NEW MEXICO OIL CONSERVATION COMMSSION

# MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

| | | | | | |
|---|---|---|---|---|---|
| Type Test: [XX] Initial [ ] Annual [ ] Special | | | Test Date: 2-2-80 | | |
| Company: Consolidated Oil & Gas, Inc. | | Connection: | | | |
| Pool: Basin Dakota | | Formation: Dakota | | Unit: | |
| Completion Date | Total Depth | Plug Back TD: 7066 | Elevation | Farm or Lease Name: Gross | |
| Csg. Size: 5 1/2 / Wt. / d / Set At: 7077 | | Perforations: From 6838 To 7064 | | Well No.: 1-M | |
| Tbg. Size: 1 1/2 / Wt. / d / Set At: 6901 | | Perforations: From To | | Unit: 1 / Sec.: 7 / Twp.: 31 / Rge.: 12 | |
| Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Dual Gas | | Packer Set At: 6740 | | County: San Juan | |
| Producing Thru: Tubing | Reservoir Temp. °F | Mean Annual Temp. °F | Baro. Press. – $P_a$: 12.0 | State: New Mexico | |
| L | H | Gg: .650 | % $CO_2$ | % $N_2$ | % $H_2S$ |
| Prover: 6" nipple | Meter Run | Taps | | | |

## FLOW DATA

| NO. | Prover Line Size X Orifice Size | Press. p.s.i.g. | Diff. $h_w$ | Temp. °F | TUBING DATA Press. p.s.i.g. | TUBING DATA Temp. °F | CASING DATA Press. p.s.i.g. | CASING DATA Temp. °F | Duration of Flow |
|---|---|---|---|---|---|---|---|---|---|
| SI | 15 days | | | | 1380 | | Pkr. | | |
| 1. | 2" X 3/4" | | | | 113 | 60 | Pkr. | | 3 hours |
| 2. | | | | | | | | | |
| 3. | | | | | | | | | |
| 4. | | | | | | | | | |
| 5. | | | | | | | | | |

## RATE OF FLOW CALCULATIONS

| NO. | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure $P_m$ | Flow Temp. Factor Ft. | Gravity Factor Fg | Super Compress. Factor, Fpv | Rate of Flow Q, Mcfd |
|---|---|---|---|---|---|---|---|
| 1 | 11.00 | | 125 | 1.000 | 1.240 | 1.012 | 1725 |
| 2 | | | | | | | |
| 3 | | | | | | | |
| 4 | | | | | | | |
| 5 | | | | | | | |

| NO. | $P_t$ | Temp. °R | $T_r$ | Z |
|---|---|---|---|---|
| 1. | | | | |
| 2. | | | | |
| 3. | | | | |
| 4. | | | | |
| 5. | | | | |

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas _____ XXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure _____ P.S.I.A. _____ P.S.I.A.
Critical Temperature _____ R _____ R

$P_c$ 1392 $P_c^2$ 1937664

| NO | $P_t^2$ | $P_w$ | $P_w^2$ | $P_c^2 - P_w^2$ |
|---|---|---|---|---|
| 1 | 15625 | | 252523 | 1685141 |
| 2 | | | | |
| 3 | | | | |
| 4 | | | | |
| 5 | | | | |

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.1499$

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.1105$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1916$

FEB 27 1980
OIL CON. COM.
DIST. 3

Absolute Open Flow 1916 Mcfd @ 15.025 Angle of Slope θ _____ Slope, n .75

Remarks: _____

| Approved By Commission: | Conducted By: | Calculated By: | Checked By: |
|---|---|---|---|
| | A. Hughes | Neil Tefteller | |