

**NEW MICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL**

c/SF
Form C-122 F.1e
Revised 9-1-65

RECEIVED

Type Test ☐ Initial ☐ Annual ☐ Special						Test Date 12/23/82		JAN 21 1983	
Company Samedan Oil Corp.						Connection Air		O. C. D.	
Pool <i>Poco Hays W/O</i>						Formation Abo		ARTESIA OFFICE	
Completion Date 12/7/82 12-24-82		Total Depth 4650		Flow back To 4600		Elevation 3699.4		Turn of Lease Time State 16	
Coq. Size 4 1/2	Wt. 9.5	d	Set At 4650	Perforations: From 4198 To 4216		Well No. 4		Unit 16	
Tiq. Size 2 1/16	Wt. 3.25	d	Set At 4500	Perforations: From To		Unit 16		Twp. 7s Rge. 26E	
Type well - Single - Provenhead - G.G. or G.O. Multiple Dual						Packer Set At 4500		County Chaves	
Producing Thru Csg.		Reservoir Temp. °F 116 @ 4207		Mean Annual Temp. °F 60		Baro. Press. - P _a 13.2		State N.M.	
L 4207	H 4207	Gg .6692	% CO ₂ 2.85	% N ₂ 5.061	% H ₂ S	Prover	Meter Run 4	Taps Flg.	

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. hw	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							978				
1.	4 x 1.250			265	8.0	97	935				1 hr.
2.	4 x 1.250			250	17.0	100	900				1 hr.
3.	4 x 1.250			250	42.0	100	815				1 hr.
4.	4 x 1.250			270	95.0	90	610				1 hr.
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mscf/d
1	7.469	47.18	278.2	.9662	1.223	1.020	425
2	7.469	66.89	263.2	.9636	1.223	1.019	600
3	7.469	105.14	263.2	.9636	1.223	1.019	943
4	7.469	164.02	283.2	.9723	1.223	1.021	1487
5							

NO.	P _t	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	A.P.I. Gravity of Liquid Hydrocarbons	Specific Gravity Separator Gas	Specific Gravity Flowing Fluid	Critical Pressure	Critical Temperature
1.	.41	557	1.53	.961	dry		.6692		672	363
2.	.39	560	1.54	.964						
3.	.39	560	1.54	.964						
4.	.42	550	1.52	.959						
5.										

NO.	P _c	P _w	P _c ²	P _w ²	P _c ² - P _w ²
1	991.2	982.5	982400	965200	17200
2					
3					
4					
5					

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.699$		(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.399$	
$ADP = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.081$			

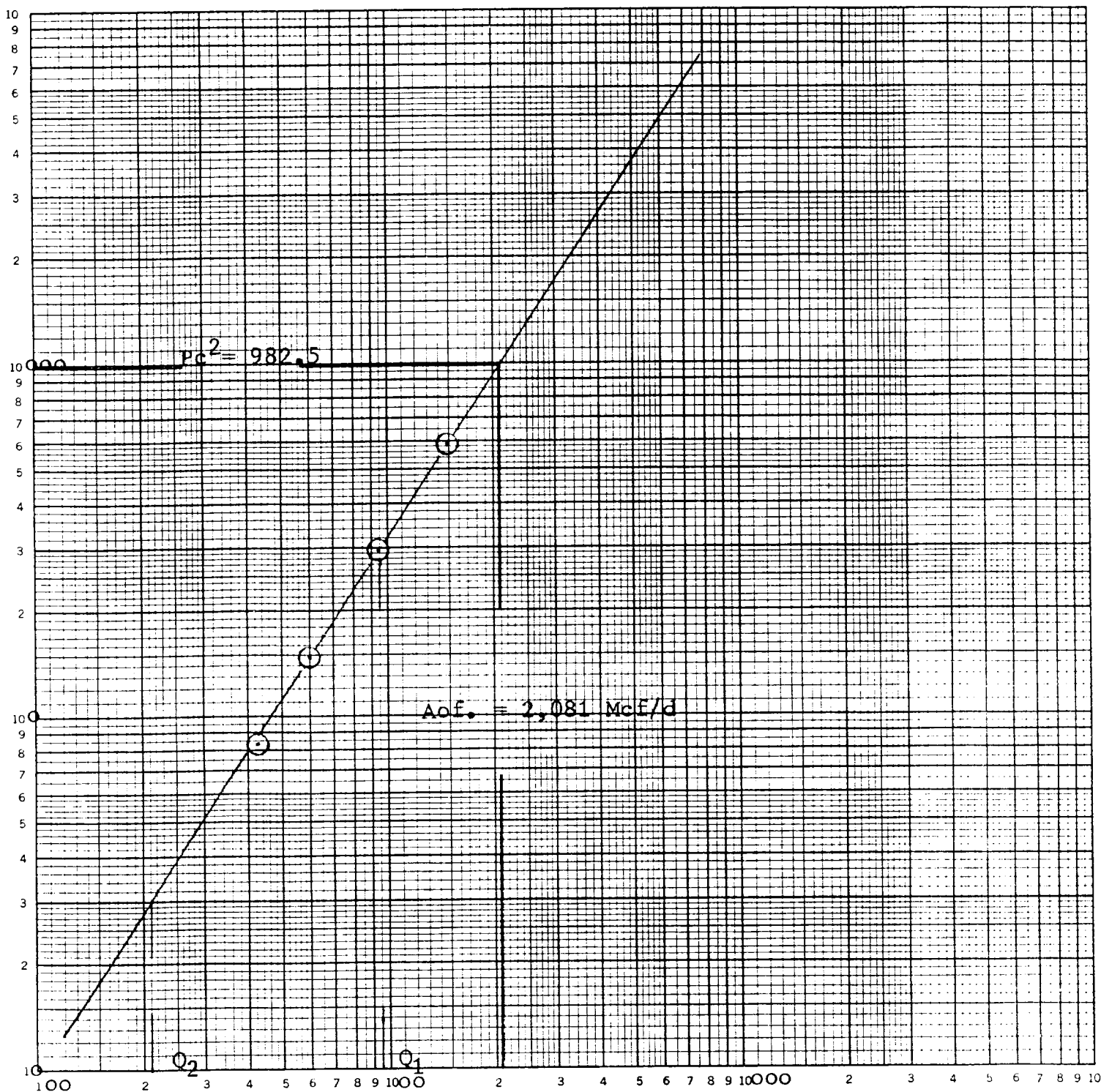
Absolute Open Flow 2,081	Mold @ 15.025	Angle of Slope 56.75	Slope, n .656
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Remarks:			
Approved By: _____	Conducted By: _____	Calculated By: _____	Checked By: _____
Davis Services, Inc. Rick Pagan			

COMPANY: SAMEDAN OIL CORP.
 CASE : STATE 16
 WELL NO.: 4
 LOC. : SEC. 16 TWP. 7s RGE. 26e
 DATE : 12/23/82

46 7403

LOGARITHMIC 3 X 3 CYCLES
 KEUFFEL & ESSER CO. MADE IN U.S.A.



$$\begin{aligned}
 Q_1 \text{ Log } 950 &= 2.977724 \\
 Q_2 \text{ Log } 210 &= 2.322219 \\
 n &= .6555 \\
 \theta &= 56.75
 \end{aligned}$$

WORKSHEET FOR CALCULATION OF STATIC COLUMN WELLHEAD PRESSURE (P_w)
 COMPANY Samedan Oil Corp. LEASE State 16 WELL NO. 4 DATE 12/23/82

 LOCATION: Unit P Section 16 Township 7s Range 26 E
L 4207 H 4207 L/H 1.000 G .6692 % CO₂ 2.85 % N₂ 5.061 % H₂S

 d Annulus F_r.0071790 GH 2815 P_{Cr} 672 T_{Cr} 363

TABLE IX & X

LINE	1st Rate			2nd Rate			3rd Rate			4th Rate	
	1st	2nd	1st	2nd	1st	2nd	1st	2nd	1st	2nd	
1 Q_m	.425	.425	.600	.600	.943	.943	.943	.943	1.487	1.487	
2 T_w (W.H. °R)	534	534	534	534	534	534	534	534	534	534	
3 T_s (B.H. °R)	576	576	576	576	576	576	576	576	576	576	
4 $T = \frac{T_w + T_s}{2}$	555	555	555	555	555	555	555	555	555	555	
5 Z (Est.)	.867	.860	.871	.865	.882	.876	.908	.903			
6 TZ	481.2	477.3	483.4	480.1	489.5	486.2	503.9	501.2			
7 GH/TZ	5.850	5.898	5.823	5.864	5.751	5.790	5.586	5.617			
8 e^s (Table XIV)	1.245	1.248	1.244	1.246	1.241	1.243	1.233	1.234			
9 $1 - e^{-s}$ (Table XIV)	.197	.198	.196	.197	.194	.195	.189	.190			
10 P_t	948.2	948.2	913.2	913.2	828.2	828.2	623.2	623.2			
11 $P_t^2/1000$	899.1	899.1	833.9	833.9	685.9	685.9	388.4	388.4			
12 F_r (Table XV)	.0071790	.0071790	.0071790	.0071790	.0071790	.0071790	.0071790	.0071790			
13 $F_c = F_r TZ$	3.454	3.427	3.470	3.466	3.514	3.490	3.618	3.598			
14 $F_c Q_m$	1.468	1.456	2.082	2.068	3.314	3.291	5.380	5.350			
15 $L/H (F_c Q_m)^2$	2.155	2.121	4.336	4.276	10.982	10.833	28.941	28.623			
16 $F_w = L/H (F_c Q_m)^2 (1 - e^{-s})$	.425	.421	.851	.844	2.130	2.114	5.469	5.436			
17 $P_w^2 = P_t^2 + F_w$	899.5	899.5	834.8	834.8	688.0	688.0	393.8	393.8			
18 $P_s^2 = e^s P_w^2$	1120.2	1122.2	1038.5	1040.1	853.6	854.9	485.6	486.1			
19 P_s	1058.4	1059.3	1019.1	1019.8	923.9	924.6	696.9	697.2			
20 $P = \frac{P_t + P_s}{2}$	1003.3	1003.8	966.1	966.5	876.1	876.4	660.0	660.2			
21 $P_r = (P/P_{cr})$	1.49	1.49	1.44	1.44	1.30	1.30	.98	.98			
22 $T_r = (T/T_{cr})$	1.53	1.53	1.53	1.53	1.53	1.53	1.53	1.53			
23 Z (Table XI)	.860	.860	.865	.865	.876	.876	.903	.903			

NEW-TEX LAB

PHONE 505/393-3581

P. O. BOX 1161

611 W. SNYDER

HOBBS, NEW MEXICO 88240

ANALYSIS CERTIFICATE

CLIENT: DAVIS SERVICES INC
ADDRESS: P O BOX 2033
CITY, STATE: HOBBS NM 88240

ANALYSIS NUMBER: 8912
DATE OF RUN: 12/23/82
DATE SECURED: 12/23/82

SAMPLE IDENT: SAMEDAN OIL - STATE 15 #1
SAMPLING PRESS: SAMPLING TEMP:

***** GAS ANALYSIS *****

	MOLE PERCENT	GAL/ MOF
NITROGEN	5.061	
CARBON DIOXIDE	2.850	
METHANE	84.190	
ETHANE	4.603	1.228
PROPANE	1.711	0.470
ISO-BUTANE	0.306	0.100
NORMAL BUTANE	0.596	0.187
ISO-PENTANE	0.189	0.069
NORMAL PENTANE	0.212	0.077
HEXANES	0.127	0.052
HEPTANES PLUS	0.155	0.071
TOTAL	100.000	2.154

PROPANE GRM: 0.47 BUTANES GRM: 3.17
ETHANE GRM: 1.23 PENTANES PLUS GRM: 0.27

SPECIFIC GRAV (CALC): 3.6892
MOLE WEIGHT: 19.40

TEMPERATURE (°F)	PRESSURE (PSIA)	WET	D6
14.696	1017	1233	
14.650	1014	1231	
14.730	1019	1233	
14.735	1020	1233	