NEW MEXICO OIL CONSERVATION COMMISSION

MULTIPOINT A.. ONE POINT BACK PRESSURE TEST ..OR GAS WELL

Form C-122
Revised 9-1-65

RECEIVED

SEP 14 1981

O. C. D.

ARTESIA, OFFICE

C/SF C-122

Type Test: [X] Initial [ ] Annual [ ] Special				Test Date: 9-3-81	
Company: Southland Royalty Company		Connection: To the Air			
Pool: ~~Undesignated~~ Turkey Track - Atoka Gas		Formation: Atoka		Unit	
Completion Date: 2-10-81	Total Depth: 11,791		Plug Back TD: 11,100	Elevation: 3423.5	Farm or Lease Name: 35 Empire Federal ~~35~~ Com
Csg. Size: 4 1/2 / Wt.: 13.5 / d: 3.920 / Set At: 11,791			Perforations: From 10,757 To 10,778		Well No.: 1
Tbg. Size: 2 3/8 / Wt.: 4.7 / d: 1.995 / Set At: 10,635			Perforations: From 0 To 0		Unit K / Sec. S35 / Twp. T-18-S / Rge. R-29-E
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single			Packer Set At: 10,635		County: Eddy
Producing Thru: Tbg	Reservoir Temp. °F: 181 @ 10,768.	Mean Annual Temp. °F: 60.0	Baro. Press. – P_a: 13.2		State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
10,768.	10,768.	0.622	0.00	0.01	0.00	0.0	2.0	Flange

	FLOW DATA				TUBING DATA		CASING DATA		
NO.	Prover Line Size X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI					3085.	70.			50.0
1.	2.00 x 0.750	313.	7.0	116.	2420.	80.	0.	0.	1.0
2.	2.00 x 0.750	330.	14.0	109.	2066.	85.	0.	0.	1.0
3.	2.00 x 0.750	308.	23.0	96.	1760.	65.	0.	0.	1.0
4.	2.00 x 0.750	306.	36.5	84.	1430.	70.	0.	0.	1.0
5.									

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	2.71	47.78	326.2	0.9501	1.2680	1.0214	160.
2.	2.71	69.32	343.2	0.9560	1.2680	1.0236	233.
3.	2.71	85.95	321.2	0.9671	1.2680	1.0241	293.
4.	2.71	107.94	319.2	0.9777	1.2680	1.0261	373.
5.							

NO.	P_t	Temp. °R	T_t	Z
1.	0.49	576.	1.58	0.959
2.	0.51	569.	1.56	0.954
3.	0.48	556.	1.52	0.953
4.	0.48	544.	1.49	0.950
5.				

Gas Liquid Hydrocarbon Ratio 0.0 Mcf/bbl.

A.P.I. Gravity of Liquid Hydrocarbons 0.0 Deg.

Specific Gravity Separator Gas 0.622 XXXXXXXXX

Specific Gravity Flowing Fluid XXXXX 0.622

Critical Pressure 671. P.S.I.A. 671. P.S.I.A.

Critical Temperature 365. R 365. R

P_c 3086.7 P_c^2 9527.

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1	5920.	2412.	5817.	3711.
2	4323.	2056.	4225.	5302.
3	3144.	1771.	3135.	6393.
4	2083.	1439.	2071.	7456.
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.2777$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.2777$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 476.$

Absolute Open Flow 476. Mcfd @ 15.025 Angle of Slope θ 45.0 Slope, n 1.000

Remarks:

Approved By Commission:	Conducted By:	Calculated By:	Checked By:
	Northern Natural Gas	Ray Nokes	Ray Nokes