Form C-122
Revised 9-1-65

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

copy to J.F.

RECEIVED
JAN 10 1967
O. C. C.
ARTESIA, OFFICE

Type Test: [X] Initial [ ] Annual [ ] Special

Test Date: 12-28-66

Company: STANDARD OIL CO. OF TEXAS		Connection: TRANSWESTERN			
Pool: ATOKA		Formation: PENN			Unit
Completion Date: 10-1-66	Total Depth: 9070	Plug Back TD: [illegible]34	Elevation: 3332' GL		Farm or Lease Name: R. TERRY ET AL
Csg. Size: 4 1/2	Wt.: 9.5 / 11.6	d: [illegible].090 / 4.000	Set At: 9067	Perforations: From [illegible] To [illegible]	Well No.: 2
Tbg. Size: 2 3/8	Wt.: 4.7	d: 1.995	Set At: 8840	Perforations: From OPEN To ENDED	Unit / Sec.: 15 / Twp.: 18 / Rge.: 26
Type Well — Single — Bradenhead — G.G. or G.O. Multiple: SINGLE				Packer Set At: [illegible]	County: EDDY
Producing Thru: TUBING	Reservoir Temp. °F: 157 @ [illegible]	Mean Annual Temp. °F: —		Baro. Press. — P_a: [illegible]	State: NEW MEXICO

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
—	—	[illegible]	[illegible].56	[illegible]	0.[illegible]	—	2.067	FLANGE

FLOW DATA

NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Tubing Data Press. p.s.i.g.	Tubing Data Temp. °F	Casing Data Press. p.s.i.g.	Casing Data Temp. °F	Duration of Flow
SI							[illegible]	[illegible]	[illegible]	—	72
1.	2"	.875	6/64	[illegible]	[illegible]"	[illegible]	[illegible]	[illegible]	[illegible]	—	2.5
2.	2"	.875	8/64	[illegible]	[illegible]"	[illegible]	[illegible]	[illegible]	[illegible]	—	2.0
3.	2"	.875	10/64	865	48"	90	[illegible]	[illegible]	[illegible]	—	2.0
4.	2"	.875	12/64	860	70"	90	[illegible]	[illegible]	[illegible]	—	24.0
5.											

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	3.720	[illegible]	[illegible]3.2	0.9777	1.270	[illegible]	766.8
2.	3.720	[illegible]	873.2	0.98[illegible]	1.270	[illegible]	899.1
3.	3.720	[illegible]	878.2	0.9723	1.270	[illegible]	1006.9
4.	3.720	[illegible]	873.2	0.972[illegible]	1.270	1.[illegible]	1212.6
5.							

NO.	P_r	Temp. °R	T_r	Z
1.	1.2[illegible]	54[illegible]	1.5[illegible]	[illegible]
2.	1.3[illegible]	54[illegible]	1.5[illegible]	[illegible]
3.	1.30	550	1.52	[illegible]
4.	1.30	550	1.52	0.8[illegible]
5.				

Gas Liquid Hydrocarbon Ratio: 380[illegible] Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons: [illegible] Deg.
Specific Gravity Separator Gas: 0.620[illegible] | XXXXXXXXX
Specific Gravity Flowing Fluid: XXXXX | —
Critical Pressure: 67[illegible] P.S.I.A. | — P.S.I.A.
Critical Temperature: 361 R | — R

P_c: 306[illegible].2 P_c^2: [illegible] *

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1	—	2450.[illegible]	[illegible]3.5	[illegible]85.[illegible]
2	—	2308.2	[illegible]7.8	40[illegible]
3	—	2142.2	[illegible].0	480[illegible]
4	—	1871.2	[illegible]01.4	5887.[illegible]
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2}$ = 1.595

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 1.460

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n$ = 1775

Absolute Open Flow: 1775. Mcfd @ 15.025 | Angle of Slope: [illegible] | Slope, n: 0.808

Remarks: * BOTTOM HOLE PRESSURE @ (-5638) 8970'

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
[illegible signature]	COLEMAN PET. ENG.	JOE A. COLEMAN	JOE A. COLEMAN