Submit in duplicate to appropriate district office
See Rule 401 & Rule 1122

State of New Mexico
Energy, Minerals and Natural Resources Department

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Form C-122
Revised 4-1-91

OIL CONSERVATION DIVISION

P.O. Box 2088
Santa Fe, New Mexico 87504-2088

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator: Union Oil Company of California						Lease or Unit Name: CRAWFORD 27			
Type Test: [X] Initial [ ] Annual [ ] Special						Test Date: 4-24-92		Well No.: 3	
Completion Date: 4-24-92		Total Depth: 11,392'		Plug Back TD: 10471		Elevation: 3315' GR		Unit Ltr. - Sec. - TWP - Rge.: L 27 24S 26E	
Csg. Size: 5½	Wt.: 17	d:	Set At: 10,800'	Perforations: From: 10108	To: 10126			County: Eddy	
Tbg. Size: 2 3/8	Wt.: 4.7	d: 1.995	Set At: 10,017'	Perforations: From:	To:			Pool: White City Pennsylvanian Gas	
Type Well - Single - Bradenhead - G.G. or G.O. Multiple: single				Packer Set At: 10,017'				Formation: Strawn	
Producing Thru: TBG	Reservoir Temp. °F: 175 @ 10117'		Mean Annual Temp. °F: 60	Baro. Press - P_a: 13.2				Connection: Will connect 5-2-92	
L: *10117	H: 10117	Gg: .652	% CO_2: .34	% N_2: .70	% H_2S:	Prover:		Meter Run: 3.826	Taps: FLG

FLOW DATA / TUBING DATA / CASING DATA

NO.	Prover Line Size X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Tubing Press. p.s.i.g.	Tubing Temp. °F	Casing Press. p.s.i.g.	Casing Temp. °F	Duration of Flow
SI					4850		Pkr		72 hr.
1.	3 X 1.000	600	10.00	74	4550		"		1 hr.
2.	3 X 1.000	600	24.00	74	4250		"		1 hr.
3.	3 X 1.000	600	54.00	70	3610		"		1 hr.
4.	3 X 1.000	600	22.00	70	2610		"		1 hr.
5.									

RATE OF FLOW CALCULATIONS

NO.	COEFFICIENT (24 HOUR)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg.	Super Compress. Factor, F pv.	Rate of Flow Q, Mcfd
1.	4.758	78.31	613.2	.9868	1.238	1.062	483
2.	4.758	121.31	613.2	.9868	1.238	1.062	749
3.	4.758	181.97	613.2	.9905	1.238	1.062	1128
4.	10.88	116.15	613.2	.9905	1.238	1.062	1646
5.							

NO.	P_r	Temp. °R	T_r	Z
1.	.91	534	1.42	.886
2.	.91	534	1.42	.886
3.	.91	530	1.41	.886
4.	.91	530	1.41	.886
5.				

Gas Liquid Hydrocarbon Ratio: 55.6 Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons: 54.0 Deg.
Specific Gravity Separator Gas: .652 XXXXXXXXX
Specific Gravity Flowing Fluid: XXXXX
Critical Pressure: 670 P.S.I.A. P.S.I.A.
Critical Temperature: 375 R R

P_c 4856.0 P_c^2 23580.7

NO.	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1.		4663.8	21751.0	1829.7
2.		4349.7	18919.9	4660.8
3.		3707.9	13748.5	9832.2
4.		2679.5	7179.7	16401.0
5.				

1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1/438$

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.256$

$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 2.067$

Absolute Open Flow: 2,067 Mcfd @ 15.025 | Angle of Slope θ: 57.9 | Slope, n: .6268

Remarks: *=BHP INSTRUMENT SET @ THIS DEPTH
**=KNOWN BHPS CLACULATED BACK TO SURFACE WELL MADE 3.0 BBLS 54.0 CONDENSATE DURING TEST

Approved By Division	Conducted By:	Calculated By:	Checked By:
	PRO WELL TESTERS	BM	David Krueger/UNOCAL DBK