

RECEIVED

Type Test: ☒ Initial ☐ Annual ☐ Special						Test Date: 4-8-82		APR 28 1982	
Company: <u>PERRY R. BASS</u>				Connection: <u>Natural Gas Pipeline</u>				O. C. D.	
Pool: <u>Bass</u>				Formation: <u>Atoka</u>				Unit: <u>ARTESIA, OFFICE</u>	
Completion Date: <u>4-6-82</u>		Total Depth: <u>12,377</u>		Plug Back TD: <u>11,310</u>		Elevation: <u>799</u>		Form or Lease Name: <u>Big Eddy</u>	
Csg. Size: <u>5 1/2</u>	Wt.: <u>17</u>	d: <u>4.892</u>	Set At: <u>12,377</u>	Perforations: From _____ To _____		Well No.: <u>79Y</u>			
Ring Size: <u>2 3/8</u>	Wt.: <u>4.7</u>	d: <u>1.995</u>	Set At: <u>11,069</u>	Perforations: From <u>11,069</u> To <u>11,069</u>		Unit: <u>J</u> Sec. <u>21</u> Twp. <u>21</u> Rge. <u>21</u>			
Type Well - Single - Broadhead - G.C. or G.O. Multiple						Packer Set At: <u>11,069</u>		County: <u>Eddy</u>	
Producing Thru: <u>Tubing</u>		Reservoir Temp. °F: <u>281 @ 11,069</u>		Mean Annual Temp. °F: <u>13.2</u>		Baro. Press. - P _a : <u>13.2</u>		State: <u>New Mexico</u>	
L: <u>11,069</u>	H: <u>11,069</u>	Gg: <u>.68</u>	% CO ₂ : <u>-</u>	% N ₂ : <u>-</u>	% H ₂ S: <u>-</u>	Prover: <u>-</u>	Meter Run: <u>2.900</u>	Taps: <u>pipe</u>	

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow	
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h _w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.		Temp. °F
SI	2.900		1.625								
1.	2.900		1.625	448	3.7	70	4130	71	0		1.16
2.	2.900		1.625	448	15.7	68	3230	71	30		1.00
3.	2.900		1.625	448	21.8	70	2695	68	30		1.00
4.	2.900		1.625	463	23.1	70	2040	65	30		1.50
5.	2.900		1.625	463	21.1	72	1640	68	30		3.50

RATE OF FLOW CALCULATIONS							
NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P _m	Flow Temp. Factor Ft	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	16.41	41.30	461	.9905	1.213	1.0477	853.12
2	16.41	85.07	461	.9924	1.213	1.0541	1771.39
3	16.41	98.83	461	.9905	1.213	1.0477	2041.50
4	16.41	104.86	476	.9905	1.213	1.0477	2164.28
5	16.41	100.22	476	.9887	1.213	1.0477	2066.45

NO.	P _r	Temp. °R	T _r	Z	Gas Liquid Hydrocarbon Ratio	Mcf/bbl.
					112.0189	
1	6.19	531	1.37	0.890	A.P.I. Gravity of Liquid Hydrocarbons: <u>50</u>	Deq.
2	4.85	531	1.37	0.733	Specific Gravity Separator Gas: <u>.68</u>	X X X X X X X X
3	4.04	528	1.37	0.670	Specific Gravity Flowing Fluid: <u>X X X X X</u>	
4	3.07	525	1.36	0.669	Critical Pressure: <u>669</u> P.S.I.A.	P.S.I.A.
5	2.47	528	1.37	0.691	Critical Temperature: <u>385</u> R	R

NO.	P _r	P _w	P _w ²	P _r ² - P _w ²
1	17164.45	4144	17172.74	6059.66
2	10517.05	3248	10549.50	12682.90
3	7263.03	2723	7414.73	15817.67
4	4161.60	2068	4276.62	18955.78
5	2689.60	1668	2782.22	20450.18

(1) $\frac{P_c^2}{P_c^2 - P_w^2} =$ _____

AOG = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n =$ _____

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2} \right]^n =$ _____

Absolute Open Flow: <u>2.6 Mcf</u>	Mcfd @ 15.025: _____	Angle of Slope θ: <u>45°</u>	Slope, n: <u>1.000</u>
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Remarks: _____

Approved By Commission: _____	Conducted By: _____	Calculated By: _____	Checked By: _____
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