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State of New Mexico
Energy, Minerals and Natural Resources Dep:

Form C-122
Revised 4-1-91

OIL CONSERVATION DIVISION NOV - 7 1995
P.O. Box 2088
Santa Fe, New Mexico 87504-2088

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator <i>Enron Oil & Gas Company</i>						Lease or Unit Name <i>Sandtank 6 Fed</i>					
Type Test ☒ Initial ☐ Annual ☐ Special						Test Date <i>10-24-96</i>		Well No. <i>1</i>			
Completion Date <i>9-29-96</i>		Total Depth <i>11765</i>		Plug Back TD <i>11743</i>		Elevation <i>3554' GR</i>		Unit Ltr. - Sec. - TWP - Rge. <i>6 18-S 30-E</i>			
Csg. Size <i>5 1/2</i>	Wt. <i>17</i>	d <i>4.892</i>	Set At <i>11765</i>	Perforations: From: <i>11,334</i> To: <i>11,344</i>				County <i>Eddy</i>			
Tbg. Size <i>2 7/8</i>	Wt. <i>6.5</i>	d <i>2.441</i>	Set At <i>11,346</i>	Perforations: From: To:				Pool <i>Sand Tank MORROW</i>			
Type Well - Single - Bradenhead - G.G. or G.O. Multiple <i>Single</i>						Packer Set At <i>N/A</i>		Formation <i>Morrow</i>			
Producing Thru <i>tbg</i>		Reservoir Temp. °F <i>187</i>		Mean Annual Temp. °F <i>60°</i>		Baro. Press - P _a <i>13.2</i>		Connection <i>Sales</i>			
L <i>11.297</i>	H <i>11.297</i>	G _g <i>.660</i>	% CO ₂ <i>.55</i>	% N ₂ <i>.52</i>	% H ₂ S <i>0</i>	Prover <i>0</i>		Meter Run <i>4.026</i>	Taps <i>F/G</i>		

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
SI							<i>2620</i>		<i>N/A</i>	<i>N/A</i>	<i>24 hrs</i>
1.	<i>4.026 X</i>	<i>2.250</i>		<i>442</i>	<i>2.9</i>	<i>82</i>	<i>2420</i>	<i>68</i>			<i>1 hrs</i>
2.	<i>4.026 X</i>	<i>2.250</i>		<i>448</i>	<i>7.3</i>	<i>80</i>	<i>2470</i>	<i>68</i>			<i>1 hrs</i>
3.	<i>4.026 X</i>	<i>2.250</i>		<i>455</i>	<i>16.8</i>	<i>102</i>	<i>2350</i>	<i>62</i>			<i>1 hrs</i>
4.	<i>4.026 X</i>	<i>2.250</i>		<i>462</i>	<i>29.7</i>	<i>98</i>	<i>2190</i>	<i>62</i>			<i>1 hrs</i>
5.											

RATE OF FLOW CALCULATIONS							
NO.	COEFFICIENT (24 HOUR)	$h_w P_m$	Pressure P _m	Flow Temp. Factor F _t	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd
1.	<i>25.64</i>	<i>36.33</i>	<i>455.2</i>	<i>.9795</i>	<i>1.231</i>	<i>1.048</i>	<i>1177</i>
2.	<i>25.64</i>	<i>58.0</i>	<i>461.2</i>	<i>.9813</i>	<i>1.231</i>	<i>1.048</i>	<i>1882</i>
3.	<i>25.64</i>	<i>88.6</i>	<i>468.2</i>	<i>.9619</i>	<i>1.231</i>	<i>1.044</i>	<i>2808</i>
4.	<i>25.64</i>	<i>118.8</i>	<i>475.2</i>	<i>.9653</i>	<i>1.231</i>	<i>1.044</i>	<i>3778</i>
5.							

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	A.P. I Gravity of Liquid Hydrocarbons	Specific Gravity Separator Gas	Specific Gravity Flowing Fluid	Critical Pressure	Critical Temperature
1.	<i>.80</i>	<i>542</i>	<i>1.44</i>	<i>.910</i>	<i>36.534</i>	<i>53.8</i>	<i>.660</i>	<i>XXXXXX</i>	<i>673</i>	<i>374</i>
2.	<i>.80</i>	<i>540</i>	<i>1.44</i>	<i>.910</i>						
3.	<i>.83</i>	<i>562</i>	<i>1.50</i>	<i>.918</i>						
4.	<i>.82</i>	<i>538</i>	<i>1.49</i>	<i>.917</i>						
5.										

NO.	P _i ²	P _w	P _w ²	P _c ² - P _w ²
1.	<i>5905.5</i>	<i>2436.5</i>	<i>5936.6</i>	<i>997.1</i>
2.	<i>6166.3</i>	<i>2491.6</i>	<i>6207.8</i>	<i>1259.9</i>
3.	<i>5584.7</i>	<i>2382.5</i>	<i>5676.1</i>	<i>1257.7</i>
4.	<i>4854.1</i>	<i>2239.9</i>	<i>5017.3</i>	<i>1916.4</i>
5.				

1) $\frac{P_c^2}{P_c^2 - P_w^2} = 3.618$

2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.518$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 9.514$

Absolute Open Flow *9.514* Mcfd @ 15.025

Angle of Slope Θ *54.3*

Slope, n *.718*

Remarks: *Well made 11 BBLS of oil @ 53.8 API Gravity*

Approved By Division	Conducted By:	Calculated By:	Checked By:
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Betty Gildon

Betty Gildon
Regulatory Analyst

915/686-3714

11/6/96