STATE OF NEW MEXICO
ENERGY AND MINERALS DEPARTMENT

OIL CONSERVATION DIVISION
P. O. BOX 2088
SANTA FE, NEW MEXICO 87501

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O. C. D.
ARTESIA, OFFICE

Form C-122
Revised 10-1-78

45F File

MULTIPOINT AND ONE POINT BACK PRESSURE TEST FOR GAS WELL

Type Test: ☐ Initial ☐ Annual ☒ Special — Test Date: 6/18/84

Company: Hamon Oil Company	Connection: El Paso			
Pool: Carlsbad, South (Morrow)	Formation: Morrow			Unit
Completion Date: 4/27/74	Total Depth: ~~11903~~ 11,898	Plug Back TD: 11430	Elevation: 3289 KB	Farm or Lease Name: State K 4401
Csg. Size: 5½ / Wt.: 17.0 / 20.0 / d: 4.892 / 4.778	Set At: 11902	Perforations: From 11204 To 11208		Well No.: 1
Tbg. Size: 2 7/8 / Wt.: 6.5 / d: 2.441	Set At: 11110	Perforations: From OPEN ENDED To		Unit: C / Sec.: 2 / Twp.: 24s / Rge.: 26e
Type Well – Single – Bradenhead – G.C. or G.O. Multiple: Single		Packer Set At: 11110		County: Eddy
Producing Thru: Tubing	Reservoir Temp. °F: 198 @ 11100'	Mean Annual Temp. °F: 60	Baro. Press. – P_a: 13.2	State: New Mexico

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
11206	-	0.5741	0.661	0.514	-	-	4.026	F

FLOW DATA

NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	TUBING DATA Press. p.s.i.g. DWT	TUBING DATA Temp. °F	CASING DATA Press. p.s.i.g.	CASING DATA Temp. °F	Duration of Flow
SI											
1.	4.026	4/64	1.000	562	3.0	74	3275	78	Packer		90.75 hrs.
2.	4.026	5.5/64	1.000	562	6.7	74	3195	78			0.50 hrs.
3.	4.026	6/64	1.000	547	15.2	70	3135	78			1.00 hrs.
4.	4.026	7/64	1.000	547	42.0	68	2825	78			1.00 hrs.
5.	4.026	8/64	1.000	547	74.0	67	2520	78			1.00 hrs.

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	4.753	41.54	575.2	0.9868	1.320	1.039	267.21
2	4.753	62.08	575.2	0.9868	1.320	1.039	399.34
3	4.753	92.28	560.2	0.9905	1.320	1.039	595.83
4	4.753	153.39	560.2	0.9924	1.320	1.040	993.25
5	4.753	203.60	560.2	0.9933	1.320	1.040	1319.57

NO.	P_t	Temp. °R	T_t	Z
1	0.85	534	1.56	0.927
2	0.85	534	1.56	0.927
3	0.83	534	1.56	0.927
4	0.83	528	1.54	0.925
5	0.83	527	1.54	0.925

Gas Liquid Hydrocarbon Ratio: Dry Gas Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons: - Deg.
Specific Gravity Separator Gas: 0.5741 XXXXXXXXX
Specific Gravity Flowing Fluid: XXXXX
Critical Pressure: 575 P.S.I.A. - P.S.I.A.
Critical Temperature: 342 R - R

P_c 4112.2 P_c^2 16910.2

NO	P_t^2	P_w	P_w^2	$P_c^2 - P_w^2$
1		3992.2	15937.7	972.5
2		3935.2	15485.8	1424.4
3		3816.2	14563.4	2346.8
4		3595.2	12925.5	3984.7
5		3290.2	10825.4	6084.8

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 2.779$ (2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 2.345$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 3094.39$

Absolute Open Flow: 3094 Mcfd @ 15.025
Angle of Slope θ: 50° 11'
Slope, n: 0.834

Remarks: * BHP @ (-7919) 11206' Used for Pressure Calculations.

Approved By Division	Conducted By:	Calculated By:	Checked By:
	JARREL WELL TESTING, INC.	Joe A. Coleman	Joe A. Coleman