



Measurement Repository

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Analysis

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Last Modified 6/6/2025 11:16:36 AM By

Meter ID: 90301204 Lease Name: **COTTON DRAW CVX CDP1**
Effective Date: 05/01/2025 Producer:
Line Pressure: 0 Line Flow Rate: 0
Line Temperature: 0 Analysis Type: GAS
Analysis Use: Accounting Analysis Pressure Base: 14.73
Analysis Date: 05/22/2025 Analyzed By:
Sampled By: Sample Taken Date: 05/22/2025
Sample Type: COMP Cylinder Number:

Composition

	Mol %	GPM
Carbon Dioxide:	0.886	
Nitrogen:	1.617	
Methane:	74.6824	
Ethane:	12.1229	3.254
Propane:	6.2719	1.7342
Isobutane:	0.819	0.269
Normal Butane:	2.02	0.6392
Isopentane:	0.447	0.1641
Normal Pentane:	0.482	0.1754
Hexanes:	0.651	0.2851

[View optional composition fields](#)

Total: 100 6.521

[Hide all composition fields](#)

Sample Condition

Condition	Real BTU/SCF	Ideal BTU/SCF	Relative Density	Compressibility (Z)
Water Saturated:	1275.245	0	0	0
Dry:	1297.833	0	0.7679	0
As Delivered:	0	0	0	0

Water Content (lb/mmcsfd):

0

26# GPM:

0.020

[Hide all sample condition fields](#)

Comments:

TCEQ Emission Event Reporting
Component Calculation SpreadsheetTarga Resources
Field Event Emissions Calc sheet

Leak Calculations

Date/Time of Discovery 6/25/25 13:59
Date/Time Leak was Isolated 6/25/25 18:40
Diameter of hole, In
Diameter of Pipe, In
Pipeline Initial Pressure, PSIG

Blowdowns Controlled?

Yes

Blowdown Calculations

Blowdown #1
Diameter of Pipe, In 12
Length Blown Down, Ft 10560
Pipeline Initial Pressure, PSIG 1150
Pipeline End Pressure, PSIG 0
Temperature (F) inside pipe 60
Blowdown #1 Volume 648.84

Blowdown #3
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #2 Volume 0.00

Blowdown #5
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #3 Volume 0.00

Blowdown #2
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #4 Volume 0.00

Blowdown #4
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #5 Volume 0.00

Blowdown #6
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #6 Volume 0.00

Blowdown #7
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #4 Volume 0.00

Blowdown #8
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #5 Volume 0.00

Blowdown #9
Diameter of Pipe, In
Length Blown Down, Ft
Pipeline Initial Pressure, PSIG
Pipeline End Pressure, PSIG
Temperature (F) inside pipe
Blowdown #6 Volume 0.00

Gas Composition

Gas Component	Mole %
H2S	
Carbon Dioxide	
Nitrogen	
Methane	
Ethane	
Propane	
iso-Butane	
n-Butane	
iso-Pentane	
n-Pentane	
Cyclohexane	
Hexanes	
Heptanes	
Octanes	
Nonanes	
Decanes	
Benzene	
Toluene	
Xylenes	
Ethylbenzene	

TCEQ Emission Event Reporting Component Calculation Spreadsheet



Targa Resources
Field Event Emissions Calc sheet

Time of Event, HR =	4.68
Leak Volume, MCF =	0.00
Blowdown Volume, MCF =	648.84
Total Volume, MCF =	648.84

Component	Total Pounds Vented + Flared	Flow Rate (lb/hr)	Flow Rate (lb/24-Hours)	Reportable Quantity 24 hours	Exceeded RQ?	REPORT OR OK?
Carbon Monoxide (CO)	0.00	0.00	0.00	5,000.00	No	OK!
Hydrogen Sulfide	0.00	0.00	0.00	100.00	No	OK!
Oxides of Nitrogen (NOx) NRC	0.00	0.00	0.00	1,000.00	No	OK!
Oxides of Nitrogen (NOx) TCEQ	0.00	0.00	0.00	5,000.00	No	OK!
Sulfur Dioxide	0.00	0.00	0.00	500.00	No	OK!
Natural Gas VOCs	0.00	0.00	0.00	5,000.00	No	OK!
Component	Total Pounds Vented + Flared	Flow Rate (lb/hr)	Flow Rate (lb/24- Hours)	Reportable Quantity 24 hours	Exceeded RQ?	REPORT OR OK?
Benzene	0.00	0.00	0.00	10.00	No	OK!
Butane	0.00	0.00	0.00	5,000.00	No	OK!
Carbon Monoxide (CO)	0.00	0.00	0.00	5,000.00	No	OK!
Cyclohexane	0.00	0.00	0.00	1,000.00	No	OK!
Decane	0.00	0.00	0.00	5,000.00	No	OK!
Ethylbenzene	0.00	0.00	0.00	1,000.00	No	OK!
Heptane	0.00	0.00	0.00	5,000.00	No	OK!
Hexane	0.00	0.00	0.00	5,000.00	No	OK!
Hydrogen Sulfide	0.00	0.00	0.00	100.00	No	OK!
Nonane	0.00	0.00	0.00	5,000.00	No	OK!
Oxides of Nitrogen (NOx)	0.00	0.00	0.00	1,000.00	No	OK!
Octane	0.00	0.00	0.00	5,000.00	No	OK!
Pentane	0.00	0.00	0.00	5,000.00	No	OK!
Propane	0.00	0.00	0.00	5,000.00	No	OK!
Sulfur Dioxide	0.00	0.00	0.00	500.00	No	OK!
Toluene	0.00	0.00	0.00	1,000.00	No	OK!
Xylene	0.00	0.00	0.00	100.00	No	OK!

Updated 09/19/2023

Sante Fe Main Office
Phone: (505) 476-3441

General Information
Phone: (505) 629-6116

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State of New Mexico
Energy, Minerals and Natural Resources
Oil Conservation Division
1220 S. St Francis Dr.
Santa Fe, NM 87505

DEFINITIONS

Action 478781

DEFINITIONS

Operator: Targa Northern Delaware, LLC. 110 W. 7th Street, Suite 2300 Tulsa, OK 74119	OGRID: 331548
	Action Number: 478781
	Action Type: [C-129] Venting and/or Flaring (C-129)

DEFINITIONS

<p>For the sake of brevity and completeness, please allow for the following in all groups of questions and for the rest of this application:</p> <ul style="list-style-type: none">• this application's operator, hereinafter "this operator";• venting and/or flaring, hereinafter "vent or flare";• any notification or report(s) of the C-129 form family, hereinafter "any C-129 forms";• the statements in (and/or attached to) this, hereinafter "the statements in this";• and the past tense will be used in lieu of mixed past/present tense questions and statements.

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QUESTIONS

Action 478781

QUESTIONS

Operator: Targa Northern Delaware, LLC. 110 W. 7th Street, Suite 2300 Tulsa, OK 74119	OGRID: 331548
	Action Number: 478781
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Prerequisites <i>Any messages presented in this section, will prevent submission of this application. Please resolve these issues before continuing with the rest of the questions.</i>	
Incident Well	Unavailable.
Incident Facility	[fAPP2123031392] TARGA NORTHERN DELAWARE, LLC.

Determination of Reporting Requirements <i>Answer all questions that apply. The Reason(s) statements are calculated based on your answers and may provide additional guidance.</i>	
Was this vent or flare caused by an emergency or malfunction	Yes
Did this vent or flare last eight hours or more cumulatively within any 24-hour period from a single event	No
Is this considered a submission for a vent or flare event	Yes, major venting and/or flaring of natural gas.
<i>An operator shall file a form C-141 instead of a form C-129 for a release that, includes liquid during venting and/or flaring that is or may be a major or minor release under 19.15.29.7 NMAC.</i>	
Was there at least 50 MCF of natural gas vented and/or flared during this event	Yes
Did this vent or flare result in the release of ANY liquids (not fully and/or completely flared) that reached (or has a chance of reaching) the ground, a surface, a watercourse, or otherwise, with reasonable probability, endanger public health, the environment or fresh water	No
Was the vent or flare within an incorporated municipal boundary or within 300 feet from an occupied permanent residence, school, hospital, institution or church in existence	No

Equipment Involved	
Primary Equipment Involved	Not answered.
Additional details for Equipment Involved. Please specify	Not answered.

Representative Compositional Analysis of Vented or Flared Natural Gas <i>Please provide the mole percent for the percentage questions in this group.</i>	
Methane (CH4) percentage	75
Nitrogen (N2) percentage, if greater than one percent	2
Hydrogen Sulfide (H2S) PPM, rounded up	0
Carbon Dioxide (CO2) percentage, if greater than one percent	1
Oxygen (O2) percentage, if greater than one percent	0
<i>If you are venting and/or flaring because of Pipeline Specification, please provide the required specifications for each gas.</i>	
Methane (CH4) percentage quality requirement	Not answered.
Nitrogen (N2) percentage quality requirement	Not answered.
Hydrogen Sulfide (H2S) PPM quality requirement	Not answered.
Carbon Dioxide (CO2) percentage quality requirement	Not answered.
Oxygen (O2) percentage quality requirement	Not answered.

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QUESTIONS, Page 2

Action 478781

QUESTIONS (continued)

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	Action Number: 478781
	Action Type: [C-129] Venting and/or Flaring (C-129)

QUESTIONS

Date(s) and Time(s)	
Date vent or flare was discovered or commenced	06/24/2025
Time vent or flare was discovered or commenced	01:59 PM
Time vent or flare was terminated	06:40 PM
Cumulative hours during this event	5

Measured or Estimated Volume of Vented or Flared Natural Gas	
Natural Gas Vented (Mcf) Details	Not answered.
Natural Gas Flared (Mcf) Details	Cause: Equipment Failure Pipeline (Any) Natural Gas Flared Released: 649 Mcf Recovered: 0 Mcf Lost: 649 Mcf.
Other Released Details	Not answered.
Additional details for Measured or Estimated Volume(s). Please specify	Not answered.
Is this a gas only submission (i.e. only significant Mcf values reported)	Yes, according to supplied volumes this appears to be a "gas only" report.

Venting or Flaring Resulting from Downstream Activity	
Was this vent or flare a result of downstream activity	No
Was notification of downstream activity received by this operator	Not answered.
Downstream OGRID that should have notified this operator	Not answered.
Date notified of downstream activity requiring this vent or flare	Not answered.
Time notified of downstream activity requiring this vent or flare	Not answered.

Steps and Actions to Prevent Waste	
For this event, this operator could not have reasonably anticipated the current event and it was beyond this operator's control.	True
Please explain reason for why this event was beyond this operator's control	Gas was routed to a portable flare to facilitate a pig receiver block valve replacement.
Steps taken to limit the duration and magnitude of vent or flare	Operations personnel blew down the line as expeditiously as possible for the safety of personnel and equipment.
Corrective actions taken to eliminate the cause and reoccurrence of vent or flare	The pig receiver block valve was replaced, line determined to be safely operated and returned to service.

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ACKNOWLEDGMENTS

Action 478781

ACKNOWLEDGMENTS

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	Action Number: 478781
	Action Type: [C-129] Venting and/or Flaring (C-129)

ACKNOWLEDGMENTS

<input checked="" type="checkbox"/>	I acknowledge that I am authorized to submit a <i>Venting and/or Flaring</i> (C-129) report on behalf of this operator and understand that this report can be a complete C-129 submission per 19.15.27.8 and 19.15.28.8 NMAC.
<input checked="" type="checkbox"/>	I acknowledge that upon submitting this application, I will be creating a new incident file (assigned to this operator) to track any C-129 forms, pursuant to 19.15.27.7 and 19.15.28.8 NMAC and understand that this submission meets the notification requirements of Paragraph (1) of Subsection G and F respectively.
<input checked="" type="checkbox"/>	I hereby certify the statements in this report are true and correct to the best of my knowledge and acknowledge that any false statement may be subject to civil and criminal penalties under the Oil and Gas Act.
<input checked="" type="checkbox"/>	I acknowledge that the acceptance of any C-129 forms by the OCD does not relieve this operator of liability should their operations have failed to adequately investigate, report, and remediate contamination that poses a threat to groundwater, surface water, human health, or the environment.
<input checked="" type="checkbox"/>	I acknowledge that OCD acceptance of any C-129 forms does not relieve this operator of responsibility for compliance with any other applicable federal, state, or local laws and/or regulations.

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CONDITIONS

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	Action Number: 478781
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CONDITIONS

Created By	Condition	Condition Date
amberg	If the information provided in this report requires an amendment, submit a [C-129] Amend Venting and/or Flaring Incident (C-129A), utilizing your incident number from this event.	6/25/2025