

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND IE POINT BACK PRESSURE TEST GAS WELL

Form C-122
Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special				Test Date 7-11-77							
Company UNION TEXAS PETROLEUM CORP.				Connection Northern Natural Gas Company							
Pool Eumont				Formation Queen							
Completion Date 12-16-76		Total Depth 5711		Plug Back TD 3490							
				Elevation 3545' DF							
Farm or Lease Name Britt "B"				Well No. 2							
Csg. Size 5.500	Wt. 14.0	d 5.012	Set At 5710	Perforations: From 3155 To 3245							
Tbg. Size 2.375	Wt. 4.7	d 1.995	Set At 3302	Perforations: From -- To --							
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Gas - Gas Multiple				Packer Set At 3302							
Producing Thru Casing		Reservoir Temp. °F 90 @ 3200		Mean Annual Temp. °F 80							
				Baro. Press. - P _g 13.2							
L .3200	H 3200	G _g .664	% CO ₂ ---	% N ₂ ---	% H ₂ S ---						
Prover ---				Meter Run 4.0	Taps Pipe						
FLOW DATA											
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	TUBING DATA		CASING DATA		Duration of Flow
							Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	
SI											
1.	4.000 x 2.000			77	.7	70	0	0	517		69.5
2.	4.000 x 2.000			79	1.5	69	0	0	454	72	1.5
3.	4.000 x 2.000			79	2.9	70	0	0	413	73	1.5
4.	4.000 x 2.000			74	5.5	69	0	0	377	74	1.5
5.							0	0	329	76	1.5
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd				
1	23.25	8.21	89.8	.9907	1.2272	1.0087	234				
2	23.25	11.73	91.8	.9911	1.2272	1.0089	335				
3	23.25	16.33	92.0	.9905	1.2272	1.0089	466				
4	23.25	21.95	87.6	.9918	1.2272	1.0086	627				
5											
NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ 0 _____ Mcf/bbl.						
1.	.13	530	1.40	.983	A.P.I. Gravity of Liquid Hydrocarbons _____ 0 _____ Deg.						
2.	.14	529	1.40	.982	Specific Gravity Separator Gas .664 X X X X X X X X						
3.	.14	530	1.40	.982	Specific Gravity Flowing Fluid X X X X X .664						
4.	.13	529	1.40	.983	Critical Pressure 669 P.S.I.A. 669 P.S.I.A.						
5.					Critical Temperature 378 R 378 R						
P _c 529.2 P _c 280											
NO.	P _t ²	P _w	P _w ²	P _c ² - P _w ²	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.7676$	(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.7676$					
1	218	467	218	62	AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1,107$						
2	182	427	182	98							
3	152	393	154	126							
4	117	349	122	158							
5											
Absolute Open Flow 1,107 _____ Mcfd @ 15.025 Angle of Slope θ 45.0 Slope, n 1.000											
Remarks: _____											
Approved By Commission: _____ Conducted By: Pual Granger Calculated By: Bill Higgins Checked By: _____											

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DEC 23 1977

OIL CONSERVATION COMM.
HOBBS, N. M.