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NEW MEXICO OIL CONSERVATION COMMISSION

MAY 1 6 1966

NULTI-POINT BACK PRESSURE TEST FÜR GAS WELLS   AFTERIA, OFFICE SIZE				,					). E. r	Form C-
### Annual Special Date of Test		•	MULT	I-POINT E	BACK PRES	SSURE- TE	ST FOR GA	ART S WELLS	ESIA, OF	Revised 12-1-
### Annual Special Date of Test	ool Red 1	Lake		Formation	1 <b>P</b> e	mnaylvar	ian	County		<b>86</b> y
Resolve Oil & Refining Company   Lease   Chalk Rimff Draw Unit 1   Well No.   5										
t H Sec. 8 Twp 18-3 Rge. 27-5 Purchaser (No commection)  ing 5-1/2 wt. 17.0 I.D. 4.892 Set at 9590 Perf. 9505 To 9555  ing 2-5/8 wt. 4.6 I.D. 1.995 Set at 9405 Perf. To -  Pay: From 9505 To 9555 L 9505 xG G.H. Bar.Press. 13.2  ducing Thru: Casing Tubing X Type Well Single e of Completion:(Not completed) Packer 9405 Reservoir Temp. 155°P  COBSERVED DATA  ted Through (Prover) (Obtain) (Prover) (Obtain) Press. Diff. Temp. Press. Temp. Press. Temp. Duration (Orifice) Size psig h <sub>N</sub> Or. psig Or. psig Or. psig Or. psig Or. Hr.  14 2 3.8 SS 2557 60 Packer - 4.25  4 2 1.8 SS 2557 60 Packer - 4.25  FLOW CALCULATIONS  FLOW Camp. Packer - 4.25  Flow Camp. Packer - 6.00  Flow Camp. Packer - 7.00  Flow Cam										
ing 5-1/2 wt. 17.0 I.D. 4.882 Set at 9590 Perf. 9505 To 9555 ing 2-3/8 wt. 4.6 I.D. 1.995 Set at 9405 Perf To -  Pay: From 9505 To 9555 L 9505 xG —GL Bar.Press. 13.2  ducing Thru: Casing Tubing X Type Well Single-Bradenhead-G. G. or G.O. Dual Reservoir Temp. 135°7  ducing Thru: Casing Tubing X Type Well Single-Bradenhead-G. G. or G.O. Dual Reservoir Temp. 135°7  Type Taps  Flow Data (Prover) (Shoke) (Actor) Type Taps  Flow Data (Prover) (Shoke) (Orifice) Press. Diff. Temp. Press. Temp. Fress. Temp. Of Flow Original Size Size psig h, OF, psig O										
Pay: From   9305   To   9555   9505   xG   -GL   Bar.Press.   15.2										
Pay:   From   9505   To   9555   9505   xG   -GL   Bar.Press   15.2										
Compact   Casing										
Single-Bradenhead-G. G. or G.O. Dual   Single-Bradenhead-G. G. or G.O. Dual   Single-Bradenhead-G. G. or G.O. Dual   Completion: (Not completed)   Packer   Size										2000
Conficient   Pressure   Flow Calculations		_				Sir	gle-Brade	enhead-G.	G. or (	G.O. Dual
Type Taps	oc or compre	OTOII.	· · · · · · · · · · · · · · · · · · ·	racke			neservo	orr leumb•	155	<u> </u>
Flow Data						ED DATA				
Prover   (prince)   Press   Diff   Temp   Press   Temp   Press   Temp   Duration of Flow   Size   Size   psig   hw   OF   psig   OF   psig   OF   psig   OF   psig   OF   Psis   OF   OF   OF   OF   OF   OF   OF   O	sted Through	(Prove	r) (discise)	(Meter)				Type Tap	)s	
Continue	<del></del>									
	(sateti)	(Orific	ce)		-				1	Duration of Flow
	Size	Size	psig	h <sub>w</sub>		<del> </del>		1	F.	
		201	7.8						+	69 Shut-in
Plow Calculations	1	. 1				<del></del>			+	
Pressure   Flow Calculations   Flow Temp.   Gravity   Compress.   Rate of Flow Calculations   Factor	_	2"		<del> </del>					<del>†</del>	
FLOW CALCULATIONS	4"	2"	16.8		55	858			+	
See   1.0078   1.018   1.002   888   1430   1.0430   1.0450   1.016   1.002   1519   1.0280   1.016   1.002   2138   2419   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.0069   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   2475   1.016   1.002   1.016   1.002   2475   1.016   1.002   1.016   1.002   1.016   1.016   1.002   1.002   1.002   1.002   1.002   1.002   1.002   1.	Q-Uncorrec	ted		ressure	Flow Fac	Temp.	Gravity Factor	Facto		Q-MCFPD
1.0430	<u> </u>	/ V	Wb.I.	pota		t				
1.0260   1.016   1.002   2138   2419   1.0049   1.006   1.002   2475										
PRESSURE CALCULATIONS  Additional Hydrocarbon Ratio 322,030 cf/bbl. Specific Gravity Separator Gas 52 deg. Specific Gravity Flowing Fluid 63 (1-e-5) Pc 3790.2 Pc 14360 x 10.3  Pressure Measured with Subsurface Gauge  Pwe 10-5 Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Fc Separator Gas 52 deg. Specific Gravity Flowing Fluid 63 Pc 14360 x 10.3  Pressure Measured with Subsurface Gauge  Pwe 10-5 Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Fc Separator Gas 52 deg. Specific Gravity Flowing Fluid 63 Pc 14360 x 10.3  Pt (psia) Pt FcQ (FcQ)2 (FcQ)2 Pw2 Pc-Pw Cal. Pw Fc Separator Gas 52 deg. Specific Gravity Separator Gas 52 deg. Specific Gravity Flowing Fluid 63 deg. Specific Grav										
Specific Gravity Separator Gas   Specific Gravity Separator Gas   Specific Gravity Flowing Fluid	2419				1.0048					···-
Pwe 10-5 Pt (psia) Pt (psi	rity of Liqui	ld Hydrod	arbons	,630	cf/bbl.		Speci Speci	fic Gravi	ty Flow	ing Fluid age
Pt (psia) Pt FcQ (FcQ) <sup>2</sup> (FcQ) <sup>2</sup> Pw2 Pc-Pw Cal. Pw Pc  S228.2  10421 5945 85.5  2652.2  1080.2  11016 48.3  1252.2  Delute Potential: 2730 MCFPD; n 0.87  PANY Burble 011 & Refining Company  RESS Reg 1600, Maland, Table  OT and TITLE Petrolem Engineer, 1) Galacie  PANY Part of the Potential Section of the Pw Pc  PANY Part of the Potential Section of the Pw Pc  PANY Part of the Potential Section of the Pw Pc  PANY Part of the Potential Section of the Pw Pc  PANY Part of the Potential Section of the Pw Pc  Pany Pc Pw		- Measure	ed with Su	beurface	Cauge	<del>-</del>				<del></del>
1042  5945   85.5   2652.2   7054   7322   70.0   2850.2   3350   11016   48.3   252.2   2730   MCFPD; n 0.87	"	$P_{\mathbf{t}}^{2}$	F <sub>c</sub> Q	$(F_cQ)^2$	(F	$(cQ)^2$		$P_c^2 - P_w^2$	Ca	P.W.
2652.2 7054 7382 70.0 1850.2 3350 11016 48.3 1252.2 1568 12796 35.0  PANY Burble Oil & Refining Company RESS Row 1600, Milland, Torme IT and TITLE Petrolem Engineer, Verkelnik RESSED PANY	3228.Z							3945	<del></del>	И
1880.2 1252.2 1568 12796 1568 12796 33.0  PANY Bushle Oil & Refining Company RESS Reg 1600, Midland, Terms IT and TITLE Petrolem Engineer, The Malnik RESSED PANY	2652.2									
Pany Bubble 011 & Refining Company RESS Reg 1600, Midland, Terms RESSED PANY Strolem Engineer, Westalnik	1830.2					3	350	11016		
PANY Burble Oil & Refining Company RESS Roy 1600, Midland, Tourse RT and TITLE Petroleum Engineer, Wilkelink RESSED PANY	1252.2			<del> </del>		1	568	12796	<del> </del>	1
PANY Burble Oil & Refining Company RESS Roy 1600, Midland, Tourse RT and TITLE Petroleum Engineer, Wilkelink RESSED PANY			2750	<del></del>				L		
RESS Reg 1600, Midland, Terms IT and TITLE Petrolem Engineer, Weskalnik PANY				- A		n 0.87				
TT and TITLE Petrolem Engineer, VESKalnik PANY	RESS	m 1600.	Mdland.	Torre				<del></del>		
PANY	NT and TITLE	Petrole	nun Engine	. 174	skalı	ik			·····	
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	LPANY				REM	ARKS	<del></del>	<del></del>		<u></u>

## INSTRUCTIONS

This form is to be used for reporting multi-point back pressure tests on gas wells in the State, except those on which special orders are applicable. Three copies of this form and the back pressure curve shall be filed with the Commission at Box 871, Santa Fe.

The log log paper used for plotting the back pressure curve shall be of at least three inch cycles.

## NOMENCLATURE

- Q I Actual rate of flow at end of flow period at W. H. working pressure  $(P_w)$ . MCF/da. @ 15.025 psia and 60° F.
- P<sub>C</sub>= 72 hour wellhead shut-in casing (or tubing) pressure whichever is greater. psia
- Pw Static wellhead working pressure as determined at the end of flow period. (Casing if flowing thru tubing, tubing if flowing thru casing.) psia
- Pt Flowing wellhead pressure (tubing if flowing through tubing, casing if flowing through casing.) psia
- Pf Meter pressure, psia.
- $h_{\boldsymbol{w}}\textbf{I}$  Differential meter pressure, inches water.
- $F_g$ : Gravity correction factor.
- $F_{t}$  Flowing temperature correction factor.
- Fpv Supercompressability factor.
- n I Slope of back pressure curve.

Note: If  $P_{\rm W}$  cannot be taken because of manner of completion or condition of well, then  $P_{\rm W}$  must be calculated by adding the pressure drop due to friction within the flow string to  $P_{\rm t}$ .