AKM Measurement Services, LLC
Carlsbad, New Mexico

AKM MEASUREMENT SERVICES,LLC. Natural Gas Analysis Report
GPA 2172-09/API 14.5 Report with GPA 2145-16 Physical Properties

	Sample Information
Sample Name	LOST TANK 18 FACILITY HP VRU 3
Technician	ANTHONY DOMINGUEZ
Analyzer Make & Model	INFICON MICRO GC
Last Calibration/Validation Date	12-15-2023
Meter Number	16427V
Air temperature	57
Flow Rate (MCF/Day)	492
Heat Tracing	HEATED HOSE & GASIFIER
Sample description/mtr name	LOST TANK 18 FACILITY HP VRU 3
Sampling Method	FILL & EMPTY
Operator	OCCIDENTAL PETROLEUM, OXY USA INC
State	NEW MEXICO
Region Name	PERMIAN_RESOURCES
Asset	NEW MEXICO
System	LOST TANK
FLOC	OP-DELNE-BT010
Sample Sub Type	CTB
Sample Name Type	METER
Vendor	AKM MEASUREMENT
Cylinder #	38947
Sampled by	SCOTT
Sample date	12-12-2023
Analyzed date	12-19-2023
Method Name	C9
Injection Date	2023-12-19 16:54:11
Report Date	2023-12-19 16:55:47
EZReporter Configuration File	1-16-2023 OXY GPA C9+ H2S #2.cfgx
Source Data File	53d6f6b5-4467-4841-89c9-4fae48334cc6
NGA Phys. Property Data Source	GPA Standard 2145-16 (FPS)
Data Source	INFICON Fusion Connector

Component Results

Component Name	Peak Area	Raw Amount	Response Factor	Norm Mole%	Gross HV (Dry) (BTU / Ideal cu.ft.)	Relative Gas Density (Dry)	GPM (Dry) (Gal. / 1000 cu.ft.)	
Nitrogen	4568.9	0.2600	0.00005691	0.2564	0.0	0.00248	0.028	
Methane	456273.6	33.2457	0.00007286	32.7797	331.8	0.18157	5.613	
CO2	30720.0	1.4627	0.00004761	1.4422	0.0	0.02191	0.249	
Ethane	576932.1	26.5931	0.00004609	26.2203	465.1	0.27222	7.082	
H2S	0.0	0.0000	0.00000000	0.0000	0.0	0.00000	0.000	
Propane	760744.0	24.9277	0.00003277	24.5783	619.8	0.37420	6.839	
iso-butane	300846.6	3.3273	0.00001106	3.2807	106.9	0.06584	1.084	
n-Butane	758257.0	8.3375	0.00001100	8.2207	268.8	0.16497	2.618	
iso-pentane	132666.7	1.2963	0.00000977	1.2781	51.3	0.03184	0.472	
n-Pentane	135071.5	1.2676	0.00000938	1.2499	50.2	0.03114	0.458	
hexanes	50692.0	0.4997	0.00000986	0.4927	23.5	0.01466	0.205	
heptanes	27428.0	0.1657	0.00000604	0.1633	9.0	0.00565	0.076	
octanes	6748.0	0.0362	0.00000537	0.0357	2.2	0.00141	0.018	
nonanes+	614.0	0.0020	0.00000326	0.0020	0.1	0.00009	0.001	
Total:		101.4216		100.0000	1928.9	1.16798	24.743	

Results Summary

Result	Dry	Sat.	
Total Un-Normalized Mole%	101.4216		
Pressure Base (psia)	14.730		
Temperature Base (Deg. F)	60.00		
Flowing Temperature (Deg. F)	114.3		

Result	Dry	Sat.
Flowing Pressure (psia)	102.1	
Gross Heating Value (BTU / Ideal cu.ft.)	1928.9	1895.3
Gross Heating Value (BTU / Real cu.ft.)	1948.6	1915.7
Relative Density (G), Real	1.1794	1.1705

Monitored Parameter Report

Parameter	Value	Lower Limit	Upper Limit	Status
Total un-normalized amount	101.4216	97.0000	103.0000	Pass

UPSET FLARING EVENT SPECIFIC JUSTIFICATIONS FORM

Facility: Lost Tank 18 CPF **Flare Date:** 01/21/2025

Duration of Event: 2 Hours 30 Minutes **MCF Flared:** 294

Start Time: 01:30 AM **End Time:** 04:00 AM

Cause: Emergency Flare > Equipment Malfunctions > Production Separator & Tester > Dump Stick

Method of Flared Gas Measurement: Gas Flare Meter

1. Reason why this event was beyond Operator's control:

The emissions were caused by the sudden, unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and maintenance practices. Internal Oxy procedures ensure that upon a sudden and unexpected flaring event, production techs are promptly notified and are instructed to assess the issue as soon as possible to take prompt corrective action and minimize emissions. In this situation, there were continuing dump stick issues that was causing it open on 1011 production separator and the tester due to the flowrate transmitter was showing an abnormal rate when it was gas, which in turn, caused the valve didn't shut itself close. During this time, the facility low pressure side was flaring and kept pressuring up as result of the equipment malfunction with the production separator and the tester, which then tripped the Hihi pressure on the VRT, and triggered a COC of the facility itself and a flaring event to occur. A review of the event indicated that the flare valve didn't open due to it being frozen on the air supply because of the extreme freezing weather conditions and temperatures affecting the equipment. The air supply issue was resolved, and the production separator oil dump was placed into a level control to avoid potential issues. Oxy operators consistently monitor the facility for any deviations from normal operating parameters; however, this was an abnormal failure that would be difficult to predict. Prior to the flaring incident occurring, all OXY operations and equipment were operating at peak optimization levels. This flaring situation was beyond OXY's control, but Oxy took all possible measures to reduce emissions effectively during this circumstance. This flaring event's duration and volume result from several intermittent flares over 24 hours.

2. Steps Taken to limit duration and magnitude of venting or flaring:

It is OXY's policy to route all stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, that is beyond Oxy's control to avoid, prevent or foresee, to minimize emissions as much as possible as part of the overall steps taken to limit duration and magnitude of flaring. The flare at this facility has a 98% combustion efficiency to lessen emissions as much as possible. In this situation, there were continuing dump stick issues that was causing it open on 1011 production separator and the tester due to the flowrate transmitter was showing an abnormal rate when it was gas, which in turn, caused the valve didn't shut itself close. During this time, the facility low pressure side was flaring and kept pressuring up as result of the equipment malfunction with the production separator and the tester, which then tripped the Hihi pressure on the VRT, and triggered a COC of the facility itself and a flaring event to occur. A review of the event indicated that the flare valve didn't open due to it being frozen on the air supply because of the extreme freezing weather conditions and temperatures affecting the

equipment. The air supply issue was resolved, and the production separator oil dump was placed into a level control to avoid potential issues. Steps were immediately taken to reduce and mitigate the volume of gas being sent to flare by choking back several wells and reduce the amount of gas being sent to the flare. Prior to the flaring incident occurring, all OXY operations and equipment were operating at peak optimization levels. This flaring situation was beyond OXY's control, but Oxy took all possible measures to reduce emissions effectively during this circumstance.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

Oxy's ability to take corrective action to prevent and address malfunctions in this type of circumstance is limited. Despite proper design and operation of the production separator and testers, unexpected mechanical or technical issues can arise without warning and are often unforeseeable, leading to unforeseen equipment malfunctions, especially during extreme freezing weather conditions and temperatures.

Sante Fe Main Office
Phone: (505) 476-3441

General Information
Phone: (505) 629-6116

Online Phone Directory
https://www.emnrd.nm.gov/ocd/contact-us

State of New Mexico
Energy, Minerals and Natural Resources
Oil Conservation Division
1220 S. St Francis Dr.
Santa Fe, NM 87505

DEFINITIONS

Operator: OXY USA INC P.O. Box 4294 Houston, TX 772104294	OGRID: 16696
	Action Number: 428890
	Action Type: [C-129] Venting and/or Flaring (C-129)

DEFINITIONS

For the sake of brevity and completeness, please allow for the following in all groups of questions and for the rest of this application:

- this application's operator, hereinafter "this operator";
- venting and/or flaring, hereinafter "vent or flare";
- any notification or report(s) of the C-129 form family, hereinafter "any C-129 forms";
- the statements in (and/or attached to) this, hereinafter "the statements in this";
- and the past tense will be used in lieu of mixed past/present tense questions and statements.

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QUESTIONS

Action 428890

QUESTIONS

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	Action Number: 428890
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Prerequisites	
Any messages presented in this section, will prevent submission of this application. Please resolve these issues before continuing with the rest of the questions.	
Incident Well	*Unavailable.*
Incident Facility	**[fAPP2226965761] Lost Tank 18 CPF**

Determination of Reporting Requirements	
Answer all questions that apply. The Reason(s) statements are calculated based on your answers and may provide addional guidance.	
Was this vent or flare caused by an emergency or malfunction	Yes
Did this vent or flare last eight hours or more cumulatively within any 24-hour period from a single event	No
Is this considered a submission for a vent or flare event	**Yes, minor venting and/or flaring of natural gas.**
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during venting and/or flaring that is or may be a major or minor release under 19.15.29.7 NMAC.	
Was there **at least 50 MCF** of natural gas vented and/or flared during this event	Yes
Did this vent or flare result in the release of **ANY** liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No
Was the vent or flare within an incorporated municipal boundary or withing 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	No

Equipment Involved	
Primary Equipment Involved	Other (Specify)
Additional details for Equipment Involved. Please specify	Emergency Flare > Equipment Malfunctions > Production Separator & Tester > Dump Stick

Representative Compositional Analysis of Vented or Flared Natural Gas	
Please provide the mole percent for the percentage questions in this group.	
Methane (CH4) percentage	33
Nitrogen (N2) percentage, if greater than one percent	0
Hydrogen Sulfide (H2S) PPM, rounded up	0
Carbon Dioxide (C02) percentage, if greater than one percent	1
Oxygen (02) percentage, if greater than one percent	0
If you are venting and/or flaring because of Pipeline Specification, please provide the required specifications for each gas.	
Methane (CH4) percentage quality requirement	*Not answered.*
Nitrogen (N2) percentage quality requirement	*Not answered.*
Hydrogen Sufide (H2S) PPM quality requirement	*Not answered.*
Carbon Dioxide (C02) percentage quality requirement	*Not answered.*
Oxygen (02) percentage quality requirement	*Not answered.*

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QUESTIONS (continued)

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	Action Number: 428890
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Date(s) and Time(s)	
Date vent or flare was discovered or commenced	01/21/2025
Time vent or flare was discovered or commenced	01:30 AM
Time vent or flare was terminated	04:00 AM
Cumulative hours during this event	3

Measured or Estimated Volume of Vented or Flared Natural Gas	
Natural Gas Vented (Mcf) Details	*Not answered.*
Natural Gas Flared (Mcf) Details	Cause: Other | Other (Specify) | Natural Gas Flared | Released: 294 Mcf | Recovered: 0 Mcf | Lost: 294 Mcf.
Other Released Details	*Not answered.*
Additional details for Measured or Estimated Volume(s). Please specify	Gas Flare Meter
Is this a gas only submission (i.e. only significant Mcf values reported)	**Yes, according to supplied volumes this appears to be a "gas only" report.**

Venting or Flaring Resulting from Downstream Activity	
Was this vent or flare a result of downstream activity	No
Was notification of downstream activity received by this operator	*Not answered.*
Downstream OGRID that should have notified this operator	*Not answered.*
Date notified of downstream activity requiring this vent or flare	*Not answered.*
Time notified of downstream activity requiring this vent or flare	*Not answered.*

Steps and Actions to Prevent Waste	
For this event, this operator could not have reasonably anticipated the current event and it was beyond this operator's control.	True
Please explain reason for why this event was beyond this operator's control	The emissions were caused by the sudden, unavoidable breakdown of equipment or process that was beyond the owner/operator's control and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and maintenance practices. Internal Oxy procedures ensure that upon a sudden and unexpected flaring event, production techs are promptly notified and are instructed to assess the issue as soon as possible to take prompt corrective action and minimize emissions. In this situation, there were continuing dump stick issues that was causing it open on 1011 production separator and the tester due to the flowrate transmitter was showing an abnormal rate when it was gas, which in turn, caused the valve didn't shut itself close. During this time, the facility low pressure side was flaring and kept pressuring up as result of the equipment malfunction with the production separator and the tester, which then tripped the Hihi pressure on the VRT, and triggered a COC of the facility itself and a flaring event to occur. A review of the event indicated that the flare valve didn't open due to it being frozen on the air supply because of the extreme freezing weather conditions and temperatures affecting the equipment. The air supply issue was resolved, and the production separator oil dump was placed into a level control to avoid potential issues. Oxy operators consistently monitor the facility for any deviations from normal operating parameters; however, this was an abnormal failure that would be difficult to predict. Prior to the flaring incident occurring, all OXY operations and equipment were operating at peak optimization levels. This flaring situation was beyond OXY's control, but Oxy took all possible measures to reduce emissions effectively during this circumstance. This flaring event's duration and

	volume result from several intermittent flares over 24 hours.
Steps taken to limit the duration and magnitude of vent or flare	It is OXY's policy to route all stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, that is beyond Oxy's control to avoid, prevent or foresee, to minimize emissions as much as possible as part of the overall steps taken to limit duration and magnitude of flaring. The flare at this facility has a 98% combustion efficiency to lessen emissions as much as possible. In this situation, there were continuing dump stick issues that was causing it open on 1011 production separator and the tester due to the flowrate transmitter was showing an abnormal rate when it was gas, which in turn, caused the valve didn't shut itself close. During this time, the facility low pressure side was flaring and kept pressuring up as result of the equipment malfunction with the production separator and the tester, which then tripped the Hihi pressure on the VRT, and triggered a COC of the facility itself and a flaring event to occur. A review of the event indicated that the flare valve didn't open due to it being frozen on the air supply because of the extreme freezing weather conditions and temperatures affecting the equipment. The air supply issue was resolved, and the production separator oil dump was placed into a level control to avoid potential issues. Steps were immediately taken to reduce and mitigate the volume of gas being sent to flare by choking back several wells and reduce the amount of gas being sent to the flare. Prior to the flaring incident occurring, all OXY operations and equipment were operating at peak optimization levels. This flaring situation was beyond OXY's control, but Oxy took all possible measures to reduce emissions effectively during this circumstance.
Corrective actions taken to eliminate the cause and reoccurrence of vent or flare	Oxy's ability to take corrective action to prevent and address malfunctions in this type of circumstance is limited. Despite proper design and operation of the production separator and testers, unexpected mechanical or technical issues can arise without warning and are often unforeseeable, leading to unforeseen equipment malfunctions, especially during extreme freezing weather conditions and temperatures.

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ACKNOWLEDGMENTS

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	Action Number: 428890
	Action Type: [C-129] Venting and/or Flaring (C-129)

ACKNOWLEDGMENTS

☑	I acknowledge that I am authorized to submit a *Venting and/or Flaring* (C-129) report on behalf of this operator and understand that this report can be **a complete** C-129 submission per 19.15.27.8 and 19.15.28.8 NMAC.
☑	I acknowledge that upon submitting this application, I will be creating a new incident file (assigned to this operator) to track any C-129 forms, pursuant to 19.15.27.7 and 19.15.28.8 NMAC and understand that this submission meets the notification requirements of Paragraph (1) of Subsection G and F respectively.
☑	I hereby certify the statements in this report are true and correct to the best of my knowledge and acknowledge that any false statement may be subject to civil and criminal penalties under the Oil and Gas Act.
☑	I acknowledge that the acceptance of any C-129 forms by the OCD does not relieve this operator of liability should their operations have failed to adequately investigate, report, and remediate contamination that poses a threat to groundwater, surface water, human health, or the environment.
☑	I acknowledge that OCD acceptance of any C-129 forms does not relieve this operator of responsibility for compliance with any other applicable federal, state, or local laws and/or regulations.

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CONDITIONS

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	Action Number: 428890
	Action Type: [C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
shelbyschoepf	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	2/5/2025