STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

OIL CONSERVATION DIVISION

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Form C-122
Revised 10-1-78

C/SF
C-122

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

RECEIVED
MAY - 7 1982
O. C. D.
ARTESIA, OFFICE

Type Test: [x] Initial [ ] Annual [ ] Special				Test Date: 3-12-82	
Company: Yates Petroleum Corporation		Connection: Transwestern Pipeline Company			
Pool: Pecos SLope Abo		Formation: Abo		Unit: LG-250	
Completion Date: 12-31-81	Total Depth: 4150'	Plug Back TD: 4087'	Elevation: 3838' KB, 3932' GR	Farm or Lease Name: Margaret RQ State	
Csg. Size: 4-1/2" / Wt.: 9.5# / d: 4.090" / Set At: 4150'		Perforations: From 3601' To 3750'		Well No.: 1	
Tbg. Size: 2-3/8" / Wt.: 4.7# / d: 1.995" / Set At: 3658'		Perforations: From - To -		Unit: K / Sec.: 36 / Twp.: 4S / Rge.: 24E	
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single		Packer Set At: None		County: Chaves	
Producing Thru: Tubing	Reservoir Temp. °F: 93° @ 4147	Mean Annual Temp. °F: 60	Baro. Press. – P_a: 13.2	State: New Mexico	

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
3658	3658	0.668	0.79	5.73	0	---	2"	Flange

NO.	FLOW DATA: Prover Line Size x Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	TUBING DATA: Press. p.s.i.g.	Temp. °F	CASING DATA: Press. p.s.i.g.	Temp. °F	Duration of Flow
SI					998				days
1.	2.067 x 1.000	230	10	54	912	64			24 hrs
2.	2.067 x 1.000	230	24	54	850	64			24 hrs
3.	2.067 x 1.000	375	36	63	790	66			24 hrs
4.	2.067 x 1.000	375	75	63	747	66			24 hrs
5.									

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	4.946	49.32	243.2	1.006	1.224	1.024	307
2.	4.946	76.40	243.2	1.006	1.225	1.024	476
3	4.946	118.22	388.2	0.9971	1.224	1.037	740
4.	4.946	170.63	388.2	0.9971	1.224	1.037	1068
5							

NO.	P_t	Temp. °R	T_r	Z
1	0.367	514	1.412	0.954
2.	0.367	514	1.412	0.954
3.	0.586	523	1.437	0.930
4.	0.586	523	1.437	0.930
5				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas 0.668 XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX
Critical Pressure 662 P.S.I.A. _____ P.S.I.A.
Critical Temperature 364 R _____ R

P_c 1011.2 P_c^2 1022.5

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1	837.6		838.8	183.7
2	745.1		748.0	274.5
3	645.1		652.2	370.3
4	577.9		592.8	429.7
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 2.246$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 3.217$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 3,300$

Absolute Open Flow 3,300 Mcfd @ 15.025 | Angle of Slope θ _____ | Slope, n 1.444

Remarks: Static pressures by Bennett Wireline, flowing pressures by DWT calculations.
Worksheet C-122D attached

Approved By Division	Conducted By:	Calculated By:	Checked By:
	David Weaver	Albert R. Stall	