

OIL CONSERVATION DIVISION

STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Form C-122
Revised 10-1-78

RECEIVED *cl SF*
File

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special					Test Date 12-9-87		JAN 26 1988				
Company McCLELLAN OIL CORP. ✓				Connection AIR		Unit O.C.D.					
Pool S. Pecos Sine Alito				Formation ABO		Unit AMERADA OFFICE					
Completion Date 12-7-87		Total Depth 4690		Plug Back TD 4641		Elevation 3790 GN		Farm or Lease Name PENJACK FED.			
Csg. Size 4 1/2	Wt. 10.5	d	Set At 4641	Perforations: From 4285 To 4428		Well No. 6					
Thq. Size 2 3/8	Wt.	d	Set At 4243	Perforations: From OPEN To ENDED		Unit L	Sec. 7	Twp. 10	Rye. 26		
Type Well - Single - Brdenhead - G.G. or G.O. Multiple SINGLE					Packer Set At NONE		County CHAVES				
Producing Thru TUBING		Reservoir Temp. °F 8		Mean Annual Temp. °F		Baro. Press. - P _g		State NEW MEXICO			
L	H	G _g	% CO ₂	% N ₂	% H ₂ S	Prover 2"	Meter Run	Taps			
		.62									
FLOW DATA					TUBING DATA		CASING DATA		Duration of Flow		
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							970		972		
1.	2	x	1/16	957		65	957		959		1 hr.
2.	2	x	1/8	913		66	913		915		"
3.	2	x	7/32	737		66	737		742		"
4.	2	x	5/16	425		66	425		519		"
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd				
1	.06045		970.2	.9952	1.27	1.0897	81				
2	.2648		926.2	.9952	1.27	1.0848	336				
3	.8393		750.2	.9943	1.27	1.0679	849				
4	1.6720		438.2	.9943	1.27	1.0385	961				
5.											
NO.	R ₁	Temp. °R	T ₁	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.					A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.	
1.					Specific Gravity Separator Gas _____ X X X X X X X X					Specific Gravity Flowing Fluid _____ X X X X X	
2.					Critical Pressure _____ P.S.I.A.					Critical Temperature _____ R	
3.											
4.											
5.											
P _c 1077.2	P _c ² 1160.36										
NO	P _i ²	P _w	P _w ²	P _c ² - P _w ²	(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.4187$	(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.2416$					
1		1056.2	1115.6	44	AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1193$						
2		1008.2	1016.5	144							
3		824.2	679.3	481							
4		585.2	342.5	818							
5											
Absolute Open Flow 1193 Mcfd @ 15.025					Angle of Slope @ 58.25		Slope, n .6188				
Remarks: ALL BOTTOM HOLE PRESSURES DONE WITH AMERADA TYPE GAUGE.											
Approved By Division			Conducted By: KELTIC SERVICE			Calculated By: MIKE KELLY			Checked By:		

*Post FD-2
1-1-88
comp + BK*

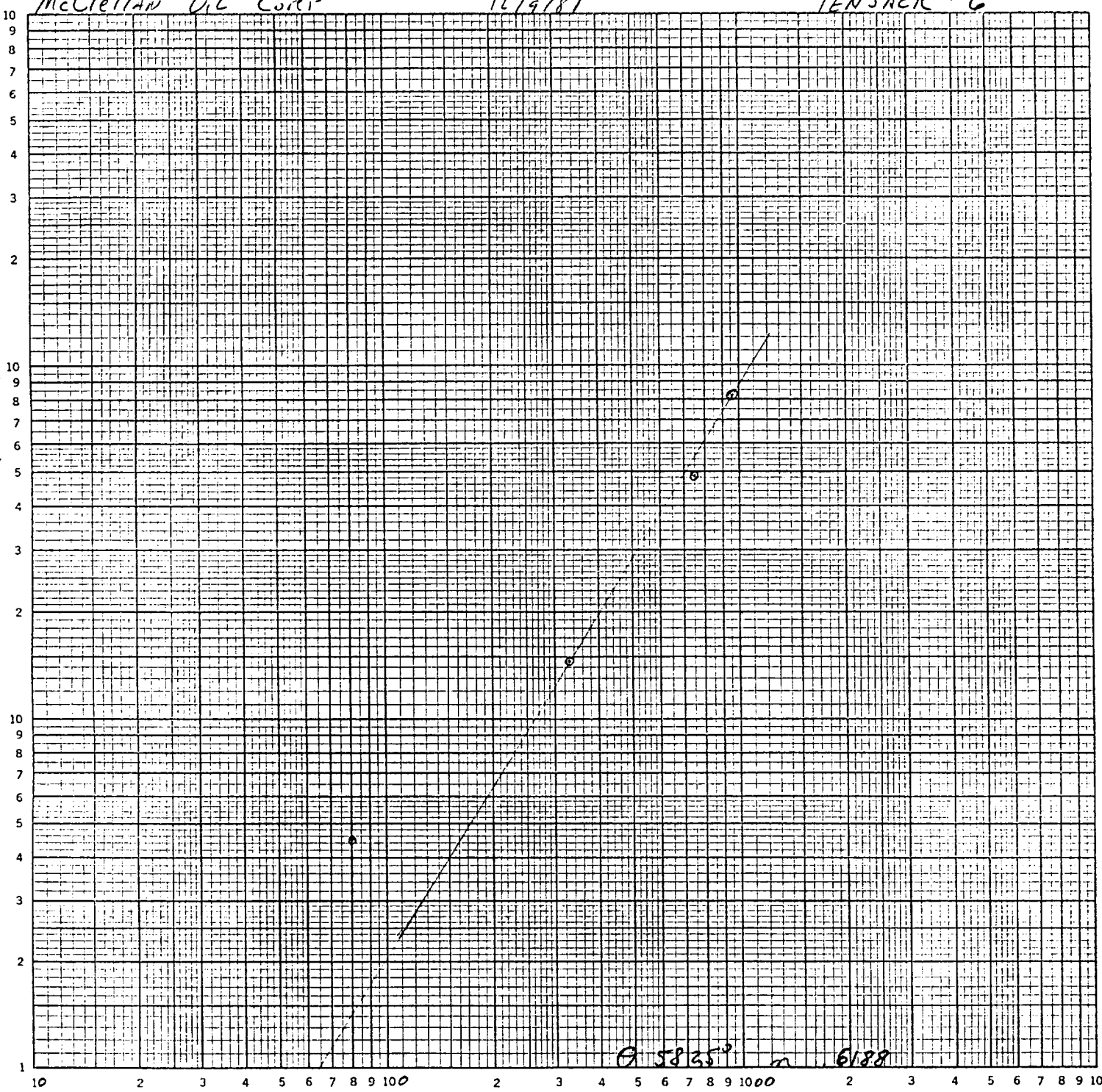
McClellan Oil Corp

12/9/87

PENJACK #6

$P^2 - P^2(000)$ 467400

K₀Σ LOGARITHMIC 3 X 3 CYCLES
KEUFFEL & ESSER CO. MADE IN U.S.A.



Q 5835' m 6188

Q
MSCFPD