Submit in duplicate to appropriate district office
See Rule 401 & Rule 1122

FEB 19 1992

State of New Mexico
Energy, Minerals and Natural Resources Department

OIL CONSERVATION DIVISION

P.O. Box 2088
P.B.R Regulatory Section Santa Fe, New Mexico 87504-2088

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MAR - 9 1992
O. C. D.
ARTESIA, OFFICE

Form C-122
Revised 4-1-91

dsf
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MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator: PHILLIPS PETROLEUM				Lease or Unit Name: Muskegon "17" State Com	
Type Test: [X] Initial [ ] Annual [ ] Special				Test Date: 2-14-92	Well No.: 1
Completion Date: 2/14/92	Total Depth: 10880'	Plug Back TD: 10756'		Elevation: 3614' GL	Unit Ltr. - Sec. - TWP - Rge.: N, Sec. 17 T17S R29-E
Csg. Size: 5½" / Wt.: 20# / d: / Set At: 10880'		Perforations: From: 10541' To: 10582'			County: Eddy
Tbg. Size: 2 7/8" / Wt.: / d: 2.441 / Set At: 10481'		Perforations: From: To:			Pool: S. Empire Morrow
Type Well - Single - Bradenhead - G.G. or G.O. Multiple: SINGLE		Packer Set At: 10468'			Formation:
Producing Thru: TUBING	Reservoir Temp. °F: 179 @ 10449	Mean Annual Temp. °F: 60°	Baro. Press - P_a: 13.2		Connection: TO AIR

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
*10445	10445	.670	2.34	.62			3.826	FLG

NO.	FLOW DATA: Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	TUBING DATA: Press. p.s.i.g.	Temp. °F	CASING DATA: Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							2579	63	PKR		90 HRS
1.	4	X	1.250	510	9"	95°	2275	66	" "		1 HR
2.	4	x	1.250	510	18"	93°	2129	67	" "		1 HR
3.	4	X	1.250	510	52"	70°	1852	68	" "		1 HR
4.	4	X	1.500	510	24"	91°	1602	68	" "		1 HR
5.											

RATE OF FLOW CALCULATIONS

NO.	COEFFICIENT (24 HOUR)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg.	Super Compress. Factor, Fpv.	Rate of Flow Q, Mcfd
1.	7.483	68.62	523.2	.9680	1.222	1.046	635
2.	7.483	97.04	523.2	.9697	1.222	1.046	900
3.	7.483	164.94	523.2	.9905	1.222	1.052	1572
4.	10.88	112.05	523.2	.9715	1.222	1.046	1514
5.							

NO.	P_r	Temp. °R	T_r	Z
1.	.77	555	1.46	.914
2.	.77	553	1.45	.914
3.	.77	530	1.39	.903
4.	.77	551	1.45	.914
5.				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons 57.1 @ 60 Deg.
Specific Gravity Separator Gas _____ XXXXXXXXX
Specific Gravity Flowing Fluid XXXXX _____
Critical Pressure 677 P.S.I.A. _____ P.S.I.A.
Critical Temperature 379 R _____ R

P_c 2848.8 P_c^2 8115.6

NO.	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1.		2610.6	6815.2	1300.4
2.		2468.4	6092.9	2022.3
3.		2199.5	4837.8	3277.8
4.		1929.4	3722.5	4393.1
5.				

1) $\frac{P_c^2}{P_c^2 - P_w^2}$ = 2.476 (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 2.476

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 3.892

Post ID-2
5-8-92
comp + BP

Absolute Open Flow 3,892 Mcfd @ 15.025 Angle of Slope θ 45 Slope, n 1.000

Remarks: *= BHP INSTRUMENT SET AT THIS DEPTH.
WELL MADE 2.8 BBLS 57.1 API CONDENSATE.

Approved By Division	Conducted By:	Calculated By:	Checked By:
	JOHN WEST ENGINEERING	BM	BM