STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

Form C-122
Revised 10-1-78

RECEIVED
AUG 1 1 1982
O. C. D.
ARTESIA, OFFICE

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test: [X] Initial [ ] Annual [ ] Special				Test Date: 8-2-82	
Company: Hondo Oil and Gas Company		Connection: Not Connected			
Pool: N. Turkey Track Morrow		Formation: Morrow Gas			
Completion Date: 8-2-82	Total Depth: 11425		Plug Back TD: 11326	Elevation: 3421.4 GR	Farm or Lease Name: Turkey 4 State
Csg. Size: 5.5 / Wt.: 17 / d: 4.892 / Set At: 11425			Perforations: From 11136 To 11167		Well No.: 1
Tbg. Size: 2.375 / Wt.: 4.7 / d: 1.995 / Set At: 11001			Perforations: From Open To Ended		Unit: F / Sec.: 4 / Twp.: 19S / Rge.: 29E
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single			Packer Set At: 11001		County: Eddy
Producing Thru: Tbg.	Reservoir Temp. °F: 175@ 11152'	Mean Annual Temp. °F: 60	Baro. Press. – P_a: 13.2		State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
11001	11001	.7167	6.893	1.180	-0-		4"	Flg.

	FLOW DATA				TUBING DATA		CASING DATA		
NO.	Prover Line Size	X Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI						3132		Pkr.		66 Hrs.
1.	4	x 1	317	8.5	90	3012	73			1 Hr.
2.	4	x 1	319	16	88	2957	73			1 Hr.
3.	4	x 1	317	15	83	2903	73			1 Hr.
4.	4	x 1	343	48	92	2725	73			1 Hr.
5.	4	x 1	564	43	85	2570	73			1 Hr.

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	4.753	52.98	330.2	.9723	1.181	1.029	298
2.	4.753	72.91	332.2	.9741	1.181	1.030	411
3.	4.753	70.38	330.2	.9786	1.181	1.030	398
4.	4.753	130.76	356.2	.9706	1.181	1.031	734
5.	4.753	157.54	577.2	.9768	1.181	1.054	910

NO.	P_t	Temp. °R	T_t	Z
1	.47	550	1.44	.945
2.	.48	548	1.43	.942
3.	.47	543	1.42	.943
4.	.51	552	1.44	.940
5	.83	545	1.42	.900

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons 54.8° @ 60°F Deg.
Specific Gravity Separator Gas .717 XXXXXXXXX
Specific Gravity Flowing Fluid XXXXX
Critical Pressure 697 P.S.I.A. _____ P.S.I.A.
Critical Temperature 383 R _____ R

P_c 4422.2 P_c^2 19555.85

NO	P_t^2	* P_w	P_w^2	$P_c^2 - P_w^2$
1		4289.2	18397.24	1158.61
2		4199.2	17633.28	1922.57
3		4140.2	17141.26	2414.59
4		3891.2	15141.44	4414.41
5		3678.2	13529.16	6026.69

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 3.24$

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 2.24$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 2049$

Absolute Open Flow 2049 Mcfd @ 15.025
Angle of Slope θ 55° 39'
Slope, n .684

Remarks: *BHP measured at mid point of perforations 11152'. Produced 2 bbls. of distillate and 0 bbls. water.

Approved By Division	Conducted By:	Calculated By:	Checked By:
	L. Ray Sutton	J. Cogburn	S. D. Smith