

MULTIPOINT

ONE POINT

PARTIAL WELL

APPROXIMATE

FOR GAS WELL

RECEIVED

Type Test		☒ Initial		☐ Annual		☐ Special		Test Date		10-20-76		OCT 27 1976			
Company				Monsanto Company				Connection				None			
Well				Burton Flat (Morrow)				Formation				Morrow			
Completion Date				10-20-76				Total Depth				11572 11560			
Plug Back TD				11572 11524				Elevation				3220 ft. 3241 D.F.			
Form or Lease Name				Cerf Federal				Well No.				2			
Casing Size		7.00"		Wt.		26.00#		Set At		11560		Perforations:			
From		11414		To		11460		Perforations:		From		To			
2.875"		Wt.		6.50#		Set At		11108		Perforations:		From			
NULOC		2.441"		Set At		11108		Perforations:		From		To			
Type Well - Single - Bradenhead - G.G. or G.O. Multiple								Packer Set At		11108		County			
Dual Completion Gas-Gas								Packer Set At		11108		Eddy			
Producing Thru				Tubing				Reservoir Temp. °F				Mean Annual Temp. °F			
11437				11437				164 @ 11437				60			
Baro. Press. - P _a				13.2				State				New Mexico			
L		H		Gg		% CO ₂		% N ₂		% H ₂ S		Prover			
11437		11437		0.596		0.00		0.00		0.00		X			
FLOW DATA				TUBING DATA				CASING DATA				Duration of Flow			
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow				
SI	23 Hrs.						2700	66							
1.	3.00		1.50	520	5.00"	84	2307	69			1.00 Hr.				
2.	3.00		1.50	520	13.00"	84	2010	70			1.00 Hr.				
3.	3.00		1.50	520	27.00"	81	1694	71			1.00 Hr.				
4.	3.00		1.50	520	39.00"	84	1449	71			1.00 Hr.				
5.															
RATE OF FLOW CALCULATIONS															
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd								
1.	11.13	51.633	533.20	0.9777	1.2953	1.0400	757								
2.	11.13	83.256	533.20	0.9777	1.2953	1.0400	1220								
3.	11.13	119.985	533.20	0.9804	1.2953	1.0400	1764								
4.	11.13	144.204	533.20	0.9777	1.2953	1.0400	2114								
5.															
NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.										
1.	0.79	544	1.52	0.921	A.P.I. Gravity of Liquid Hydrocarbons _____ None Produced _____ Deg.										
2.	0.79	544	1.52	0.920	Specific Gravity Separator Gas _____ 0.596 _____ X X X X X X X X X										
3.	0.79	541	1.51	0.920	Specific Gravity Flowing Fluid _____ X X X X X _____ 0.596										
4.	0.79	541	1.51	0.920	Critical Pressure _____ 671 _____ P.S.I.A. _____ 671 _____ P.S.I.A.										
5.					Critical Temperature _____ 358 _____ R _____ 358 _____ R										
P _r 2713.2 P _w 7361					(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.52908$										
NO.	P _r ²	P _w ²	P _w ²	P _c ² - P _w ²	(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 1.52908$										
1.	2321.4	5389	1973		AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2697$										
2.	2006.0	4024	3337												
3.	1596.0	2547	4814												
4.	1463.3	2141	5220												
5.															
Absolute Open Flow					2697		Mcf @ 15.025								
Angle of Slope					45		Slope, n 1.00								
Remarks:															
Approved By Commission:			Conducted By: WEST TEXAS CONSULTING SERVICE, INC.			Calculated By: H. L. Hagler		Checked By:							