AP- 37

STAGE 2 REPORT (Even+4) Date 6-6-13



AMARILLO 921 North Bivins Amarillo, Texas 79107 Phone 806.467.0607 Fax 806.467.0622

AUSTIN 911 W. Anderson Lane Suite 202 Austin, Texas 78757 Phone 512.989.3428 Fax 512.989.3487

PREPARED FOR:

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PLAINS MARKETING, L.P. 333 CLAY STREET SUITE 1600 HOUSTON, TEXAS 77002

MIDLAND 2901 State Highway 349

Midland, Texas 79706 Phone 432.522.2133 Fax 432.522.2180

SAN ANTONIO 11 Commercial Place Schertz, Texas 78154 Phone 210.265.8025 Fax 210.568.2191

OKLAHOMA CITY 7700 North Hudson Suite 10 Oklahoma City, Oklahoma 73116 Phone 405.486.7032

HOBBS

318 East Taylor Street Hobbs, New Mexico 88241 Phone 505.393.4261 Fax 505.393.4658

ARTESIA 408 W. Texas Ave. Ariesia, New Mexico 88210 Phone 575.746.8768 Fax 505.746.8905 PREPARED BY:

TALON/LPE 921 N. Bivins

AMARILLO, TEXAS 79107

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MOBILE DUAL PHASE EXTRACTION REPORT

2013 SEP 20 P 2: 04

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I. MDPE SUMMARY REPORT AND WASTE DISPOSITION

A. MDPE Results

The following report summarizes data collected during the scheduled 24-hour High Vacuum Multi-Phase Extraction (MDPE) event conducted on February 27-28, 2013, at the Lovington Deep 6 Pipeline release site, located in Lea County, New Mexico. The objective of the MDPE treatment was to remove both vapor and liquid phase separated hydrocarbons (PSH) from onsite groundwater wells. Talon/LPE utilized an MDPE unit which consisted of an SVE extraction pump capable of generating vacuum up to 25" hg. Off gas vapors extracted from the extraction wells were destroyed using a propane-fired 1000-SCFM thermal oxidizer capable of processing 172.96 lbs/hr of gasoline.

A total of 9.5 hours (0.40 days) of PSH recovery was performed due to freezing of propane tank and inability of vendor to refill. MW2, MW13, MW-14, MW15, MW16 & MW17 for 9.5 hours.

Prior to and immediately following the event, the groundwater wells were gauged for groundwater elevation and PSH. Depth to groundwater ranges were measured in feet below the top of casing. Refer to Attachment 1 for a summary of data collected during the MDPE event.

The volume of PSH removed during the MDPE event is shown to reflect the portions of PSH in the liquid phase and as off-gas vapor. Air removal rates were calculated from velocity measurements recorded at the influent manifold prior to entry into the MDPE unit. PSH recovery and air flow data has been detailed and is contained in Table 1. One influent air sample was collected over the course of the event. This sample was submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The influent sample was tested for Total-Gas Analysis (Hydrocarbon Composition) by GPA 2261-C6+. Laboratory analytical results can be found in Attachment 2.

Based on a combination of field vapor screening and collected laboratory samples, a combined estimated total of 285.44 equivalent gallons of hydrocarbons (Total) were removed during the event. The combined volume of hydrocarbons were comprised of approximately 280 gallons of PSH (liquid phase) and approximately 5.44 gallons as off-gas vapor. The calculations used to estimate the off-gas vapor mass recovered reflect the mass of total hydrocarbons recovered and does not necessarily equate to an equal mass of the product released. The mass recovery calculations may be affected by variations in the specific gravity of hydrocarbon released, age of release, activity of aerobic and/or anaerobic processes, and site specific geochemical factors.

The cumulative air flow measurements for the MDPE event were calculated using a combination of field data measurements and Preso® B+ manufacturer provided formulas. Air flow rates extracted from the recovery wells averaged 119.22 SCFM during the event.

A portion of the extracted air flow rates measured is attributable to compressed air, which was "injected" into the extraction wells. This "injected" air is introduced into the extraction wells for the purpose of enhancing liquid recovery rates.

B. Air Quality

One influent air sample was collected during the event. The sample was submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The maximum influent concentration was recorded as 7,440 ppmv for Hydrocarbon Composition. Laboratory analytical results can be found in Attachment 2.

C. Waste Management and Disposition

A cumulative total of 1,679 gallons of fluid were generated during this event. The fluids were temporarily transferred to an on-site storage tank prior to being transferred to an authorized disposal facility. A copy of the waste ticket can be found in Attachment 4.

II. SYSTEM OPERATION DATA AND MASS RECOVERY CALCULATIONS

Formulae:

Concentration (C_mg/l) = $\frac{\text{C_ppmv x Mol. wt. in mg(estimated) x } 1000 \text{ x } 0.000001}{0.0821 \text{ x Temp (K)}}$

Recovery (lbs) = (lbs/hr) x (hrs)

Correction Factor (CF) = PID Reading(ppm)
PID Reading at Time of Laboratory Analysis

8.34 lbs x 0.82 average specific gravity of light crude = 6.84 lbs light crude gallon water (estimated) gallon

Table 1

System Operation Data and Mass Recovery Calculations Influent Temp. (°6 FID Reading (ppm) Adjusted Lab Result (ppmv) djusted Lai Result (rng/L) Differentia signed Lai Correction Total Period (hours) Vacuum (In. h20) Lab Resul Flow (SCFM) Time pressure (in. h20) (lbe/hr) (In. hg) (ppmv) (CF) (lbs) 62 19 258.57 7440.00 0.72 5325 15:30 0.5 56 159.41 35789 6.40 3.82 1.91 1.91 16:00 0.5 62 19 258.57 55.1 158,12 50000 7440.00 7440.00 1.00 7440 8.95 5.29 2.64 4.55 17:00 62 18 244.96 31.6 125.49 36705 7440.00 0.73 5462 6.57 3.08 3.08 7.63 18:00 50000 7440.00 1.00 11.10 60 17 231.35 19.8 103.27 7440 8,98 3,47 3.47 16.5 224.55 7440 19:00 7440.00 1.00 3.53 56 19.3 104.31 50000 9.05 3.53 14.63 20:00 52 15.5 210.94 19.9 110.21 49766 7440.00 1.00 7405 9.08 3.74 3.74 18.37 21:00 50 15.5 210.94 19.8 110.15 50000 7440.00 1.00 9.16 3.77 3.77 22.14 22:00 50 15.5 210.94 18.9 107.62 50000 7440.00 1.00 7440 9,16 3.68 3.68 25.83 23:00 15.5 108.75 7440 50 210.94 19.3 50000 7440.00 1.00 9,16 3.72 3.72 29.55 0:00 50 15 204.14 19.9 11232 50000 7440.00 1.00 7440 9.16 3.85 3.85 33.40 1:00 50 15 204.14 19.7 111.76 50000 7440.00 1.00 7440 9.16 3.83 3.83 37.22 Event stopped short @ 01:45 due to freezing of propene and insbility for vendor to refill tank 54.91 16,50 Averages: 224.55 27.23 119.22 47478.18 Total 37.22 PSH Mase Recovered in Vapor Phase = 5.44 FID maximum Concentration = 50,000 PPM Ex: Conversion from ppmv to mg/L (influent 1) Molecul Temp. Temp. **Gas Constant** Conc. Conc **Total Hydrocarbon Recovery** (ppmv) (Grame) (atm) (atm.liter/K.mole) (F) (K) (C_mg/l) 5325 28.6008 0.0821 62 Inputs are the green values. PSH Mass Recovered in Vapor Phase = 37.22 Calculated values are yellow. Constants are purple values. PSH Mass Recovered in Liquid Phase = 1915.20 Liquid-phase Hydrocarbon Recovery TOTAL = 1952.42 lbs [] * r2 * h = volume 285.44 gallons Gallons removed determined at time of pick up PSH Volume in Gallons= SG = 0.82 PSH Mess in Pounds= 19153

M Ve	L (Wt. %) Hydrocarbon to	Molecular Weight Calculations							
20 40	L (W. 76) Hydrocarbon d	component	Molecular Weight (g/mol)	mol%					
Compound	Molecular Weight (g/mol)	Wt. %	=	ppmv	Nitrogen (N2)	28.016	97.0480		
Methane (CH4)	16.04	0		0.00	Methane (CH4)	16.0425	0.0000		
Ethane (C2H6)	30.07	0		0.00	Carbon Dioxide (CO2)	44.011	2.7070		
Propane (C3H8)	44.10	0		0.00	Ethane (C2H6)	30.089	0.0000		
Iso-Butane (C4H10)	58.12	0.006		60.00	Propane (C3H8)	44.0956	0.0000		
N-Butane (C4H10)	58.12	0.016		160.00	Iso-Butane (C4H10)	58,1222	0.0030		
Iso-Pentane (C4H12)	72.15	0.048		480.00	N-Butane (C4H10)	58.1222	0.0080		
N-Pentane (C5H12)	72.15	0.091		910.00	Iso-Pentane (C4H12)	72.1488	0.0190		
Hexane+ (C6H14)	97.40	0.583		5830.00	N-Pentane (C5H12)	72.1488	0.0360		
			Total	7440.00	Hexane+	97.3968	0.1790		
*Hexane+ is treate	d as 60% hexanes, 30 % hepta	nes, and 10 % o	ctanes, as su	ch its		Total	100		
	93.1887)+(0.3*100.2019)+(0.1*					Calculated MW	28,6008		

sum (Individual component IfW x their reported mol%) Calculated MW=

% Vol x 10,000

MDPE Field Logs

					MDPE FIE	LD NOTES	3							
Site Name	e:	Lovington	Deep 6				Event #:1							
Location:		Lea Count	y, NM					Arrive at site: 2/27/13 13:30						
Date:		2/28/2013												
Job#:		700376.05	1.05		SRS:	2002-103	112	Start Vac:	2/27/13 14:45					
Phase:		MDPE4			Unit:	1107		Stop Vac:	2/28/13 1:00					
Onsite Pe	rsonnel:	L. Bridges	& B. Hunti	ngton				Leave Site:	2/28/13 12:30					
			5.00440											
					GAUGIN	G DATA	., .							
WELL#		BEFORE			AFTER		_	COMME	NTS					
	PSH	GW	PSH-T	PSH	GW	PSH-T								
MW-2	63.63	67.81	4.18	64.35	64.72	0.37	Stinger set @ 6							
MW-13	64.33	68.89	4.56	65.05	65.38	0.33	Stinger set @ 6							
MW-14	64.95	65.83	0.88	-	65.13		Stinger set @ 6	35'						
MW-15	64.86	64.93	0.07		lot Gauge									
MW-16	64.45	65.98	1.53	64.73	64.74	0.01	Stinger set @ 6							
MW-17	64.13	68.13	4.00	64.78	65.08	0.30	Stinger set @ 6	65' <u> </u>						
MW-3		64.78												
						<u> </u>								
									- 					

					L <u>.</u>									
WASTE:	H2O:	1399		PSH:	280	L	TOTAL (GAL):	1679						
Sample		Ana		Date:		me:	Comments:	FID	000					
INFLU		C		27-Feb-13		:00 PM		FID = >50	000					
-				-										

Sample Name	Analysis	Date:	Time:	Comments:
INFLUENT	C6+	27-Feb-13	16:00:00 PM	FID = >50000
-	<u>-</u>	-	-	-
-	-	-	-	-
-	-	_	-	-
-	-	-	-	-

Notes:		
Tank #1 - Total	l 53.75" with PSH@44.75" = Total 1679 gallons and PSH at 280 gallons	
Hand Bailed MV	W15	
Adjusted vacuur	um and well depth as discussed w/pm	
Started stinger a	at 65 and adjusted from there	

Start Date: 28-Feb-13 MDPE FIELD DATA - 24hr 1107 Event#1

			Well Flow					Well Data										
TIME	SAMPLE	Inflent temp.	Diff.	Vac	FID	Propane	EXHAUST			COMMENTS:								
	TAKEN	(°f)	Pressure	(In.Hg)	Composite	Tank	TEMPF	MW2	MW13	MW14	MW16	MW17						
			(INH20)		(PPM)	(%-size)		VAC (INH2O)	VAC (INH2O)	VAC (INH2O)	VAC (INH2O)	VAC (INH2O)						
			2" Preso			75		V/10 (I/1/120)	V/10 (I/11 120)	V/10 (111120)	V/10 (II 11 120)	VAO (INTIZO)						
15:30		62	56.6	19	35789	32	1406	5.9	24.8	21.5	17.8	10.8						
16:00	*	62	55.1	19	>50k	70	1408	5.8	23.9	22	11,9	9.1						
17:00		62	31.8	18	36705	69	1407	5	22.4	15.8	9.3	8.1						
18:00		60	19.8	17	>50k	64	1410	2.7	19.6	12.9	8.8	6.5						
19:00		56	19.3	16.5	>50k	59	1410	3.1	20.1	13,3	9,1	6.5						
20:00		52	19.9	15.5	49766	55	1408	3.2	20.4	13	9	5.6						
21:00		50	19.8	15.5	>50k	50	1410	3,3	19.9	12.8	8.7	6.3						
22:00		50	18.9	15.5	>50k	45	1410	2.8	20.4	13.2	8.4	6.2						
23:00		50	19.3	15.5	>50k	41	1407	2.4	20.1	13.8	7.3	6.3						
0:00		50	19.9	15	>50k	36	1415	3.2	19.8	12.9	7.9	6.2						
1:00		50	19.7	15	>50k	33	1409	2.9	19.9	13.6	7.1	6.1						

Soil Vacuum Influence

Observation Well	MW15
Extraction Well (EW)	MW2
Time:	In.H2O
16:00	0.05

Laboratory Analytical Results



HOMBICH LABORA OF H 2 CLUBA EPAPRATAJE NO TE EDELOTO E E (AS 77 E TERME TOBLESE

Certificate of Analysis

Number: 1030-2013030100-001A

Simon I. Walshe, CAPM

Talon/LPE 921 N. Bivins St. Amarillo Texas 79107 March 06, 2013

Sample ID:

Station Name:

Sample Point:

Influent #1

Sampled By: Sample Of:

BH

Station Number:

Station Location:

Hobbs, NM.

Sample Date:

Spot Gas 02/28/2013 10:00

Sample Conditions: N.G. Pres., N.G. Temp.

PO / Ref. No:

ANALYTICAL DATA

Components	Mol %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	DK	3/5/2013 4:16:22 AM
Nitrogen	97.048	95.089				
Carbon Dioxide	2.707	4.167				
Iso Butane	0.003	0.006	0.001			
n-Butane	0.008	0.016	0.003			
Iso Pentane	0.019	0.048	0.007			
n-Pentane	0.036	0.091	0.013			
Hexanes Plus	0.179	0.583	0.078			
	100.000	100.000	0.102			
	C2 +	C3 +	iC5 +			
GPM TOTAL:	0.102	0.102	0.098			
Relative Density	Real Gas			0.9871		
Calculated Molecular	Weight			28.59		
Compressibility Factor GPA 2172-09 Calculate Calculated Gross BT	on:			0.9996		

Calculated Gross BTU per ft³ @14.650 psia & 60°F

Real Gas:

Dry BTU:

12

Water Sat. Gas Base BTU:

11

Comments:

H2O Mol% - 1.75_Wt% - 1.11

Staly

Hydrocarbon Laboratory Manager

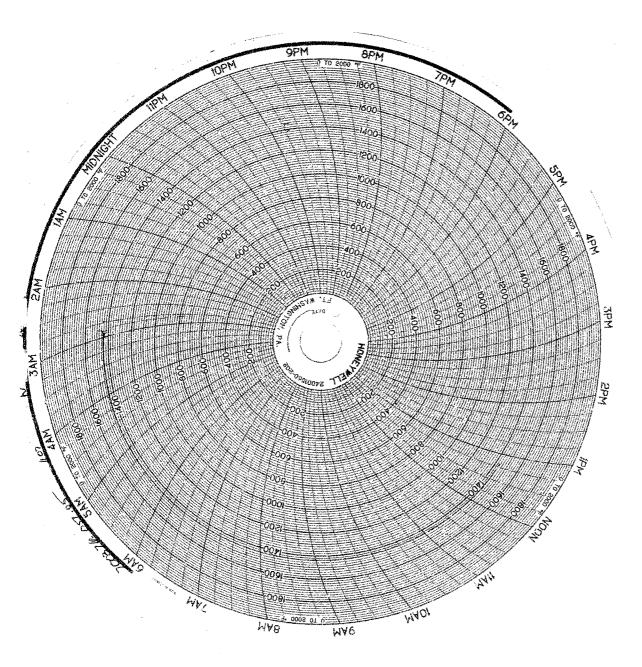
Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated

SPL, Inc. Analysis Request Chain of Custody Record

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			Sample	i i	site		Cylinder Tracking In:		info ¹														
Sample ID (used to log/track sample)	Sample Date	Sample Time	Type (Gas/Liq.	Duplicale	Composite	Spot	Cylinder #	Date Out	Date in			İ									Corr	ments	
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Oxidizer Charts



Waste Ticket

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