

Certificate of Analysis

Number: 6030-23110129-001A

Artesia Laboratory 200 E Main St. Artesia, NM 88210 Phone 575-746-3481

Chandler Montgomery Occidental Petroleum 1502 W Commerce Dr. Carlsbad, NM 88220 Nov. 14, 2023

Field: PERMIAN_RESOURCES Sampled By: Raul Salazar
Station Name: Falcon Ridge CPF Production #2 Sample Of: Gas Spot
Station Number: 16840p Sample Date: 11/13/2023 08:48

Station Location: OP-L3821-BT001 Sample Conditions: 109 psig, @ 93.8 °F Ambient: 51 °F Sample Point: Meter run Effective Date: 11/13/2023 08:48 Formation: NEW_MEXICO Method: GPA-2261M

Formation: NEW_MEXICO Method: GPA-2261M
County: Lea, NM Cylinder No: 4030-004290
Well Name: Instrument: 70104251 (Infic

Well Name: Instrument: 70104251 (Inficon GC-MicroFusion)

Type of Sample: : Spot-Cylinder Last Inst. Cal.: 11/06/2023 0:00 AM

Heat Trace Used: N/A Analyzed: 11/14/2023 08:47:52 by EBH

Sampling Method: : Fill and Purge Flow Rate mcf/d: Sampling Company: :SPL - OXY

Analytical Data

Hydrogen Sulfide	Components	Un-normalized Mol %	Mol. %	Wt. %	GPM at 14.65 psia	
Nitrogen 1.4421 1.4865 1.8527 Carbon Dioxide 0.3635 0.3747 0.7337 Methane 71.8252 74.0368 52.8427 Ethane 12.0641 12.4356 16.6361 3.321 Propane 6.7642 6.9725 13.6788 1.918 Iso-Butane 0.7457 0.7687 1.9878 0.251 n-Butane 1.9680 2.0286 5.2457 0.639 Iso-Pentane 0.5003 0.5157 1.6554 0.188 n-Pentane 0.5069 0.5225 1.6772 0.189 Hexanes 0.3635 0.3747 1.4366 0.154 Heptanes 0.3195 0.3293 1.4680 0.152 Octanes 0.1422 0.1466 0.7450 0.075 Nonanes Plus 0.0066 0.0068 0.0388 0.004 97.0118 100.0000 100.0000 6.891 Calculated Physical Properties Total C9+ Calculated Mo	Hydrogen Sulfide	0.0000	0.0010	0.0015		
Carbon Dioxide 0.3635 0.3747 0.7337 Methane 71.8252 74.0368 52.8427 Ethane 12.0641 12.4356 16.6361 3.321 Propane 6.7642 6.9725 13.6788 1.918 Iso-Butane 0.7457 0.7687 1.9878 0.251 n-Butane 1.9680 2.0286 5.2457 0.639 Iso-Pentane 0.5003 0.5157 1.6554 0.188 n-Pentane 0.5069 0.5225 1.6772 0.189 Hexanes 0.3635 0.3747 1.4366 0.154 Heptanes 0.3195 0.3293 1.4680 0.152 Octanes 0.1422 0.1466 0.7450 0.075 Nonanes Plus 0.0066 0.0068 0.0388 0.004 97.0118 100.0000 100.0000 6.891 Calculated Physical Properties Total C9+ Calculated Molecular Weight 22.48 128.26 Compressibility Fac						
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Iso-Butane	Ethane	12.0641	12.4356	16.6361	3.321	
n-Butane 1.9680 2.0286 5.2457 0.639 Iso-Pentane 0.5003 0.5157 1.6554 0.188 n-Pentane 0.5069 0.5225 1.6772 0.189 Hexanes 0.3635 0.3747 1.4366 0.154 Heptanes 0.3195 0.3293 1.4680 0.152 Octanes 0.1422 0.1466 0.7450 0.075 Nonanes Plus 0.0066 0.0068 0.0388 0.004 97.0118 100.0000 100.0000 6.891 Calculated Physical Properties Total C9+ Calculated Molecular Weight 22.48 128.26 Compressibility Factor 0.9959 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F 60°F	Propane	6.7642	6.9725	13.6788	1.918	
Iso-Pentane	Iso-Butane	0.7457	0.7687	1.9878	0.251	
n-Pentane 0.5069 0.5225 1.6772 0.189 Hexanes 0.3635 0.3747 1.4366 0.154 Heptanes 0.3195 0.3293 1.4680 0.152 Octanes 0.1422 0.1466 0.7450 0.075 Nonanes Plus 0.0066 0.0068 0.0388 0.004 97.0118 100.0000 100.0000 6.891 Calculated Physical Properties Total C9+ Calculated Molecular Weight 22.48 128.26 Compressibility Factor 0.9959 4.4283 Relative Density Real Gas 0.7790 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F	n-Butane	1.9680	2.0286	5.2457	0.639	
Hexanes	Iso-Pentane	0.5003	0.5157	1.6554	0.188	
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Octanes Nonanes Plus 0.1422 0.0066 97.0118 0.1466 0.0068 100.0000 0.7450 100.0000 0.075 0.004 6.891 Calculated Physical Properties Calculated Molecular Weight Calculated Molecular Weight Compressibility Factor Relative Density Real Gas GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F Total 22.48 128.26 0.7790 4.4283 C9+ 128.26 4.4283	Hexanes	0.3635	0.3747	1.4366	0.154	
Nonanes Plus 0.0066 97.0118 0.0068 100.0000 0.0388 100.0000 0.004 6.891 Calculated Physical Properties Total C9+ 128.26 Calculated Molecular Weight Compressibility Factor Relative Density Real Gas GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F 4.4283	Heptanes	0.3195	0.3293	1.4680	0.152	
Calculated Physical Properties Total C9+ Calculated Molecular Weight 22.48 128.26 Compressibility Factor 0.9959 Relative Density Real Gas 0.7790 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F	Octanes	0.1422	0.1466	0.7450	0.075	
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Calculated Molecular Weight 22.48 128.26 Compressibility Factor 0.9959 Relative Density Real Gas 0.7790 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F		97.0118	100.0000	100.0000	6.891	
Compressibility Factor 0.9959 Relative Density Real Gas 0.7790 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F	Calculated Physical I	Properties	Tot	al	C9+	
Relative Density Real Gas 0.7790 4.4283 GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F		3	22.4	48	128.26	
GPA 2172 Calculation: Calculated Gross BTU per ft³ @ 14.65 psia & 60°F				-		
Calculated Gross BTU per ft³ @ 14.65 psia & 60°F	,		0.779	90	4.4283	
Pool Coo Dry PTI 1222 0 6074 4		ΓU per ft³ @ 14.65 ps	sia & 60°F			
	Real Gas Dry BTU		1322		6974.4	
Water Sat. Gas Base BTU 1300.3 6852.4		-		-		
Ideal, Gross HV - Dry at 14.65 psia 1317.5 6974.4		-	_	-		
Ideal, Gross HV - Wet 1294.4 6852.4	Ideal, Gross HV - Wet	t	1294	.4	6852.4	

Comments: H2S Field Content 10 ppm

Hydrocarbon Laboratory Manager

The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.

Quality Assurance:

UPSET FLARING EVENT SPECIFIC JUSTIFICATIONS FORM

Facility: Falcon Ridge Tankless CPF Flare Date: 12/20/2023

Duration of Event: 4 Hours 40 Minutes **MCF Flared:** 1470

Start Time: 12:00 AM End Time: 04:40 AM

Cause: Emergency Flare > High O2 Detected by Targa's O2 Sensor > Targa ESD Valve Shut > Compressor

Malfunctions

Method of Flared Gas Measurement: Gas Flare Meter

1. Reason why this event was beyond Operator's control:

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction, or complete shut-in of a gas pipeline by a third-party downstream pipeline operator, which impacted Oxy's ability to send gas to a third-party downstream gas pipeline. This interruption, restriction, or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. In this case, this flaring event occurred due to an unexpected shut in and/or restriction of flow intake by Targa, which was caused by high O2 in the gas service line. Targa has a strict threshold for the O2 with due to a proximity to a gas plant. When Oxy's new wells brought unexpected O2 into the sales lines, Targa's meter sensed it and its ESD valve closed. Once Targa's ESD shut, Oxy had to purge the O2 from the gas line system by flaring the gas multiple instances over the course of a 24-Hour period to ensure all O2 was cleared and removed from the system. This was intermittent throughout the morning and afternoon due to O2 gas being unexpectedly going into the wells and coming back through the system. Throughout this time, compression equipment in the late afternoon began to malfunction as well due to being shut in multiple times and the units had trouble keep up due to constant high line pressure. This event could not have been foreseen, avoided or planned for as a full train was purged prior to use, and unfortunately, few pockets of O2 occurred once production began through the train, therefore purging the O2 to the flare was a necessary action.

2. Steps Taken to limit duration and magnitude of venting or flaring:

It is OXY's policy to route its stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, as the part of the overall process or steps to take to limit duration and magnitude of flaring. Oxy personnel are in the field 24/7 and can physically see when we are flaring which in turn are communicated to additional Oxy field personnel. Internal OXY procedures ensure that upon notice of flaring, malfunction gas compressor unit and/or multiple unit shutdown alarms, increased sensor line pressure alarms, etc., field production technician personnel are promptly notified, and are instructed to assess the issue as soon as possible to take prompt corrective action and minimize emissions. Oxy production technicians must assess whether the issue or circumstance is due to damage and repair is needed, or whether there are other reasons for its cause. In this case, this flaring event occurred due to an unexpected shut in and/or restriction of flow intake by Targa, which was caused by high O2 in the gas service line. Targa has a strict threshold for the O2 with due to a proximity to a gas plant. When Oxy's new wells brought unexpected O2 into the sales lines, Targa's meter sensed it and its ESD valve closed. Once Targa's ESD shut, Oxy had to purge the O2 from the gas line system by flaring the gas multiple instances over the course of a 24-Hour period to ensure all O2 was cleared and removed from the

system. This was intermittent throughout the morning and afternoon due to O2 gas being unexpectedly going into the wells and coming back through the system. Wells were choked back, and production techs worked to get the compression equipment purged of O2 and back online. Oxy production techs consistently worked with Targa personnel to get technicians dispatched to re-open their ESD valve and begin taking gas again as a test quality measure to ensure all O2 was cleared, on several occasions.

3. Corrective Actions taken to eliminate the cause and reoccurrence of venting or flaring:

Oxy is limited in its corrective actions to eliminate the cause and potential reoccurrence of O2 accidently pushed into the sales gas service system pipeline. OXY makes every effort to control and minimize emissions as much as possible. The limited reactive actions that Oxy can do in this circumstance is to immediately purge the O2 from the system as well as continually communicate with Targa personnel throughout these types of situations.

District I
1625 N. French Dr., Hobbs, NM 88240
Phone: (575) 393-6161 Fax: (575) 393-0720

District II 811 S. First St., Artesia, NM 88210 Phone:(575) 748-1283 Fax:(575) 748-9720

District III 1000 Rio Brazos Rd., Aztec, NM 87410 Phone:(505) 334-6178 Fax:(505) 334-6170

1220 S. St Francis Dr., Santa Fe, NM 87505 Phone:(505) 476-3470 Fax:(505) 476-3462

State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. **Santa Fe, NM 87505**

DEFINITIONS

Action 300186

DEFINITIONS

Operator:	OGRID:
OXY USA INC	16696
P.O. Box 4294	Action Number:
Houston, TX 772104294	300186
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

DEFINITIONS

For the sake of brevity and completeness, please allow for the following in all groups of questions and for the rest of this application:

- this application's operator, hereinafter "this operator";
- · venting and/or flaring, hereinafter "vent or flare";
- any notification or report(s) of the C-129 form family, hereinafter "any C-129 forms";
- the statements in (and/or attached to) this, hereinafter "the statements in this";
- and the past tense will be used in lieu of mixed past/present tense questions and statements.

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State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. **Santa Fe, NM 87505**

QUESTIONS

Action 300186

Phone:(505) 476-3470 Fax:(505) 476-3462		
	QUESTIONS	
Operator:	·	OGRID:
OXY USA INC		16696
P.O. Box 4294 Houston, TX 772104294		Action Number: 300186
		Action Type:
		[C-129] Venting and/or Flaring (C-129)
QUESTIONS		
Prerequisites Any messages presented in this section, will prevent submission of this application. Please resolve	a these issues before continuing w	ith the rest of the questions
		tal the rest of the questions.
Incident Well	Unavailable.	
Incident Facility	[fAPP2331575145] Falcon	Ridge Tankless CPF
Determination of Deposition Requirements		
Determination of Reporting Requirements Answer all questions that apply. The Reason(s) statements are calculated based on your answers a	and may provide addional quidance	<u>a</u>
Was this vent or flare caused by an emergency or malfunction	Yes	
Did this vent or flare last eight hours or more cumulatively within any 24-hour	100	
period from a single event	No	
Is this considered a submission for a vent or flare event	Yes, major venting and/or	r flaring of natural gas.
An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during	venting and/or flaring that is or ma	y be a major or minor release under 19.15.29.7 NMAC.
Was there at least 50 MCF of natural gas vented and/or flared during this event	Yes	
Did this vent or flare result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No	
Was the vent or flare within an incorporated municipal boundary or withing 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	No	
Factor and broad and		
Equipment Involved	1	
Primary Equipment Involved	Other (Specify)	
Additional details for Equipment Involved. Please specify	Emergency Flare > High O Compressor Malfunctions	v2 Detected by Targa's O2 Sensor > Targa ESD Valve Shut >
Representative Compositional Analysis of Vented or Flared Natural Gas Please provide the mole percent for the percentage questions in this group.		
Methane (CH4) percentage	74	
Nitrogen (N2) percentage, if greater than one percent	1	
Hydrogen Sulfide (H2S) PPM, rounded up	10	
Carbon Dioxide (C02) percentage, if greater than one percent	0	
Oxygen (02) percentage, if greater than one percent	0	
If you are venting and/or flaring because of Pipeline Specification, please provide the required spe		
Methane (CH4) percentage quality requirement	Not answered.	
Nitrogen (N2) percentage quality requirement	Not answered.	
Hydrogen Sufide (H2S) PPM quality requirement	Not answered.	

Not answered.

Not answered.

Carbon Dioxide (C02) percentage quality requirement

Oxygen (02) percentage quality requirement

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State of New Mexico Energy, Minerals and Natural Resources Oil Conservation Division 1220 S. St Francis Dr. Santa Fe, NM 87505

QUESTIONS, Page 2

Action 300186

C	UEST	IONS ((continue	d)

Operator:	OGRID:
OXY USA INC	16696
P.O. Box 4294	Action Number:
Houston, TX 772104294	300186
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

QUESTIONS

Date(s) and Time(s)	
Date vent or flare was discovered or commenced	12/20/2023
Time vent or flare was discovered or commenced	12:00 AM
Time vent or flare was terminated	04:40 AM
Cumulative hours during this event	5

Measured or Estimated Volume of Vented or Flared Natural Gas	
Natural Gas Vented (Mcf) Details	Not answered.
Natural Gas Flared (Mcf) Details	Cause: Other Other (Specify) Natural Gas Flared Released: 1,470 Mcf Recovered: 0 Mcf Lost: 1,470 Mcf.
Other Released Details	Not answered.
Additional details for Measured or Estimated Volume(s). Please specify	Gas Flare Meter
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.

Venting or Flaring Resulting from Downstream Activity	
Was this vent or flare a result of downstream activity	No
Was notification of downstream activity received by this operator	Not answered.
Downstream OGRID that should have notified this operator	Not answered.
Date notified of downstream activity requiring this vent or flare	Not answered.
Time notified of downstream activity requiring this vent or flare	Not answered.

	not allowed.
Date notified of downstream activity requiring this vent or flare	Not answered.
Time notified of downstream activity requiring this vent or flare	Not answered.
Steps and Actions to Prevent Waste	
For this event, this operator could not have reasonably anticipated the current event and it was beyond this operator's control.	True

Please explain reason for why this event was beyond this operator's control

The emissions event was caused by the unforeseen, unexpected, sudden, and unavoidable interruption, restriction, or complete shut-in of a gas pipeline by a third-party downstream pipeline operator, which impacted Oxy's ability to send gas to a third-party downstream gas pipeline. This interruption, restriction, or complete shut-in of the gas pipeline by a third-party pipeline operator is downstream of Oxy's custody transfer point and out of Oxy's control to avoid or prevent from happening and did not stem from any of Oxy's upstream facility activity that could have been foreseen and avoided, and could not have been avoided by good design, operation, and preventative maintenance practices. In this case, this flaring event occurred due to an unexpected shut in and/or restriction of flow intake by Targa, which was caused by high O2 in the gas service line. Targa has a strict threshold for the O2 with due to a proximity to a gas plant. When Oxy's new wells brought unexpected O2 into the sales lines, Targa's meter sensed it and its ESD valve closed. Once Targa's ESD shut, Oxy had to purge the O2 from the gas line system by flaring the gas multiple instances over the course of a 24-Hour period to ensure all O2 was cleared and removed from the system. This was intermittent throughout the morning and afternoon due to O2 gas being unexpectedly going into the wells and coming back through the system. Throughout this time, compression equipment in the late afternoon began to malfunction as well due to being shut in multiple times and the units had trouble keep up due to constant high line pressure. This event could not have been foreseen, avoided or planned for as a full train was purged prior to use, and unfortunately, few pockets of O2 occurred once production began through the train, therefore

1	purging the O2 to the flare was a necessary action.
Steps taken to limit the duration and magnitude of vent or flare	It is OXY's policy to route its stranded gas to a flare during an unforeseen and unavoidable emergency or malfunction, as the part of the overall process or steps to take to limit duration and magnitude of flaring. Oxy personnel are in the field 24/7 and can physically see when we are flaring which in turn are communicated to additional Oxy field personnel. Internal OXY procedures ensure that upon notice of flaring, malfunction gas compressor unit and/or multiple unit shutdown alarms, increased sensor line pressure alarms, etc., field production technician personnel are promptly notified, and are instructed to assess the issue as soon as possible to take prompt corrective action and minimize emissions. Oxy production technicians must assess whether the issue or circumstance is due to damage and repair is needed, or whether there are other reasons for its cause. In this case, this flaring event occurred due to an unexpected shut in and/or restriction of flow intake by Targa, which was caused by high O2 in the gas service line. Targa has a strict threshold for the O2 with due to a proximity to a gas plant. When Oxy's new wells brought unexpected O2 into the sales lines, Targa's meter sensed it and its ESD valve closed. Once Targa's ESD shut, Oxy had to purge the O2 from the gas line system by flaring the gas multiple instances over the course of a 24-Hour period to ensure all O2 was cleared and removed from the system. This was intermittent throughout the morning and afternoon due to O2 gas being unexpectedly going into the wells and coming back through the system. Wells were choked back, and production techs worked to get the compression equipment purged of O2 and back online. Oxy production techs consistently worked with Targa personnel to get technicians dispatched to re-open their ESD valve and begin taking gas again as a test quality measure to ensure all O2 was cleared, on several occasions.
Corrective actions taken to eliminate the cause and reoccurrence of vent or flare	Oxy is limited in its corrective actions to eliminate the cause and potential reoccurrence of O2 accidently pushed into the sales gas service system pipeline. OXY makes every effort to control and minimize emissions as much as possible. The limited reactive actions that Oxy can do in this circumstance is to immediately purge the O2 from the system as well as continually communicate with Targa personnel throughout these types of situations.

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ACKNOWLEDGMENTS

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ACKNOWLEDGMENTS

>	I acknowledge that I am authorized to submit a Venting and/or Flaring (C-129) report on behalf of this operator and understand that this report can be a complete C-129 submission per 19.15.27.8 and 19.15.28.8 NMAC.
V	I acknowledge that upon submitting this application, I will be creating a new incident file (assigned to this operator) to track any C-129 forms, pursuant to 19.15.27.7 and 19.15.28.8 NMAC and understand that this submission meets the notification requirements of Paragraph (1) of Subsection G and F respectively.
V	I hereby certify the statements in this report are true and correct to the best of my knowledge and acknowledge that any false statement may be subject to civil and criminal penalties under the Oil and Gas Act.
V	I acknowledge that the acceptance of any C-129 forms by the OCD does not relieve this operator of liability should their operations have failed to adequately investigate, report, and remediate contamination that poses a threat to groundwater, surface water, human health, or the environment.
~	I acknowledge that OCD acceptance of any C-129 forms does not relieve this operator of responsibility for compliance with any other applicable federal, state, or local laws and/or regulations.

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CONDITIONS

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P.O. Box 4294	Action Number:
Houston, TX 772104294	300186
	Action Type:
	[C-129] Venting and/or Flaring (C-129)

CONDITIONS

Created By	Condition	Condition Date
marialuna2	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	1/4/2024