# 1R-455

## REPORTS (Event4) DATE: 6-5-13



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ENVIRONMENTAL CONSULTING ENGINEERING DRILLING CONSTRUCTION EMERGENCY RESPONSE

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### MOBILE DUAL PHASE EXTRACTION REPORT CD VACUUM TO JAL 14 INCH MAINLINE 3 PIPELINE RELEASE LEA COUNTY, NEW MEXICO 2013 SEP 20 P 2: 03 SRS # 2003-00117 NMOCD# 1R-0455

**PREPARED FOR:** 

PLAINS MARKETING, L.P. 333 CLAY STREET SUITE 1600 HOUSTON, TEXAS 77002

**PREPARED BY:** 

TALON/LPE 921 N. Bivins Amarillo, Texas 79107

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Attachment 1 - MDPE field logs Attachment 2 - Laboratory Analytical Results Attachment 3 – Oxidizer Charts Attachment 4 – Waste Ticket

### I. MDPE SUMMARY REPORT AND WASTE DISPOSITION

### A. MDPE Results

The following report summarizes data collected during the 12-hour High Vacuum Multi-Phase Extraction (MDPE) event conducted from April 23 - 24, 2013 at the Vacuum to Jal 14 Inch Mainline 3 Pipeline release site, located in Lea County, New Mexico. The objective of the MDPE treatment was to remove both vapor and liquid phase separated hydrocarbons (PSH) from onsite groundwater wells. Talon/LPE utilized an MDPE unit which consisted of an SVE extraction pump capable of generating vacuum up to 25" hg. Off gas vapors extracted from the extraction wells were destroyed using a propane-fired 1000-SCFM thermal oxidizer capable of processing 172.96 lbs/hr of gasoline.

A total of 12 hours (0.5 days) of PSH recovery was performed. RW-1, RW-3, RW-4, & RW-5 for 12 hours.

Prior to and immediately following the event, the groundwater wells were gauged for groundwater elevation and PSH. Depth to groundwater ranges were measured in feet below the top of casing. Refer to Attachment 1 for a summary of data collected during the MDPE event.

The volume of PSH removed during the MDPE event is shown to reflect the portions of PSH in the liquid phase and as off-gas vapor. Air removal rates were calculated from velocity measurements recorded at the influent manifold prior to entry into the MDPE unit. PSH recovery and air flow data has been detailed and is contained in Table 1. Two influent air samples were collected over the course of the event. These samples were submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. Both influent samples were tested for Total-Gas Analysis (Hydrocarbon Composition) by GPA 2261-C6+. Laboratory analytical results can be found in Attachment 2.

Based on a combination of field vapor screening and collected laboratory samples, a combined estimated total of 121.38 equivalent gallons of hydrocarbons (Total) were removed during the event. The combined volume of hydrocarbons were comprised of approximately 96 gallons of PSH (liquid phase) and approximately 25.38 gallons as off-gas vapor. The calculations used to estimate the off-gas vapor mass recovered reflect the mass of total hydrocarbons recovered and does not necessarily equate to an equal mass of the product released. The mass recovery calculations may be affected by variations in the specific gravity of hydrocarbon released, age of release, activity of aerobic and/or anaerobic processes, and site specific geochemical factors.

The cumulative air flow measurements for the MDPE event were calculated using a combination of field data measurements and Preso® B+ manufacturer provided formulas. Air flow rates extracted from the recovery wells averaged 271.45 SCFM during the event.

### Vacuum to Jal 14 Inch Mainline 3 – 700376.128.04 - SRS# 2003-00117 – Event 4 – 12 Hour

A portion of the extracted air flow rates measured is attributable to compressed air, which was "injected" into the extraction wells. This "injected" air is introduced into the extraction wells for the purpose of enhancing liquid recovery rates.

### B. Air Quality

Two influent air samples were collected during the event. These samples were submitted for laboratory testing in order to compare the predicted vapor concentrations (based on field-screening or calculated based on fuel consumption) to the actual vapor concentrations. The maximum influent concentration was recorded as 17,120 ppmv for Hydrocarbon Composition. Laboratory analytical results can be found in Attachment 2.

### C. Waste Management and Disposition

A cumulative total of 1,621 gallons of fluid were generated during this event. The fluids were transferred to an on-site storage tank prior to being hauled to an authorized disposal facility. A copy of the disposal ticket can be found in Attachment 4.

### **II. SYSTEM OPERATION DATA AND MASS RECOVERY CALCULATIONS**

### Formulae:

Concentration (C\_mg/l) =  $\underline{C_ppmv \ x \ Mol. \ wt. \ in \ mg(estimated) \ x \ 1000 \ x \ 0.000001}$ 0.0821 x Temp (K)

Recovery Rate (lbs/hr) =	(C_mg/l) x 2.2 x (Flowrate) x 60 x 28.32
	1,000,000

Recovery (lbs) = (lbs/hr) x (hrs)

Correction Factor (CF) =	FID Reading(ppmv)
	FID Reading at Time of Laboratory Analysis

<u>8.34 lbs</u>	x 0.82 average specific gravity of light crude =	6.84 lbs light crude
gallon water	(estimated)	gallon

Table 1 System Operation Data and Mass Recovery Calculations

Time	Period (hours)	Influent Temp. (*9	Vacuum (In. hg)	Vacuum (in. h20)	Differential pressure (in. h20)	Flow (SCFM)	FID Readings (ppm)	Lab Result (ppmv)	Assigned Lab Result (ppmv)	Correction Factor (CF)	Adjusted Lab Result (ppmv)	Adjusted Lab Result (mg/L)	Recovery (Ibe/hr)	Recovery in Period (lbs)	Total Recovery (ibs)
20:30	0.5	58	13.5	183.72	106.1	269.94	50000	-	17120.00	1.22	20931	25.80	26.03	13.02	13.02
21:00	0.5	56	13.5	183.72	105.4	269.57	40897	17120.00	17120.00	1.00	17120	21.18	21.35	10.67	23.69
22:00		56	13	176.92	104.3	272.20	36721	-	17120.00	0.90	15372	19.02	19.35	19.35	43.04
23:00	1	54	13	176.92	101	268.38	29312	-	17120.00	0.72	12270	15.24	15.29	15.29	58.33
0:00	1	50	12.5	170.11	89.4	257.19	25555	- 1	17120.00	0.62	10698	13.39	12.88	12.88	71.21
1:00	1	50	12.5	170.11	81.5	245.57	19911	-	17120.00	0.49	8335	10.43	9.58	9.58	80.79
200	1	48	12.5	170.11	77.3	239.63	1178	-	17120.00	0.03	493	0.62	0.58	0.56	81.34
3:00	1	46	12	163.31	85.6	256.25	12511	-	7020.00	2.78	19358	23.90	22.90	22.90	104.24
4:00	1	48	11.5	156.50	91.7	268.36	10963	-	7020.00	2.42	16963	20.86	20.93	20.93	125.16
5:00	1	48	11	149.70	99.6	283.45	8174		7020.00	1.80	12647	15.55	16.48	16.48	141.64
6:00	1	50	11	-149.70	110.1	297.43	6218	-	7020.00	1.37	9621	11.79	13.10	13.10	154.75
7:00	1	50	11	149.70	113.4	301.85	4537	7020.00	7020.00	1.00	7020	8.60	9.70	9.70	164 45
8:00	1	50	11	149.70	111.3	299,04	4319		7020.00	0.95	6683	8.19	9.15	9.15	173.60
verages:		51.08	12.15	165.40	98.21	271.45	19253.54			PSH Mass Re	covered in Vaj		Total	173.60 25.38	gallons

### FID maximum Concentration = 50,000 PPM

Ex: Conversi	on from ppm	to mg/L (inf	luent 1)			
Measured Conc.	Molecular WL	Pressure	Gas Constant	Temp.	Temp.	Conc.
(ppmv)	(Grams)	(atm)	(atm.liter/K.mole)	(F)	(K)	( C_mg/l)
20931	29.0857	1	0.0821	58	287.444444	2579990347

### Inputs are the green values. Calculated values are yellow.

Constante are purple values.

as are the blue values.

Liquid-phase Hydrocarbon Recovery [] \* r2 \* h = volume

Gallons removed determined at time of pick up

PSH Volume in Gallons= PSH Mass in Pounds=

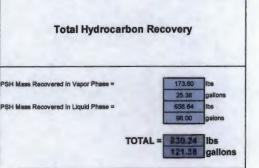
96 656 64

	% Vol. Hydrocarbon to pp	max Influent			Molecula	r Weight Calculations		
	% vol. Hydrocarbon to pp	my - imineur	1		component	Molecular Weight (g/mol)	mol%	
Compound	Molecular Weight (g/mol)	% Vol	=	ppmv	Nitrogen (N2)	28.016	94.845	
Methane (CH4)	16.04	0		0.00	Methane (CH4)	16.0425	0.0000	
Ethane (C2H6)	30.07	0		0.00	Carbon Dioxide (CO2)	44.011	4.5470	
Propane (C3H8)	44.10	0.023		230.00	Ethane (C2H6)	30,069	0.0000	
Iso-Butane (C4H10)	58.12	0.036		360.00	Propane (C3H8)	44.0956	0.0150	
N-Butane (C4H10)	58.12	0.13		1300.00	Iso-Butane (C4H10)	58.1222	0.0180	
Iso-Pentane (C4H12)	72.15	0.201		2010.00	N-Butane (C4H10)	58.1222	0.0650	
N-Pentane (C5H12)	72.15	0.181		1810.00	Iso-Pentane (C4H12)	72,1488	0.0810	
Hexane+ (C6H14)	97.40	1.141		11410.00	N-Pentane (C5H12)	72.1488	0.0730	
			Total	17120.00	Hexane+	97.3966	0.3560	
*Hexane+ is treat	ed as 60% hexanes, 30 % heptar	nes, and 10 % oc	tanes, as suc	th its		Total	100	
(0.6	*93.1887)+(0.3*100.2019)+(0.1*1	114.2285) = 97.3	966			Calculated MW	29.085	
			-		Molecula	r Weight Calculations		
	% Vol. Hydrocarbon to pp	my - Influent	2	the second	component	Molecular Weight (g/mol)	mol%	
Compound	Molecular Weight (g/mol)	% Vol	=	ppmv	Nitrogen (N2)	28.016	97.861	
Methane (CH4)	16.04	0		0.00	Methane (CH4)	16.0425	0.0000	
Ethane (C2H6)	30.07	0		0.00	Carbon Dioxide (CO2)	44.011	1.9040	
Propane (C3H8)	44.10	0.006		60.00	Ethane (C2H6)	30.069		
Propane (C3H8) Iso-Butane (C4H10)		0.006					0.0000	
Iso-Butane (C4H10) N-Butane (C4H10)	44.10 58.12 58.12			60.00 100.00 350.00	Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10)	30.069 44.0956 58.1222	0.0000	
Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12)	44.10 58.12	0.01		60.00 100.00	Ethane (C2H6) Propane (C3H8)	30.069 44.0956	0.0000	
Iso-Butane (C4H10)	44.10 58.12 58.12	0.01 0.035		60.00 100.00 350.00	Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10)	30.069 44.0956 58.1222	0.0000	
Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12)	44.10 58.12 58.12 72.15	0.01 0.035 0.056		60.00 100.00 350.00 560.00	Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10)	30.069 44.0956 58.1222 58.1222	0.0000 0.0040 0.0050 0.0170 0.0220	
Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12) N-Pentane (C5H12)	44.10 58.12 58.12 72.15 72.15	0.01 0.035 0.056 0.058	Total	60.00 100.00 350.00 560.00 580.00	Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12)	30.069 44.0956 58.1222 58.1222 72.1488	0.0000 0.0040 0.0050 0.0170 0.0220 0.0230 0.1640	
Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12) N-Pentane (C5H12) Hexane+ (C6H14)	44.10 58.12 58.12 72.15 72.15	0.01 0.035 0.056 0.058 0.537		60.00 100.00 350.00 560.00 580.00 <u>5370.00</u> <b>7020.00</b>	Ethane (C2H6) Propane (C3H8) Iso-Butane (C4H10) N-Butane (C4H10) Iso-Pentane (C4H12) N-Pentane (C5H12)	30.069 44.0956 58.1222 58.1222 72.1488 72.1488	0.0000 0.0044 0.0056 0.0177 0.0226 0.0236	

sum (Individual component MW x their reported mol%) Calculated MW=

opmv=

% Vol x 10,000



Vacuum to Jal 14 Inch Mainline 3 - 700376.128.04 - SRS# 2003-00117 - Event 4 - 12 Hour

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ATTACHMENT 1 MDPE Field Logs

					MDPE FIE	LD NOTES	3			
Site Name	e:	Vac to Jal	14 Inch #3	3				Event #:	4	
Location:		Eunice, NI	М					Arrive at site:	4/23/2013 18:00	
Date:		4/23-24/13	3							
Job#:		700376.12	28.04		SRS#:	2003-001	17	Start Vac:	4/23/2013 20:00	
Phase:		MDPE4			Unit:	1107		Stop Vac:	4/24/2013 8:00	
Onsite Pe	rsonnel:	L. Bridges	& B. Hunti	ington				Leave Site:	4/24/2013 9:30	
					GAUGIN	IG DATA				
WELL#		BEFORE			AFTER			COMMEN	ITS	
	PSH	GW	PSH-T	PSH	GW	PSH-T				
RW-1	49.29	49.95	0.66	-	50.10	-	Stinger set @ 5	50'		
RW-2	49.61	49.86	0.25	N	lot Gauge	d				
RW-3	50.15	50.46	0.31	-	50.33	-	Stinger set @ 5	50'		
RW-4	48.63	49.48	0.85	-	49.41	-	Stinger set @ 5	50'		
RW-5	49.11	52.16	3.05	-	50.67	-	Stinger set @ 5	50'		
MW-1	50.82	51.06	0.24	N	lot Gauge	11				
WASTE:	H2O:	1525		PSH:	96		TOTAL (GAL):	1621		
Sample		Ana		Date:		me:	Comments:			
INFLU	ENT 1	Ce	5+	4/23/2013	21:00		FID = 40897			

-1	oampie Mame	Principala	Date.	11110.	Comments.
[	INFLUENT 1	C6+	4/23/2013	21:00	FID = 40897
	INFLUENT 2	C6+	4/24/2013	7:00	FID = 4537
ſ					
ſ					

Notes: Tank #1 = Total fluids at 63 inches. PSH at 59.25 inches= 1,621 total gallons with 96 gallons of PSH

Start Date:	4/23/2013		MDPE FIELD DATA									
			Well Flow					Well Data				
TIME	SAMPLE	Inflent temp.	Diff.	Vac	FID	Propane	EXHAUST			COMMENTS:		
	TAKEN	(°f)	Pressure	(In.Hg)	Composite	Tank	TEMP F	RW-1	RW-3	RW-4	RW-5	$\searrow$
			(INH20)		(PPM)	(%-size)		VAC (INH2O)				
	*		2" Preso			500 Gal.				VAC (INT20)	VAC (IN120)	VAC (INH2O)
20:30		58	106.1	13.5	>50000	85	1412	10.3	24.1	23.6	26.7	>
21:00	*	56	105.4	13.5	40897	82	1409	12	26.6	24.2	29.5	> <
22:00		56	104.3	13	36721	79	1415	8.6	25.3	22.3	27.3	$>\!$
23:00		54	101	13	29312	76	1412	9.7	24.6	20.4	24.1	>
0:00		50	89.4	12.5	25555	74	1411	10.5	23.5	18.8	21.8	>>
1:00		50	81.5	12.5	19911	72	1413	9.6	21.7	16	22.3	>
2:00		48	77.3	12.5	1178	70	1409	9	19.8	13.9	22.7	$>\!$
3:00		46	85.6	12	12511	68	1413	11.5	18.5	15.9	20.6	$\searrow$
4:00		48	91.7	11.5	10963	66	1411	13.6	17.1	18.7	19.3	$\searrow$
5:00		48	99.6	11	8174	64	1408	18.7	16.9	20	16.5	$\searrow$
6:00		50	110.1	11	6218	62	1410	20.4	15.7	21.6	14.9	>
7:00	*	50	113.4	11	4537	60	1413	21.6	14.3	23.7	13.4	> <
8:00		50	111.3	11	4319	58	1411	21.9	13.8	24.1	12.9	> <

### Soil Vacuum Influence

Observation Well	MW-1
Extraction Well (EW)	RW-1
Time:	In. H2O
21:00	0
7:00	0

Vacuum to Jal 14 Inch Mainline 3 – 700376.128.04 - SRS# 2003-00117 – Event 4 – 12 Hour

## ATTACHMENT 2

Laboratory Analytical Results



### **Certificate of Analysis**

Number: 1030-2013040736-001A

May 03, 2013 Simon I. Walshe, CAPM Talon/LPE 921 N. Bivins St. Amarillo Texas 79107 Sample ID: Sampled By: LB Station Name : influent #1 Sample Of: Gas Spot Station Number : 700376.128.04

Station Location : Eunice, NM. Vac to Jal 14" #3 Sample Point:

Sample Date: 04/23/2013 21:00 Sample Conditions: N.G. Pres., N.G. Temp. PO / Ref. No:

### ANALYTICAL DATA

Components	Moi %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	JD	5/2/2013 10:04:15 AM
Nitrogen	94.845	91.404				
Carbon Dioxide	4.547	6.884				
Propane	0.015	0.023	0.004			
Iso Butane	0.018	0.036	0.006			
n-Butane	0.065	0.130	0.020			
Iso Pentane	0.081	0.201	0.029			
n-Pentane	0.073	0.181	0.026			
Hexanes Plus	0.356	1.141	0.154			
	100.000	100.000	0.239			
	C2 +	C3 +	iC5 +			
GPM TOTAL :	0.239	0.239	0.209			
Relative Density	Real Gas			1.0036		
Calculated Molecular	Weight			29.07		
Compressibility Facto	r			0.9996		
GPA 2172-09 Calculation						
Calculated Gross BT	U per ft <sup>3</sup> @14.650	psia & 60°F				
Real Gas: Dry BT			27			
Water	Sat. Gas_Base BTL Mol% - 1.75_Wt%		27			

Stally 22.

Hydrocarbon Laboratory Manager

**Quality Assurance:** 

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated

ROUSTON LABORATORIES SULL NERVER OFF SULL NERVER SELECTOR SULL NERVER SECOND



HOUSTON LABORATORIA actor NIERC - MIEBORIA HOUSTON, TEMISITTAN PHONE CHISI BOUT

### **Certificate of Analysis**

Number: 1030-2013040736-002A

May 03, 2013 Simon I. Walshe, CAPM Talon/LPE 921 N. Bivins St. Amarillo Texas 79107 Sampled By: LB Sample ID: Sample Of: Station Name : Gas Influent #2 Spot Station Number : 700376.128.04 Sample Date: 04/24/2013 07:00 Station Location : Eunice, NM. Sample Conditions: N.G. Pres. N.G. Temp. Vac to Jal 14" #3 PO / Ref. No: Sample Point:

### **ANALYTICAL DATA**

Components	Mol %	Wt %	GPM at 14.650 psia	Method	Lab Tech.	Date Analyzed
				GPA-2261 M	JD	5/2/2013 10:23:54 AM
Nitrogen	97.861	96.353				
Carbon Dioxide	1.904	2.945				
Propane	0.004	0.006	0.001			
Iso Butane	0.005	0.010	0.002			
n-Butane	0.017	0.035	0.005			
Iso Pentane	0.022	0.056	0.008			
n-Pentane	0.023	0.058	0.008			
Hexanes Plus	0.164	0.537	0.071			
	100.000	100.000	0.095			
	C2 +	C3 +	iC5 +			
GPM TOTAL :	0.095	0.095	0.087			
Relative Density	Real Gas			0.9822		
Calculated Molecular	Weight			28.45		
Compressibility Factor				0.9997		
GPA 2172-09 Calculatio						
Calculated Gross BT		psia & 60°F				
Real Gas: Dry BT			11			
•	Sat. Gas_Base BT	J:	11			
Comments : H2O	Mol% - 1.75_Wt%	- 1.115				

Stally

Hydrocarbon Laboratory Manager

Quality Assurance:

The above analyses are performed in accordance with ASTM, UOP or GPA guidelines for quality assurance, unless otherwise stated

SPL, Inc. Analysis Request Chain of Custody Record

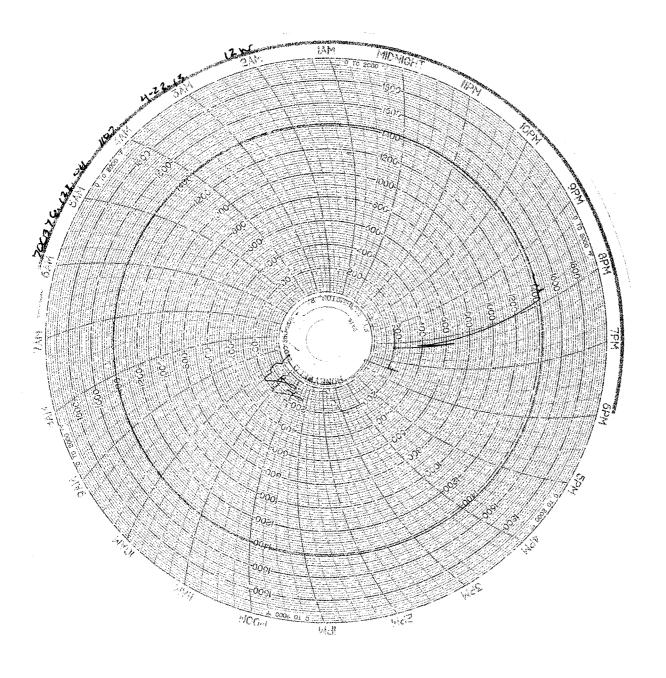
IPL					SPL Work Order No.:					Acct.	Acct. Mate Code:						Dept. Code			SPL						
					**************************************					NEEDS CLIENT CODE										Page 1	of 1					
Report To: (Company Name):	Talon/LPE, Ltd.					Project/Station Name: Project/St					ation Number: Project/State					tion Location:						sted TAT				
Address:	ress: 921 N. Bivins St.						Infleent Soit Vapor- 700371				0376	128.04 Var. to								3						
				Special Instructions: Vacto Jul 14" # 3					3				Ēus	-, -, -,	Nn	<b>`</b>										
City/State/Zip: Amarillo TX 79107																	10 busir	ness days								
Contact:							Indicate Billing Type: Net 30 day Acct.					Check #														
	806-350-8872 Fax: 806-467-0622					(Place "X", where appropriate) Credit Card					Contact SPL, Inc for CC payment a								aemer	nts.		:				
Invoice To:											Requested Analysis										es May Apply e for details)					
(Company Name):											(Place an "X" next to Sample ID below)															
Address:	921 N. Bivins	s St.					Terms: Cylinders will be rented for																			
							S10/cyl. All cylinders checked out are to be returned within 21 days.																			
City/State/Zip:	Amarillo			TX		107	whether the																			
Contact:			the second se				Cyfinders no will be con	l Š																		
Client PO# or Ref. No.:	806-467-060	1	Fax: N/A	000-	372-66	03	billed at cu	61-																		
Contract/Proposal #:		e Di	_Q5270				1			1-22	-23															
(i.e. SPLQ####	·	371								GPA-2261-C6+																
	0		Sample	ate	site	_	Cylind	der Tracking Info																		
Sample ID (used to log/track sample)	Sample Date	Sample Time	Type (Gas/Liq.	Duplicate	Composite	Spot	Cylinder #	Date Out	Date In	1		·										Cor	ments			
(used to tograden semiple)	Dute	1 mile	/Solid)	B	ð		Cyandes #	Date Out	Date in														initenta			
I-flut#1	4-23-13	2100	GAS							X																
I.flat#2	4-24.13	0760	b							X																
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Vacuum to Jal 14 Inch Mainline 3 – 700376.128.04 - SRS# 2003-00117 – Event 4 – 12 Hour

ATTACHMENT 3 Oxidizer Charts



Vacuum to Jal 14 Inch Mainline 3 - 700376.128.04 - SRS# 2003-00117 - Event 4 - 12 Hour

ATTACHMENT 4 Waste Ticket NA HOUR SERVICE, GALL SE DVINDTON 456-4940 DATUM 308-4950

GANDY CORPORATION LOUBSTOLVER MEDICORDER REAL FROMES - VACUUM TROCKS - WINCH TRUCKS MAR GREANING - ROUSTABOLITING PROMINES

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