MULTIPOINT AI ONE POINT BACK PRESSURE TES FOR GAS WELL

RECEIVED
MAY 25 1981
O. C. D.
ARTESIA, OFFICE

Type Test: 4 pt. ☒ Initial ☐ Annual ☐ Special				Test Date: 5-13-81	
Company: DINERO OPERATING COMPANY		Connection: EL PASO NATURAL GAS COMPANY			Unit
Pool: Dublin Ranch Atoka		Formation: Atoka			
Completion Date: 3-16-81	Total Depth: 12740	Plug Back TD: 12060	Elevation	Farm or Lease Name: Big Chief Com	
Csg. Size: 5½ / Wt.: 17# / d: 4.892 / Set At: 12740		Perforations: From 11417 To 11769		Well No.: 2	
Tbg. Size: 2 3/8 / Wt.: 4.7# / d: 1.995 / Set At: 11292		Perforations: From To		Unit: N / Sec.: 22 / Twp.: 22 / Rge.: 28	
Type Well – Single – Bradenhead – G.G. or G.O. Multiple: Single		Packer Set At: 11292		County: Eddy	
Producing Thru: Tbg.	Reservoir Temp. °F: 190	Mean Annual Temp. °F: 60°	Baro. Press. – P_a: 13.2	State: New Mexico	

L	H	Gg	% CO_2	% N_2	% H_2S	Prover	Meter Run	Taps
*11593	11593	.580	.49	.76	.06		4.0"	Flg.

**2.0013

FLOW DATA / TUBING DATA / CASING DATA

NO.	Prover Line Size	X	Orifice Size	Press. p.s.i.g.	Diff. h_w	Temp. °F	Press. p.s.i.g.	Temp. °F	Press. p.s.i.g.	Temp. °F	Duration of Flow
SI							3945				
1.	4.0	X	1.750	414	3.06	84	3795				30 min.
2.	4.0	X	1.750	427	8.41	72	3689				1 hr.
3.	4.0	X	1.750	433	25.0	56	3408				1 hr.
4.	4.0	X	1.750	438	47.61	43	2962				1 hr.
5.											

RATE OF FLOW CALCULATIONS

NO.	Coefficient (24 Hour)	$\sqrt{h_w P_m}$	Pressure P_m	Flow Temp. Factor Ft.	Gravity Factor Fg	Super Compress. Factor, Fpv	Rate of Flow Q, Mcfd
1	14.93	36.16	427.2	.9777	1.313	1.030	714
2.	14.93	60.84	440.2	.9887	1.313	1.035	1220
3	14.93	105.62	446.2	1.004	1.313	1.039	2160
4.	14.93	146.57	451.2	1.017	1.313	1.043	3048
5							

NO.	P_r	Temp. °R	T_r	Z
1	.64	544	1.54	.942
2.	.66	532	1.50	.934
3	.66	516	1.46	.927
4	.67	503	1.42	.919
5				

Gas Liquid Hydrocarbon Ratio _____ Mcf/bbl.
A.P.I. Gravity of Liquid Hydrocarbons _____ Deg.
Specific Gravity Separator Gas .580 XXXXXXXXXX
Specific Gravity Flowing Fluid XXXXX
Critical Pressure 672 P.S.I.A. _____ P.S.I.A.
Critical Temperature 354 R _____ R

P_c 3958.2 P_c^2 15667.3

NO	P_w	P_w^2	$P_c^2 - P_w^2$
1	3811.9	14530.6	1136.7
2	3710.0	13764.1	1903.2
3	3444.6	11865.3	3802.0
4	3026.2	9158.9	6508.4
5			

(1) $\frac{P_c^2}{P_c^2 - P_w^2} = 2.4072$

(2) $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 1.939367$

AOF = Q $\left[\frac{P_c^2}{P_c^2 - P_w^2}\right]^n = 5.911$

Absolute Open Flow 5,911 Mcfd @ 15.025 | Angle of Slope θ 53° | Slope, n .754

Remarks *Equivelnt length **Effective Dia.

Made no fluid during test.

Approved by Division	Conducted by:	Calculated by:	Checked by:
	Rea & Townley	Rea	