

NEW MEXICO OIL CONSERVATION COMMISSION
MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Form C-122
Revised 9-1-65

RECEIVED

Type Test ☒ Initial ☐ Annual ☐ Special						Test Date 10/21/75		OCT 28 1975	
Company Hanagan Petroleum Corporation				Connection None		O. C. C.			
Pool Burton Flat				Formation Morrow		Unit ARTESIA, OFFICE			
Completion Date 10/27/75		Total Depth 11375		Plug Back TD 11326		Elevation 3211 KB		Farm or Lease Name Inexco Federal	
Csg. Size 5.5	Wt. 17 & 20	d 4.892	Set At 11375	Perforations: From 11004 To 11033		Well No. 1			
Tbg. Size 2 7/8	Wt. 6.5	d 2.441	Set At 10874	Perforations: From 11101 To 11255		Unit I 12		Twp. 21S	Rys. 26E
Type Well - Single - Bradenhead - G.G. or G.O. Multiple Single						Packer Set At 10882 11050		County Eddy	
Producing Thru Tubing		Reservoir Temp. °F 184 @ 10800		Mean Annual Temp. °F 70		Baro. Press. - P _a 13.2		State New Mexico	
L 11130	H 11130	Gg 0.600	% CO ₂	% N ₂	% H ₂ S	Prover Pos. ck.	Meter Run	Taps	

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
SI	117 1/2 hrs.			3618							60 min.
1.	2"	X	14/64	3477		81	3477	81	Pkr		60 min.
2.	2"	X	16/64	3388		83	3388	83			60 min.
3.	2"	X	18/64	3349		84	3349	84			60 min.
4.	2"	X	22/64	3239		85	3239	85			60 min.
5.											

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	0.8419		3490.2	0.9804	1.291	1.102	4098.5
2.	1.112		3401.2	0.9786	1.291	1.104	5275.2
3.	1.422		3362.2	0.9777	1.291	1.106	6674.3
4.	2.162		3252.2	0.9768	1.291	1.110	9842.1
5.							

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	Dry Gas	Mcf/bbl.
1.	5.20	541	1.51	0.823	A.P.I. Gravity of Liquid Hydrocarbons	Dry Gas	Deg.
2.	5.07	543	1.52	0.820	Specific Gravity Separator Gas	0.600	X X X X X X X X
3.	5.01	544	1.52	0.817	Specific Gravity Flowing Fluid	X X X X X	
4.	4.85	545	1.52	0.811	Critical Pressure	671	P.S.I.A.
5.					Critical Temperature	358	R

$P_f = 4626.2$ $P_f^2 = 21402$				$(1) \frac{P_c^2}{P_c^2 - P_w^2} = 7.331963$		$(2) \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 7.331963$	
NO.	P _r	P _s	P _s ²	P _f ² - P _s ²			
1		4490.2	20162	1240			
2		4420.2	19538	1864			
3		4391.2	19283	2119			
4		4299.2	18483	2919			
5							

$AOF = Q \left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 72,161.9$			
Absolute Open Flow 72,161.9		Mcf @ 15.025	
Angle of Slope 45°		Slope, n 1.000	

Remarks: BHP measured with Amerada Rpg-3 gauge Serial No. 31203 0-6000 psi

Approved By Commission:	Conducted By: Tefteller, Inc.	Calculated By: B. Combest	Checked By:
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