

NEW MEXICO CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-12,
Revised 9-1-66

Corrected Report.

RECEIVED

Type Test ☒ Initial ☐ Annual ☐ Special		Test Date 10-17-80		OCT 29 1980							
Company TEXAS OIL & GAS COMPANY		Operator EPC		Unit O. C. D.							
Foot East BURTON FLAT <i>Strawn</i>		Location STRAWN		Unit ARTESIA, OFFICE							
Completion Date 10-10-80		Total Length 11,760		Elevation 10570 3279 ft.							
Casing Size 4 1/2		Set At 11,735		Well No. 1							
Tubing Size 2 3/8		Set At 10,477		From OPEN ENDED To							
Type Well - Single - Bradenhead - G.G. or G.O. Multiple SINGLE		Packer Set At 10,477		County EDDY							
Producing Thru TBG		Reservoir Temp. °F 179 @ 10,538		Mean Annual Temp. °F 60							
Baro. Press. - P ₀ 13.2		State NEW MEXICO									
L 10,538		H 10,538		G _g .673							
% CO ₂ .359		% N ₂ 1.161		% H ₂ S Prover							
Meter Run 4		Taps FLG									
FLOW DATA											
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							2395				
1.	4	x	.750	263	8.5	75	2302	65			1 HR
2.	4	x	.750	260	12	78	2260	68			1 HR
3.	4	x	.750	260	26	79	2192	70			1 HR
4.	4	x	.750	270	32	78	2116	70			1 HR
5.											
RATE OF FLOW CALCULATIONS											
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor F _g	Super Compress. Factor, F _{pv}	Rate of Flow Q, Mcfd				
1	2.661	48.45	276.2	.9859	1.219	1.027	159				
2	2.661	57.26	273.2	.9831	1.219	1.027	188				
3	2.661	84.28	273.2	.9822	1.219	1.027	276				
4	2.661	95.20	283.2	.9831	1.219	1.027	312				
5											
NO.	P ₀	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio 38.958 Mcf/bbl.						
1	.41	535	1.40	.948	A.P.I. Gravity of Liquid Hydrocarbons 54.5 @ 60 Deg.						
2	.41	538	1.41	.949	Specific Gravity Separator Gas .673 X X X X X X X X						
3	.41	539	1.41	.949	Specific Gravity Flowing Fluid X X X X X						
4	.42	538	1.41	.948	Critical Pressure 669 P.S.I.A. P.S.I.A.						
5					Critical Temperature 382 R R						
F _c 2594.1 P _c ² 6729.4					(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 5.515$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.527$						
NO.	P ₁ ²	P _w	P _w ²	P _c ² - P _w ²	A.P.I. $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = .789$						
1	*	2523.6	6368.6	360.8							
2	*	2478.3	6142.0	587.4							
3	*	2419.5	5854.0	875.4							
4	*	2347.2	5509.3	1220.1							
5											
Absolute Open Flow 789 Mcfd @ 15.025					Angle of Slope θ 61.5			Slope, n .543			
Remarks: *CALCULATED FROM KNOWN BOTTOM HOLE PRESSURES, MEASURED WITH A KUSTER GAUGE											
1 BBL. OF CONDENSATE DURING TEST.											
Approved By Commission:				Conducted By: W.S.				Calculated By: R.P.			
								Checked By: J.W.W.			