

Number: 6030-20110087-001A

Artesia Laboratory 200 E Main St. Artesia, NM 88210 Phone 575-746-3481

Chandler Montgomery Occidental Petroleum 1502 W Commerce Dr. Carlsbad, NM 88220 Nov. 17, 2020

Field: NMSW Sampled By: Jesus Escobedo Station Name: Corral Compressor Station 2 South Sample Of: Gas Spot Station Number: N/A Sample Date: 11/11/2020 01:09 Sample Point: N/A Sample Conditions: 1265 psig Ambient

Sample Point: N/A Sample Conditions: 1265 psig Ambient: 49 °F Meter Number: Effective Date: 11/11/2020 01:09
County: Eddy Method: GPA 2286

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Type of Sample: Spot-Cylinder Cylinder No: 1111-001162
Heat Trace Used: N/A Instrument: 6030 GC2 (Ag

Heat Trace Used: N/A Instrument: 6030_GC2 (Agilent GC-7890B)
Sampling Method: Fill and Purge Last Inst. Cal.: 08/25/2020 8:12 AM

Sampling Company: OXY

Analyzed: 11/17/2020 12:40:16 by PGS

Analytical Data

Components	Un-normalized Mol %	Mol. %	Wt. %	GPM at 14.65 psia		
Hydrogen Sulfide	0.000	0.000	0.000		GPM TOTAL C2+	6.390
Nitrogen	1.332	1.320	1.675		GPM TOTAL C3+	3.359
Methane	76.899	76.201	55.381		GPM TOTAL iC5+	0.805
Carbon Dioxide	0.171	0.169	0.337			
Ethane	11.459	11.355	15.468	3.031		
Propane	5.781	5.728	11.443	1.575		
Iso-butane	0.846	0.838	2.207	0.274		
n-Butane	2.259	2.238	5.893	0.705		
Iso-pentane	0.642	0.636	2.079	0.232		
n-Pentane	0.766	0.759	2.481	0.275		
Hexanes Plus	0.763	0.756	3.036	0.298		
	100.918	100.000	100.000	6.390		
Calculated Physica	Calculated Physical Properties		otal	C6+		
Relative Density Rea	al Gas	0.70	649	3.0584		
Calculated Molecula	r Weight	22	2.07	88.58		
Compressibility Fact	or	0.99	960			
GPA 2172 Calculati	on:					
Calculated Gross B	STU per ft ³ @ 14.65 p	sia & 60°F				
Real Gas Dry BTU		1;	308	4763		
Water Sat. Gas Base BTU		12	285	4680		
Ideal, Gross HV - Dry at 14.65 psia		130	2.9	4763.5		
Ideal, Gross HV - Wet		128	80.1	0.000		
Net BTU Dry Gas - real gas		1.	188			
Net BTU Wet Gas - real gas		1	167			
Commente: HOCE	iald Camtant O man					

Comments: H2S Field Content 0 ppm

Hydrocarbon Laboratory Manager

Quality Assurance: The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality

assurance, unless otherwise stated.



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Station Name: Corral Compressor Station 2 South Station Number: N/A

Sample Point: N/A Meter Number:

County: Eddy

Type of Sample: Spot-Cylinder

Heat Trace Used: N/A

Sampling Method: Fill and Purge

Nov. 17, 2020

Sampled By: Jesus Escobedo

Sample Of: Gas Spot Sample Date: 11/11/2020 01:09

Sample Conditions: 1265 psig Method: GPA 2286 Cylinder No: 1111-001162

Analyzed: 11/17/2020 13:21:28 by PGS

Sampling Company: OXY

Analytical Data

Components	Mol. %	Wt. %	GPM at 14.65 psia			
Hydrogen Sulfide	NIL	NIL		GPM TOTAL C2+	6.390	
Nitrogen	1.320	1.675		GPM TOTAL C3+	3.359	
Methane	76.201	55.381		GPM TOTAL iC5+	0.805	
Carbon Dioxide	0.169	0.337				
Ethane	11.355	15.468	3.031			
Propane	5.728	11.443	1.575			
Iso-Butane	0.838	2.207	0.274			
n-Butane	2.238	5.893	0.705			
Iso-Pentane	0.636	2.079	0.232			
n-Pentane	0.759	2.481	0.275			
Hexanes	0.374	1.443	0.152			
Heptanes Plus	0.382	1.593	0.146			
	100.000	100.000	6.390			
Calculated Physica	al Properties		Total	C7+		
Relative Density Rea	al Gas		0.7649	3.1738		
Calculated Molecula	ır Weight		22.07	91.92		
Compressibility Fact	tor		0.9960			
GPA 2172 Calculati	ion:					
Calculated Gross B	BTU per ft³ @	2 14.65 psi	a & 60°F			
Real Gas Dry BTU			1308	4850		
Water Sat. Gas Base	Water Sat. Gas Base BTU		1285	4766		
Ideal, Gross HV - Dr	y at 14.65 ps	sia	1302.9	4850.4		
Ideal, Gross HV - We	et		1280.1	NIL		
Comments: H2S F	Field Content	0 ppm				

Hydrocarbon Laboratory Manager

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Quality Assurance:



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				001170711.00		
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Carbon Dioxide	0.169	0.337	0.004			
Ethane	11.355	15.468	3.031			
Propane	5.728	11.443	1.575			
Iso-Butane	0.838	2.207	0.274			
n-Butane	2.238	5.893	0.705			
Iso-Pentane	0.636	2.079	0.232			
n-Pentane	0.759	2.481	0.275			
i-Hexanes	0.229	0.880	0.092			
n-Hexane	0.145	0.563	0.060			
Benzene	0.036	0.125	0.010			
Cyclohexane	0.091	0.348	0.031			
i-Heptanes	0.135	0.566	0.054			
n-Heptane	0.027	0.125	0.013			
Toluene	0.015	0.065	0.005			
i-Octanes	0.065	0.307	0.029			
n-Octane	0.003	0.015	0.001			
Ethylbenzene	0.001	0.002	NIL			
Xylenes	0.003	0.010	0.001			
i-Nonanes	0.005	0.025	0.002			
n-Nonane	0.001	0.003	NIL			
i-Decanes	NIL	NIL	NIL			
n-Decane	NIL	0.001	NIL			
Undecanes	NIL	0.001	NIL			
Dodecanes	NIL	NIL	NIL			
Tridecanes	NIL	NIL	NIL			
Tetradecanes Plus	NIL	NIL	NIL_			
	100.000	100.000	6.390			



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 Cylinder No:
 1111-001162

Analyzed: 11/17/2020 13:21:28 by PGS

Nov. 17, 2020

Sampling Company: OXY

Calculated Physical PropertiesTotalCalculated Molecular Weight22.073

GPA 2172 Calculation:

Calculated Gross BTU per ft³ @ 14.65 psia & 60°FReal Gas Dry BTU1308.0Water Sat. Gas Base BTU1285.2Relative Density Real Gas0.7649Compressibility Factor0.9960

Comments: H2S Field Content 0 ppm

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Hydrocarbon Laboratory Manager

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UPSET FLARING EVENT SPECIFIC JUSTIFICATIONS FORM

Facility: Corral 2S CS Date: 08/28/2021

Duration of event: 2 Hours 50 minutes **MCF Flared:** 996

1st Event Start Time: 01:50 PM **1st Event End Time:** 03:20 PM

2nd Event Start Time: 04:30 PM **2nd Event End Time:** 05:30 PM

Cause: Downstream Activity > Enterprise > ETC

Method of Flared Gas Measurement: Gas Flare Meter

Well API Associated with Facility: 30-015-44507 Corral Fly 02 01 State #021H

Comments: This upset event was not caused by any wells associated with the facility. This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control, and did not stem from activity that could have been foreseen and avoided, and could not have been avoided or prevented by good design, operation, and preventative maintenance practices.

1. Reason why this event was beyond Operator's control:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction or complete shut-in of a gas pipeline by a third-party pipeline operator, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices.

In this case, there were two (2) flaring events that were triggered by the same cause as a result of downstream activity by third party pipeline operator ETC, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening. The first event occurred from 01:50 PM to 03:20 PM, with a total of 411 MCF flared and the second event occurred from 04:30 PM to 05:30 PM, with a total of 585 MCF flared. Both events occurred as a result of Oxy exporting gas to Enterprise during a scheduled ETC gas curtailment for plant maintenance, from August 24th to August 28th, 2021. Due to additional issues on their end, ETC had to extend the duration of their curtailment due communication and programing issues with their pipeline sales control valve, which malfunctioned twice, therefore prompting Enterprise's sales pipeline pressure to spike higher, and triggering two flaring event at Oxy's Corral 2S compressor station. This event is out of OXY's control yet, OXY made every effort to control and minimize emissions as much as possible.

2. Steps Taken to limit duration and magnitude of venting or flaring:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction or complete shut-in of a gas pipeline by a third-party pipeline operator, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices.

This facility is unmanned, except when Oxy production techs are gathering data daily or conducting daily walkthroughs to ensure that there are no problems, circumstances and/or assist other personnel on-site for maintenance purposes. In this case, the increased spike in Enterprise's pipeline pressure forced Oxy's upstream facility to route all its stranded gas to a flare, as it was not able to push all its gas into Enterprises' gas pipeline due to the restrictions of gas flow placed on the pipeline, caused by ETC's maintenance gas curtailment and their communication and programing issues with their pipeline sales control valve. On both occasions, Oxy production techs, immediately upon receiving high pressure line alarms, arrived at the facility and began inspecting the equipment and contacting Enterprise personnel to determine cause of the spike in the pipeline pressure. Oxy production techs were informed during the first flaring event by Enterprise personnel that ETC had to call out a measurement tech from Midland to troubleshoot and repair the control valve, but it would take some time to resolve. Therefore, Oxy production techs began procedures to choke back production to minimize emissions, and stayed on location until flaring ceased when Enterprise was able to bring their pipeline pressure down so that our sales gas could get into their sales pipeline, which then in turn, ceased flaring at Oxy's compressor station. During the second event, Oxy production techs, immediately upon receiving high pressure line alarms yet again, arrived at the facility and began inspecting the equipment and contacting Enterprise personnel to determine cause of the spike in the pipeline pressure and learning that ETC's pipeline sales flow control valve started opening and closing erratically, i.e. malfunctioning yet again, due to on-going communication control valve issues. ETC again had dispatched techs to resolve their issues and when Enterprise was able to bring their pipeline pressure down so that Oxy's sales gas could get into their sales pipeline, did flaring from the second event cease.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

Oxy cannot take any corrective actions to eliminate the cause and potential reoccurrence of an Enterprise gas flow pipeline restriction or shut-in, as this control issue is downstream of Oxy's custody transfer point and out of Oxy's control to avoid, prevent from happening or reoccurring. Enterprise's downstream facilities and associated facilities and/or operators, such as ETC., may have issues which will reoccur from time to time and may trigger a spike in their gas line pressure, which in turn, directly impacts Oxy's ability to send gas to them. When Enterprise has downstream activity issues or greatly struggles to handle the volume of gas being sent to them by Oxy, Enterprise then restricts Oxy's ability to send gas, which then prompts Oxy to route all of its stranded gas not pushed into the Enterprise gas pipeline, to flare. OXY makes every effort to control and minimize emissions as much as possible. The only actions that Oxy can take and handle that is within its control, is to keep continually communicate with Enterprise personnel during these types of situations.

Operator:

<u>District I</u> 1625 N. French Dr., Hobbs, NM 88240 Phone:(575) 393-6161 Fax:(575) 393-0720 District II

811 S. First St., Artesia, NM 88210 Phone:(575) 748-1283 Fax:(575) 748-9720 District III

1000 Rio Brazos Rd., Aztec, NM 87410 Phone:(505) 334-6178 Fax:(505) 334-6170

1220 S. St Francis Dr., Santa Fe, NM 87505 Phone:(505) 476-3470 Fax:(505) 476-3462

OXY USA INC

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. **Santa Fe, NM 87505**

QUESTIONS

Action 47834

QUESTIONS

OGRID:

16696

P.O. Box 4294 Houston, TX 772104294	Action Number: 47834		
Housion, TX TT2104234	Action Type:		
	[C-129] Venting and/or Flaring (C-129)		
QUESTIONS	•		
Prerequisites			
Any messages presented in this section, will prevent submission of this application. Please resolve	re these issues before continuing with the rest of the questions.		
Incident Well	[30-015-44507] CORRAL FLY 02 01 STATE #021H		
Incident Facility	Not answered.		
Determination of Reporting Requirements			
Answer all questions that apply. The Reason(s) statements are calculated based on your answers	and may provide addional guidance.		
Was or is this venting and/or flaring caused by an emergency or malfunction	Yes		
Did or will this venting and/or flaring last eight hours or more cumulatively within any 24-hour period from a single event	No		
Is this considered a submission for a venting and/or flaring event	Yes, major venting and/or flaring of natural gas.		
As a second of the second of t			
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during	y venting and/or flaring that is or may be a major or minor release under 19.15.29.7 NMAC.		
Was there or will there be at least 50 MCF of natural gas vented and/or flared during this event	Yes		
Did this venting and/or flaring result in the release of ANY liquids (not fully and/or			
completely flared) that reached (or has a chance of reaching) the ground, a	No		
surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water			
Was the venting and/or flaring within an incorporated municipal boundary or			
withing 300 feet from an occupied permanent residence, school, hospital,	No		
institution or church in existence			
Equipment Involved			
Primary Equipment Involved	Other (Specify)		
Additional details for Equipment Involved. Please specify	Emergency Flare > Downstream Activity > Enterprise > ETC		
Representative Compositional Analysis of Vented or Flared Natural Gas			
Please provide the mole percent for the percentage questions in this group.			
Methane (CH4) percentage	76		
Nitrogen (N2) percentage, if greater than one percent	1		
Hydrogen Sulfide (H2S) PPM, rounded up	0		
Carbon Dioxide (C02) percentage, if greater than one percent	0		

Oxygen (02) percentage quality requirement	Not answered.				
Date(s) and Time(s)					
Date venting and/or flaring was discovered or commenced	08/28/2021				
Time venting and/or flaring was discovered or commenced	01:50 PM				
Time venting and/or flaring was terminated	05:30 PM				
Cumulative hours during this event	3				

0

Not answered.

Not answered.

Not answered.

Not answered.

Measured or Estimated Volume of Vented or Flared Natural Gas		
Natural Gas Vented (Mcf) Details	Not answered.	

Oxygen (02) percentage, if greater than one percent

Methane (CH4) percentage quality requirement

Hydrogen Sufide (H2S) PPM quality requirement

Carbon Dioxide (C02) percentage quality requirement

Nitrogen (N2) percentage quality requirement

lf you are venting and/or flaring because of Pipeline Specification, please provide the required specifications for each gas

Natural Gas Flared (Mcf) Details	Cause: Other Other (Specify) Natural Gas Flared Released: 996 Mcf Recovered: 0 Mcf Lost: 996 Mcf]		
Other Released Details	Not answered.		
Additional details for Measured or Estimated Volume(s). Please specify	Gas Flare Meter		
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.		

Venting or Flaring Resulting from Downstream Activity				
Was or is this venting and/or flaring a result of downstream activity Yes				
Was notification of downstream activity received by you or your operator	No			
Downstream OGRID that should have notified you or your operator	[713731] Enterprise Crude Pipeline LLC			
Date notified of downstream activity requiring this venting and/or flaring	Not answered.			
Time notified of downstream activity requiring this venting and/or flaring	Not answered.			

steps and Actions to Prevent Waste				
For this event, the operator could not have reasonably anticipated the current event and it was beyond the operator's control.	True			
Please explain reason for why this event was beyond your operator's control	See Justification Form>The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction or complete shut-in of a gas pipeline by a third-party pipeline operator, which impacted Oxy's ability to send gas to a third-party gas pipeline. This interruption, restriction or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices.			
Steps taken to limit the duration and magnitude of venting and/or flaring	See Justification Form> This facility is unmanned, except when Oxy production techs are gathering data daily or conducting daily walk-throughs to ensure that there are no problems, circumstances and/or assist other personnel on-site for maintenance purposes. In this case, the increased spike in Enterprise's pipeline pressure forced Oxy's upstream facility to route all its stranded gas to a flare, as it was not able to push all its gas into Enterprises' gas pipeline due to the restrictions of gas flow placed on the pipeline, caused by ETC's maintenance gas curtailment and their communication and programing issues with their pipeline sales control valve. On both occasions, Oxy production techs, immediately upon receiving high pressure line alarms, arrived at the facility and began inspecting the equipment and contacting Enterprise personnel to determine cause of the spike in the pipeline pressure.			
Corrective actions taken to eliminate the cause and reoccurrence of venting and/or flaring	See Justification Form > Oxy cannot take any corrective actions to eliminate the cause and potential reoccurrence of an Enterprise gas flow pipeline restriction or shut-in, as this control issue is downstream of Oxy's custody transfer point and out of Oxy's control to avoid, prevent from happening or reoccurring. Enterprise's downstream facilities and associated facilities and/or operators, such as ETC., may have issues which will reoccur from time to time and may trigger a spike in their gas line pressure, which in turn, directly impacts Oxy's ability to send gas to them. When Enterprise has downstream activity issues or greatly struggles to handle the volume of gas being sent to them by Oxy, Enterprise then restricts Oxy's ability to send gas, which then prompts Oxy to route all of its stranded gas not pushed into the Enterprise gas pipeline, to flare. OXY makes every effort to control and minimize emissions as much as possible. The only actions that Oxy can take and handle that is within its control, is to keep continually communicate with Enterprise personnel during these types of situations.			

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CONDITIONS

Action 47834

CONDITIONS

Operator:	OGRID:
OXY USA INC	16696
P.O. Box 4294	Action Number:
Houston, TX 772104294	47834
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
marialuna	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	9/12/2021