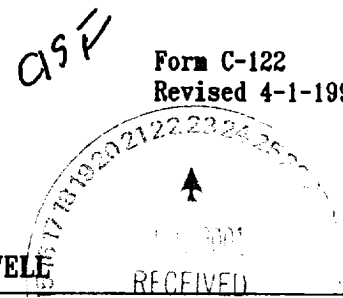


Submit in duplicate to  
appropriate district office  
See Rule 401 & Rule 1122

State of New Mexico  
Energy, Minerals and Natural Resources Department

OIL CONSERVATION DIVISION  
P.O. Box 2088  
Santa Fe, New Mexico 87504-2088

Form C-122  
Revised 4-1-1991



MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

|                                                                                                                           |               |                         |                           |                                   |                                   |                         |                                       |                                             |  |
|---------------------------------------------------------------------------------------------------------------------------|---------------|-------------------------|---------------------------|-----------------------------------|-----------------------------------|-------------------------|---------------------------------------|---------------------------------------------|--|
| Operator<br>Read & Stevens, Inc.                                                                                          |               |                         |                           |                                   | Lease or Unit Name<br>West Dayton |                         |                                       |                                             |  |
| Test Type<br><input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special |               |                         |                           |                                   | Test Date<br>July 11, 2001        |                         | Well No.<br>#1                        |                                             |  |
| Completion Date                                                                                                           |               | Total Depth             |                           | Plug Back TD                      |                                   | Elevation               |                                       | Unit Ltr - Sec - TWP - Rge.<br>19/ 18s/ 26e |  |
| Csg. Size<br>4.500                                                                                                        | Wt.<br>15.100 | d<br>3.826              | Set At                    | Perforation:<br>From 1306 To 1314 |                                   |                         | County<br>Eddy                        |                                             |  |
| Tbg. Size<br>2.375                                                                                                        | Wt.<br>4.600  | d<br>1.995              | Set At<br>1200            | Perforation:<br>From To           |                                   |                         | Pool<br>Rio Penasco<br>San Andres GRS |                                             |  |
| Type Well-Single-Bradenhead-G.G. or G.O. Multiple<br>Single                                                               |               |                         |                           |                                   |                                   | Packer Set At<br>1200   |                                       | Formation<br>San Andres                     |  |
| Producing Thru<br>Tubing                                                                                                  |               | Reservoir Temp.F<br>100 |                           | Mean Annual Temp.F<br>60          |                                   | Baro. Pressure<br>13.20 |                                       | Connection<br>8-1-01                        |  |
| L<br>1310                                                                                                                 | H<br>1310     | Gg<br>.752              | % CO <sub>2</sub><br>3.85 | % N <sub>2</sub><br>3.29          | % H <sub>2</sub> S                | Prover<br>2"            | Meter Run<br>Taps                     |                                             |  |

| FLOW DATA        |                                        |                |                         |            | TUBING DATA    |            | CASING DATA    |            | SIP/FLOW<br>DURATION<br>( HRS. ) |
|------------------|----------------------------------------|----------------|-------------------------|------------|----------------|------------|----------------|------------|----------------------------------|
| NO.              | ( PROVER )<br>LINE SIZE x ORIFICE SIZE | PRESS.<br>PSIG | DIFF.<br>h <sub>v</sub> | TEMP.<br>F | PRESS.<br>PSIG | TEMP.<br>F | PRESS.<br>PSIG | TEMP.<br>F |                                  |
| SHUT-IN PRESSURE |                                        |                |                         |            | 397            | 60         |                |            | 24                               |
| 1.               | 2.00 x .50                             | 2.44           |                         | 60         | 315            | 60         |                |            | 1                                |
| 2.               | 2.00 x .50                             | 4.17           |                         | 60         | 293            | 60         |                |            | 1                                |
| 3.               | 2.00 x .75                             | 8.13           |                         | 60         | 253            | 60         |                |            | 1                                |
| 4.               | 2.00 x 1.00                            | 5.25           |                         | 60         | 104            | 60         |                |            | 1                                |

RATE OF FLOW CALCULATIONS

| NO. | COEFFICIENT<br>( 24 HOUR ) | h <sub>v</sub> P <sub>m</sub> | PRESSURE<br>P <sub>m</sub> | FLOW TEMP.<br>FACTOR F <sub>t</sub> | GRAVITY FACTOR<br>F <sub>g</sub> | SUPER COMPRESS.<br>FACTOR F <sub>pv</sub> | RATE OF FLOW<br>( Q ) MCFD |
|-----|----------------------------|-------------------------------|----------------------------|-------------------------------------|----------------------------------|-------------------------------------------|----------------------------|
| 1.  | 4.388                      | 15.640                        | 15.6                       | 1.0000                              | 1.1531                           | 1.0017                                    | 79.3                       |
| 2.  | 4.388                      | 17.370                        | 17.4                       | 1.0000                              | 1.1531                           | 1.0019                                    | 88.1                       |
| 3.  | 9.694                      | 21.330                        | 21.3                       | 1.0000                              | 1.1531                           | 1.0023                                    | 239.0                      |
| 4.  | 17.530                     | 18.450                        | 18.5                       | 1.0000                              | 1.1531                           | 1.0020                                    | 373.7                      |

| NO. | P <sub>r</sub> | TEMP. | T <sub>r</sub> | Z     |
|-----|----------------|-------|----------------|-------|
| 1.  | .023           | 520   | 1.321          | .9966 |
| 2.  | .026           | 520   | 1.321          | .9963 |
| 3.  | .032           | 520   | 1.321          | .9954 |
| 4.  | .027           | 520   | 1.321          | .9960 |

|                                    |          |          |
|------------------------------------|----------|----------|
| Gas-Liquid Hydrocarbon Ratio       | .6       | Mcf/bbl  |
| API Gravity of Liquid Hydrocarbons | 50.000   | Deg.     |
| Specific Gravity Separator Gas     | .752     |          |
| Specific Gravity Flowing Fluid     | 3.163    |          |
| Critical Pressure                  | 673 PSIA | 555 PSIA |
| Critical Temperature               | 393 R    | 1162 R   |

|         |       |           |                 |
|---------|-------|-----------|-----------------|
| $P_C =$ | 410.2 | $P_C^2 =$ | 168.3           |
| NO.     | $P_w$ | $P_w^2$   | $P_C^2 - P_w^2$ |
| 1.      | 328.3 | 107       | 60.500          |
| 2.      | 306.3 | 93        | 74.451          |
| 3.      | 266.7 | 71        | 97.136          |
| 4.      | 118.3 | 13        | 154.271         |

$$(1) \frac{P_C^2}{P_C^2 - P_W^2} = 1.091 \quad (2) \left[ \frac{P_C^2}{P_C^2 - P_W^2} \right]^n = 1.088$$

$$AOP = Q \left[ \frac{P_C^2}{P_C^2 - P_W^2} \right]^n = 406$$

|                                              |              |                                 |                                           |
|----------------------------------------------|--------------|---------------------------------|-------------------------------------------|
| Absolute Open Flow<br>406                    | Mcf @ 15.025 | Angle of Slope - 46.0           | Slope, a .966                             |
| Remarks<br>Liquid at surface during rate #3. |              |                                 |                                           |
| Approved By Division:                        |              | Conducted By:<br>Brian Stearmer | Calculated By:<br>BPT System/SCHLUMBERGER |
|                                              |              | Checked By:<br>Dick Simper      |                                           |