

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

|                                                                                                                           |                     |                                                           |                            |
|---------------------------------------------------------------------------------------------------------------------------|---------------------|-----------------------------------------------------------|----------------------------|
| Type Test<br><input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special |                     | Test Date<br>10-7-1994                                    |                            |
| Company<br>Barbara Fasken                                                                                                 |                     | Connection<br>Pipeline                                    |                            |
| Pool<br>Indian Basin                                                                                                      |                     | Formation<br>Strawn                                       |                            |
| Completion Date<br>9-28-1994                                                                                              | Total Depth<br>8980 | Plug Back TD<br>8941                                      | Elevation<br>3856 G.L.     |
| Tram or Lease Name<br>Durham Shell Fed                                                                                    |                     |                                                           |                            |
| Coq. Size<br>4.5                                                                                                          | Wt.<br>11.6         | d<br>4.000                                                | Set At<br>8980             |
| Perforations:<br>From 8525 To 8892                                                                                        |                     | Well No.<br>#1                                            |                            |
| Thg. Size<br>2.375                                                                                                        | Wt.<br>4.7          | d<br>1.995                                                | Set At<br>8390             |
| Perforations:<br>From - To -                                                                                              |                     | Unit      Sec.      Twp.      Rge.<br>8      21s      24e |                            |
| Type Well - Single - Bordenhead - G.G. or G.O. Multiple<br>Single (gas)                                                   |                     | Packer Set At<br>8358                                     |                            |
| Producing Thru<br>Tbg. (gas)                                                                                              |                     | County<br>Eddy                                            |                            |
| Reservoir Temp. °F<br>147 # 8709                                                                                          |                     | Mean Annual Temp. °F<br>60                                |                            |
| Duro. Press. - P <sub>g</sub><br>13.2                                                                                     |                     | State<br>New Mexico                                       |                            |
| L<br>8709                                                                                                                 | H<br>8709           | Gg<br>0.637                                               | % CO <sub>2</sub><br>4.144 |
| % N <sub>2</sub><br>0.598                                                                                                 |                     | % H <sub>2</sub> S<br>0.00                                | Prover<br>0.00             |
| Meter Run<br>3.0                                                                                                          |                     | Taps<br>Flg.                                              |                            |

| FLOW DATA |                  |   |              |                 |                      |          | TUBING DATA     |          | BHP DATA        |          | Duration of Flow |
|-----------|------------------|---|--------------|-----------------|----------------------|----------|-----------------|----------|-----------------|----------|------------------|
| NO.       | Prover Line Size | X | Orifice Size | Press. p.s.i.g. | Diff. h <sub>w</sub> | Temp. °F | Press. p.s.i.g. | Temp. °F | Press. p.s.i.g. | Temp. °F |                  |
| SI        |                  |   |              |                 |                      |          | 2522            | 60       | 3213            | 147      | 72.0             |
| 1.        | 3.0              | x | 1.0          | 7.65            | 1.7                  | 110      | 2332            | 60       | 2986            | 147      | 1.0              |
| 2.        | 3.0              | x | 1.0          | 7.7             | 2.25                 | 110      | 2130            | 60       | 2800            | 147      | 1.0              |
| 3.        | 3.0              | x | 1.0          | 7.7             | 2.6                  | 100      | 1910            | 60       | 2569            | 147      | 1.0              |
| 4.        | 3.0              | x | 1.0          | 7.7             | 3.4                  | 100      | 1530            | 60       | 2167            | 147      | 1.0              |
| 5.        |                  |   |              |                 |                      |          |                 |          |                 |          |                  |

| RATE OF FLOW CALCULATIONS |                       |                  |                         |                       |                   |                                           |                     |
|---------------------------|-----------------------|------------------|-------------------------|-----------------------|-------------------|-------------------------------------------|---------------------|
| NO.                       | Coefficient (24 Hour) | $\sqrt{h_w P_m}$ | Pressure P <sub>m</sub> | Flow Temp. Factor Ft. | Gravity Factor Fg | Super. Compress. Factor, F <sub>spv</sub> | Rate of Flow O, Mcd |
| 1                         | 24.5                  | 13.01            | 850                     | 0.9551                | 1.253             | 1.055                                     | 402                 |
| 2                         | 24.5                  | 17.33            | 850                     | 0.9551                | 1.253             | 1.055                                     | 536                 |
| 3                         | 24.5                  | 20.02            | 850                     | 0.9636                | 1.253             | 1.059                                     | 627                 |
| 4                         | 24.5                  | 26.18            | 850                     | 0.9636                | 1.253             | 1.059                                     | 820                 |
| 5                         |                       |                  |                         |                       |                   |                                           |                     |

|     |                |          |                |       |                                       |           |
|-----|----------------|----------|----------------|-------|---------------------------------------|-----------|
| NO. | R <sub>g</sub> | Temp. °R | T <sub>g</sub> | Z     | Gas Liquid Hydrocarbon Ratio 24.3     | Mcf/Subl. |
| 1   | 1.24           | 570      | 1.57           | 0.899 | A.P.L. Gravity of Liquid Hydrocarbons | Dec.      |
| 2   | 1.24           | 570      | 1.57           | 0.899 | Specific Gravity Separator Gas 0.637  | XXXXXXX   |
| 3   | 1.24           | 560      | 1.54           | 0.891 | Specific Gravity Flowing Fluid XXXXX  |           |
| 4   | 1.24           | 560      | 1.54           | 0.891 | Critical Pressure 687                 | P.S.I.A.  |
| 5   |                |          |                |       | Critical Temperature 363              | R         |

P<sub>g</sub> 3226      P<sub>w</sub> 10.41 x 10<sup>6</sup>

|     |                |                |                             |                             |                                                           |
|-----|----------------|----------------|-----------------------------|-----------------------------|-----------------------------------------------------------|
| NO. | P <sub>1</sub> | P <sub>2</sub> | P <sub>1</sub> <sup>2</sup> | P <sub>2</sub> <sup>2</sup> | P <sub>1</sub> <sup>2</sup> - P <sub>2</sub> <sup>2</sup> |
| 1   |                | 2999           | 8.99                        | 1.413                       |                                                           |
| 2   |                | 2813           | 7.91                        | 2.494                       |                                                           |
| 3   |                | 2582           | 6.67                        | 3.741                       |                                                           |
| 4   |                | 2180           | 4.75                        | 5.655                       |                                                           |
| 5   |                |                |                             |                             |                                                           |

(1)  $\frac{P_g^2}{P_1^2 - P_2^2} = 4.17$       (2)  $\left[ \frac{P_g^2}{P_1^2 - P_2^2} \right]^n = 2.05$

AOF = Q  $\left[ \frac{P_g^2}{P_1^2 - P_2^2} \right]^n = 1098$

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|                                                                             |                               |                          |                |
|-----------------------------------------------------------------------------|-------------------------------|--------------------------|----------------|
| Absolute Open Flow 1098                                                     | Mcf @ 15.025                  | Angle of Slope α         | Slope, n 0.502 |
| Remarks: Bottom hole pressures obtained from pressure bombs hung @ mid-perf |                               |                          |                |
| Approved By Division                                                        | Conducted By: KELTIC SERVICES | Calculated By: JIM SMITH | Checked By:    |