

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

Type Test ☒ Initial ☐ Annual ☐ Special		Test Date 6-26-87	
Company Amoco Production Company		Connection	
Pool Bravo Dome		Formation Tubb	
Completion Date 4-29-81		Total Depth 2802	Plug Back TD 2761
		Elevation 4542	Unit BDCDGU
Csg. Size 5.50	Wt. 14	d 4.9	Set At 2802
Perforations: From 2141 To 2188		Well No. 1935-111G	
Tub. Size 2.875	Wt. 6.5	d 2.441	Set At 2138
Perforations: From To		Unit G 11 19 35	
Type Well - Single - Standhead - G.G. or G.O. Multiple Single		Packer Set At 2100	County Union
Producing Thru Tubing	Reservoir Temp. °F 90	Mean Annual Temp. °F 50	Baro. Press. - P _g 12.25
State New Mexico			
L	H	Cg	% CO ₂ 100
			% N ₂ 0
			% H ₂ S. 0
Prover		Meter Run 4.0	Taps Flange

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
1.	4.026 x	1.50		218	31	60	219	60	0		24 hrs
2.	4.026 x	1.50		228	26	62	228	62	0		24 hrs
3.	4.026 x	1.50		243	15	61	244	61	0		24 hrs
4.	4.026 x	1.50		259	1	60	258	60	0		24 hrs
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor F _t	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcd
1.							778
2.							736
3.							563
4.							245
5.							

NO.	P _t	Temp. °R	Z	Gas Liquid Hydrocarbon Ratio	Mcf/bbl.
1.				0	
2.					
3.					
4.					
5.					

A.P.I. Gravity of Liquid Hydrocarbons _____ Deg. Specific Gravity Separator Gas 1.529 Specific Gravity Flowing Fluid XXXXX Critical Pressure 1072 P.S.I.A. Critical Temperature 496 R			
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$P_c = 287.25$ $P_c^2 = 82,512$	$(1) \frac{P_c^2}{P_c^2 - P_w^2} = 2.7974$	$(2) \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.7054$																														
<table border="1" style="width: 100%; border-collapse: collapse;"> <tr> <th>NO.</th> <th>P_t²</th> <th>P_w</th> <th>P_w²</th> <th>P_c² - P_w²</th> </tr> <tr> <td>1.</td> <td></td> <td>230.25</td> <td>53,015</td> <td>29,496</td> </tr> <tr> <td>2.</td> <td></td> <td>240.25</td> <td>57,720</td> <td>24,792</td> </tr> <tr> <td>3.</td> <td></td> <td>255.25</td> <td>65,152</td> <td>17,359</td> </tr> <tr> <td>4.</td> <td></td> <td>271.25</td> <td>73,576</td> <td>8,935</td> </tr> <tr> <td>5.</td> <td></td> <td></td> <td></td> <td></td> </tr> </table>	NO.	P _t ²	P _w	P _w ²	P _c ² - P _w ²	1.		230.25	53,015	29,496	2.		240.25	57,720	24,792	3.		255.25	65,152	17,359	4.		271.25	73,576	8,935	5.					$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2104$	
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1.		230.25	53,015	29,496																												
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Absolute Open Flow 2104 Mcld @ 15.025	Angle of Slope @ 44.0537	Slope, n 0.9675
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Remarks: Test was run from a low flowing tubing pressure to a high flowing tubing pressure to minimize liquid loading effects.

Approved by Commission:	Conducted by: RANDY MAHANNAH	Calculated by: RICHARD ROETH	Checked by:
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