STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

OIL CONSERVATION DIVISION

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Form C-122
Revised 10-1-78

RECEIVED
MAY 11 1981
O. C. D.
ARTESIA, OFFICE

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test: [X] Initial [ ] Annual [ ] Special			Test Date: 5-5-81	
Company: Hondo Oil & Gas Company	Connection: None			Unit
Pool: ~~Undesignated~~ No. Illinois Camp	Formation: Morrow			
Completion Date: 5-1-81	Total Depth: 10790	Plug Back TD: 10718	Elevation: 3590 G.L.	Farm or Lease Name: Exxon "A" State
Csg. Size: 5 1/2 / Wt.: 17 / d: 4.892 / Set At: 10790	Perforations: From 10522 To 10530			Well No.: 1
Tbg. Size: 2.375 / Wt.: 4.7 / d: 1.995 / Set At: 10449	Perforations: From 10452 To 10455			Unit: H / Sec.: 16 / Twp.: 18S / Rge.: 28E
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single		Packer Set At: 10449		County: Eddy
Producing Thru: Tbg.	Reservoir Temp. °F: 160 @ 10776	Mean Annual Temp. °F: 60°	Baro. Press. – P_a: 13.2	State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
10452	10452	.646	.61	.46	-0-		4"	Flg.

FLOW DATA / TUBING DATA / CASING DATA

NO.	Prover Line Size X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Tubing Press. p.s.i.g.	Tubing Temp. °F	Casing Press. p.s.i.g.	Casing Temp. °F	Duration of Flow
SI					3056		Pkr.		114.5 Hrs.
1.	4 x 1.250	493	9	94	2446	69	Pkr.		1 Hr.
2.	4 x 1.250	490	12	83	2273	71	Pkr.		1 Hr.
3.	4 x 1.250	491	21	70	1987	72	Pkr.		1 Hr.
4.	4 x 1.250	495	38	76	1641	73	Pkr.		1 Hr.
5.									

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	7.469	67.50	506.2	.9688	1.244	1.041	633
2.	7.469	77.71	503.2	.9786	1.244	1.043	737
3.	7.469	102.90	504.2	.9905	1.244	1.047	992
4.	7.469	138.97	508.2	.9850	1.244	1.047	1332
5.							

NO.	P_r	Temp. °R	T_r	Z
1	.75	554	1.49	.923
2.	.75	543	1.47	.920
3.	.75	530	1.43	.912
4.	.76	536	1.44	.913
5				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons 54 @ 60° Deg.
Specific Gravity Separator Gas .646 XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX
Critical Pressure 673 P.S.I.A. _____ P.S.I.A.
Critical Temperature 371 R _____ R

*P_c 4114.2 P_c^2 16926.6

NO	P_w	P_w^2	$P_c^2 - P_w^2$
1	*3431.2	11773.1	5153.5
2	*3214.2	10331.1	6595.5
3	*2812.2	7908.5	9018.1
4	*2343.2	5490.6	11436.0
5			

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.877$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.656$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1643$

Absolute Open Flow 1643 Mcfd @ 15.025 | Angle of Slope θ 51° 19' | Slope, n .801

Remarks: BHP at mid point of perforations 10526
Via bottom hole bomb
Produced 2 bbl. distillate

Approved By Division	Conducted By:	Calculated By:	Checked By:
	Ross Trevino	J. D. Cogburn	J. V. Curfew

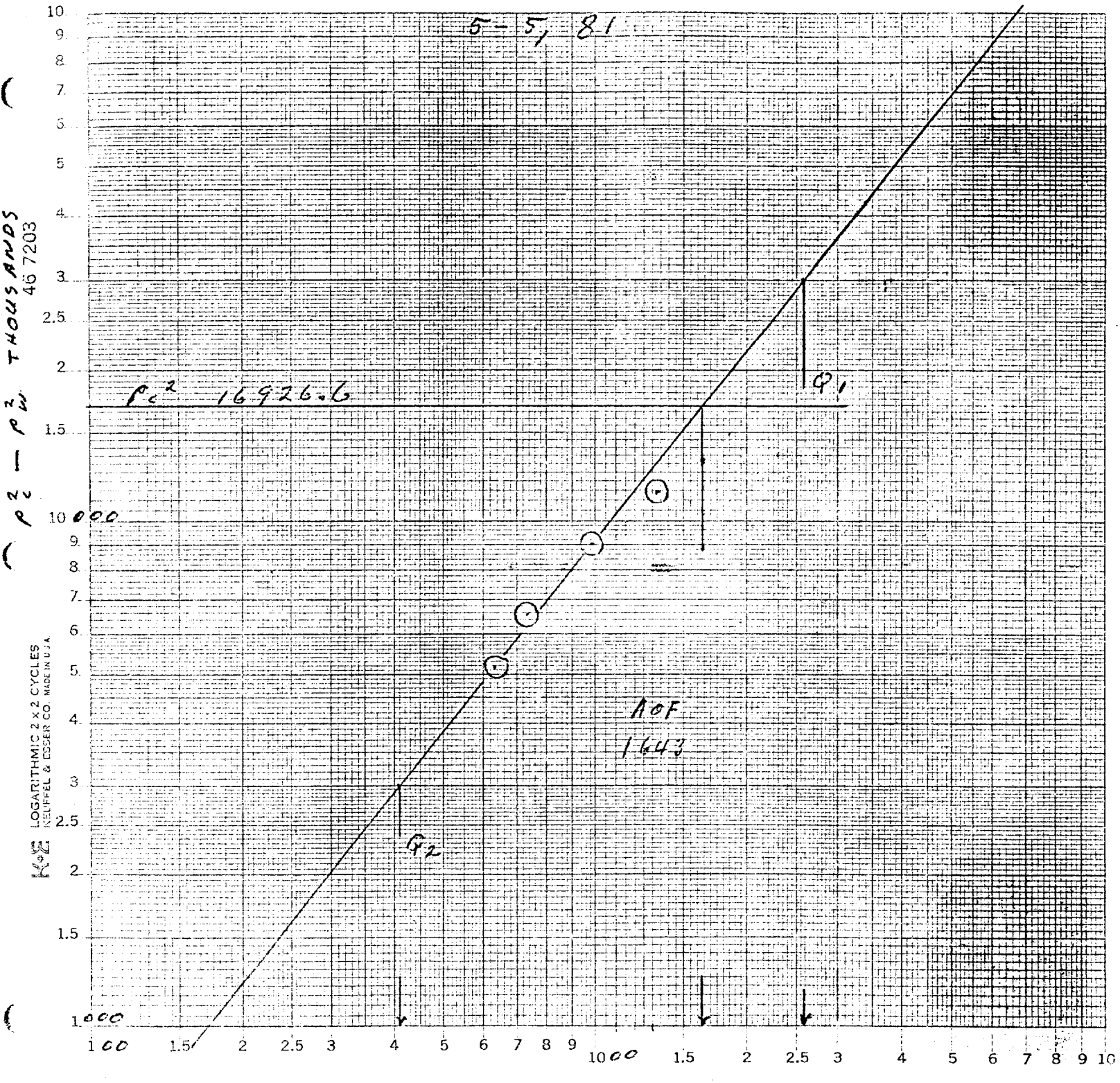
MONDO OIL & GAS CO.

EXXON A STATE NO. 1

UNIT H 16 18S 28E

EDDY COUNTY N. MEXICO

5-5, 81



$q_1 = 2590$, LOG 3.4132998

$q_2 = 410$, LOG 2.6127839

$n = .8005159 = .801$