NEW MEXICO OIL CONSERVATION COMMSSION

# MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

C-122
9-1-65

| | | | | | |
|---|---|---|---|---|---|
| Type Test: [X] Initial [ ] Annual [ ] Special | | | | Test Date: 6-2-67 | |
| Company: Tenneco Oil Co. | | Connection | | | |
| Pool: Blanco Mesa Verde | | Formation: Mesa Verde | | Unit | |
| Completion Date | Total Depth | Plug Back TD: 7445 | | Elevation: 6728 | Farm or Lease Name: Dawson "A" |
| Csg. Size: 4.5 / Wt. / d / Set At: 7464 | | Perforations: From 5138 To 5365 | | | Well No.: 1 |
| Tbg. Size: 2.375 / Wt. / d / Set At: 7250 | | Perforations: From To | | | Unit: N / Sec.: 4 / Twp.: 27 / Rge.: 8 |
| Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Dual Gas | | | Packer Set At: 7250 | | County: San Juan |
| Producing Thru | Reservoir Temp. °F @ | Mean Annual Temp. °F | Baro. Press. – $P_a$: 12.0 | | State: New Mexico |

| L | H | Gg | % $CO_2$ | % $N_2$ | % $H_2S$ | Prover | Meter Run | Taps |
|---|---|---|---|---|---|---|---|---|
| | | | | | | | | |

## FLOW DATA / TUBING DATA / CASING DATA

| NO. | Prover Line Size | X | Orifice Size | Press. p.s.i.g. | Diff. $h_w$ | Temp. °F | Tubing Press. p.s.i.g. | Tubing Temp. °F | Casing Press. p.s.i.g. | Casing Temp. °F | Duration of Flow |
|---|---|---|---|---|---|---|---|---|---|---|---|
| SI | | | | | | | Pkr. | | 929 | | |
| 1. | 2 x 3/4 | | | | | | Pkr. | | 348 | 60 | 3 hrs |
| 2. | | | | | | | | | | | |
| 3. | | | | | | | | | | | |
| 4. | | | | | | | | | | | |
| 5. | | | | | | | | | | | |

## RATE OF FLOW CALCULATIONS

| NO. | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure $P_m$ | Flow Temp. Factor Ft. | Gravity Factor Fg | Super Compress. Factor, Fpv | Rate of Flow Q, Mcfd |
|---|---|---|---|---|---|---|---|
| 1 | 12.3650 | | 360 | 1.000 | .9608 | 1.037 | 4439 |
| 2. | | | | | | | |
| 3. | | | | | | | |
| 4. | | | | | | | |
| 5. | | | | | | | |

RECEIVED
AUG 22 1967
OIL CON. COM.
DIST. 3

| NO. | $P_t$ | $P_t^2$ | Z |
|---|---|---|---|
| 1. | | | |
| 2. | | | |
| 3. | | | |
| 4. | | | |
| 5. | | | |

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

$P_c$ 941 $P_c^2$ 885481

| NO | $P_t^2$ | $P_w$ | $P_w^2$ | $P_c^2 - P_w^2$ |
|---|---|---|---|---|
| 1 | 129600 | | 192755 | 692726 |
| 2 | | | | |
| 3 | | | | |
| 4 | | | | |
| 5 | | | | |

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.2783$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.2022$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 5337$

Absolute Open Flow 5337 Mcfd @ 15.025 | Angle of Slope θ _____ | Slope, n .75

Remarks: _____

| Approved By Commission: | Conducted By: | Calculated By: | Checked By: |
|---|---|---|---|
| | | Neil Teftteller | |