# ILLEGIBLE

NEW MEXICO OIL CONSERVATION COMMSSION

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised

RECEIVED
NOV 15 1968
OIL CON. COM
DIST 3

| | | | | | |
|---|---|---|---|---|---|
| Type Test: ☒ Initial ☐ Annual ☐ Special | | | Test Date: 11-1-68 | | |
| Company: Moore Oil and Gas | Connection: El Paso Natural Gas | | | | |
| Pool: Basin | Formation: Dakota | | | Unit | |
| Completion Date: 10-24-68 | Total Depth: 7775 | Plug Back TD: 7771 | Elevation: 6210 Gr | Farm or Lease Name: Hale | |
| Csg. Size: 4½ | Wt.: 10.5 | d: 4.052 | Set At: 7765 | Perforations: From 7568 To 7690 | Well No.: 4 |
| Tbg. Size: 2-3/8 | Wt.: 4.7 | d: | Set At: 7667 | Perforations: From open ended To | Unit: H / Sec.: 34 / Twp.: 31N / Rge.: 8W |
| Type Well – Single – Bradenhead – G.G. or G.O. Multiple: GG Dual | | | Packer Set At: 7667 | County: San Juan | |
| Producing Thru: Tubing | Reservoir Temp. °F: e | Mean Annual Temp. °F | Baro. Press. – $P_a$ | State: New Mexico | |

| L | H | Gg | % $CO_2$ | % $N_2$ | % $H_2S$ | Prover | Meter Run | Taps |
|---|---|---|---|---|---|---|---|---|
| | | | | | | | | |

| | FLOW DATA | | | | TUBING DATA | | CASING DATA | | |
|---|---|---|---|---|---|---|---|---|---|
| NO. | Prover Line Size | X Orifice Size | Press. p.s.i.g. | Diff. $h_w$ | Temp. °F | Press. p.s.i.g. | Temp. °F | Press. p.s.i.g. | Temp. °F | Duration of Flow |
| SI | 2 | 3/4 | | | | 2005 | | 684 | | |
| 1. | | | | | | 1703 | | 685 | | 3 hr |
| 2. | | | | | | | | | | |
| 3. | | | | | | | | | | |
| 4. | | | | | | | | | | |
| 5. | | | | | | | | | | |

RATE OF FLOW CALCULATIONS

| NO. | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure $P_m$ | Flow Temp. Factor Ft | Gravity Factor Fg | Super Compress. Factor, Fpv | Rate of Flow Q, Mcfd |
|---|---|---|---|---|---|---|---|
| 1 | 12.365 | | 1708 | 1.000 | .9258 | 1.014 | 1495 |
| 2 | | | | | | | |
| 3 | | | | | | | |
| 4 | | | | | | | |
| 5 | | | | | | | |

| NO. | $P_t$ | Temp. °R | $T_r$ | Z |
|---|---|---|---|---|
| 1 | | | | |
| 2 | | | | |
| 3 | | | | |
| 4 | | | | |
| 5 | | | | |

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.

A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.

Specific Gravity Separator Gas _____ XXXXXXXXX

Specific Gravity Flowing Fluid XXXXX

Critical Pressure _____ P.S.I.A. _____ P.S.I.A.

Critical Temperature _____ R _____

$P_c^2$ = _____ $\frac{P_c^2}{P_c^2 - P_w^2}$ = 1.0552 (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 1.0403

$\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 1556

Absolute Open Flow 1555 Mcfd @ 15.025 Angle of Slope θ _____ Slope, n _____

Remarks: _____

| Approved By Commission: | Conducted By: | Calculated By: | Checked By: |
|---|---|---|---|
| | | | |