ENERGY AND MINERALS DEPARTMENT SANTA FE, NEW MEXICO 87 Revised 10-1-78

MULTIPOINT A , ONE POINT BACK PRESSURE TE T FOR GAS WELL

RECEIVED BY
AUG 3 1 1983
O. C. D.
ARTESIA, OFFICE

Type Test: [X] Initial [ ] Annual [ ] Special — Test Date: 6/19/82

Company: Exxon Company USA	Connection: None			
Pool: Burton Flats, ~~Morrow~~	Formation: Morrow			Unit:
Completion Date: 6/19/82	Total Depth: ~~11467'~~ 11,470	Plug Back TD: 11378'	Elevation: ~~3236'~~ GL 3262	Farm or Lease Name: Yates ~~Federal~~ C Fed.
Csg. Size: 5" / Wt.: 18.0 / d: 4.276 / Set At: 9781 11467'		Perforations: From 11040' To 11110'		Well No.: 1
Tbg. Size: 2 7/8" / Wt.: 6.5 / d: 2.441 / Set At: 10950'		Perforations: From Open To Ended		Unit: C / Sec.: 31 / Twp.: 20s / Rge.: 28e
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single		Packer Set At: 10950'		County: Eddy
Producing Thru: Tubing	Reservoir Temp. °F: 184 @ 10950'	Mean Annual Temp. °F: 60	Baro. Press. – P_a: 13.2	State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
11075'	–	0.5951	0.983	0.438	–	–	2.900 X 1.000	Flg.

FLOW DATA / TUBING DATA / CASING DATA

NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Tubing Press. p.s.i.g. DWT	Tubing Temp. °F	Casing Press. p.s.i.g.	Casing Temp. °F	Duration of Flow
SI							2788	60	PACKER		66.25 hrs
1.	2.900	5.7/64	1.00	495	2	80	2613	60			1.0 hr
2.	2.900	7/64	1.00	495	19	90	2185	60			1.0 hr
3.	2.900	9.1/64	1.00	495	24	83	1844	60			1.0 hr
4.	2.900	11.3/64	1.00	500	52	92	1411	60			1.0 hr
5.											

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	4.801	31.88	508.2	0.9813	1.296	1.036	201.66
2	4.801	98.26	508.2	0.9723	1.296	1.033	614.06
3	4.801	110.44	508.2	0.9786	1.296	1.035	696.00
4.	4.801	163.36	513.2	0.9706	1.296	1.032	1018.13
5							

NO.	P_t	Temp. °R	T_t	Z
1	0.75	540	1.54	0.932
2.	0.75	550	1.57	0.937
3.	0.75	543	1.55	0.934
4	0.76	552	1.58	0.939
5				

Gas Liquid Hydrocarbon Ratio: Dry Gas Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons: – Deg.
Specific Gravity Separator Gas: 0.5951 XXXXXXXXX
Specific Gravity Flowing Fluid: XXXXX
Critical Pressure: 675 P.S.I.A. ____ P.S.I.A.
Critical Temperature: 350 R ____ R

P_c 3646.2 * P_c^2 13294.8

NO.	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1		3409.2	11622.6	1672.2
2		2894.2	8376.4	4918.4
3		2626.2	6896.9	6397.9
4		1947.2	3791.6	9503.2
5				

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 1.399$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.371$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1396$

Absolute Open Flow: 1396 Mcfd @ 15.025 — Angle of Slope θ: 46°49' — Slope, n: 0.939

Remarks: * BOTTOM HOLE PRESSURE @ (-7813)11075' USED FOR PRESSURE CALCULATIONS
WELL PRODUCED NO FLUID DURING TEST
7" CASING SET @ 10395'

Approved By Division	Conducted By:	Calculated By:	Checked By:
	JARREL WELL TESTING, INC	D. Dickerson	D. Dickerson