2	11.6	0.376
17	22.0	1968.5	1642.5	12.2	0.352
18	24.0	1973.9	1647.9	12.8	0.332
19	26.0	1979.4	1653.4	13.4	0.314
20	28.0	1982.9	1656.9	13.9	0.298
21	30.0	1987.0	1661.0	14.4	0.283
22	35.0	1995.9	1669.9	15.4	0.252
23	40.0	2002.4	1676.4	16.3	0.228
24	45.0	2008.6	1682.7	17.1	0.207
25	50.0	2014.9	1688.9	17.8	0.191
26	55.0	2020.3	1694.3	18.4	0.176
D 27	60.6	2025.7	1699.7	18.9	0.163
SECOND FLOW					
E 1	0.0	357.4			
2	4.0	332.5	-25.0		

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
SECOND FLOW - CONTINUED					
3	8.0	332.5	0.0		
4	12.0	358.1	25.7		
5	16.0	376.7	18.6		
6	20.0	393.5	16.8		
7	24.0	406.7	13.2		
8	28.0	413.1	6.3		
9	32.0	423.0	9.9		
10	36.0	433.7	10.7		
11	40.0	444.1	10.5		
12	44.0	451.9	7.8		
13	48.0	461.7	9.8		
14	52.0	471.6	9.9		
15	56.0	477.9	6.3		
F 16	60.1	488.6	10.7		
SECOND CLOSED-IN					
F 1	0.0	488.6			
2	1.0	754.5	265.9	1.0	1.965
3	2.0	912.9	424.3	2.0	1.649
4	3.0	1014.4	525.8	2.9	1.480
5	4.0	1081.1	592.5	3.8	1.361
6	5.0	1135.1	646.5	4.7	1.269
7	6.0	1161.4	692.8	5.6	1.193
8	7.0	1216.3	727.7	6.5	1.131
9	8.0	1247.6	758.9	7.3	1.078
10	9.0	1272.2	783.6	8.1	1.033
11	10.0	1294.4	805.8	9.0	0.991
12	12.0	1324.1	835.5	10.6	0.918
13	14.0	1348.2	859.6	12.1	0.860
14	16.0	1365.0	876.4	13.6	0.811
15	18.0	1378.8	890.2	14.9	0.769
16	20.0	1389.9	901.3	16.3	0.730
17	22.0	1399.0	910.4	17.6	0.697
18	24.0	1406.1	917.5	18.8	0.668
19	26.0	1412.4	923.8	20.1	0.640
20	28.0	1417.8	929.1	21.2	0.616
21	30.0	1422.4	933.8	22.3	0.594
22	35.0	1432.1	943.4	25.0	0.545
23	40.0	1439.9	951.3	27.5	0.504
24	45.0	1446.7	958.1	29.8	0.469
25	50.0	1451.9	963.3	31.8	0.440
26	55.0	1457.4	968.8	33.8	0.414
27	60.0	1461.6	972.9	35.6	0.391
28	70.0	1469.6	981.0	38.9	0.353
29	80.0	1475.7	987.1	41.8	0.321
30	90.0	1482.1	993.5	44.4	0.295
31	100.0	1487.5	998.9	46.7	0.273
32	110.0	1494.1	1005.5	48.8	0.255
33	120.0	1498.7	1010.1	50.7	0.238
34	135.0	1506.6	1018.0	53.2	0.217
35	150.0	1513.5	1024.9	55.3	0.200
36	165.0	1519.8	1031.1	57.3	0.185

REMARKS:

TICKET NO: 92285700

WELL LOCK NO: 4365 HOUR: 24



GAUGE N 1113

DEPTH: 8537.0

REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
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












SECOND CLOSED-IN - CONTINUED

G 37	181.8	1527.5	1038.9	59.1	0.171
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REF	MINUTES	PRESSURE	ΔP	$\frac{t \times \Delta t}{t + \Delta t}$	$\log \frac{t + \Delta t}{\Delta t}$
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REMARKS:

		O.D.	I.D.	LENGTH	DEPTH	
1		DRILL PIPE.....	4.500	3.826	7820.0	
3		DRILL COLLARS.....	6.250	2.250	494.0	
50		IMPACT REVERSING SUB.....	5.750	3.000	1.0	8304.0
3		DRILL COLLARS.....	6.250	2.250	91.0	
5		CROSSOVER.....	5.750	3.000	1.0	
13		DUAL CIP SAMPLER.....	5.000	0.750	7.0	
60		HYDROSPRING TESTER.....	5.000	0.750	5.0	8407.0
80		AP RUNNING CASE.....	5.000	3.060	4.0	8409.0
15		JAR.....	5.000	1.750	5.0	
16		VR SAFETY JOINT.....	5.000	1.000	3.0	
70		OPEN HOLE PACKER.....	6.750	1.530	5.8	8424.0
70		OPEN HOLE PACKER.....	6.750	1.530	5.8	8430.0
19		ANCHOR PIPE SAFETY JOINT.....	5.750	1.500	5.0	
5		CROSSOVER.....	5.750	3.000	1.0	
3		DRILL COLLARS.....	6.250	2.250	87.0	
5		CROSSOVER.....	5.750	3.000	1.0	
20		FLUSH JOINT ANCHOR.....	5.750	2.870	10.0	
81		BLANKED-OFF RUNNING CASE.....	5.750		4.0	8537.0
		TOTAL DEPTH				8540.0

EQUATIONS FOR DST LIQUID WELL ANALYSIS

Transmissibility	$\frac{kh}{\mu} = \frac{162.6 QB}{m}$	$\frac{\text{md-ft}}{\text{cp}}$
Indicated Flow Capacity	$kh = \frac{kh}{\mu} \mu$	md-ft
Average Effective Permeability	$k = \frac{kh}{h}$	md
Damage Ratio	$DR = .183 \frac{P^* - P_f}{m}$	—
Theoretical Potential w / Damage Removed	$Q_1 = Q DR$	BPD
Approx. Radius of Investigation	$r_i = 4.63 \sqrt{kt}$	ft

EQUATIONS FOR DST GAS WELL ANALYSIS

Indicated Flow Capacity	$kh = \frac{1637 Q_g T}{m}$	md-ft
Average Effective Permeability	$k = \frac{kh}{h}$	md
Skin Factor	$S = 1.151 \left[\frac{m(P^*) - m(P_f)}{m} - \text{LOG} \frac{k(t/60)}{\phi \mu c_f r_w^2} + 3.23 \right]$	—
Damage Ratio	$DR = \frac{m(P^*) - m(P_f)}{m(P^*) - m(P_f) - 0.87 mS}$	—
Indicated Flow Rate (Maximum)	$AOF_1 = \frac{Q_g m(P^*)}{m(P^*) - m(P_f)}$	MCFD
Indicated Flow Rate (Minimum)	$AOF_2 = Q_g \sqrt{\frac{m(P^*)}{m(P^*) - m(P_f)}}$	MCFD
Approx. Radius of Investigation	$r_i = 0.032 \sqrt{\frac{k(t/60)}{\phi \mu c_f}}$	ft