

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

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Form C-123
Revised 9-1-65

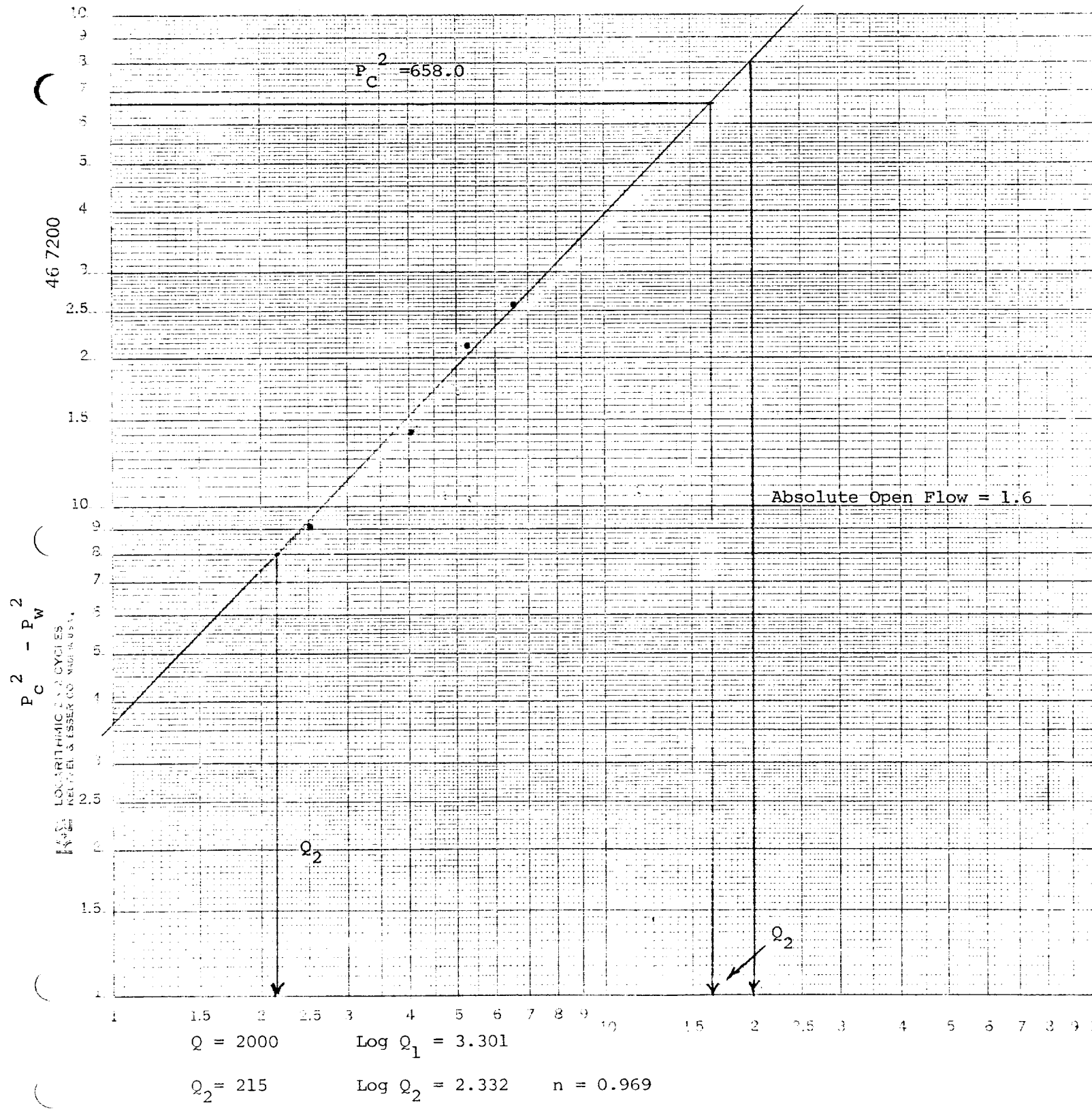
APR 17 1984

O. C. D.

ARTESIA, OFFICE

Type Test		☒ Initial		☐ Annual		☐ Special		Test Date		APR 17 1984																																																																																															
Company GETTY OIL COMPANY ✓				Connection NONE				Unit																																																																																																	
Pool PECOS SLOPE ABO				Formation ABO				Farm or Lease Name GETTY P.S. 18 FEDERAL																																																																																																	
Completion Date 4-11-84		Total Depth 4200'		Plug Back TD 4156'		Elevation 3746.1 3755.7		Well No. 1																																																																																																	
Csg. Size 4.5	Wt. 10.5	d 4.052	Set At 4200'	Perforations: From 3780 To 3978		Unit 1		Sec. 18		Twp. 6S																																																																																															
Tbg. Size 2 3/8	Wt. 4.7	d 1.995	Set At 3744'	Perforations: From Open To Ended		Age. 26E		County Chaves		State New Mexico																																																																																															
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single				Packer Set At None				Prover Meter Run 3"																																																																																																	
Producing Thru Tbg. L 3744		Reservoir Temp. °F 101° 4200		Mean Annual Temp. °F 60		Baro. Press. - P _a 13.2		Prover -		Tape Flange																																																																																															
<table border="1"> <thead> <tr> <th colspan="6">FLOW DATA</th> <th colspan="2">TUBING DATA</th> <th colspan="2">CASING DATA</th> <th rowspan="2">Duration of Flow</th> </tr> <tr> <th>NO.</th> <th>Prover Line Size</th> <th>X</th> <th>Orifice Size</th> <th>Press. p.s.i.g.</th> <th>Diff. h_w</th> <th>Temp. °F</th> <th>Press. p.s.i.g.</th> <th>Temp. °F</th> <th>Press. p.s.i.g.</th> <th>Temp. °F</th> </tr> </thead> <tbody> <tr> <td>SI</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>82°</td> <td>798</td> <td>82°</td> <td>797</td> <td>82°</td> <td></td> </tr> <tr> <td>1.</td> <td>3" x 7/8</td> <td></td> <td></td> <td>300</td> <td>68</td> <td>82°</td> <td>566</td> <td>82°</td> <td>620</td> <td>82°</td> <td>1.25</td> </tr> <tr> <td>2.</td> <td>3" x 7/8</td> <td></td> <td></td> <td>300</td> <td>44</td> <td>82°</td> <td>611</td> <td>82°</td> <td>654</td> <td>82°</td> <td>.75</td> </tr> <tr> <td>3.</td> <td>3" x 7/8</td> <td></td> <td></td> <td>300</td> <td>26</td> <td>82°</td> <td>667</td> <td>82°</td> <td>704</td> <td>82°</td> <td>.75</td> </tr> <tr> <td>4.</td> <td>3" x 7/8</td> <td></td> <td></td> <td>300</td> <td>10</td> <td>82°</td> <td>705</td> <td>82°</td> <td>740</td> <td>82°</td> <td>.75</td> </tr> <tr> <td>5.</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> </tr> </tbody> </table>												FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	SI						82°	798	82°	797	82°		1.	3" x 7/8			300	68	82°	566	82°	620	82°	1.25	2.	3" x 7/8			300	44	82°	611	82°	654	82°	.75	3.	3" x 7/8			300	26	82°	667	82°	704	82°	.75	4.	3" x 7/8			300	10	82°	705	82°	740	82°	.75	5.											
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1.	3" x 7/8			300	68	82°	566	82°	620	82°	1.25																																																																																														
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5.																																																																																																									
RATE OF FLOW CALCULATIONS																																																																																																									
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd																																																																																																		
1	3.657	145.94	313.2	.9795	1.218	1.030	655.8																																																																																																		
2	3.657	117.39	313.2	.9795	1.218	1.030	527.1																																																																																																		
3	3.657	90.24	313.2	.9795	1.218	1.030	405.7																																																																																																		
4	3.657	55.96	313.2	.9795	1.218	1.030	251.5																																																																																																		
5																																																																																																									
NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.		A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.																																																																																																		
1.	0.47	542	1.42	0.943	Specific Gravity Separator Gas 0.674		X X X X X X X X																																																																																																		
2.	0.47	542	1.42	0.943	Specific Gravity Flowing Fluid _____ X X X X X																																																																																																				
3.	0.47	542	1.42	0.943	Critical Pressure _____ 669 _____ P.S.I.A.		P.S.I.A.																																																																																																		
4.	0.47	542	1.42	0.943	Critical Temperature _____ 281 _____ R		R																																																																																																		
5.																																																																																																									
P _c 811.2		P _c 2 658.0																																																																																																							
NO.	P _r 2	P _w	P _w 2	P _c 2 - P _w 2	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 5.264$		(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 5.00$																																																																																																		
1		633.2	400.9	257.1																																																																																																					
2		667.2	445.2	212.8																																																																																																					
3		717.2	514.4	143.6																																																																																																					
4		753.2	567.3	90.7																																																																																																					
5																																																																																																									
Absolute Open Flow 1,650 Mcfd @ 15.025					Angle of Slope @ _____		Slope, n 0.969																																																																																																		
Remarks: Test was run from higher rates to lower rates due to well loading problems.																																																																																																									
Approved By Commission:			Conducted By: Manuel Martinez			Calculated By: Phil Smith		Checked By: Don Steinnud																																																																																																	

Post ID 2
5-18-84
Comp & BK



NEW-TEX LAB

PHONE 505/393-3561

P. O. BOX 1161

611 W. SNYDER

HOBBS, NEW MEXICO 88240

ANALYSIS CERTIFICATE

CLIENT: GETTY OIL CO
ADDRESS: BOX 730
CITY, STATE: HOBBS NM 88240

ANALYSIS NUMBER: 3000
DATE OF RUN: 04/12/84
DATE SECURED: 04/11/84

SAMPLE IDENT: GETTY P.S. 19 FEDERAL #1

SAMPLING PRESS: SAMPLING TEMP: _____

***** GAS ANALYSIS *****

	MOLE PERCENT	GAL/ MCF
NITROGEN	3.914	
CARBON DIOXIDE	4.604	
METHANE	84.397	
ETHANE	4.166	1.111
PROPANE	1.564	0.429
ISO-BUTANE	0.261	0.085
NORMAL BUTANE	0.509	0.160
ISO-PENTANE	0.171	0.062
NORMAL PENTANE	0.157	0.057
HEXANES	0.257	0.105
HEPTANES PLUS	0.000	0.000
TOTAL	100.000	2.009

PROPANE GPM:	0.43	BUTANES GPM:	0.24
ETHANE GPM:	1.11	PENTANES PLUS GPM:	0.22

SPECIFIC GRAV (CALC): 0.6740
MOLE WEIGHT: 19.52

HHV-BTU/CU FT	PRESSURE (PSIA)	WET	DRY
	14.696	999	1016
	14.650	995	1013
	14.730	1001	1019
	14.735	1001	1019

DEANE SIMPSON

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