

45F  
C-122 45GS

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

RECEIVED

MAR 12 1982

O. C. D.  
ARTESIA, OFFICE

|                                                            |  |                                    |  |                                       |  |                                        |  |
|------------------------------------------------------------|--|------------------------------------|--|---------------------------------------|--|----------------------------------------|--|
| <input checked="" type="checkbox"/> Initial                |  | <input type="checkbox"/> Annual    |  | <input type="checkbox"/> Special      |  | Test Date<br>2 9 82                    |  |
| Operator<br>Tenneco Oil Company                            |  |                                    |  | Connection<br>None                    |  |                                        |  |
| Location<br>Turkey Track                                   |  |                                    |  | Formation<br>Morrow                   |  |                                        |  |
| Well No.<br>2-3782                                         |  | Total Depth<br>11589'              |  | Plug Back To<br>11252'                |  | Flow Rate<br>3321 G/L                  |  |
| Casing Size<br>2 3/8"                                      |  | Set At<br>4.892                    |  | Perforations<br>From 11120' To 11204' |  | Santo Hil 2                            |  |
| Casing Weight<br>4.7                                       |  | Set At<br>1.995                    |  | Perforations<br>From 11084' To 11104' |  | 1Y                                     |  |
| Type Well - Surface - 1 (downward - G.C. or G.O. Multiple) |  |                                    |  | Packer Set At<br>11084'               |  | County<br>Eddy                         |  |
| Producing Test<br>Tbg                                      |  | Reservoir Temp. *F<br>185 @ 11084' |  | Mean Annual Temp. *F<br>60            |  | Burst. Press. - P <sub>b</sub><br>13.2 |  |
| L<br>11084                                                 |  | H<br>11084                         |  | G <sub>g</sub><br>.6804               |  | State<br>New Mexico                    |  |
|                                                            |  |                                    |  | % CO <sub>2</sub><br>.749             |  | % N <sub>2</sub><br>.658               |  |
|                                                            |  |                                    |  | % H <sub>2</sub> S<br>2.900           |  | Pressure<br>2.900                      |  |

| FLOW DATA |                        |        |                 |                |             |             | PACKER DATA    |             |                |             |
|-----------|------------------------|--------|-----------------|----------------|-------------|-------------|----------------|-------------|----------------|-------------|
| NO        | Prover<br>Line<br>Size | X      | Orifice<br>Size | Press.<br>psia | Diff.<br>hw | Temp.<br>°F | Press.<br>psia | Temp.<br>°F | Press.<br>psia | Temp.<br>°F |
| 1         | 2.9                    | 4/64   | 1.00            | 315            | 8           | 77          | 3220           | 60          | 3220           | 60          |
| 2         | 2.9                    | 5/64   | 1.00            | 330            | 16          | 74          | 2855           | 60          | 2855           | 60          |
| 3         | 2.9                    | 6.5/64 | 1.00            | 310            | 25          | 65          | 2632           | 60          | 2632           | 60          |
| 4         | 2.9                    | 9/64   | 1.00            | 330            | 60          | 60          | 2325           | 60          | 2325           | 60          |
| 5         |                        |        |                 |                |             |             | 1810           | 60          | 1810           | 60          |

| RATE OF FLOW CALCULATIONS |                         |                  |                            |                                        |                                     |                                              |                          |
|---------------------------|-------------------------|------------------|----------------------------|----------------------------------------|-------------------------------------|----------------------------------------------|--------------------------|
| NO.                       | Coefficient<br>(X Hour) | $\sqrt{h_w P_m}$ | Pressure<br>P <sub>m</sub> | Flow Temp.<br>Factor<br>F <sub>1</sub> | Gravity<br>Factor<br>F <sub>g</sub> | Super<br>Compress.<br>Factor, F <sub>2</sub> | Rate of Flow<br>Q (BC/D) |
| 1                         | 4.801                   | 51.24            | 328.2                      | .9840                                  | 1.213                               | 1.032                                        | 303                      |
| 2                         | 4.801                   | 74.10            | 343.2                      | .9868                                  | 1.213                               | 1.033                                        | 410                      |
| 3                         | 4.801                   | 89.89            | 323.2                      | .9952                                  | 1.213                               | 1.034                                        | 539                      |
| 4                         | 4.801                   | 143.50           | 343.2                      | .9905                                  | 1.213                               | 1.035                                        | 857                      |

| NO | K   | Temp. *F | T <sub>1</sub> | Z    | Gas Liquid Hydrocarbon Ratio          | 37.135    |
|----|-----|----------|----------------|------|---------------------------------------|-----------|
| 1  | .49 | 537      | 1.41           | .939 | A.P.I. Gravity of Liquid Hydrocarbons | 60.6 @ 60 |
| 2  | .51 | 534      | 1.40           | .937 | Specific Gravity Separator Gas        | .680      |
| 3  | .48 | 525      | 1.38           | .935 | Specific Gravity Flowing Fluid        | XXXXXX    |
| 4  | .51 | 530      | 1.39           | .934 | Critical Pressure                     | 672 PSIA  |
| 5  |     |          |                |      | Critical Temperature                  | 381 °F    |

|   |        |         |        |                                                                |                                                            |
|---|--------|---------|--------|----------------------------------------------------------------|------------------------------------------------------------|
| 1 | 3255.2 | 10455.6 |        |                                                                |                                                            |
| 2 | 2870.2 | 8238.0  | 2215.6 | (1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.270$                      | (2) $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.206$ |
| 3 | 2648.0 | 7011.9  | 3441.7 | AOF = Q $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.205$ |                                                            |
| 4 | 2341.7 | 5483.6  | 4970.0 |                                                                |                                                            |
| 5 | 1827.8 | 3340.9  | 7112.7 |                                                                |                                                            |

|                                                                |       |               |                  |      |          |      |
|----------------------------------------------------------------|-------|---------------|------------------|------|----------|------|
| Absolute Flow                                                  | 1,205 | Mold @ 15.025 | Angle of Slope θ | 48.5 | Slope, n | .885 |
| Results WELL MADE 2.4 BBLs CONDENSATE DURING TEST = 14.40 BC/D |       |               |                  |      |          |      |

|                                          |                                          |                             |                                               |
|------------------------------------------|------------------------------------------|-----------------------------|-----------------------------------------------|
| Approved by Division<br><i>Q. Wilson</i> | Conducted By:<br>JARREL WELL TESTING INC | Calculated By:<br>R. Reston | Checked By: PE #2208<br><i>Joe A. Coleman</i> |
|------------------------------------------|------------------------------------------|-----------------------------|-----------------------------------------------|