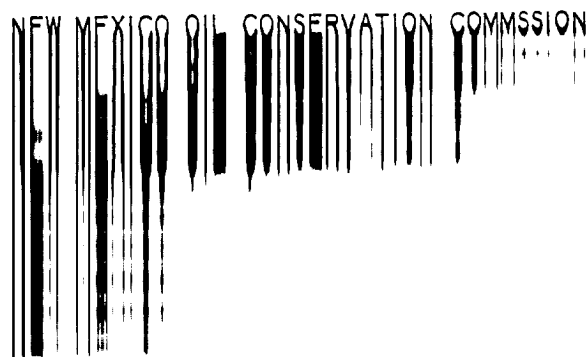


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C-122



Form C-122



MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

RECEIVED

Type Test ☒ Initial ☐ Annual ☐ Special					Test Date 12/17/73		JAN 2 1974									
Company Felmont Oil Company					Connection None		O. E. C.									
Pool Atoka Penn					Formation Atoka <i>HOYCO</i>		UARTERIA, OFFICE									
Completion Date 11/30/73		Total Depth 9102		Plug Back TD 9058		Elevation 3304 KB		Farm or Lease Name Felmont-Atoka Com								
Csg. Size 4 1/2	Wt. 10.5	d 4.09	Set At 9100	Perforations: From 8926 To 9032		Well No. 1										
Tbg. Size 2 7/8	Wt. 6.5	d 2.441	Set At 8788	Perforations: From open end To		Unit Sec. Twp. Rge. D 12 18S 26E										
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single					Packer Set At 8788		County Eddy									
Producing Thru Tubing		Reservoir Temp. °F 60°		Mean Annual Temp. °F 13.2		Baro. Press. - P _a New Mexico										
L 8788	H 8788	G _g .6556	% CO ₂ 0.98	% N ₂ 0.50	% H ₂ S ---	Prover X	Meter Run	Taps								
FLOW DATA												TUBING DATA		CASING DATA		Duration of Flow
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F						
SI							2634					74				
1.	2	X	1/2	326		68	326	68				1				
2.	2	X	5/16	698		70	698	70				1				
3.	2	X	1/4	957		68	957	68				1				
4.	2	X	3/16	1385		68	1385	68				1				
5.																
RATE OF FLOW CALCULATIONS																
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor F _t	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd									
1	4.279		339.2	.9924	1.235	1.033	1838									
2	1.672		711.2	.9905	1.235	1.070	1556									
3	1.087		970.2	.9924	1.235	1.098	1419									
4	0.6082		1398.2	.9924	1.235	1.142	1190									
5																
NO.	P _f	Temp. °R	T _f	Z	Gas Liquid Hydrocarbon Ratio <u>TSTM</u> Mcf/bbl.											
1	0.50	528	1.41	.938	A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.											
2	1.06	530	1.42	.874	Specific Gravity Separator Gas <u>.6556</u> X X X X X X X X											
3	1.44	528	1.41	.829	Specific Gravity Flowing Fluid <u>X X X X X</u>											
4	2.07	528	1.41	.767	Critical Pressure <u>674</u> P.S.I.A. P.S.I.A.											
5					Critical Temperature <u>374</u> R R											
P _c <u>3427.2</u> P _c ² <u>11746*</u>					(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.059$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.059$											
NO.	P _f ²	P _w *	P _w ²	P _c ² - P _w ²	AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1946$											
1		808.2	653	11093												
2		1050.2	1103	10643												
3		1333.2	1777	9969												
4		1717.2	2949	8797												
5																
Absolute Open Flow <u>1946</u> Mcfd @ 15.025					Angle of Slope @ <u>45°</u>		Slope, n <u>1.00</u>									
Remarks: <u>* From BHP gauge @ 8700</u>																
Approved By Commission:			Conducted By: <i>Ralph B. Quinn</i>			Calculated By: <i>Donna Holler</i>		Checked By:								