

Chandler Montgomery Occidental Petroleum 1502 W Commerce Dr. Certificate of Analysis

Number: 6030-20110087-001A

Artesia Laboratory 200 E Main St. Artesia, NM 88210 Phone 575-746-3481

Nov. 17, 2020

Carlsbad, NM 88220 Field: NMSW Station Name: **Corral Compressor Station 2 South** Station Number: N/A Sample Point: N/A Meter Number: County: Eddy Type of Sample: Spot-Cylinder Heat Trace Used: N/A Sampling Method: Fill and Purge Sampling Company:OXY

Sampled By: Jesus Escobedo Sample Of: Gas Spot Sample Date: 11/11/2020 01:09 Sample Conditions: 1265 psig Ambient: 49 °F 11/11/2020 01:09 Effective Date: GPA 2286 Method: Cylinder No: 1111-001162 Instrument: 6030_GC2 (Agilent GC-7890B) Last Inst. Cal.: 08/25/2020 8:12 AM Analyzed: 11/17/2020 12:40:16 by PGS

Analytical Data

Components	Un-normalized Mol %	Mol. %	Wt. %	GPM at 14.65 psia		
Hydrogen Sulfide	0.000	0.000	0.000		GPM TOTAL C2+	6.390
Nitrogen	1.332	1.320	1.675		GPM TOTAL C3+	3.359
Methane	76.899	76.201	55.381		GPM TOTAL iC5+	0.805
Carbon Dioxide	0.171	0.169	0.337			
Ethane	11.459	11.355	15.468	3.031		
Propane	5.781	5.728	11.443	1.575		
Iso-butane	0.846	0.838	2.207	0.274		
n-Butane	2.259	2.238	5.893	0.705		
Iso-pentane	0.642	0.636	2.079	0.232		
n-Pentane	0.766	0.759	2.481	0.275		
Hexanes Plus	0.763	0.756	3.036	0.298		
	100.918	100.000	100.000	6.390		
Calculated Physical P	Calculated Physical Properties		otal	C6+		
Relative Density Real C	Gas	0.76	649	3.0584		
Calculated Molecular W	Veight	22	.07	88.58		
Compressibility Factor		0.99	960			
GPA 2172 Calculation	1:					
Calculated Gross BTL	J per ft ³ @ 14.65 p	sia & 60°F				
Real Gas Dry BTU		13	308	4763		
Water Sat. Gas Base B		12	285	4680		
Ideal, Gross HV - Dry at 14.65 psia		130	-	4763.5		
Ideal, Gross HV - Wet		128	•••	0.000		
Net BTU Dry Gas - real			188			
Net BTU Wet Gas - rea	al gas	11	167			

Comments: H2S Field Content 0 ppm

Hydrocarbon Laboratory Manager

Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.



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Sampled By:Jesus EscobedoSample Of:GasSpotSample Date:11/11/2020 01:09Sample Conditions:1265 psigMethod:GPA 2286Cylinder No:1111-001162Analyzed:11/17/2020 13:21:28 by PGSSampling Company:OXY

Analytical Data

Components	Mol. %	Wt. %	GPM at 14.65 psia			
Hydrogen Sulfide	NIL	NIL		GPM TOTAL C2+	6.390	
Nitrogen	1.320	1.675		GPM TOTAL C3+	3.359	
Methane	76.201	55.381		GPM TOTAL iC5+	0.805	
Carbon Dioxide	0.169	0.337				
Ethane	11.355	15.468	3.031			
Propane	5.728	11.443	1.575			
Iso-Butane	0.838	2.207	0.274			
n-Butane	2.238	5.893	0.705			
Iso-Pentane	0.636	2.079	0.232			
n-Pentane	0.759	2.481	0.275			
Hexanes	0.374	1.443	0.152			
Heptanes Plus	0.382	1.593	0.146			
	100.000	100.000	6.390			
Calculated Physica	al Properties		Total	C7+		
Relative Density Re	al Gas		0.7649	3.1738		
Calculated Molecula	r Weight		22.07	91.92		
Compressibility Fact	tor		0.9960			
GPA 2172 Calculat	ion:					
Calculated Gross E	BTU per ft ³ @	2 14.65 psi	a & 60°F			
Real Gas Dry BTU			1308	4850		
Water Sat. Gas Bas	e BTU		1285	4766		
Ideal, Gross HV - Di	ry at 14.65 ps	sia	1302.9	4850.4		
Ideal, Gross HV - W			1280.1	NIL		
•		•				

Comments: H2S Field Content 0 ppm

Hydrocarbon Laboratory Manager

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Sampled By:Jesus EscobedoSample Of:GasSpotSample Date:11/11/2020 01:09Sample Conditions:1265 psigMethod:GPA 2286Cylinder No:1111-001162Analyzed:11/17/2020 13:21:28 by PGSSampling Company:OXY

Analytical Data						
Components	Mol. %	Wt. %	GPM at 14.65 psia			
Hydrogen Sulfide	NIL	NIL		GPM TOTAL C2+	6.390	
Nitrogen	1.320	1.675				
Methane	76.201	55.381				
Carbon Dioxide	0.169	0.337				
Ethane	11.355	15.468	3.031			
Propane	5.728	11.443	1.575			
Iso-Butane	0.838	2.207	0.274			
n-Butane	2.238	5.893	0.705			
Iso-Pentane	0.636	2.079	0.232			
n-Pentane	0.759	2.481	0.275			
i-Hexanes	0.229	0.880	0.092			
n-Hexane	0.145	0.563	0.060			
Benzene	0.036	0.125	0.010			
Cyclohexane	0.091	0.348	0.031			
i-Heptanes	0.135	0.566	0.054			
n-Heptane	0.027	0.125	0.013			
Toluene	0.015	0.065	0.005			
i-Octanes	0.065	0.307	0.029			
n-Octane	0.003	0.015	0.001			
Ethylbenzene	0.001	0.002	NIL			
Xylenes	0.003	0.010	0.001			
i-Nonanes	0.005	0.025	0.002			
n-Nonane	0.001	0.003	NIL			
i-Decanes	NIL	NIL	NIL			
n-Decane	NIL	0.001	NIL			
Undecanes	NIL	0.001	NIL			
Dodecanes	NIL	NIL	NIL			
Tridecanes	NIL	NIL	NIL			
Tetradecanes Plus	NIL	NIL	NIL			
	100.000	100.000	6.390			



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Sampled By:Jesus EscobedoSample Of:GasSpotSample Date:11/11/2020 01:09Sample Conditions:1265 psigMethod:GPA 2286Cylinder No:1111-001162Analyzed:11/17/2020 13:21:28 by PGSSampling Company:OXY

Calculated Physical Properties	Total
Calculated Molecular Weight	22.073
GPA 2172 Calculation:	
Calculated Gross BTU per ft ³ @ 14.65 p	sia & 60°F
Real Gas Dry BTU	1308.0
Water Sat. Gas Base BTU	1285.2
Relative Density Real Gas	0.7649
Compressibility Factor	0.9960
Comments: H2S Field Content 0 ppm	

Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.

Hydrocarbon Laboratory Manager

UPSET EVENT SPECIFIC JUSTIFICATIONS FORM

Facility: Corral 2S CS	Date: 08/19/2021
Duration of event: 30 minutes	MCF Flared: 58
Start Time: 03:30 PM	End Time: 04:00 PM
Cause: Compressor Malfunctions > Multi- Unit Shutdown	
Method of Flared Gas Measurement: Gas Flare Meter	

Well API Associated with Facility: 30-015-44507 Corral Fly 02 01 State #021H

Comments: This upset event was not caused by any wells associated with the facility. This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control, and did not stem from activity that could have been foreseen and avoided, and could not have been avoided or prevented by good design, operation, and preventative maintenance practices.

1. Reason why this event was beyond Operator's control:

This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control, and did not stem from activity that could have been foreseen and avoided, and could not have been avoided or prevented by good design, operation, and preventative maintenance practices. Internal OXY procedures ensure that upon gas compressor unit and/or multiple unit shutdown, due to malfunction and/or alarms, production techs are promptly notified, and are instructed to assess the issue as soon as possible in order to take prompt corrective action and minimize emissions.

In this case, Oxy production techs determined that it was an unexpected and reasonably unforeseeable malfunction of compressor units 1, 3 & 4 which automatically shut down on a fuel skid malfunction alarm at the Corral 2N compressor station. This event is out of OXY's control yet OXY made every effort to control and minimize emissions as much as possible. Though sudden and unexpected malfunctioning compressor issues occurred at the Corral 2N compressor station, OXY routed the overflow of stranded gas to flare at Corral 2S compressor station in an effort to mitigate emissions for this event as the flare at this location can accommodate a higher volume of gas and as a safety measure effort to protect equipment, environment, and personnel. This event could not have been foreseen, avoided or planned for as notwithstanding compressor engine design and operation, compressors are inherently dynamic and even the smallest alarms, false or true, can be sudden, reasonably unforeseeable and unexpected which can cause compression malfunctions to occur. This event is out of OXY's control yet, OXY made every effort to control and minimize emissions as much as possible.

2. Steps Taken to limit duration and magnitude of venting or flaring:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control, and did not stem from activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. Oxy engages in respectable and good facility operation practices while also maintaining its continuous facility equipment preventative maintenance program. Notwithstanding compressor engine design and operation, compressors are inherently dynamic and even the smallest alarms, false or true, can be sudden, reasonably unforeseeable and unexpected which can cause compression malfunctions to occur.

Internal OXY procedures ensure that upon gas compressor unit and/or multiple unit shutdown, due to malfunction and/or alarms, production techs are promptly notified, and are instructed to assess the issue as soon as possible in order to take prompt corrective action and minimize emissions. This facility is unmanned, except when Oxy production techs are gathering data daily or conducting daily walk-throughs to ensure that there are no problems, circumstances and/or assist other personnel on-site for maintenance purposes. In this case, Oxy production techs, who were on site at the time, determined that the cause of the malfunctions of USA gas compressor units 1, 3 & 4 were due to a fuel skid malfunction alarms, which occurred simultaneously. Oxy production techs quickly cleared the alarms, reset the panels, and restarted the compressors. All three compressor units were working as designed and operated normally prior to the sudden and without warning malfunctions. Flaring ceased. Though sudden and unexpected malfunctioning compressor issues occurred at the Corral 2N compressor station, OXY routed the overflow of stranded gas to flare at Corral 2S compressor station in an effort to mitigate emissions for this event as the flare at this location can accommodate a higher volume of gas and as a safety measure effort to protect equipment, environment, and personnel.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

Oxy is limited in the corrective actions available to them to eliminate the cause and potential reoccurrence of compressor malfunctions as notwithstanding compressor engine design and operation, compressors are inherently dynamic and even the smallest alarms, false or true, can be sudden, reasonably unforeseeable and unexpected which can cause compression malfunctions to occur, thereby, triggering the unit's sensors to automatically shut down the unit to avoid catastrophic damage to the internal engine components.

District I 1625 N. French Dr., Hobbs, NM 88240 Phone:(575) 393-6161 Fax:(575) 393-0720 District II

811 S. First St., Artesia, NM 88210 Phone:(575) 748-1283 Fax:(575) 748-9720

District III

1000 Rio Brazos Rd., Aztec, NM 87410 Phone:(505) 334-6178 Fax:(505) 334-6170

District IV 1220 S. St Francis Dr., Santa Fe, NM 87505 Phone: (505) 476-3470 Fax: (505) 476-3462

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

QUESTIONS

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Action 46466

QUESTIONS

Operator:	OGRID:	
OXY USA INC P.O. Box 4294	16696 Action Number:	
Houston, TX 772104294	46466	
	Action Type:	
	[C-129] Venting and/or Flaring (C-129)	
QUESTIONS		
Prerequisites		
Any messages presented in this section, will prevent submission of this application. Please resolve	these issues before continuing with the rest of the questions.	
Incident Well	[30-015-44507] CORRAL FLY 02 01 STATE #021H	
Incident Facility	Not answered.	
Determination of Reporting Requirements		
Answer all questions that apply. The Reason(s) statements are calculated based on your answers an	nd may provide addional guidance.	
Was or is this venting and/or flaring caused by an emergency or malfunction	Yes	
Did or will this venting and/or flaring last eight hours or more cumulatively within any 24-hour period from a single event	No	
Is this considered a submission for a notification of a major venting and/or flaring	Yes, minor venting and/or flaring of natural gas.	
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during v	enting and/or flaring that is or may be a major or minor release under 19.15.29.7 NMAC.	
Was there or will there be at least 50 MCF of natural gas vented and/or flared		
during this event	Yes	
Did this venting and/or flaring result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public	No	
health, the environment or fresh water		
Was the venting and/or flaring within an incorporated municipal boundary or withing 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	Νο	
	I	
Equipment Involved		
Primary Equipment Involved	Other (Specify)	
Additional details for Equipment Involved. Please specify	Emergency Flare > Compressor Malfunctions > Multi- Unit Shutdown	
Representative Compositional Analysis of Vented or Flared Natural Gas		
Please provide the mole percent for the percentage questions in this group.		
Methane (CH4) percentage	76	
Nitrogen (N2) percentage, if greater than one percent	1	
Hydrogen Sulfide (H2S) PPM, rounded up	0	
Carbon Dioxide (C02) percentage, if greater than one percent	0	
Oxygen (02) percentage, if greater than one percent	0	
If you are venting and/or flaring because of Pipeline Specification, please provide the required spec		
Methane (CH4) percentage quality requirement	Not answered.	
Nitrogen (N2) percentage quality requirement	Not answered.	
Hydrogen Sufide (H2S) PPM quality requirement	Not answered.	
Carbon Dioxide (C02) percentage quality requirement	Not answered.	
Oxygen (02) percentage quality requirement	Not answered.	
Date(s) and Time(s)		
Date venting and/or flaring was discovered or commenced	08/19/2021	
Time venting and/or flaring was discovered or commenced	03:30 PM	
Time venting and/or flaring was terminated	04:00 PM	
Cumulative hours during this event	0	
	1	

Measured or Estimated Volume of Vented or Flared Natural Gas

Natural Gas Vented (Mcf) Details

Received by OCD: 9/3/2021 8:58:17 PM

Natural Gas Flared (Mcf) Details	Cause: Other Other (Specify) Natural Gas Flared Released: 58 Mcf Recovered: 0 Mcf Lost: 58 Mcf]
Other Released Details	Not answered.
Additional details for Measured or Estimated Volume(s). Please specify	Gas Flare Meter
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.

Venting or Flaring Resulting from Downstream Activity				
Was or is this venting and/or flaring a result of downstream activity	No			
Date notified of downstream activity requiring this venting and/or flaring	Not answered.			
Time notified of downstream activity requiring this venting and/or flaring	Not answered.			

Steps and Actions to Prevent Waste				
For this event, the operator could not have reasonably anticipated the current event and it was beyond the operator's control.	True			
Please explain reason for why this event was beyond your operator's control	See Justification Form > This emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable breakdown of equipment or process that was beyond the owner/operator's control, and did not stem from activity that could have been foreseen and avoided, and could not have been avoided or prevented by good design, operation, and preventative maintenance practices. Internal OXY procedures ensure that upon gas compressor unit and/or multiple unit shutdown, due to malfunction and/or alarms, production techs are promptly notified, and are instructed to assess the issue as soon as possible in order to take prompt corrective action and minimize emissions.			
Steps taken to limit the duration and magnitude of venting and/or flaring	See Justification Form > Internal OXY procedures ensure that upon gas compressor unit and/or multiple unit shutdown, due to malfunction and/or alarms, production techs are promptly notified, and are instructed to assess the issue as soon as possible in order to take prompt corrective action and minimize emissions. This facility is unmanned, except when Oxy production techs are gathering data daily or conducting daily walk-throughs to ensure that there are no problems, circumstances and/or assist other personnel on-site for maintenance purposes. In this case, Oxy production techs, who were on site at the time, determined that the cause of the malfunctions of USA gas compressor units 1, 3 & 4 were due to a fuel skid malfunction alarms, which occurred simultaneously. Oxy production techs quickly cleared the alarms, reset the panels, and restarted the compressors.			
Corrective actions taken to eliminate the cause and reoccurrence of venting and/or flaring	See Justification Form > Oxy is limited in the corrective actions available to them to eliminate the cause and potential reoccurrence of compressor malfunctions as notwithstanding compressor engine design and operation, compressors are inherently dynamic and even the smallest alarms, false or true, can be sudden, reasonably unforeseeable and unexpected which can cause compression malfunctions to occur, thereby, triggering the unit's sensors to automatically shut down the unit to avoid catastrophic damage to the internal engine components.			

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State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

CONDITIONS

Operator:	OGRID:
OXY USA INC	16696
P.O. Box 4294	Action Number:
Houston, TX 772104294	46466
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
marialuna	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	9/3/2021

CONDITIONS

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Action 46466