## NEW MEXICO OIL CONSERVATION COMMISSION

Form C-122
Revised 12-1-55

## MULTI-POINT BACK PRESSURE TEST FOR GAS WELLS

Size   psig   hw   OF.   psig	Pool	_Underlane	rted		For	mation	Pieta	gred Clif	¥s.	_County	Sea 3	<u>luan</u>	
Parchaser   Sec. 90   Pap. 111   Rge. 112   Purchaser   Section   Page	Init	ial 🗶	A	nnuzl_			Spec	ial		_Date of	Test	mgust	27, 1957
Perf. To To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 Set at 185 Perf. To Subing 1 Wt. 175 I.D. 1.00 I.D. 185	Comp	any Artee	011 & Co	Comp	my _		lease 🚇	reater		Wel	1 No	6	
Tubing   Wt.   To   I.D.   Set at   Set   Perf.   To   Set	Unit	<b>K</b> S	ec. <b>20</b>	_Twp	3711	Rge	. 114	Purcl	naser_	uthern Un	Lon Car	Cong	any
Pressure	Casi	ng 7 5/8 W	t	I.D.	7.0	Set	at_ <b>\7</b>	Pe:	rf	2570	To	1606	
Pressure	ľubi	ng <b>1</b> W	t1.70	I.D.	1.0	Set	at_ <b>86</b>	Per	rf	2658	То	1680	
Type Well   A.   A.   A.   A.   A.   A.   A.													12psia
Type Taps    Choke   C													
Cested Through (December 1997)  Cested Through (Choke) (Market)  Flow Data  Flow Data  Tubing Data  Condition (Orifice)  Size (Choke) (Press.) Diff. Temp. Press. Temp. Press. Temp. Ouration of Flow Size (Choke)  Size (Choke) (Press.) Diff. Temp. Press. Temp. Press. Temp. Of Flow Orifice)  Size (Choke) (Press.) Diff. Temp. Press. Temp. Press. Temp. Orifice  Flow Calculations  Flow Calculations  Flow Temp. Flow Temp. Flow Temp. Factor	Date	of Complet	ion:	set 0.	1957	_Packer	Baker	Sing	gle-Brade Reservo	enhead-G. oir Temp	G. or (	3.0. I	Dual
Flow Data    Tubing Data   Casing Data   Casing Data													
Continue   Confice   Press   Diff   Temp.   Press   Temp.   Press   Temp.   Duration of Flow   Size   Size   psig   h_w   OF.   psig	<b>Test</b>	ed Through	(Prover	(Cho	<u>ke) (</u>	Votes)				Type Tap	s		
Control   Cont		/p				Dice	m-					<del></del>	Dunation
FLOW CALCULATIONS  FLOW CALCULATIONS  FACTOR	No.		(Orific	۱ ۱			-	:			1		of Flow
FLOW CALCULATIONS  FLOW CALCULATIONS  Coefficient  (24-Hour)    (25-WCFPD    (24-Hour)    (24-Ho		Size	Size	p	sig	h <sub>w</sub>	°F.					+	
FLOW CALCULATIONS  Coefficient  (0. Coefficient (24-Hour)	$\frac{SI}{1.}$		0.79	9									
FLOW CALCULATIONS  Coefficient  (24-Hour)  (	2.												
FLOW CALCULATIONS  Coefficient Pressure Flow Temp. Gravity Compress. Rate of Flow Q-MCFPD Psia Ft Fg Factor	3.			-								+	
Coefficient  (24-Hour)	5.											工	
Coefficient  (24-Hour)						ī	יו מש כאדו	CIII A TTON	3				
C24-Hour)   V   hwpf   psia   Ft   Fg   Fpv   @ 15.025 psia	Т	Coeffici	ent	<del> </del>	Pre			Temp.	Gravity				
PRESSURE CALCUIATIONS  Is Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	No.	(2) Have	~)   _ /	<u> </u>		030	Fac	tor	Factor	Facto			
PRESSURE CALCULATIONS  as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	_		· / V	"wPf									
PRESSURE CALCULATIONS  as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	2.	19.3650							0.9000	1.0	<del>3</del> 7	<del></del>	/ <b></b>
PRESSURE CALCULATIONS  as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	3.								· · · · · · · · · · · · · · · · · · ·				
PRESSURE CALCULATIONS  as Liquid Hydrocarbon Ratio cf/bbl. Specific Gravity Separator Gas	5.		<del></del>		+								
avity of Liquid Hydrocarbons deg. Specific Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub> P <sub>C</sub> P <sub>C</sub> P <sub>C</sub> Gravity Flowing Fluid  P <sub>C</sub> P <sub>S</sub> P <sub>C</sub>	<u> </u>					PRI	ESSURE C	ALCULATIO	ONS				
(1-e <sup>-8</sup> )  P <sub>C</sub> The P <sub>C</sub> P <sub>C</sub> The P <sub>C</sub> T													
To. Pw Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Pc Pc Pc Pw Pc Pc Pc Pc Pw Pc		-					deg.		Speci	liic Gravi	ty Fio	_	
Pt (psia)  Pt Fc (FcQ) (FcQ) Pw2  Pt (psia)  Pt Fc (I-e-s)  Pw2  Pc-Pw Cal.  Pw Fc  Pw Fc  Cal.  Pw Fc  Pw	3			(1-0					- c		c		
Desolute Potential: Mon MCFPD; n  COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS  COMPANY CO	No -l	$P_{\mathbf{w}}$	<sub>P</sub> 2	рQ		(F <sub>-</sub> Q) <sup>2</sup>	(F	-0)2	P. 2	P2-P2	C.	al.	P.,,
Absolute Potential: MO1 MCFPD; n  COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS  VITNESSED  COMPANY  COMPANY  COMPANY  COMPANY  COMPANY  COMPANY		Pt (psia)	^t	· c		(- C≪)	(i	_e-s)	- W-	- G - W	1		P <sub>C</sub>
Absolute Potential: MO1 MCFPD; n  COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS  VITNESSED  COMPANY  COMPANY  COMPANY  COMPANY  COMPANY  COMPANY	; <u> </u>								97.344	534.60	1		
Absolute Potential: MO1 MCFPD; n O. COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS ACCOMPANY COMPANY	3.												
Absolute Potential: MO1 MCFPD; n O. COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS ACCOMPANY COMPANY	<u>+</u> •												
COMPANY ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS COMPANY COMPA										<u> </u>			
ADDRESS AGENT and TITLE ORIGINAL SIGNED BY L. M. STEVENS PLOMPANY  OFFICIAL SIGNED BY L. M. STEVENS  OMPANY  OFFICIAL SIGNED BY L. M. STEVENS		ANT					MCFPD;	n	3.85		25.00	Market Market	
VITNESSED SEP 13 195/		77.00					Marico				Z	TIT	
COMPANY			ORIGINA	L SIGNEI	BY L.	M. STEVE	INS	Distric	t_Enginee	7	RL	MI	<b>n</b> /
REMARKS CON COM.											CED	1 3 19	57
							REM	ARKS		1	AU M	ON. C	OM.

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q = Actual rate of flow at end of flow period at W. H. working pressure (Pw). MCF/da. @ 15.025 psia and 600 F.
- $P_c$  72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- PwT Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- $h_{\mbox{\scriptsize W}}\mbox{\small I}$  Differential meter pressure, inches water.
- $F_g = Gravity$  correction factor.
- $F_t$  Flowing temperature correction factor.
- $F_{pv}$  Supercompressability factor.
- n I Slope of back pressure curve.

Note: If  $P_W$  cannot be taken because of manner of completion or condition of well, then  $P_W$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{t}$ .

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