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See Rule 401 & Rule 1122

State of New Mexico  
Energy, Minerals and Natural Resources Department

OIL CONSERVATION DIVISION

P.O. Box 2088  
Santa Fe, New Mexico 87504-2088

RECEIVED

Form C-122  
Revised 4-1-91

JUN - 2 1992

O. C. D.  
OFFICE

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Operator <b>MW PETROLEUM CORPORATION</b>						Lease or Unit Name <b>HOC FED. GAS COM.</b>					
Type Test <input checked="" type="checkbox"/> Initial <input type="checkbox"/> Annual <input type="checkbox"/> Special						Test Date <b>5/20-21/92</b>			Well No. <b>2</b>		
Completion Date <b>3/17/92</b>		Total Depth <b>7800</b>		Plug Back TD <b>7780</b>		Elevation			Unit Ltr. - Sec. - TWP - Rge. <b>D 13 22S 23E</b>		
Csg. Size <b>5 1/2"</b>	Wt. <b>d</b>	d	Set At <b>7800</b>	Perforations: From: <b>7629</b> To: <b>7758</b>			County <b>EDDY</b>				
Tbg. Size <b>2 3/8"</b>	Wt. <b>4.7</b>	d <b>1.995</b>	Set At <b>7523</b>	Perforations: From:                      To:			Pool <b>INDIAN BASIN</b>				
Type Well - Single - Bradenhead - G.G. or G.O. Multiple <b>SINGLE</b>						Packer Set At <b>7523</b>			Formation <b>UPPER PENN</b>		
Producing Thru TBG		Reservoir Temp. °F <b>149 @ 7325</b>		Mean Annual Temp. °F <b>60°</b>		Baro. Press - P <sub>a</sub> <b>13.2</b>			Connection		
L <b>7523</b>	H <b>7523</b>	Gg <b>.627</b>	% CO <sub>2</sub> <b>.32</b>	% N <sub>2</sub> <b>.94</b>	% H <sub>2</sub> S	Prover		Meter Run <b>4.026</b>		Taps <b>FLG</b>	

  

FLOW DATA						TUBING DATA		CASING DATA		Duration of Flow
NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h <sub>w</sub>	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	
SI										
1.	4	X	1.250	681	59.29	65	950		PKR	
2.							800		PKR	
3.										
4.										
5.										

  

RATE OF FLOW CALCULATIONS							
NO.	COEFFICIENT (24 HOUR)		Pressure P <sub>m</sub>	Flow Temp. Factor Ft	Gravity Factor Fg	Super Compress. Factor, F <sub>pv</sub>	Rate of Flow Q, Mcfd
1.	7.469	202.88	694.2	.9952	1.263	1.071	2,040
2.							
3.							
4.							
5.							

  

NO.	P <sub>r</sub>	Temp. °R	T <sub>r</sub>	Z	Gas Liquid Hydrocarbon Ratio	Mcf/bbl
1.	1.03	525	1.43	.871	A.P.I. Gravity of Liquid Hydrocarbons <b>61.5 @ 60°</b>	Deg.
2.					Specific Gravity Separator Gas <b>.627</b>	XXXXXXXXXX
3.					Specific Gravity Flowing Fluid <b>XXXXXX</b>	G MIX = .721
4.					Critical Pressure <b>671</b> P.S.I.A.	668 P.S.I.A.
5.					Critical Temperature <b>365</b> R	398 R

  

P<sub>c</sub> 963.2    P<sub>c</sub><sup>2</sup> 927.8

NO.	P <sub>t</sub> <sup>2</sup>	P <sub>w</sub>	P <sub>w</sub> <sup>2</sup>	P <sub>c</sub> <sup>2</sup> - P <sub>w</sub> <sup>2</sup>
1.		696.3	484.8	442.9
2.				
3.				
4.				
5.				

1)  $\frac{P_c^2}{P_c^2 - P_w^2} = 2.095$       (2)  $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 2.095$

AOF = Q       $\left[ \frac{P_c^2}{P_c^2 - P_w^2} \right]^n = 4.274$

Absolute Open Flow <u>4,274</u> Mcfd @ 15.025	Angle of Slope $\Theta$ <u>45</u>	Slope, n <u>1.000</u>
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Remarks: WELL MADE 11.0 BBLs 61.5 API GR CONDENSATE DURING TEST AND 4.0 BBLs. H2O. A ONE  
(1) POINT WAS CONDUCTED DUE TO WELL LOGGS OFF ON LOW RATES AND SHUT-INS ALSO SIP  
WAS USED FROM PREVIOUS INFORMATION AS COMPLETED.

Approved By Division	Conducted By: <b>JOHN WEST ENGINEERING</b>	Calculated By: <b>BM</b>	Checked By: <b>BM</b>
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